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SPECIAL TOPIC: Single-atom Catalysts

Coordination structure dominated performance of single-atomic Pt catalyst for anti-Markovnikov hydroboration of alkenes

Qi Xu^{1†}, ChenXi Guo^{2†}, Shubo Tian^{1†}, Jian Zhang¹, Wenxing Chen³, Weng-Chon Cheong¹, Lin Gu⁴, Lirong Zheng⁵, Jianping Xiao², Qiang Liu¹, Bijie Li¹, Dingsheng Wang^{1*} and Yadong Li¹

ABSTRACT The rational design of efficient single-atomic (SA) catalysts is essential and highly desirable but impeded by the lack of sufficient acknowledge between structure and property. To this end, it is critical to clarify the effect of the coordination structure of active metal centers on the catalytic activities for the design of such catalysts. Here, we report that different coordination structures of SA Pt catalysts can dramatically influence their activities for anti-Markovnikov hydroboration of alkenes. Compared with the other two coordination structures (Pt-N₄ and Pt-O₂), the SA Pt species coordinated with three O atoms (Pt-O₃) display the highest turnover number value of 3288 for the hydroboration reaction to access the important alkylboronic esters. Density functional theory calculations reveal that a superior catalytic activity can be expected for alkene hydroboration over the three O coordinated Pt species due to the lowest reaction energy (ΔG) limiting step from the reaction phase diagram.

Keywords: single-atomic Pt catalyst, coordination structure, anti-Markovnikov hydroboration of alkenes, DFT calculations

INTRODUCTION

Single-atomic (SA) catalysts have recently attracted extensive attention due to their specific activity, ultrahigh atomic utilization, and uniform active sites [1–14]. In such catalysts, individual metal atoms are commonly isolated and stabilized by coordinated atoms from sup-

ports [15–20]. Similar to homogenous catalysts, subtle differences in species and quantity of coordinated atoms will exert an important influence on the geometric and electronic structures of these metal atoms, which can further affect their catalytic activities [21–26]. Therefore, it is important to explore the relationship between the coordination structure and performance of SA catalysts, which has been scarcely investigated so far [27–29]. To deeply understand this relationship, clarifying the catalytic performances of a series of SA catalysts with different coordination structures is highly desirable and will be of great significance for guiding the synthesis of better-performing SA catalysts.

Alkylboronic esters are key intermediates in organic synthesis for constructing various C–C, C–O, and C–N bonds [30,31]. Catalytic hydroboration of alkenes with good regioselectivity is one of the direct and effective methods to synthesize such compounds [32,33]. Compared with traditional homogeneous catalysts for this reaction, the development of corresponding heterogeneous catalysts lags far behind, although they are more promising in practical applications because of the easy recovery of catalysts for reducing the cost and residual metal contamination [34]. Moreover, considering the copious waste in the reaction caused by the widely used boron source as bis(pinacolato)diboron (B₂Pin₂) [35], the hydroboration with pinacolborane (HBPin) is more

¹ Department of Chemistry, Tsinghua University, Beijing 100084, China

² State Key Laboratory of Catalysis, Dalian Institute of Chemical Physics, Chinese Academy of Sciences, Dalian 116023, China

³ Beijing Key Laboratory of Construction Tailorable Advanced Functional Materials and Green Applications, School of Materials Science and Engineering, Beijing Institute of Technology, Beijing 100081, China

⁴ Beijing National Laboratory for Condensed Matter Physics, Institute of Physics, Chinese Academy of Sciences, Beijing 100190, China

⁵ Beijing Synchrotron Radiation Facility, Institute of High Energy Physics, Chinese Academy of Sciences, Beijing 100049, China

[†] These authors contributed equally to this work.

Corresponding author (email: wangdingsheng@mail.tsinghua.edu.cn)

atom-economical and attractive but very challenging because of the low reactivity of HBPin [36–39]. Therefore, to realize the heterogeneous catalytic hydroboration of alkenes with HBPin as the boron source, it is crucial and imperative to prepare highly efficient heterogeneous catalysts.

