



# Preparation of branched polyurethane curing agent by condensation polymerization and radical polymerization

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## Abstract

A new PU curing agent with branched structure was prepared by esterification, radical polymerization and reaction of TDI. Unsaturated content (itaconic acid) was added in esterification of adipic acid and 1,4-butanediol, which prepared linear molecule poly (itaconic acid-adipic acid-1,4-butanediol). Then, azodiisobutyronitrile was used to initiate polymerization to form branched molecule (CPBIA). CPBIA reacted with semi-blocked TDI to prepare TDI-CPBIA. These polymers were characterized by FT-IR, <sup>1</sup>H NMR and GPC. Their structure was confirmed. The adjustment of polycondensation and radical polymerization by the raw material ratio and reaction temperature could yield the desired PU curing agent with branched structure and fine solubility. According primary experiments, TDI-CPBIA had fine application performance. The coating had good hardness (6H), thermal performance ( $T_0 > 250$  °C), adhesion (level 1) and impact strength (> 50 cm). This PU curing agent has fine application performance.

**Keywords** Polyurethane · Branched polymer · PU curing agent

## 1 Introduction

The demand for eco-friendly coatings, like waterborne coatings [1, 2], high solid coatings [3], UV curable coatings [4, 5] and powder coatings [6], has increased rapidly. Environmental concerns were the major factors behind this shift, such as recycling or waste disposal at the end of their life circle, volatile organic solvent emissions.

Polyurethane coatings had become the mainstream coatings for industrial coatings and civilian coatings because of their advantages such as good appearance, high hardness, abrasion resistance, wide applicable temperature and low cost [7]. Curing agent was a very important component in the coating system. The usual curing agents included toluene diisocyanate (TDI) trimer [8], 4,4'-methylenediphenyl diisocyanate (MDI) [9, 10], hexamethylene diisocyanate (HDI) [11] and isophorone diisocyanate (IPDI) [12]. Diphenylmethane diisocyanate (MDI) was used as curing agent for its low toxicity [13, 14]. For its

symmetry of MDI molecular structure, the strength, wear resistance and elasticity of coating film prepared by MDI were better than that of TDI. It was found by Yao Xiao et al. [10] that MDI-50-based waterborne polyurethane showed better properties compared to IPDI based waterborne polyurethane. Davletbaeva, I. M. found that segmented polyurethanes with the predetermined length of the rigid block were formed in the case of 4,4'-MDI, while the use of polyisocyanate gave rise to framed aromatic polyurethanes [15]. Though there were many kinds of the PU curing agents, TDI and its derivatives were the most popular.

However, free toluene diisocyanate (TDI) was often contained in the curing agent of polyurethane coatings, which has a great influence on the environment [16].

TDI-TMP prepolymer was prepared with TDI and trimethylolpropane (TMP) at certain condition [17]. It was the most common polyurethane curing agent and one of the earliest isocyanate prepolymer components [17]. There was a problem of free TDI in the curing

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agent because TDI was toxic [18, 19]. There were many researches on how to reduce the content of free TDI in TDI prepolymer, which were summarized as follows: molecular sieve adsorption [20], extraction [21, 22], chemical reaction [23], thin film evaporation [24, 25] and azeotropic distillation [26].

Molecular sieve was silicate crystals by artificial hydrothermal synthesis with highly efficient, deep and selective adsorbents, so it had high separation precision and separation rate [27]. Marans [20] used X type zeolite molecular sieve to adsorb free TDI in the tower. The prepolymer was put into the molecular sieve tower and made contact to promote the absorption of free TDI. The temperature of the prepolymer entering the tower was about 20 ~ 100 °C. The temperature of the tower was 40 ~ 85 °C. The temperature of molecular sieve and prepolymer was 50 ~ 75 °C. Then, molecular sieve was removed by filtration or centrifugation. TDI content of the prepolymer was greatly reduced. This method also avoided the possibility of reducing the effective NCO in the prepolymer by high temperature heating in the thin film evaporator. This process could reduce the mass fraction of TDI in the prepolymer by 50 ~ 99%.

The extraction method was based that the higher molecular weight fraction of the reaction product was soluble in the strong solvent, while the unreacted free TDI was only soluble in hydrocarbon or naphthenic hydrocarbon solvents, such as gasoline, petroleum ether, hexane, cyclohexane, benzene or its mixture. The extraction method included supercritical fluid extraction and ordinary solvent extraction. Robin [22] used carbon dioxide (or ethane, propane, butane and ethylene) as extractant. The mass fraction of isocyanate monomer in prepolymer was reduced to 0.03%, and the mass fraction of isocyanate dimers was reduced to less than 1%. Zhang Jie [28] used petroleum ether as the extractant and continuous circulation extraction, but the result was not very ideal. However, the separation effect was better with the azeotropic distillation.

Chemical reaction method could be divided into two kinds, the direct synthesis method and the catalytic polymerization method. The principle of catalytic polymerization was to add small molecule hydroxyl compounds that could react with TDI monomer and promote the polymerization of TDI-TMP in the prepolymer, so that TDI could be transformed into small molecular carbamate or TDI polymer. The content of free TDI was reduced to 0.2 ~ 0.3% [29]. In USP3384624 [30], Benzyl alcohol and benzyl alcohol derivatives with various hindrance groups on the benzene ring were added to the prepolymer, which could react with free TDI under heating to reduce free TDI content. Benzene ring and the hindrance groups on benzene ring could inhibit the

reaction between benzyl alcohol and NCO group of prepolymer, but could react with NCO group of TDI.

