

# Appendix A

## *n*-Fold Cross Validation

This technique is intended to avoid the possible bias introduced by relying on any one particular division into test and train components by partitioning the original data in several different ways and computing the average of the performances over the different partitions. When the available data is divided into  $n$  parts, this approach is called *n-fold cross-validation*. Because of the  $n$  identification and verification steps, this method is computationally expensive. An extreme variant of this is to split the  $N$  training data points into a training set of size  $N - 1$  and a test set of size 1 and average the squared error on the left-out pattern over the  $N$  possible ways of obtaining such partition.

The leave-one-out validation (LOO) can be calculated analytically for linear-in-parameter models [95]. The fuzzy model is linear in its consequent parameters. Hence, the LOO criteria and its derivatives can be easily used for these models:

$$\hat{\sigma}_{LOO}^2 = \frac{\mathbf{y}^T \mathbf{P} (\text{diag}(\mathbf{P}))^{-2} \mathbf{P} \mathbf{y}}{N}, \quad (\text{A.1})$$

where in the case of global identification,  $\mathbf{P}$  denotes the projection matrix

$$\mathbf{y} - \hat{\mathbf{y}} = \mathbf{y} - \mathbf{Q}\theta \quad (\text{A.2})$$

$$= \mathbf{y} - \mathbf{Q} (\mathbf{Q}^T \mathbf{Q})^{-1} \mathbf{Q}^T \mathbf{y} \quad (\text{A.3})$$

$$= (\mathbf{I}_N - \mathbf{Q} (\mathbf{Q}^T \mathbf{Q})^{-1} \mathbf{Q}^T) \mathbf{y} \quad (\text{A.4})$$

$$= \mathbf{P} \mathbf{y}, \quad (\text{A.5})$$

where the  $\mathbf{Q}$  matrix contains the  $N$  regressors,  $\mathbf{y}$  denotes the estimated outputs of the model, and  $\mathbf{P}\hat{\mathbf{y}}$  denotes the vector of the modeling error. The matrix  $\text{diag}(\mathbf{P})$  is the same size and has the same diagonal as  $\mathbf{P}$ , but it is zero off-diagonal, and  $\mathbf{I}_N$  represents an identity matrix.

# Appendix B

## Orthogonal Least Squares

An often applied solution is to prune the identified model trained with the classical cost function. In the following, model reduction techniques of this type will be considered. In general, it can be stated that linear model reduction methods are preferred to nonlinear ones because they are exhaustively studied and effectively applied for several types of problems. For that purpose the model should be linear in parameters. A possible method family is that of orthogonal techniques. These methods can roughly be divided into two groups: the rank-revealing ones, such as the SVD-QR algorithm, and those that evaluate the individual contribution of the rule or local models, such as the orthogonal least squares approach (OLS). This latter technique requires more computations, but for system identification purposes it is preferable as it gives a better approximation result. In this book OLS is applied for rule ranking and model reduction purposes. OLS works as follows (for a throughout discussion see [1]). Consider a general linear-in-parameters model;

$$\mathbf{y} = \mathbf{Z}\theta + \mathbf{e}, \tag{B.1}$$

where  $\mathbf{y} = [y_1, \dots, y_N]^T$  is the measured output,  $\mathbf{Z} = [\mathbf{z}_1, \dots, \mathbf{z}_n]^T$  is the regressor matrix ( $\mathbf{z}_i = [z_{i1}, \dots, z_{iN}]^T, i = 1, \dots, h$  are the regressors),  $\theta = [\theta_1, \dots, \theta_h]$  is the parameter vector and  $\mathbf{e} = [e_1, \dots, e_N]^T$  is the prediction error. OLS transforms the columns of the regressor matrix  $\mathbf{Z}$  into a set of orthogonal basis vectors in order to inspect the individual contribution of each regressor. If they were not orthogonal, they could not have been inspected individually. An orthogonalization method should be used to perform the orthogonal decomposition  $\mathbf{Z} = \mathbf{V}\mathbf{R}$  (often the simple Gram-Schmidt method is used), where  $\mathbf{V}$  is an orthogonal matrix such that  $\mathbf{V}^T \mathbf{V} = \mathbf{I}$  and  $\mathbf{R}$ . Substituting  $\mathbf{Z} = \mathbf{V}\mathbf{R}$  into Eq. B.1, we get  $\mathbf{y} = \mathbf{V}\mathbf{R}\theta + \mathbf{e} = \mathbf{V}\mathbf{g} + \mathbf{e}$ , where  $\mathbf{g} = \mathbf{R}\theta$ . Since the columns  $\mathbf{v}_i$  of  $\mathbf{V}$  are orthogonal, the sum of squares of  $y_k$  can be written as

$$\mathbf{y}^T \mathbf{y} = \sum_{i=1}^h g_i^2 \mathbf{v}_i^T \mathbf{v}_i + \mathbf{e}^T \mathbf{e}. \quad (\text{B.2})$$