Here, we demonstrate that the coordination structure of the SA Pt catalyst has a significant influence on its catalytic behavior for the anti-Markovnikov hydroboration of alkenes. Through different synthetic strategies, three SA Pt catalysts with Pt-O₃, Pt-O₂, and Pt-N₄ coordination structures are fabricated respectively. The Pt-O₃ structure of the SA Pt catalyst exhibits much higher activity for the hydroboration reaction than the other two structures (Pt-O₂ and Pt-N₄), producing the important alkylboronic esters. Further density functional theory (DFT) calculations reveal that the superior performance of Pt-O₃ in SA Pt catalyst is attributed to its adaptive reactive ability, namely suitable adsorption energies for all the adsorbates, which results in the lowest limiting reaction energy (ΔG).

EXPERIMENTAL SECTION

Materials

Iron nitrate nonahydrate $(Fe(NO_3)_3 \cdot 9H_2O, AR)$, cobalt nitrate hexahydrate $(Co(NO_3)_2 \cdot 6H_2O, AR)$, sodium borohydride $(NaBH_4, 98.0\%)$, cetyltrimethylammonium bromide (CTAB, AR), sodium hydroxide (NaOH, AR), sodium carbonate $(Na_2CO_3, 99.0\%)$, hydrochloric acid (HCl, 99.0%), ethylenediaminetetraacetic acid disodium salt (EDTA-2Na, 99.8%) were purchased from Sinopharm Chemical Reagent Co. Ltd. (China). 1-Octene $(C_8H_{16}, 98.0\%)$, tetraammineplatinum(II) chloride monohydrate (Cl₂H₁₄N₄OPt, 99.9%), hexachloroplatinic acid (H₂PtCl₆, 99.0%) were provided by Alfa Asear (China). Titanium oxide (99.8%, 5–10 nm) was purchased from Aladdin (China). Pinacol borane was purchased from Energy Chemical (China). All reagents were used without further purification.

Preparation of the catalysts

Synthesis of FeCo oxide nanosheets

The FeCo oxide nanosheets (FeCo ONs) were prepared according to a method reported in previous reference [40] with some modifications. 1.0 mmol Fe(NO₃)₃·9H₂O, 1.0 mmol Co(NO₃)₂·6H₂O and 0.5 g CTAB were dispersed into 25 mL deionized water. After continuous stirring and ultrasonic treatment until all the solutes

dissolved, freshly prepared $\mathrm{NaBH_4}$ solution (0.1 g in 10 mL water) was added dropwise slowly. After the reaction proceeded for some time, the product was centrifuged and washed with ethanol three times and finally dried under vacuum overnight at room temperature.

Synthesis of SA Pt-O₃

In a typical synthesis, 100 mg as-prepared FeCo ONs was dispersed in 25 mL water under ultrasonic vibration. Afterwards, a $\rm H_2PtCl_6$ solution (1.25 mg in 10 mL water) was added dropwise under stirring at room temperature. After stirring for 12 h, the mixed solution was centrifuged. The recovered solid was washed with deionized water and ethanol several times. After drying under vacuum overnight, the solid was transferred into a porcelain boat and then kept in a tube furnace maintaining at 100° C under 5% $\rm H_2/N_2$ atmosphere for 1 h. Finally, the SA Pt-O₃ was obtained.

Synthesis of SA Pt-O2

The SA Pt-O₂ was prepared according to a previously reported method [41]. In a typical synthesis, the titanium oxide (1 g) and an aqueous solution of sodium hydroxide (10 mol L⁻¹, 30 mL) were stirred to form a suspension. Afterwards, the mixture was transferred into a 50-mL Teflon-lined stainless-steel autoclave and hydrothermally treated at 130°C for 72 h. After cooling down to room temperature, the precipitate was separated by centrifugation and washed with deionized water until a pH near 8. The recovered solid was dried at 60°C for 12 h as titanate nanotubes). Then, (marked ammineplatinum(I) chloride monohydrate (1.82 mg) was dissolved in an aqueous solution of HCl (0.1 mol L⁻¹, 20 mL) to form a clarified solution. The as-prepared titanate nanotubes (0.2 g) were added to the above solution and mixed with ultrasonic treatment for 30 min. The mixture was continuously stirred for 12 h at room temperature. The precipitate was separated by centrifugation at 10,000 r min⁻¹ for 6 min and washed with deionized water for three times, then dried under vacuum at 60°C for 12 h. After being ground, the as-prepared precipitate was calcined in a muffle furnace at 400°C for 1 h and then kept in a tube furnace at 160°C under the 5% H₂/Ar atmosphere for 1 h with a heating rate of 2°C min⁻¹. Finally, the product, marked as SA Pt-O2, was collected without any treatment for further use.