Thin film evaporation was a method of removing free TDI from curing agent under the condition of high vacuum by using outer cooled or internally cooled thin-film evaporator. The low free TDI product has been widely used [17]. The characteristics of high vacuum thin film evaporation are products with low molecular weight, narrow molecular weight distribution, high NCO content and high crosslink density. In USP3183112 [31], the prepolymer first heated the flash and then went into the thin film evaporator to remove the TDI. At that time, the concentration of free TDI was reduced to less than 2%. In several patents [32, 33], free TDI was removed by thin film evaporator at 100–160 °C and 0.1 ~ 0.8 mm Hg. In USP 4,385,171, azeotropic distillation was used to remove free monomer. Diisocyanate content was lower than 0.05% [26].

TDI-TMP was general PU curing agent. In addition, news polymer with branched chain could be prepared by esterification, radical polymerization and reaction of –OH and –NCO of TDI. News PU curing agent had several advantages such as low toxic, low viscosity and good application properties.

## 2 Experiments

### 2.1 Materials

Itaconic acid (IA, industrial product) was purchased from Qingdao Langyatai Group Co., China. Other reagents were (analytical reagent, AR) purchased from Sinopharm chemical reagent Co., Ltd., such as adipic acid, 1,4-butanediol, tetrabutyl titanate, hydroquinone, methyl alcohol, azodiisobutyronitrile, acetone, o-chlorophenol, toluene diisocyanate (TDI) and dibutyltin dilaurate.

### 2.2 Preparation of polyester

IA, adipic acid and 1,4-butanediol esterified in four-neck flask with tetrabutyl titanate as catalyst and hydroquinone as polymerization inhibitor. Reaction conditions was the temperature 170 °C, reaction time 6 h, the mole ratio of –OH and –COOH 1.2:1. The sample was dissolved into the methanol. Then, unreacted content was removed by water extraction. The product was dried in the oven at 80 °C.

### 2.3 Polyester crosslinking

Polyester polymerized in 4-neck flask with toluene as solvent, azodiisobutyronitrile as initiator under the condition of nitrogen atmosphere, reaction temperature 80 °C, reaction time 5 h. The sample was dried for 4 h.

## 2.4 Preparation of PU curing agent

TDI and *o*-chlorophenol were added into a 4-neck flask at room temperature and nitrogen atmosphere with the mole ratio of 1:1.2 (TDI: *o*-chlorophenol). After 0.5 h, the system was heated to 90 °C and kept for 5 h. Semi-blocked TDI was prepared.

Semi-blocked TDI solution with acetone as the solvent was put into constant pressure drop funnel. It was dropped slowly into crosslinking polyester with dibutyltin dilaurate as the catalyst at 40 °C and nitrogen atmosphere for 2.5 h. The sample was dried at 40 °C for 4 h.

## 2.5 Characterization

Fourier transform infrared (FT-IR) spectra were recorded with NICOLET MAGNA-IR750 Series II from 4000 to 600  $\text{cm}^{-1}$ .

$^1\text{H}$  NMR spectra were recorded with a Bruker 300 MHz spectrometer at room temperature using DMSO- $d_6$  as the solvent.

The molecular weights were measured by gel permeation chromatography (GPC, Shodex KF-805) using a liquid chromatograph equipped with TSK gel Super Mutipore HZ-M\*2, Flow rate 0.35 ml/min, the concentration 1.0 mg/ml, injection volume 20  $\mu\text{l}$  and column temperature 40 °C. Tetrahydrofuran (THF) was used as the eluent. The calibration was polystyrene ( $M_w$  750–570  $\times 10^4$ ).

The acid value of polymer was tested according to ASTM D465-01. The acetylating reagent method (IS 354, Part-1, 1987) was used to determine the hydroxyl value.

The intrinsic viscosity of polyesters was obtained by graphical extrapolation [34].

The TGA experiments were carried out with Thermal Analyzer (STA449C) in nitrogen from 30 to 600 °C with heating rate of 10 °C/ $\text{min}^{-1}$ . The measurement conditions were as follows: sample weight 5 mg, gas flow 50  $\text{ml min}^{-1}$ , and 150  $\mu\text{l}$  open alumina pan.

The tensile property was obtained by ZWICKI of Zwick/Roell.

DSC experiments were carried out with 204-F1DSC of ETZSCH under nitrogen atmosphere. The sample of about 7 mg was heated from –100 °C to 100 °C at 10 °C/ $\text{min}^{-1}$ . Then, it was cooled to room temperature.

The morphology of the coating was characterized using field emission scanning electron microscopy (SEM, JEOL JSM-6, Japan).

The hardness method was determined by marking a surface of a film with a pencil having a different hardness. The hardness test was based on the national standard GB/T 6739-1996.

The adhesion test was based on the national standard GB/T 9286-1998, which uses the cross-cut method. The

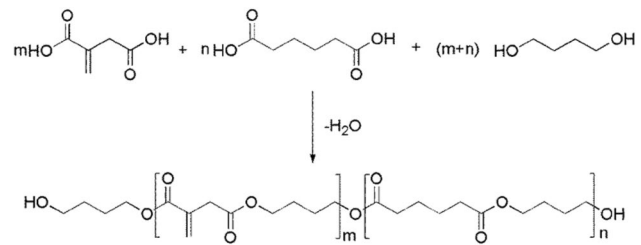


Fig. 1 The scheme of esterification

Table 1 Properties of PBIA

Sample	Acid value (mgKOH/g)	hydroxyl value (mgKOH/g)	$\eta$ (dL/g)	$M_w$	$M_n$
PBIA	40.60	251.72	0.0578	2023	1187

specific experimental method was to fix the cured coating sample on a horizontal table. The cross-cut was perpendicular to the template and the cross-shaped scratches are drawn. Then the transparent tape covered the scratches evenly, and finally the transparent tape was peeled off to observe the peeling of the scratches.