The part of the output variance  $\mathbf{y}^T \mathbf{y} / N$  explained by regressors is  $\sum_{i=1}^h g_i^2 \mathbf{v}_i^T \mathbf{v}_i / N$  and an error reduction ratio due to an individual regressor  $i$  can be defined as

$$err_i = \frac{g_i^2 \mathbf{v}_i^T \mathbf{v}_i}{\mathbf{y}^T \mathbf{y}}, \quad i = 1, \dots, h. \quad (\text{B.3})$$

This ratio offers a simple means for ordering the regressors. As [1] shows, “there are only two restrictions to the application of this subset selection technique. First, the model has to be linear in parameters. Second, the set of regressors from which the significant ones will be chosen must be precomputed.” This latter restriction is an important one because it means that all regressors are fixed during this procedure. This requirement is not met by normalized RBF networks and Takagi-Sugeno fuzzy models; therefore the original version of OLS cannot be applied. It is because the normalization denominator changes with the number of selected rules; thus the fuzzy basis functions (here: regressors) change. To overcome this problem, the value of the denominator can be fixed, but in this case interpretability issues are discarded completely. However, OLS can be very useful for various purposes; modified versions of OLS can also be applied to determine the centers of radial basis functions, or to generate Takagi-Sugeno-Kang fuzzy models.

# Appendix C

## Model of the pH Process

The modeling and control of pH (the concentration of hydrogen ions) in a continuously stirred tank reactor (CSTR) is a well-known control problem that presents difficulties due to the nonlinearity of the process dynamics. The CSTR is shown schematically in Fig. C.1.

A dynamic model of the pH in a tank can be obtained by considering the material balances on  $[Na^+]$  and the total acetate  $[HAC + AC^-]$  and assuming that the acid-base equilibrium and electroneutrality relationships hold [96].

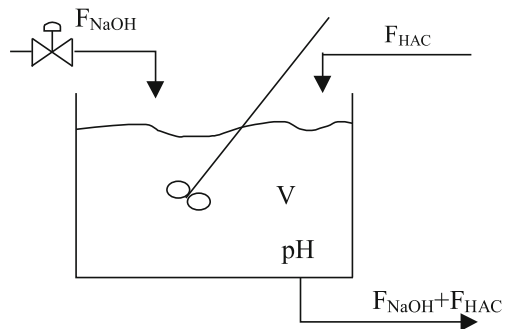
Total acetate balance:

$$F_{HAC}[HAC]_{in} - (F_{HAC} + F_{NaOH})[HAC + AC^-] = V \frac{d[HAC + AC^-]}{dt}.$$

Sodium ion balance:

$$F_{NaOH}[NaOH]_{in} - (F_{HAC} + F_{NaOH})[Na^+] = V \frac{d[Na^+]}{dt}.$$

**Fig. C.1** Scheme of the pH setup



**Table C.1** Parameters used in the simulations

Parameter	Description	Nominal value
$V$	Volume of the tank	1000 [l]
$F_{HAC}$	Flow rate of acetic acid	81 [l/min]
$F_{NaOH}$	Flow rate of NaOH	515 [l/min]
$[NaOH]_{in}$	Inlet conc. of NaOH	0.05 [mol/l]
$[HAC]_{in}$	Inlet conc. of acetic acid	0.32 [mol/l]
$[Na^+]$	Initial conc. of sodium in the CSTR	0.0432 [mol/l]
$[HAC + AC^-]$	Initial conc. of acetate in the CSTR	0.0432 [mol/l]
$K_a$	Acid equilibrium constant	$1.75310^{-5}$
$K_w$	Water equilibrium constant	$10^{-14}$

HAC equilibrium:

$$\frac{[AC^-][H^+]}{[HAC]} = K_a.$$

Water equilibrium:

$$[H^+][OH^-] = K_w.$$

Electroneutrality:

$$[Na^+] + [H^+] = [OH^-] + [AC^-].$$

The pH can be calculated from the previous equations as

$$[H^+]^3 + [H^+]^2(K_a + [Na^+]) + [H^+]( [Na^+]K_a - [HAC + AC^-]K_a - K_w ) - K_wK_a = 0,$$

$$pH = -\log[H^+].$$

The parameters used in our simulations are taken from [97] and are given in Table C.1.