Synthesis of SA Pt-N₄

The SA Pt-N₄ catalyst was synthesized based on previously reported work [42]. In a typical synthesis, 4 g

EDTA-2Na and 36 mg K₂PtCl₆ were dissolved into 100 mL deionized water, and then stirred at 80°C for 12 h. Afterwards, the solution was evaporated and transferred into a solid mixture of EDTA-2Na-Pt complex. The recovered solid was then thoroughly mixed with 40 g Na₂CO₃ powder through grinding using an agate mortar. The mixed precursors were placed in a corundum boat and annealed at 850°C with a heating rate of 3°C min⁻¹ under Ar atmosphere for 1 h. After cooling down to room temperature, the resulting powder was transferred into a diluted hydrochloric acid solution to remove soluble Na₂CO₃ salt completely. Finally, the SA Pt-N₄ was collected by vacuum infiltration and then dried in oven overnight after washing with distilled water and anhydrous ethanol for several times.

Catalytic evaluation

All operations were performed with the use of standard Schlenk techniques. Unless otherwise noted, all the experiments were carried out under N_2 atmosphere. In a typical procedure: 1-octene (1.0 mmol), pinacol borane (2.0 mmol) and the catalysts (SA Pt-O₃, SA Pt-O₂, SA Pt-N₄, Pt/substrate=0.028%) were placed in a Schlenk tube. The reactor was sealed and purged three times with N_2 at 1 MPa. Then the mixture was heated at 40°C under vigorously stirring (800 r min⁻¹) for 24 h. After the reaction, the yield was detected by gas chromatography (GC) using dodecane as the internal standard. The overall calculated turnover number (TON, =(mole of product 3)/ (mole of Pt)) was measured upon completion of reactions and the calculation of it was based on the total Pt loading in the catalysts.

Characterization

X-ray diffraction (XRD) data were obtained from a Rigaku D/max 2500Pc X-ray powder diffractometer (Japan) using a Cu K α radiation (λ =0.15418 nm). Transmission electron microscopy (TEM) images were taken on a Hitachi-7700 (Japan) operated at 100 kV. High resolution TEM (HRTEM) images were recorded on a JEOL JEM-2100F field emission transmission electron microscope (Japan) operated at 200 kV. Aberration-corrected highangle annular dark-field scanning transmission electron microscopy (AC HAADF-STEM) images were taken on a Titan 80-300 scanning/transmission electron microscope (FEI, USA) operated at 300 kV, equipped with a probe spherical aberration corrector. Inductively coupled plasma optical emission spectrometry (ICP-OES) measurements were carried out on a Thermo Fisher iCAPTM 7000 Series ICP-OES analyzer (USA). The product was identified by gas chromatography-mass spectrometry (GC-MS, Thermo Fisher Scientific-TXQ Quntum XLS, USA), and was quantitatively analyzed by GC (Shimadzu, GC-2010 Plus, Japan), equipped with FID using a capillary column (TR-5MS, from Thermo Scientific, USA; length 30 m, inner diameter 0.25 mm, film 0.25 µm) employing *n*-octanol as an internal standard. ¹H and ¹³C NMR data were acquired from a Bruker Advance III (400 MHz) spectrometer (Germany).

