



Soret–Dufour and radiative aspects in hydromagnetized nanofluid flow in stratified porous medium

M. I. Anwar^{1,2,3} · M. Ali⁴ · K. Rafique³ · S. A. Shehzad⁵

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Abstract

The numerical computations of Soret–Dufour aspects in hydromagnetics nanofluid flow in thermal stratified porous medium under radiated chemical reaction are developed. The unique similarity transformations lead to reduce the partial differential system into expressions of ordinary ones. Keller-box approach is adopted to express the numeric solutions. The impacts of embedded flow parameters on the different flow profiles signifying velocity, concentration and temperature of nanofluid are discussed via graphs. The values of $-\theta'(0)$, $-\phi'(0)$ and $-f''(0)$ in relation with the variation in sundry physical parameters are examined through numerical benchmarks. The numerical results in special cases agreed with published work showing the validity of formulated problem. It can be seen that the temperature profile enhances for cumulative values of Brownian motion and thermophoretic impacts. In addition, the enhancement in Dufour factor declines the temperature profile. On contrast, larger the Soret parameter results an increase in concentration profile. On the other hand, chemical reaction shows direct relation with temperature profile.

Keywords Radiation effect · Chemical reaction · Thermal stratification · Soret–Dufour effects · Stratified medium

1 Introduction

Soret–Dufour aspects in the heat transportation problems are of enormous curiosity and widely growing interest in such type of investigations becomes on peak due to emerging implications in distinct branches such as geosciences, chemical engineering, hydrology and petrology. Various flow analysis have been performed on these effects encountered in number of processes by means of different interesting experimental and theoretical methodologies. The creation of fluxes associated with heat-mass transfer is well-known phenomenon, the mass flux in result of temperature gradient is familiar as Soret effect. Also, Dufour effect which is the generation of energy flux from concentration gradients. These effects are second ordered phenomena that are reciprocal processes. Sometimes

these ignored and neglected in different flow problems because of very smaller order of magnitudes on comparing with Fick's and Fourier's laws aspects. According to Eckert and Drake [1], these cannot be ignored in many cases like in separation of isotope and fluids of medium molecular weight. Soret–Dufour in mass heat flow phenomenon was carried out by Chapman and Cowling [2] by employing the gases kinetic theory. Furthermore, the Soret–Dufour effects in monatomic polyatomic/gases mixtures was developed by Hirshfelder et al. [3]. In addition, flow through porous media is engaged for different purpose like as filtration and purification, the water resources underground the earth surface, disposal of nuclear wastes in the soil. In petroleum industries, these are utilized to examine the motion of natural gas, water and oil in the oil reservoirs and also used to enhance the oil recovery. With

✉ S. A. Shehzad, ali_qau70@yahoo.com | ¹Department of Mathematics, Faculty of Science, University of Sargodha, Sargodha, Pakistan. ²Higher Education Department (HED), Lahore, Punjab, Pakistan. ³School of Quantitative Sciences, Universiti Utara Malaysia, 06010 Sintok, Kedah, Malaysia. ⁴Department of Mathematics, Ripah International University, Faisalabad Campus, Faisalabad, Pakistan. ⁵Department of Mathematics, COMSATS University Islamabad, Sahiwal 57000, Pakistan.



the emerging applications, the researcher's attempts on Soret–Dufour aspects of fluid flow are referred to [4–9].

Stratification is the feature of all liquids that enclosed by differentially heated walls. The effects of thermal stratification can be produced when the thermal boundary layer continuously discharge within the medium. When a hot fluid discharge over a cold region, thermal stratification can be produced with lighter liquid overlying dense liquid. The dynamics of flows owing to a hot surface embedded in a thermally stratified fluid is characterized by the researchers in numerous studies during the last few years. Generally, thermal stratification is encountered in the heat transfer processes of chemical and hydrometallurgical industries. Existing of these effects in flow over stretchable surfaces become most valuable. For instance, during the polymer extrusion, the object pass through a die and then proceed under a suitable temperature for cooling. The rate of cooling has considerable role in the final product having suitable properties. Considering thermal stratification effects, there are pertinent research works [10–13] has been carried out by investigators in this regard.