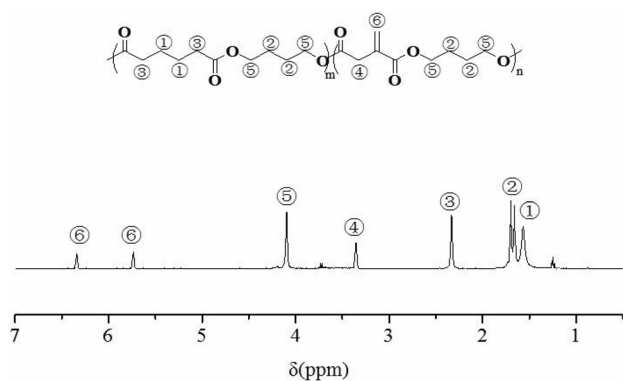
The impact performance of the paint film was the ability to resist external impact. The film was rapidly deformed under high-speed gravity without the ability to crack or fall off the horseshoe patch. The impact strength test was based on the national standard GB/T1732-93.

## 3 Results and discussion

### 3.1 Preparation of polyester

In order to prepare branched chain, IA was chosen as a monomer because it had a double group. Unsaturated polyester, poly (IA-adipic acid-1,4-butanediol) (PBIA) was prepared with IA as unsaturated acid, adipic acid as saturated acid and 1,4-butanediol as dihydric alcohol, shown in Fig. 1. The molecular weight of PBIA should be low so that the polymer could have fine solubility after crosslinking. PBIA properties were shown in Table 1. The mole ratio of –OH and –COOH was 1.2:1. Hydroxyl group was excessive. So, hydroxyl value of PBI was high and PBIA molecular was low.  $^1\text{H}$  NMR and FTIR of PBIA spectra were shown in Figs. 2 and 3.

In Fig. 2, The peaks at 1.697 and 4.124 ppm were attributed to the characteristic chemical shifts of protons in 1,4-butanediol. The peak at 3.372 ppm was attributed to the characteristic chemical shifts of protons in methylene group of IA. The peaks at 5.758 and 6.361 ppm were attributed to the characteristic chemical shifts of protons in



**Fig. 2**  $^1\text{H-NMR}$  spectrum of PBIA

double bond group of IA. The peaks at 1.57 and 2.33 ppm were attributed to the characteristic chemical shifts of protons of adipic acid.

In Fig. 3, characteristic peak at  $3547.43\text{ cm}^{-1}$  appeared due to the formation of hydroxyl group. The peaks at  $2927.14$  and  $2853.02\text{ cm}^{-1}$  were due to the telescopic vibration absorption peak of the C–H bond. Its bending vibration peak was  $1459.69$  and  $1390.11\text{ cm}^{-1}$ . The peak at  $1734.39\text{ cm}^{-1}$  was due to C=O. The peaks at  $1390.11$ ,  $1179.86\text{ cm}^{-1}$  were due to C–O–C, which confirmed ester group. The peak at  $1639.86\text{ cm}^{-1}$  was due to C=C. The peaks at  $955.71$  and  $748.29\text{ cm}^{-1}$  were due to C–O–C, which confirmed ester group. These peaks exhibited the structure of PBIA.

### 3.2 Crosslinking of PBIA

PBIA could polymerize with radical initiator because it had double bonds in its molecular chain. However,

crosslinking PBIA (CPBIA) solubility would decrease if its crosslinking degree was high. Therefore, the content of IA should be low. Meanwhile, the degree of crosslinking should be controlled. The content of double bond was controlled by feeding of IA during esterification. In polymerization, initiator was added with fare high dosage to ensure solubility of CPBIA with low crosslinking degree.

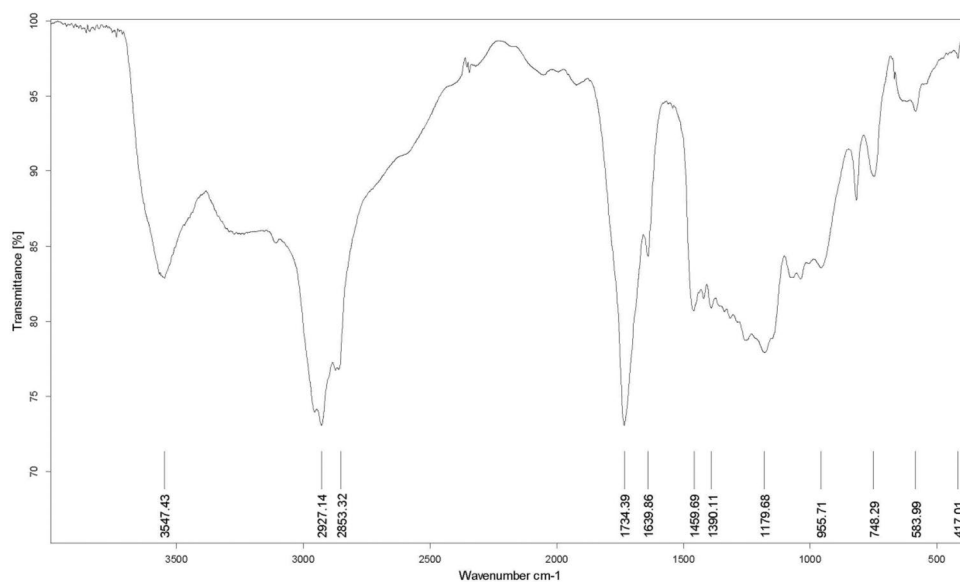
Molecular weight of CPBIA would increase after crosslinking. Its structure changed into crosslinking branched chain. CPBIA's properties were shown in Table 2. It was indicated that a part of –OH and –COOH esterified deeply because both acid value and hydroxyl value decreased comparing with Table 1. CPBIA's molecular weight increased for further esterification and crosslinking. So, its intrinsic viscosity increased obviously. Because of crosslinking of linear molecular structure, CPBIA's solubility changed greatly. CPBIA could dissolve in THF, ethyl acetate, acetone, methanol-toluene and ethanol-toluene. However, it could not dissolve in toluene, methanol and ethanol. Change of solubility was due to polar group (–OH and –COOH) and branched chain.