XAFS analysis and results

The X-ray absorption find structure (XAFS) data of the sample were collected at 1W1B station in Beijing Synchrotron Radiation Facility (BSRF). The acquired extended XAFS (EXAFS) data were processed according to the standard procedures using the ATHENA module implemented in the IFEFFIT software packages. The EXAFS spectra were obtained by subtracting the postedge background from the overall absorption and then normalizing with respect to the edge-jump step. Subsequently, k^3 -weighted $\chi(k)$ data of Pt L₃-edge was Fourier transformed to real (R) space using a hanning windows $(dk=1.0 \text{ Å}^{-1})$ to separate the EXAFS contributions from different coordination shells. To obtain the quantitative structural parameters around central atoms, least-squares curve parameter fitting was performed using the ARTE-MIS module of IFEFFIT software packages. The following EXAFS equation was used:

$$\chi(k) = \sum_{j} \frac{N_{j} S_{0}^{2} F_{j}(k)}{k R_{j}^{2}} \exp\left[-2k^{2} \sigma_{j}^{2}\right]$$

$$\times \exp\left[\frac{-2R_{j}}{\lambda(k)}\right] \sin\left[2kR_{j} + \phi_{j}(k)\right], \tag{1}$$

where S_0^2 is the amplitude reduction factor, $F_j(k)$ is the effective curved-wave backscattering amplitude, N_j is the number of neighbors in the j^{th} atomic shell, R_j is the distance between the X-ray absorbing central atom and the atoms in the j^{th} atomic shell (backscatterer), λ is the mean free path in Å, $\phi_j(k)$ is the phase shift (including the phase shift for each shell and the total central atom phase shift), σ_j is the Debye-Waller parameter of the j^{th} atomic shell (variation of distances around the average R_j). The functions $F_j(k)$, λ and $\phi_j(k)$ were calculated with the ab initio code FEFF8.2.

Computational method

The DFT calculations were conducted using the Vienna *Ab initio* Simulation Package (VASP) [43,44] applying the functional of revised Perdew-Burke-Ernzerhof (rPBE)

[45,46] and generalized gradient approximation (GGA). The interactions between electrons and atomic cores were described using the projector augmented wave (PAW) method. All the structure optimizations were conducted with a cut-off energy of 400 eV and the force convergency of 0.05 eV Å $^{-1}$. The transition states were obtained using the climbing image nudged elastic band (NEB) [47] with a same force convergency of 0.05 eV Å $^{-1}$. All the adsorption energies were referred to the gas energies of octene (C₈H₁₆), hydrogen (H₂) and HBPin. The standard thermodynamic corrections [48,49] were conducted to correct all the energies to free energy with the condition of the temperature of 313 K (correction values see Table S1).

Single atom Pt carried by three different catalysts were studied in this work, including TiO_2 (SA Pt-O₂), N-doped graphene (SA Pt-N₄) and FeCo oxide (SA Pt-O₃). The anatase TiO_2 was used as a bulk structure, where a TiO_2 (101) surface was applied with a p(2×2) unit cell. A Monkhorst-Pack k-point 1×3×1 was used in all the surface structure calculations for $TiO_2(101)$. A p(6×6) graphene surface was applied with 4 doping N. A Monkhorst-Pack k-point 2×2×1 was used in all the surface structure calculations for graphene. The spinel bulk structure $CoFe_2O_4$ was used to build the surface of FeCo oxide, where a $CoFe_2O_4(311)$ surface was used with a p(1×1) unit cell. A Monkhorst-Pack k-point 1×3×1 was

used in all the surface structure calculations for $CoFe_2O_4$ (311).

Five different key adsorbates (ad-1 to ad-5) were considered based on the catalytic system (Fig. S1a), where the linear relations, namely the scaling relations (Fig. S2), were calculated with the descriptor of the adsorption energies of C8H17* (ad-2). Six elementary reactions (Fig. S1b) were considered in this work to establish the reaction phase diagram.