Choi [14] first time introduced the nanofluid which is special class of fluids and nanotechnology is based on the nanofluid become a large field of research among the researchers during the last few decades. Nanofluids are prepared by the stable and uniform suspensions of nanometer sized solid particles called nanoparticles (Al_2O_3 , Cu, CuO) in the liquids. Nanofluid has plenty of important applications in engineering and technology and widely used for thermal processes at industrial level. Choi also described these suspensions of nanoparticles can be used for the enhancement of the thermal conductivity of other fluids because these are unique in thermal, mechanical, optical, electrical and magnetic properties. Further, he pointed out that nanofluid are best candidates for heat and mass transfer when these are compared with the other fluids. For applications of nanofluid, see [15–18].

The model of Tiwari-Das [19] and Buongiorno [20] are used widely for the behavior of nanofluid by different investigators. The Tiwari-Das model is effective especially for volumetric fraction of the nanoparticles in the parent fluids. The characterization of Brownian and thermophoresis factors is made in Buongiorno model. This model exposed improvement of heat transfer in convective states instead of the thermophysical properties of nanofluids and explained different ways to enhance the thermal conductivity in relation with the parent fluids. It is also pointed out that nanoparticles occupying Brownian motion and thermophoresis impacts cause enhancement of thermal conductivity. Recently, Sheikholeslami, and Rokni [21] considered the non-equilibrium model for the flow of nanofluid through a porous cavity. Moreover, Sheikholeslami et al. [22] used two phase model (Lagrangian-Eulerian approach)

for the flow of nanofluid through a wavy chamber. Numerous investigators [23–26] used Buongiorno model to study flow characteristics.

Several researchers explored the MHD effects in numerous energy-related flows induced by stretching sheet. MHD flows are accounted in many processes such as flow meters, MHD power generators, energy recovery, plasma studies, aerodynamic and solar energy devices. The physical effects in MHD offer influential situations in heat flow problems. The Lenz's law indicates that the electric current is induced on a moving conductor under the magnetic field impacts which comprises its own magnetic field. The motion of fluid modifies when conducting fluid moves under the impact of magnetic field, the magnetic nanoparticles interact with Lorentz forces. MHD fluids controlled system performance by means of electrically conducting fluids. For brief knowledge, one can see researcher attempts on MHD effects in references [27–36].

The chemical reaction is stimulus and widely exist in nature and well as in chemical industries. It occupies lot of applications in chemical engineering and useful in ceramics, food processing and polymer productions etc. In addition, a vast variety of situations occurs in technology where high temperature is necessary and impacts of radiation become most valuable. Some processes are power plants for power generation, spacecrafts engines, space exploration, hypersonic light and solar power devices. In view of such important reasons, many researchers [37–40] have been reported various studies in this direction.

The motivation behind the consideration of the current model is the importance of key parameters i.e. Brownian motion and thermophoretic impacts. According to Buongiorno's these impacts are triggered the enhancement of thermal conductivity of the base fluids. In addition, keep in mind the growing need of heat exchange processes in industry and nuclear reactors we develop the current nanofluid study from the Buongiorno model.

2 Problem formulation

Consider the two dimensional coordinate system in a manner that x -axis is directed to stretching sheet inserted inside the porous medium and the y -axis is upward direction to sheet. It is assumed that the stretched and free-stream velocities are defined by $u_w(x) = ae^{x/l}$ and $u_\infty(x) = 0$, where x is coordinate parallel to sheet, l is denoting length of stretching sheet while $a > 0$ is constant. Also assumed a non-uniform transversely applied magnetic field having the strength $B = B_0 e^{x/l}$. Also, no external electrical field supposed to exist, so that the impact of polarization of charges is negligibly small [41]. The induced magnetic field created by nanofluid (electrically conducting) motion is also

in negligibly small amount as in comparison with applied one. Flow geometry is illustrated in Fig. 1.

The governing equations in the usual dimensional forms are:

$$\frac{\partial v}{\partial y} + \frac{\partial u}{\partial x} = 0, \tag{1}$$

$$v \frac{\partial u}{\partial y} + u \frac{\partial u}{\partial x} = \frac{\mu}{\rho_f} \frac{\partial^2 u}{\partial y^2} - \left(\frac{v}{K} + \frac{\sigma B_0^2}{\rho_f} \right) u, \tag{2}$$

$$v \frac{\partial T}{\partial y} + u \frac{\partial T}{\partial x} = \alpha \frac{\partial^2 T}{\partial y^2} - \frac{1}{(\rho C)_f} \frac{\partial q_r}{\partial y} + \tau \left[\left(\frac{\partial T}{\partial y} \right)^2 \frac{D_T}{T_\infty} + D_B \frac{\partial T}{\partial y} \frac{\partial C}{\partial y} \right] + \frac{D_T K_T}{C_s C_{p^*}} \frac{\partial^2 C}{\partial y^2}, \tag{3}$$

$$v \frac{\partial C}{\partial y} + u \frac{\partial C}{\partial x} = D_B \frac{\partial^2 C}{\partial y^2} - R(C - C_\infty) + \frac{\partial^2 T}{\partial y^2} \frac{D_T K_T}{T_\infty}. \tag{4}$$