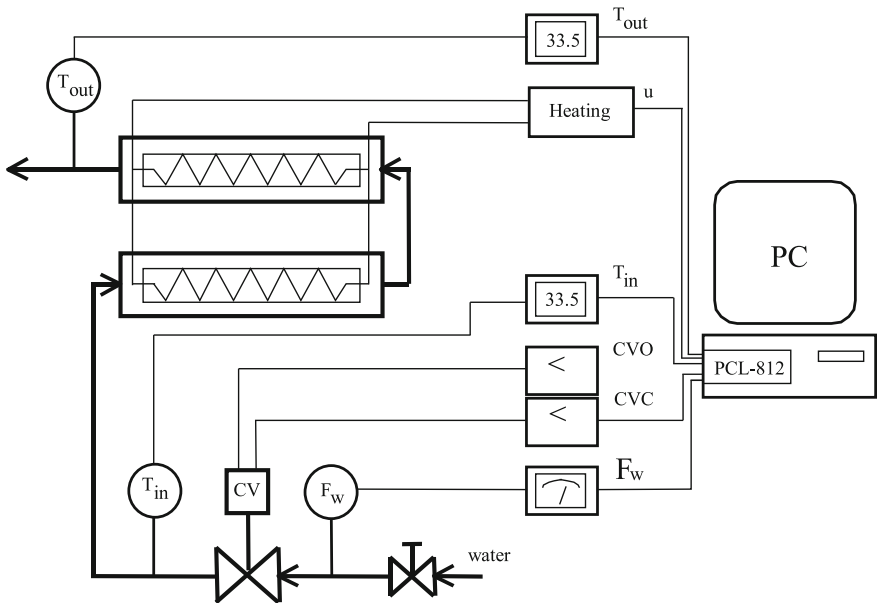
# Appendix D

## Model of Electrical Water Heater

The schematic diagram of the water heater is shown in Fig. D.1.

The water comes from the water pipeline into the heater through a control valve and a pair of metal pipes containing a cartridge heater. The control task is to control the  $T_{out}$  outlet temperature by adjusting the  $u$  heating signal of the cartridge heater.

The temperature measurement is realized using Pt100 thermometers. The system has four analog inputs (inlet temperature  $T_{in}$ , outlet temperature  $T_{out}$ , valve position, and the flow rate  $F$ ), and two digital (open and close in the valve, or CVO and



**Fig. D.1** The scheme of the physical system

CVC) and one analog output (heating control signal,  $u$ ). The heaters are linked in parallel and have a performance of 1 kW. The process is connected to a PC computer through ADVANTECH LabCard PCLD-780 and PCL-812 data acquisition boards. The GENIE 3.02 data acquisition and control software was used to filter and convert the input signals (0–5 V). The control algorithm runs in MATLAB 4.2. The sampling time of the control system is seconds [98].

For the purpose of physical modeling, the system was decomposed into four interacting elements: the cartridge heater (subscript  $h$ ), the streaming water (subscript  $w$ ), the pipe wall (subscript  $p$ ) and the environment (subscript  $e$ ). The following three heat balances in the form of partial differential equations can be established:

$$\begin{aligned} V_h \rho_h C_{ph} \frac{\partial T_h}{\partial t}(t, z) &= Q(u) - \alpha_1 A_1 (T_h - T_w), \\ V_w \rho_w C_{pw} \frac{\partial T_w}{\partial t}(t, z) + (F \rho C_p)_w \frac{\partial T_w}{\partial z}(t, z) &= \alpha_1 A_1 (T_h - T_w) - \alpha_2 A_2 (T_w - T_p), \\ V_p \rho_p C_{pp} \frac{\partial T_p}{\partial t}(t, z) &= \alpha_2 A_2 (T_w - T_p) - \alpha_e A_e (T_p - T_e), \end{aligned}$$

with  $z \in [0, L]$  where  $L$  denotes the length of the pipe. The description and the nominal values of the parameters are given in Table D.1.

**Table D.1** Parameters used in the simulation model of the heating system

Parameter	Description	Nominal value
$L$	Length of the pipe	$2 \times 48010^{-3}$ m
$\rho_h$	Density of the cartridge	$3650$ kg/m <sup>3</sup>
$C_{ph}$	Heat capacity of the cartridge	$1047$ J/kg K
$A_h$	Surface of the cartridge	$2.41 \times 10^{-2}$ m <sup>2</sup>
$V_h$	Volume of the cartridge	$4.82 \times 10^{-5}$ m <sup>3</sup>
$\alpha_1$	$h - w$ heat transfer coefficient	$316.3$ W m <sup>-2</sup> K <sup>-1</sup>
$\rho_w$	Density of the water	$1000$ kg/m <sup>3</sup>
$C_{pw}$	Heat capacity of the water	$4186$ J/kg K
$T_{in}$	Inlet water temperature	$11.8$ °C
$V_w$	Volume of the water	$1.16 \times 10^{-4}$ m <sup>3</sup>
$\alpha_2$	$w - p$ heat transfer coefficient	$1196.1$ W m <sup>-2</sup> K <sup>-1</sup>
$\rho_p$	Density of the wall	$7850$ kg/m <sup>3</sup>
$C_{pp}$	Heat capacity of the wall	$502$ J/kg K
$t_e$	Temperature of the environment	$21.6$ °C
$A_p$	Inner surface of the wall	$4.46 \times 10^{-2}$ m <sup>2</sup>
$V_p$	Volume of the wall	$7.37 \times 10^{-5}$ m <sup>3</sup>
$A_e$	Outer surface of the wall	$5.36 \times 10^{-2}$ m <sup>2</sup>
$\alpha_e$	$p - e$ heat transfer coefficient	$1015.9$ W m <sup>-2</sup> K <sup>-1</sup>

The performance of the cartridge heater is given by

$$Q(u) = Q_M \left[ u - \frac{\sin(2\pi u)}{2\pi} \right], \quad (\text{D.1})$$

where  $Q_M$  is the maximal power, and  $u$  is the heating signal (voltage). The partial differential equations are approximated by eight compartments of equal volume. As Eq. D.1 shows, the heating performance is a static nonlinear function of the heating signal (control input).



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