RESULTS AND DISCUSSION

The TEM image illustrates the hierarchical microstructure and uniform thickness of the as-prepared FeCo ONs, and the exclusive observed weak peak in the XRD pattern reveals the low crystalline of the sample (Figs S3 and S4). TEM and HAADF-STEM images indicate that the hierarchical microstructure is preserved after the adsorption of Pt element and simultaneously no visible Pt nanoparticles formed on the FeCo ONs support (Fig. 1a, b). No extra peaks consistent with Pt nanoparticles are found in the XRD pattern as well (Fig. S4). Energy-dispersive X-ray spectroscopy (EDS) shows that the Pt element is homogeneously dispersed on the support (Fig. 1c). The loading of Pt element is measured up to 0.54 weight percent (wt%) according to the analysis of ICP-OES. To further confirm the sole existence of Pt species, we performed the AC HAADF-STEM measure-

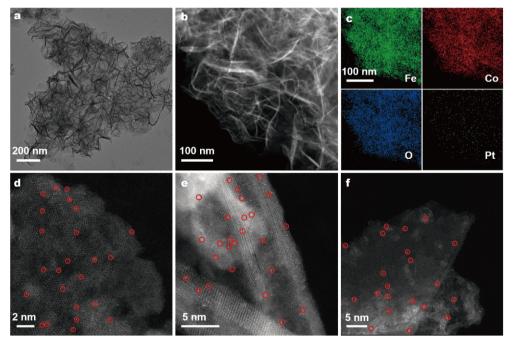


Figure 1 (a) TEM image, and (b) HAADF-STEM image of the SA Pt-O₃ sample. (c) Corresponding EDS elemental maps of Fe, Co, O and Pt. (d) AC HAADF-STEM image of the SA Pt-O₃ sample. (e, f) AC HAADF-STEM images of the SA Pt-O₂ and SA Pt-N₄.

ments on the catalyst (Fig. 1d). It can be recognized that there are only isolated bright dots corresponding to the single Pt atoms appearing on the FeCo ONs, demonstrating the sole presence of SA Pt species in the SA Pt-O₃.

To get more information about the electronic and coordination structures of the SA Pt catalyst, XAFS analysis was conducted. Fig. 2b shows the Fourier transformed EXAFS (FT-EXAFS) spectrum of SA Pt-O₃ with Pt-foil and PtO₂ as references at the Pt L₃-edge. There is only one prominent peak at 1.6 Å which can be attributed to the Pt-O contribution and no peak corresponding to Pt-Pt contribution at 2.6 Å can be observed, confirming that Pt species exist as isolated atoms stabilized by oxygen atoms. Besides, the oxidation state of these SA Pt species is also illustrated by the X-ray absorption near-edge structure (XANES) spectra (Fig. 2a). In general, the white line intensities are closely related to the oxidation state of Pt. In Fig. 2a, the white line intensity of SA Pt-O₃ is located between that of Pt foil and PtO₂, which indicates that the oxidation state of Pt in SA Pt-O3 is situated between 0 and +4. Further fitting analysis of the FT-EXAFS curve in R space confirmes that the SA Pt species are coordinated by three O atoms with a Pt–O bond distance of 1.97 Å to form the Pt-O₃ structure (Fig. 2c and Table S2). The local structure of Pt species obtained from DFT simulations is displayed in Fig. 2d.

The other two SA Pt catalysts with $Pt-O_2$ and $Pt-N_4$ coordination structures (denoted as SA $Pt-O_2$ and SA $Pt-N_4$) were synthesized according to different strategies [41,42]. As revealed by TEM images (Figs S5 and S6) and XRD patterns (Figs S7 and S8), there are no obvious peaks matching with Pt nanoparticles. EDS demonstrates that all elements are uniformly dispersed (Figs S9 and S10). The contents of Pt element were separately measured up to 0.51 wt% (SA $Pt-O_2$) and 0.56 wt% (SA $Pt-N_4$) by ICP-OES. Besides, the HAADF-STEM (Figs S11 and S12) and AC HAADF-STEM images (Fig. 1e, f) indicate that Pt element exists in isolated single atoms for both samples, which confirms the successful syntheses of the other two SA Pt catalysts.