The symbols used in above expressions are: x and y show the Cartesian coordinates measured directed to the stretching sheet and normal to it while u and v the velocity components in x and y coordinates, ρ_f the density, ν the kinematic viscosity, K the permeability of porous medium, σ the electric conductivity, B_0 the uniform magnetic field, $\alpha = \frac{k}{(\rho C)_f}$ the thermal diffusivity, τ the thermophoretic, D_B the Brownian diffusion, D_T the thermophoretic, K_T the ratio of thermal diffusion, C_s the concentration susceptibility and C_{p^*} the specific heat capacity.

Employing Rosseland approximation (radiation flux) [42] for an optically thick layer one has:

$$q_r = -\frac{4\sigma^*}{3k^*} \frac{\partial T^4}{\partial y}. \tag{5}$$

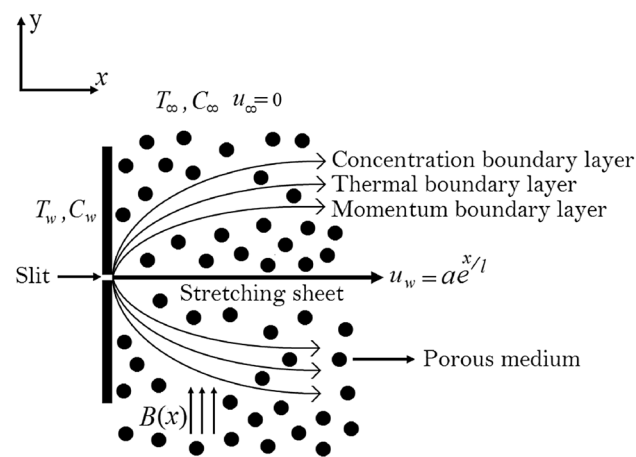


Fig. 1 Flow diagram with coordinates

The term T^4 in radiation flux formula can be solved in Taylor series about T_∞ and when high order expressions eliminate, it gives

$$T^4 \cong 4T_\infty^3 T - 3T_\infty^4. \tag{6}$$

In the view of expressions (5) and (6), Eq. (3) changes to

$$\frac{\partial T}{\partial y} + u \frac{\partial T}{\partial x} = \left(\alpha + \frac{16\sigma^* T_\infty^3}{3k^*(\rho C)_f} \right) \frac{\partial^2 T}{\partial y^2} + \tau \left[\left(\frac{\partial T}{\partial y} \right)^2 \frac{D_T}{T_\infty} + D_B \frac{\partial T}{\partial y} \frac{\partial C}{\partial y} \right] + \frac{D_T K_T}{C_s C_{p^*}} \frac{\partial^2 C}{\partial y^2}. \tag{7}$$

The subjected boundary conditions are:

$$u = u_w(x) = a e^{x/l}, v = 0, C = C_w(x), T = T_w(x) \text{ at } y = 0, \\ u \rightarrow 0, v \rightarrow 0, C \rightarrow C_\infty, T \rightarrow T_\infty = nT_w(x) + (1-n)T_o, \text{ as } y \rightarrow \infty. \tag{8}$$

where n denotes constant known as thermal stratification parameter which can be taken in the way $0 \leq n < 1$ and equal to $\frac{m_1}{1+m_1}$ where m_1 shows constant. The prescribed temperature and concentration over the stretchable surface can be defined as

$$T_w(x) = T_o + T_0 e^{x/2l}, C_w(x) = C_o + C_0 e^{x/2l} \tag{9}$$

where T_o is the reference temperature while C_o denotes the reference concentration. In order to obtain nonlinear ordinary form of flow equations, An appropriate stream function $\psi = \psi(x, y)$ satisfying continuity Eq. (1) with the similarity transformations are taken as:

$$\psi = \sqrt{2\ell} a e^{x/2l} f(\eta), \theta(\eta)(-T_\infty + T_w) = (-T_\infty + T), u = \frac{\partial \psi}{\partial y}, \\ \phi(\eta)(-C_\infty + C_w) = (-C_\infty + C), \eta = y \sqrt{\frac{a}{2\nu\ell}} e^{x/2l}, v = -\frac{\partial \psi}{\partial x}, \tag{10}$$