The structure of CPBIA was shown in Fig. 4. FTIR spectrum of CPBIA was shown in Fig. 5. Compared with Fig. 3, the peak of  $1639.86\text{ cm}^{-1}$  was very weak, which indicated that most of double bond had polymerization.

**Table 2** Properties of CPBIA

Sample	Acid value (mgKOH/g)	Hydroxyl value (mgKOH/g)	$\eta$ (dL/g)
PBIA-C	35.40	187.68	0.0861

**Fig. 3** FT–IR spectrum of PBIA



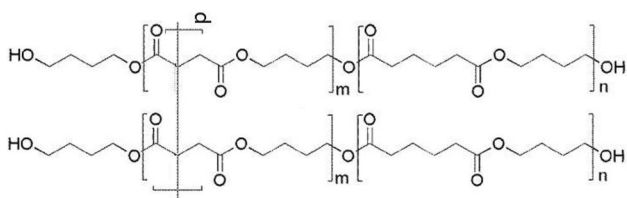


Fig. 4 The scheme of CPBIA

### 3.3 Preparation of PU curing agent

Isocyanate group of TDI could react with hydroxyl group and carboxyl group. Every molecule of CPBIA had several hydroxyl group and carboxyl group. So, the products of TDI and CPBIA would be crosslinked and insoluble. In order to ensure the solubility of curing agent, *o*-chlorophenol was chosen as blocking agent to react with one isocyanate group of TDI. Its blocking reaction rate was low. But its deblocking reaction rate was high and its deblocking reaction temperature was low [35]. After one isocyanate group of TDI reacted with *o*-chlorophenol, the activity of the rest was low. Therefore, one of isocyanate groups in TDI would be blocked by this reaction. Reaction product would have fine solubility with semi-blocked TDI because crosslinking was avoided.

New PU curing agent (TDI-CPBIA) was prepared with semi-blocked TDI and CPBIA, which FT-IR spectrum was

shown in Fig. 5. The properties of PU curing agent after deblocking were shown in Table 3 (Fig. 6).

The peak of  $3535\text{ cm}^{-1}$  was due to  $-\text{OH}$ , which indicated that CPBIA was excessive. The peaks of 3330 and 1536 were due to  $-\text{NH}$ . There is no peak of 2240–2280, which indicated that most TDI had reacted. That is to say, the concentration of free TDI was very low.

### 3.4 Performance of TDI-CPBIA

In order to investigate the properties of TDI-CPBIA, coatings were prepared based on TDI-CPBIA and poly (ethylene glycol-itaconate-succinate) (PEIS) for metal substrate. Curing temperature was  $120\text{ }^{\circ}\text{C}$ . Curing time was 2 h.

#### 3.4.1 Effect of PBIA's $M_w$

TDI-CPBIA was prepared with PBIA by crosslinking and reaction with TDI. So, PBIA's structure determined TDI-CPBIA's structure and its performance. The effect of PBIA's  $M_w$  was studied, as shown in Table 4. PBIA's  $M_w$  was controlled by modifying the ratio of components and polycondensation temperature. Then, CPBIA's  $M_w$