We next evaluated the catalytic performance of SA Pt-O₃ for the hydroboration of alkenes (Fig. 3). Initially, the hydroboration of 1-octene with the relatively inert HBPin (1) as the boron source was chosen as the model reaction. It was delighting that 1-octene (2) was almost

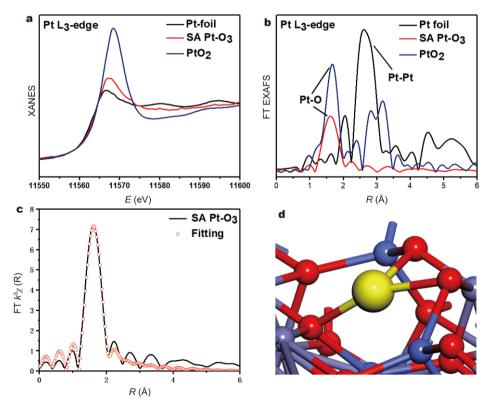


Figure 2 (a) XANES spectra at the Pt L₃-edge of the SA Pt-O₃ sample, PtO₂, and Pt foil. (b) FT-EXAFS spectra at the Pt L₃-edge of the SA Pt-O₃ sample, PtO₂, and Pt foil. (c) Corresponding fits of the EXAFS spectrum of the SA Pt-O₃ at the R space. (d) Local structure of Pt species in SA Pt-O₃ from DFT simulations. The yellow, red, blue and purple balls represent Pt, O, Co and Fe atoms, respectively.

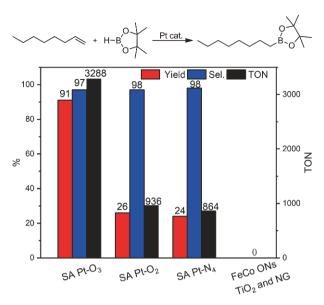


Figure 3 A performance comparison of SA Pt-O₃, SA Pt-O₂, SA Pt-N₄, and pure supports in anti-Markovnikov hydroboration of 1-octene.

completely converted to the target anti-Markovnikov addition alkylboronic ester (3) (Figs S13 and S14) in 91% yield and 97% selectivity over the SA Pt-O3 without significant alkene isomerization. The TON value of SA Pt-O₃ was up to 3288. As for the other two SA Pt catalysts, the yield of the product 3 dropped down to 26% for SA Pt-O₂ and 24% for SA Pt-N₄ accompanied by a certain degree of alkene isomerization, achieving the much lower TON values as 936 and 864, respectively. In contrast, almost no product was obtained when the pure FeCo ONs, TiO2 and N-doped graphene (NG) were used as the catalysts. These results of control experiments demonstrate that the catalytic active species is SA Pt and the different performances of the three catalysts for the hydroboration reaction are probably concerned with the distinct coordination structures of Pt atoms. After the reaction, according to HAADF-STEM, AC HAADF-STEM images and XRD pattern, the initial morphology of SA Pt-O₃ remained unchanged and no agglomeration of Pt species was found after the reaction (Figs S15 and S16).

Towards further understanding the relationship between the coordination structure and the catalytic performance of SA Pt-O₃, DFT studies were conducted to gain more insight into the catalytic mechanism and activity trend of the hydroboration reaction over the above three catalysts with different coordination structures (Fig. S17). Five different key adsorbates (ad-1 to ad-5) were considered based on the catalytic systems (Fig. S1a), where linear relations (Fig. S2), namely the scaling rela-

tions [50,51], were calculated with the descriptor of the adsorption energies of C_8H_{17} *(ad-2). Six elementary reactions (Fig. S1b) were considered in this work to establish the reaction phase diagram (RPD) [52,53] (Fig. 4a).

Two different reaction pathways were considered in this work, which can be mainly dependent on the different priorities of the first activation of ad-1 by hydrogenation (Fig. 4b, Pathway 2) or hydroboration (Fig. 4b, Pathway 1). The Pathway 1 is more favored, when the adsorption energy of ad-2, namely the descriptor (described in Fig. 4a, *X*-axis), is lower than -0.75 eV due to a higher reaction energy of R5 needed for Pathway 2. With the increase of the ad-2 adsorption energy, a higher reaction energy of R2 can be found, resulting in a difficult reaction by Pathway 1. Therefore, Pathway 2 is more favored in this case.