Equation (2), (4) and (7) reduced with the help of (10) into the following forms:

$$f''' - (K_1 + M)f' + ff'' - 2f'^2 = 0, \tag{11}$$

$$Pr_N \theta'' + Nt\theta'^2 + D_f \phi'' + f\theta' - f'\theta - \left(\frac{n}{1-n} \right) f' + Nb\theta' \phi' = 0, \tag{12}$$

$$\phi'' - Le f' \phi + Le f \phi' - Le R \phi + S_r Le \theta'' = 0. \tag{13}$$

The derivative of variables with respect to η are indicated by superscript $'$, $Pr = \frac{\nu}{\alpha}$ the Prandtl number, $Le = \frac{\nu}{D_B}$ the Lewis number, $M = \frac{2\sigma B_0^2}{a\rho_f}$ the Hartmann number, $K_1 = \frac{2\nu}{aKe^{x/2l}}$ the permeability parameter, $Pr_N = \frac{1}{Pr} \left(1 + \frac{4}{3} N \right)$ the modified Prandtl number where $N = \frac{4\sigma^* T_\infty^3}{\alpha k^* (\rho C)_f}$ the radiation constraint, $R = \frac{2lR^*}{u}$ the chemical reaction constraint,

$S_r = \frac{D_T K_T (T_w - T_\infty)}{\nu T_\infty (C_w - C_\infty)}$ the Soret number, $D_f = \frac{D_T K_T (C_w - C_\infty)}{\nu C_s C_p^* (T_w - T_\infty)}$ the Dufour number, $Nt = \frac{\tau D_T (T_w - T_\infty)}{\nu T_\infty}$ the thermophoresis parameter and $Nb = \frac{\tau D_B (C_w - C_\infty)}{\nu}$ the Brownian motion constraint. The corresponding boundary conditions (8) become

$$\begin{aligned} f(\eta) = 0, \quad f'(\eta) = 1, \quad \phi(\eta) = 1, \quad \theta(\eta) = 1 \quad \text{at } \eta = 0, \\ f'(\eta) \rightarrow 0, \quad \phi(\eta) \rightarrow 0, \quad \theta(\eta) \rightarrow 0 \quad \text{at } \eta \rightarrow \infty. \end{aligned} \tag{14}$$

The skin friction, Sherwood number and Nusselt number for the current study are regarded as

$$Nu_x = \frac{xq_w}{k(T_w - T_\infty)}, \quad Sh_x = \frac{xq_m}{D_B(C_w - C_\infty)}, \quad C_f = \frac{\tau_w}{u_w^2 \rho_f} \tag{15}$$

where $q_w = -k \frac{\partial T}{\partial y}$, $q_m = -D_B \frac{\partial C}{\partial y}$, $\tau_w = \mu \frac{\partial u}{\partial y}$, $aty = 0$,

The related terms of dimensionless reduced Nusselt number $-\theta'(0)$, reduced Sherwood number $-\phi'(0)$ and skin friction coefficient C_{fx} are:

$$\begin{aligned} C_{fx}(0) &= C_f \sqrt{\left(\frac{2l}{x}\right) Re_x}, \quad -\theta'(0) \\ &= \frac{Nu}{\left(1 + \frac{4}{3}N\right) \sqrt{\left(\frac{x}{2l}\right) Re_x}}, \quad -\phi'(0) \\ &= \frac{Sh}{\sqrt{\left(\frac{x}{2l}\right) Re_x}}. \end{aligned} \tag{16}$$

where $Re_x = \frac{U_w(x)x}{\nu}$ is the local Reynolds number. In order to get a numerical solution of the developed equations, Keller Box method is used an efficient scheme which is best for calculating boundary-layer stream. The equations proceed under the finite difference derivatives, Newton's, block-elimination methods and computed by MATLAB by defining suitable starting conditions. For detailed methodology of this procedure, see [43].