Table 3 Properties of TDI-CPBIA

Sample	Content of $-\text{NCO}$	$\eta(\text{dL/g})$
PU curing agent	2.04%	0.1

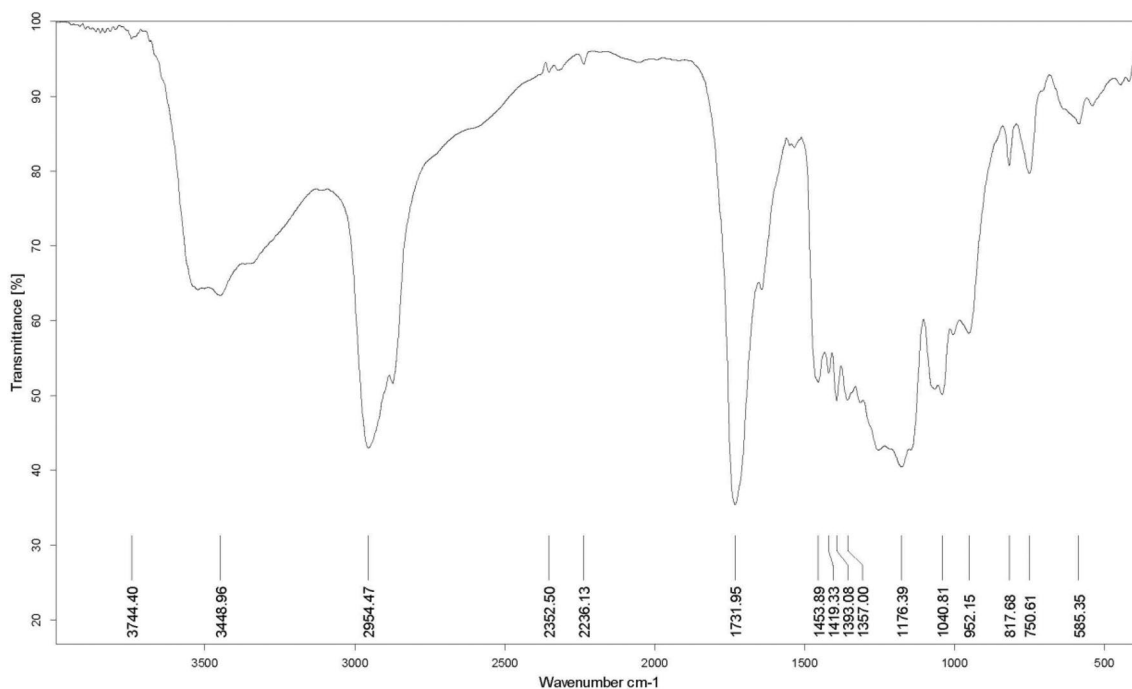
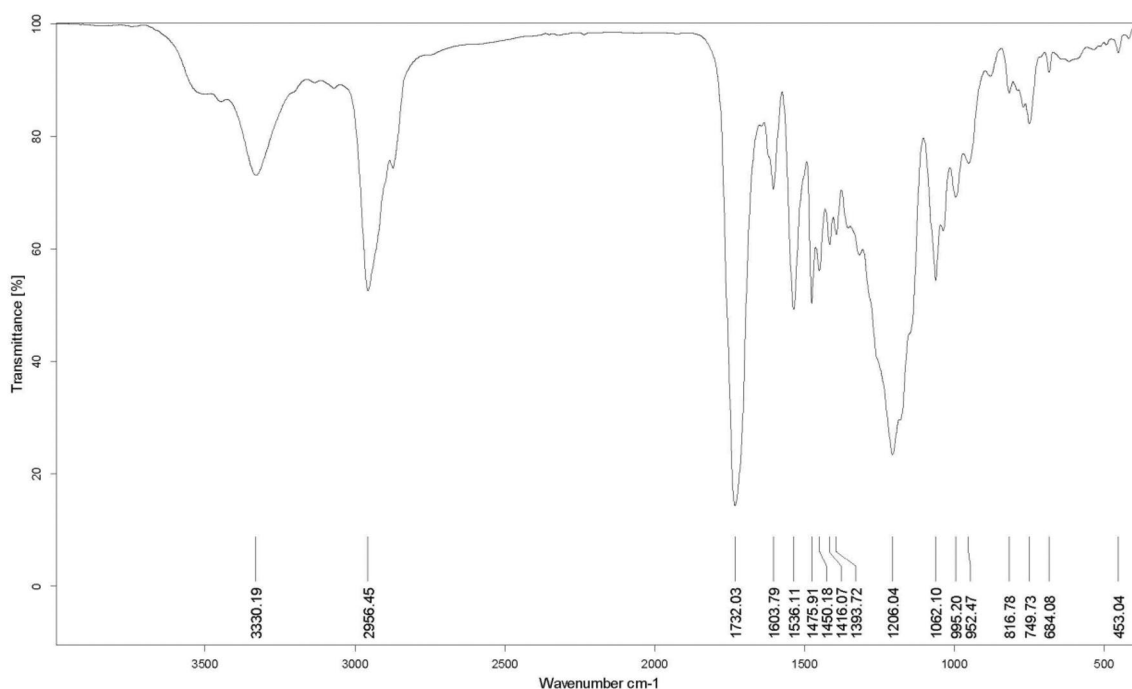


Fig. 5 FT-IR spectrum of CPBIA





**Fig. 6** FT-IR spectrum of TDI-CPBIA

**Table 4** Effect of PBIAs  $M_w$  on the properties of coating

PBIA's $M_w$	Pencil hardness (H)	Adhesion (cross cut test, 1 mm <sup>2</sup> )	Impact test (500 g, cm)	Coating thickness ( $\mu$ m)
1309	4	1	> 50	49
1678	5	1	> 50	48
2023	6	1	> 50	48
2301	6	2	> 50	49

was controlled by the dosage of initiator and polymerization temperature.

With increasing of PBIAs  $M_w$ , TDI-CPBIA had high molecular weight accordingly. After curing with polyether polyol, the degree of crosslinking would be higher. So, the hardness of the coating increased, as shown in Table 4. In term of adhesion, the performance was low when PBIAs  $M_w$  was the highest 2301. With increasing of PBIAs  $M_w$ , the branches were closer and interacted each other, which limited the branch activity. The force between coating and base material decreased accordingly. All sample performed good in impact test. In general, TDI-CPBIA was a good PU curing agent.

### 3.4.2 Thermal performance of the coating

Thermal performance of the coating was shown in Fig. 7 and Table 5 with different NCO/OH ratio. It was shown

that  $T_0$  and  $T_f$  of four sample were same, as about 255 °C and 485 °C, respectively. It indicated that these products had same structure. The difference was the temperature at different mass loss. When mass loss was lower than 50%, the curves were same. However, the ratio of mass loss decreased with NCO/OH ratio increasing when mass loss was higher than 50%. More NCO group would react with  $H_2O$  with high NCO/OH ratio. So, crosslinking degree between molecular chain increased. Therefore, the mass loss decreased.