The ΔG limiting steps can be obtained as the elementary step with the highest reaction energy in specific reaction pathways. Here, different ΔG limiting steps are demonstrated for alkene hydroboration with different adsorption energies of ad-2. Importantly, the catalytic activity can be described from the reaction energy of ΔG limiting steps. It is found that the reaction energy of ΔG limiting step for alkene hydroboration over SA Pt-O3 is just located close to the lowest reaction energy obtained from RPD, which is expected to show the highest catalytic activity (Fig. 4a). Hereafter, a theoretically predicted activity trend can be obtained to be SA Pt-O₃>SA Pt-O₂>SA Pt-N₄, which shows an excellent agreement compared with the experimental results discussed above. Note that, although the scaling relations show a general trend for the adsorption energies between different adsorbates, it may affect the predicted activity trend due to the error in the linear fitting compared to the explicit calculation. Accoordingly, The activation barriers of ΔG limiting steps were calculated to further prove the expected catalytic activity for SA Pt-O₃. R6 is obtained to be the ΔG limiting step for alkene hydroboration over SA Pt-O2, where a higher activation barrier of 1.47 eV is calculated on SA Pt-O₂ compared with that of only 0.09 eV on SA Pt-O₃. Meanwhile, the dissociative adsorption of HBPin (R1) is found to be the ΔG limiting step on SA Pt-N₄ with a higher activation barrier of 1.91 eV, while 0.47 eV of activation barrier on SA Pt-O3 is calculated.

As discussed above, the alkene hydroboration over SA Pt-O₃ is just located close to the point with the lowest ΔG limiting reaction energy. Seriously, it is difficult to judge a clear reaction mechanism for alkene hydroboration over SA Pt-O₃ due to a similar energy of ΔG limiting reaction

energy for different pathways, where it is located just at the switch point for different pathways based on the reaction phase diagram. Therefore, further DFT calculations were conducted to investigate the reaction mechanism for alkene hydroboration over SA Pt-O₃ (Fig. 5a) with the calculations of all the transition states

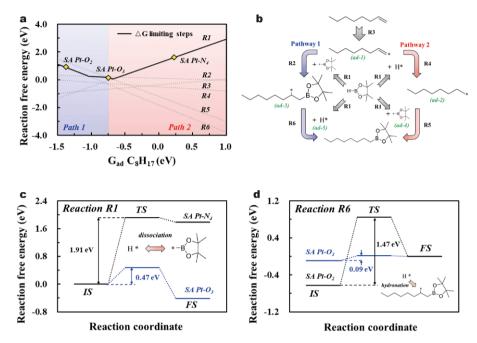


Figure 4 (a) Reaction phase diagram of alkene hydroboration (elementary steps R1–R6 see the Supplementary information). The black solid lines are ΔG limiting steps; the blue and red backgrounds refer two different reaction pathways. (b) Two different reaction pathways for alkene hydroboration. (c) Activation barriers of R1 over SA Pt-O₃ and SA Pt-O₄. (d) Activation barriers of R6 over SA Pt-O₃ and SA Pt-O₂.

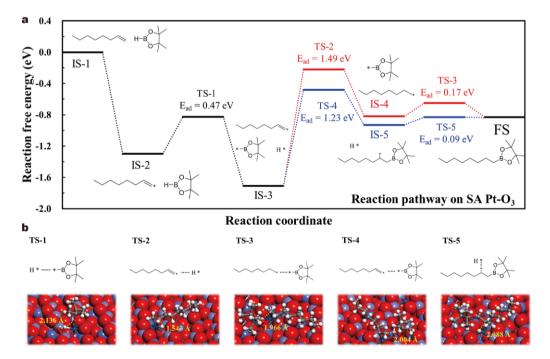


Figure 5 (a) Reaction pathways of alkene hydroboration over SA Pt- O_3 . The red and blue lines show different pathways. (b) Transition state structures performed in alkene hydroboration over SA Pt- O_3 .

(Fig. 5b).

It is found that lower activation barrier of 1.23 eV is obtained for the hydroboration of $C_8H_{17}^*$ compared with the hydrogenation (1.49 eV). Meanwhile, the following steps of both pathways show lower activation barrier affecting less the total activity. As a result, the mechanism with the hydroboration of $C_8H_{17}^*$ followed by a further hydrogenation is more favored over SA Pt-O₃. Additionally, the better activation behavior for alkene hydroboration over SA Pt-O₃ can be further proved with the lower activation barrier of ΔG limiting barrier (1.23 eV) compared with that on either SA Pt-O₂ (1.47 eV, Fig. 4c) or SA Pt-N₄ (1.91 eV, Fig. 4d).