3 Results and discussions

A series of numerical computations has been performed by implementing a useful numerical scheme called the Keller-box method on system of Eqs. (11–13) with their appropriate boundary conditions (14) to obtain an insight into the physical situation of flow configuration. These computations are obtained for numerous magnitudes of Pr, Nb, Nt, M, Le, K₁, S_r, N, R, D_f and n which are displayed in Tables 1 and 2 and graphical format (Figs. 2, 3, 4, 5, 6, 7, 8, 9, 10, 11, 12, 13, 14, 15, 16 and 17). A comparison has been provided among currently acquired results and literature

Table 1 The values of $-\theta'(0)$ for $Nt = Nb = K_1 = D_f = S_r = Le = n = R = 0$

Pr	M	N	$-\theta'(0)$	
			Bidin and Nazar [44]	Present results
1.0	0.0	0.0	0.9548	0.9548
2.0	0.0	0.0	1.4714	1.4714
3.0	0.0	0.0	1.8691	1.8691
1.0	0.0	1.0	0.5315	0.5312
1.0	1.0	0.0	-	0.8611
1.0	1.0	1.0	-	0.4505

results displaying well agreement which verify accuracy of studied problem.

Table 1 gives the accuracy of present investigation by providing agreement for $-\theta'(0)$ with other publications while Table 2 provides the clear insight of $-\theta'(0)$, $-\phi'(0)$ and $C_{fx}(0)$ vary with respect to alteration in values of Nt, Pr, Nb, M, Le, K₁, N, R, D_f, n and S_r in such a way that one parameter increases while all other parameters remain fix at particular values. One can easily noticed that $-\theta'(0)$ shows rise in case of rising values for Nt, Pr, M and K₁ but for higher the values of Le, Nb, N, R, D_f, n and S_r, $-\theta'(0)$ decreases. It is also observed that $-\phi'(0)$ increases when N, R, Nb, D_f, Le, n and S_r enhance but when Nt, Pr, M and K₁ enhance, $-\phi'(0)$ depicts decline. No changes are observed in $C_{fx}(0)$ in case of increment in Nt, Nb, Pr, Le, N, R, D_f, n and S_r while $C_{fx}(0)$ rises for M and K₁ only.

Figures 2 and 3 express the velocity profile for numerous values of the parameters characterizing the flow velocity. It is observed that increase of K₁ reduces the velocity profile. It is now a well-established fact that high resistance is offered by porous medium by means of high shear stress opposite to the flow in case of increasing permeability parameter. As a result, velocity profile decreases. Interaction of Lorentz force and flow boost up by enhancing M. Hence, the flow becomes slow and velocity profile reduces, which is illustrated in Fig. 3.

Figures 4, 5, 6, 7, 8, 9, 10 and 11 depict the impacts of different parameters on temperature distribution. It is remarked by Fig. 4 that, a rise in n leads to enhance temperature profile. A reverse trend (decrease) is noticed from temperature profile in case of increasing the values of N as described by Fig. 5. It is clear from Fig. 6 that the temperature profile enhances with the enhancing values of R. Also the temperature contour decreases by growing the magnitudes of Pr expressed by Fig. 7. The contribution of this parameter in the reduction temperature profile is justified as the ratio of viscous diffusion rate to thermal diffusion rate depicts the basic definition of Prandtl number so

Table 2 The calculations of $-\theta'(0)$, $-\phi'(0)$ and $C_{fx}(0)$ with variations

Nb	Nt	Pr	Le	M	K_1	R	N	D_f	S_r	n	$-\theta'(0)$	$-\phi'(0)$	$C_{fx}(0)$
0.1	0.1	7.0	5.0	0.1	1.0	1.0	1.0	0.1	0.1	0.1	1.0026	3.3079	1.4491
0.5	0.1	7.0	5.0	0.1	1.0	1.0	1.0	0.1	0.1	0.1	-0.1682	3.3793	1.4491
0.1	0.3	7.0	5.0	0.1	1.0	1.0	1.0	0.1	0.1	0.1	4.9156	3.0670	1.4491
0.1	0.1	8.0	5.0	0.1	1.0	1.0	1.0	0.1	0.1	0.1	1.4386	2.7411	1.4491
0.1	0.1	7.0	10.0	0.1	1.0	1.0	1.0	0.1	0.1	0.1	0.5647	5.1739	1.4491
0.1	0.1	7.0	5.0	2.5	1.0	1.0	1.0	0.1	0.1	0.1	1.2942	2.7825	2.1213
0.1	0.1	7.0	5.0	0.1	2.0	1.0	1.0	0.1	0.1	0.1	2.2214	3.0666	1.7607
0.1	0.1	7.0	5.0	0.1	1.0	3.0	1.0	0.1	0.1	0.1	0.9046	4.7633	1.4491
0.1	0.1	7.0	5.0	0.1	1.0	1.0	5.0	0.1	0.1	0.1	0.5601	3.3315	1.4491
0.1	0.1	7.0	5.0	0.1	1.0	1.0	1.0	0.3	0.1	0.1	-1.4558	3.8343	1.4491
0.1	0.1	7.0	5.0	0.1	1.0	1.0	1.0	0.1	0.3	0.1	-0.3007	3.6656	1.4491
0.1	0.1	7.0	5.0	0.1	1.0	1.0	1.0	0.1	0.1	0.2	0.4285	3.3468	1.4491