PU coating had three types of thermal decomposition, which was affected by molecular crosslinking, hydrogen bond and inner crystalline structure. Firstly, C–O and C–N bonds of PU coating were broken into isocyanate and polyol under high temperature. Secondly, carbamate was broken into primary amine, alkene and  $CO_2$ . Thirdly, elimination reaction of carbamate occurred to form secondary amine and  $CO_2$ . Reaction mechanism was shown in Fig. 8 [36, 37].

In DTG of PEIS-PU coating, there were obviously four temperature peaks, which corresponded to the temperature of maximum mass-loss rate. The first peak was at about 286 °C, which corresponded to the decomposition of ester bond in carbamic acid ester of PEIS-IU. The highest peak was at about 390 °C between 320 °C and 450 °C, which corresponded to decomposition of polyester segment. In this area, mass loss rate increased with increasing of polyester content. The last mass loss area was at 450 ~ 500 °C, which corresponded to isocyanate group. In

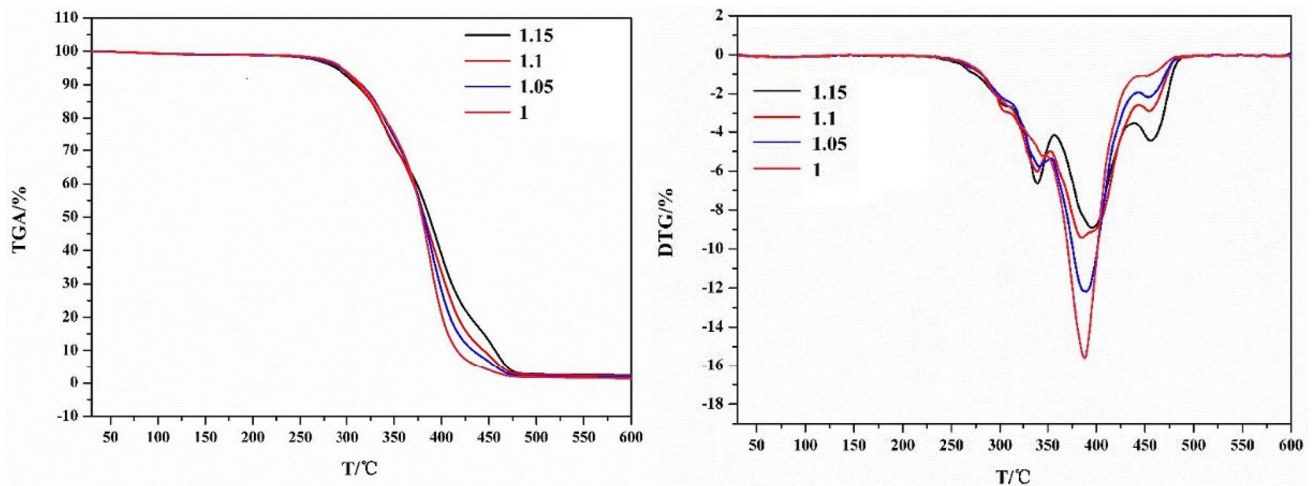


Fig. 7 TG of PEIS-PU with several NCO/OH ratio

Table 5 Thermal analysis of PEIS-PU

NCO/OH ratio	$T_0/^\circ\text{C}$	$T_{0.1}/^\circ\text{C}$	$T_{0.2}/^\circ\text{C}$	$T_{0.5}/^\circ\text{C}$	$T_{0.8}/^\circ\text{C}$	$T_f/^\circ\text{C}$
1.15	258	305	335	386	430	484
1.1	255	311	355	382	417	488
1.05	256	315	339	381	408	489
1	254	314	339	379	400	483

The numbers of 0.1, 0.2, 0.5 and 0.8 were mass loss of 10, 20, 50 and 80%, respectively

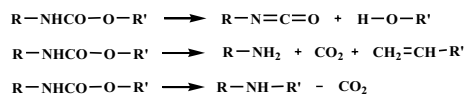


Fig. 8 The mechanism of thermal decomposition of PU coating

conclusion, coating thermostability would be better with high molar ratio to NCO/OH and low content of polyester.