CONCLUSIONS

In summary, the influence of the coordination structure on the catalytic properties of SA catalysts has been thoroughly investigated by considering three SA Pt catalysts: SA Pt-O₃, SA Pt-O₂, and SA Pt-N₄. The as-fabricated SA Pt-O₃ exhibits the highest activity in the anti-Markovnikov hydroboration of alkenes, producing the valuable alkylboronic esters with good selectivity. As revealed by DFT calculation and experimental results, the superior performance of SA Pt-O₃ is attributed to its distinctive coordination structure, which results in the lowest reaction energy of ΔG limiting step. This work may provide new insights for preparing novel betterperforming SA catalysts by changing the coordination structure of the active metal centers.

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Author contributions Xu Q designed and performed the experiments, analyzed the data, and wrote the paper. Guo C and Xiao J conducted the density functional theory calculations and contributed to the writing of the paper. Tian S and Zhang J assisted to carry out the experiments. Chen W and Zheng L helped with XAFS characterization and corresponding data analysis. Cheong WC assisted in HAADF-STEM and EDX elemental mapping characterizations. Gu L helped with the AC HAADF-STEM characterization. Liu Q and Li B helped analyze the data. Wang D and Li Y conceived the research project, analyzed the results and wrote the paper. All authors contributed to the general discussion.

Conflict of interest The authors declare that they have no conflict of interest.

Supplementary information Supporting data are available in the online version of the paper.



Qi Xu received his BSc degree from the University of Science and Technology of China in 2017. Now, he is a PhD student under the supervision of Prof. Dingsheng Wang at Tsinghua University. His research interests mainly focus on the design and fabrication of single-atomic catalysts for heterogeneous catalysis.



Chenxi Guo received his PhD degree from the Queen's University of Belfast in 2018. He is currently an Assistant Research Associate at Dalian Institute of Chemical Physics, Chinese Academy of Sciences. His research interests focus on the first principles calculations, theoretical catalysis, and rational design of catalytic materials



Shubo Tian received his BSc (2013), MSc (2016), and PhD (2019) degrees from Hebei Normal University, University of the Chinese Academy of Sciences, and Tsinghua University, respectively. He is currently a postdoctor in the National University of Singapore. His research interests are focused on the syntheses and applications of isolated single-atom-site and cluster catalysts.



Dingsheng Wang received his BSc degree from the Department of Chemistry and Physics, University of Science and Technology of China in 2004, and his PhD degree from the Department of Chemistry, Tsinghua University in 2009, under the supervision of Prof. Yadong Li. He did his postdoctoral research at the Department of Physics, Tsinghua University, with Prof. Shoushan Fan. He joined the faculty of the Department of Chemistry, Tsinghua University in 2012.

配位结构主导单原子Pt的烯烃反马氏硼氢化催化 性能

徐琪 1† ,郭辰曦 2† ,田书博 1† ,张剑 1 ,陈文星 3 ,张永臻 1 ,谷林 4 ,郑黎荣 5 ,肖建平 2 ,刘强 1 ,李必杰 1 ,王定胜 1* ,李亚栋 1

摘要 单原子催化剂的高效合理设计具有十分重要的意义,但是目前对于结构和性能之间的关联关系认知不足,严重阻碍了催化剂的发展进程。因此,清晰阐释金属活性中心的配位结构对于其催化性能的影响将有利于单原子催化剂的高效设计。本文研究报道了单原子Pt催化剂的活性中心配位结构显著影响其在烯烃反马氏硼氢化反应中的性能表现。三个O原子配位的Pt单原子催化剂(Pt-O₃)与另外两种配位结构(Pt-N₄和Pt-O₂)相比,表现出了更高的催化活性,在烯烃反马氏硼氢化反应中的转化数可达到3288. 密度泛函理论计算表明,Pt-O₃催化剂具有超高活性的主要原因是其在反应相图中具有最低的决速步能全.