### 3.4.3 Physical properties of the coating

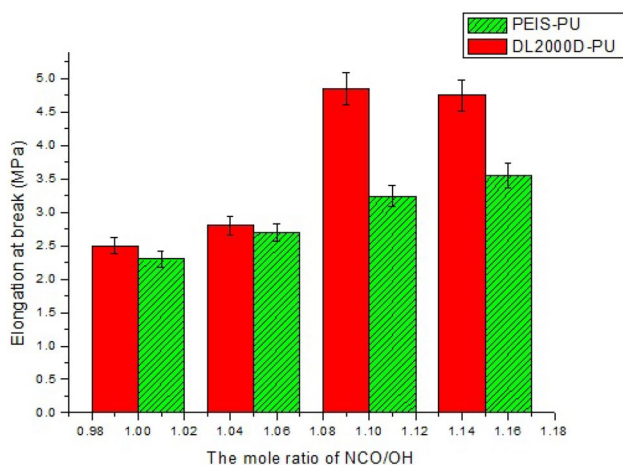
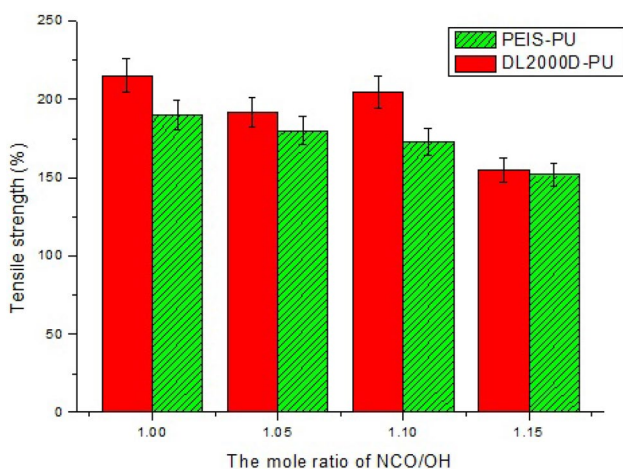
Physical properties of the coating would be different with different ratio of two components in two component polyurethane. If the component A (PU curing agent) was too little, some hydroxyl group would remain. The content of carbamic acid ester was little. In the coating, there were a lot of hydroxyl group, which was hydrophilic. Therefore, the coating was soft and low-hydrolytic resistance. On the contrary, excess isocyanate group would react with  $\text{H}_2\text{O}$  to form carbamide group with high content of component A. Crosslinking degree would increase, which made the coating fragile and low impact resistant. Optimized ratio of NCO/OH was about 1 ~ 1.15 with fine coating performance.

Coating performance was shown in Table 6 with different NCO/OH molar ratio. It was shown that it was high solid content coating (above 80%) so that low organic solvent would be needed. With the decrease of NCO/OH molar ratio, surface drying time and hard drying time increased and coating hardness decreased. Impact strength increased, too. Excessive NCO group would react with  $\text{H}_2\text{O}$  and release a lot of heat which accelerate solvent evaporation. So, drying time decreased with high NCO/OH molar ratio. Meanwhile, there were more crosslinking among coating molecule with the result of high hardness and fragile. Coating impact strength decreased with harder segment. In addition, the coating of PEIS and CPBIA had a fare drawback that it would shrink a little during curing. Heat release would be fast because NCO group of CPBIA had high reactivity. High solvent evaporation resulted in low levelling. Meanwhile, polyester had high surface tension which caused low wettability. So, the coating would shrink a little.

Mechanical properties of the coating were studied with PEIS and polyether polyol (DL2000D) as the component B. The coatings were prepared with PEIS and CPBIA (PEIS-PU) or DL2000D and CPBIA (DL2000D-PU). The results were shown in Figs. 9 and 10 with different component A/B ratio. When NCO/OH molar ratio decreased, Rigid

**Table 6** Coating performance with different NCO/OH mole ratio

NCO/OH molar ratio	Mass content /%	Surface drying time /h	Hard drying time /h	Pencil hardness (H)	Adhesion (cross cut test, 1 mm <sup>2</sup> )	Impact test (500 g, cm)
1.15	82.46	1.2	12	4	3	35
1.1	86.96	1.5	10	4	3	45
1.05	88.81	1.8	15	3	3	45
1	90	2	23	3	4	43

**Fig. 9** Tensile strength of the coating with PEIS-PU and DL2000D-PU**Fig. 10** Elongation at break PEIS-PU and DL2000D-PU

chain of carbamate decreased and soft chain of aliphatic chain and ether group increased. Meanwhile, crosslinking degree would increase with high NCO/OH molar ratio. Because of increasing of soft chain in component B and crosslinking degree decreased, the coating chain was movable and rotatable. So, tensile strength decreased as

shown in Fig. 9 and coating elongation increased as shown in Fig. 10. Comparing to PEIS, the ether group of DL2000L was more rotatable. So, with increasing of the component B, coating tensile strength decreased fast with DL2000D.

#### 3.4.4 SEM of the coating

The images of several coating fracture surface were shown in Figs. 11 and 12. It was shown that there was no tiny bubble and coating stripping and it was smooth. It was indicated that TDI-CPBIA had fine intermiscibility with PBIA and DL2000D. Two components could mix uniformly. That was the reason that the coating had good tensile strength and elongation. In Fig. 12a, there was a fissure in the coating. NCO/OH molar ratio was 1.15 for this sample. The content of NCO group was high. And that, TDI-CPBIA had branched chain. Most terminal group was -NCO. The crosslinking degree was high. During curing, the reaction between -NCO and -OH was fast. More heat was released and solvent evaporation of was fast. After the coating became solid, there was a little solvent evaporating. So, the coating shrank and broke.

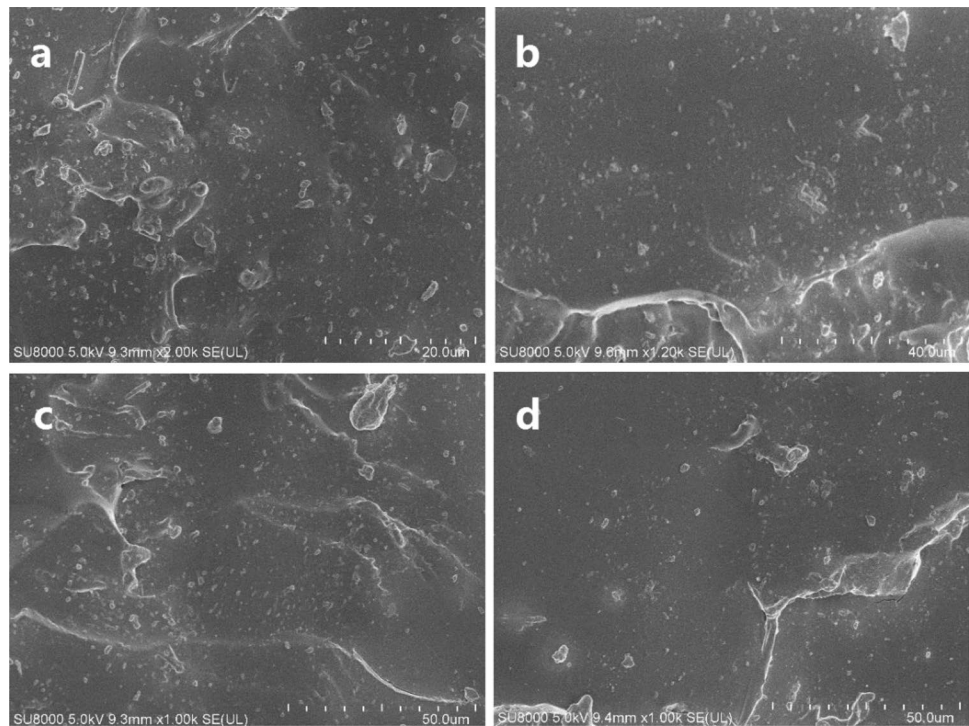
## 4 Conclusions

A PU curing agent with new structure was designed, which was branched and low toxicity. These polymers were characterized by several methods, such as <sup>1</sup>H NMR, GPC, FT-IR and so on.  $M_w$ , acid value and hydroxyl value of PBIA were about 2000, 40 and 250 mgKOH/g, respectively. The peaks of the characteristic chemical shifts of protons in 1,4-butanediol, IA and adipic acid occurred in the <sup>1</sup>H-NMR and FT-IR spectra. It was indicated that the structure of polymer was same as designed. These polymers had suitable molecular weight and solubility.

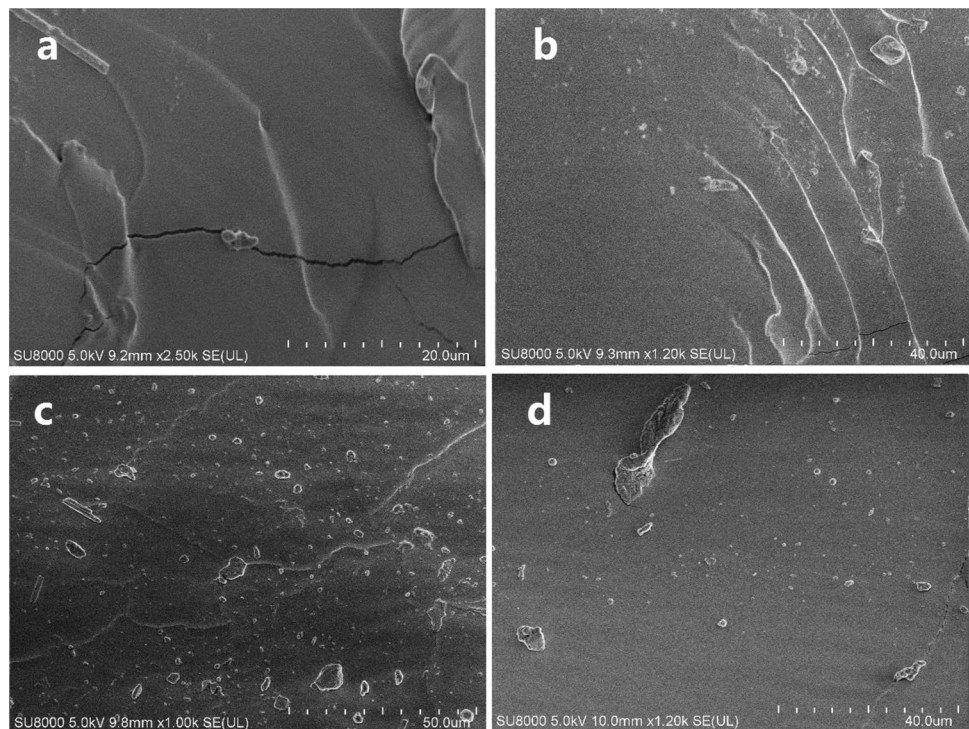
After radical polymerization, acid value and hydroxyl value of PBIA changed into 35.4 and 187.68, respectively. It was indicated that a little of acid and hydroxyl group reacted again. The peak of double bond was very weak in FT-IR spectrum. The intrinsic viscosity changed from 0.0578 to 0.0861 dL/g. PBIA was crosslinked under controllable degree.



**Fig. 11** SEM images of PBIA-PU coating with different NCO/OH molar ratio (**a** 1.15; **b** 1.1; **c** 1.05, **d** 1)



**Fig. 12** SEM images of DL2000D-PU coating with NCO/OH molar ratio (**a** 1.15; **b** 1.1; **c** 1.05, **d** 1)



It was indicated in FT-IR spectrum of TDI-CPBIA that the concentration of free TDI was very low. The new PU curing agent had a suitable content of -NCO.

TDI-CPBIA had fine application performance. Pencil hardness, adhesion and impact test were above 6 H, level

1 and 50 cm. Meanwhile, the PEIS-PU had good thermal performance with  $T_0 > 25^\circ\text{C}$ . It was shown in SEM images that there was no tiny bubble and coating stripping and it was smooth. TDI-CPBIA had fine intermiscibility with PBIA and DL2000D.

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## Compliance with ethical standards

**Conflict of interest** On behalf of all authors, the corresponding author states that there is no conflict of interest.

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