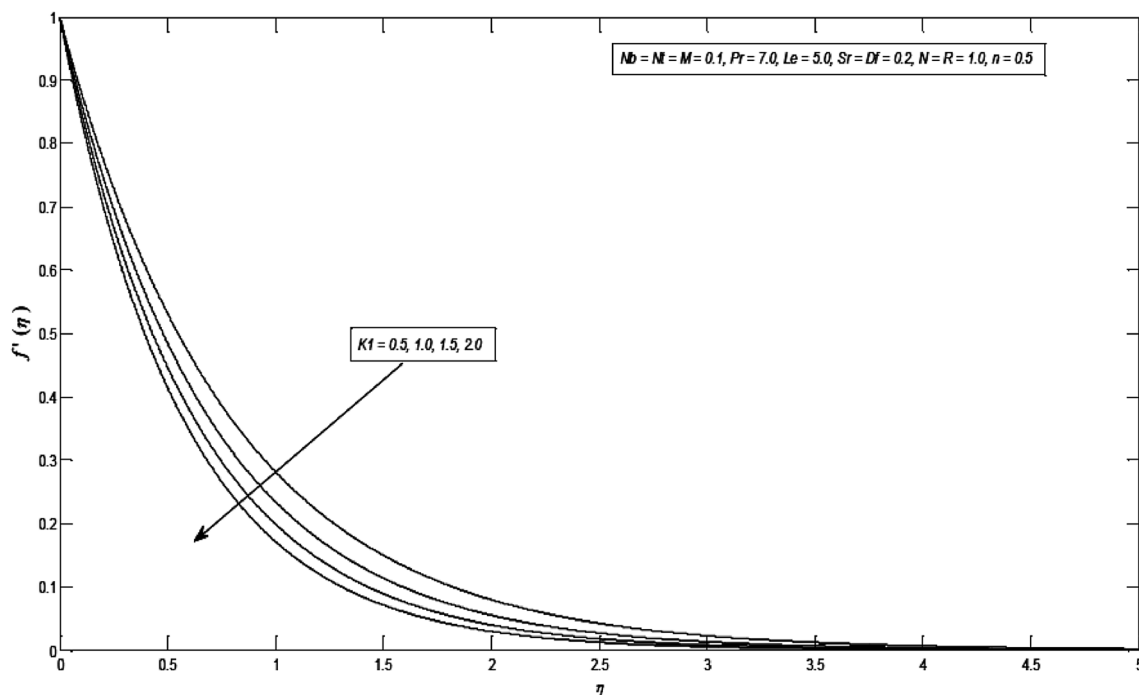


Fig. 2 The impacts of K_1 on $f'(\eta)$

that the enhancement in the size of nanoparticles and the viscosity of the parent fluid leads to enhance this number. In this way, the conduction phenomenon occurs within the flow system and the thermal diffusivity decreases. As a result, heat transfer becomes lower. The Fig. 8 represents that the temperature profile enhances by increasing Nb. This trend is also observed in case of Nt in Fig. 9. This is due to fact that the nanoparticles in the parent fluid collide each other gain kinetic energy and their motions show zig-zagging way. When Nb increases, these zigzag motions of nanoparticle become more rapid and the temperature in the hot regime rises. On the other side, good nanoparticles

distributions are related to increment of Nt because thermophoresis effects force particles to move hot to cold area. It is noted from Fig. 10 that, enhancement of M results increase in temperature profile. Since the Lorentz force decline the flow velocity, which is accompanied by rise in temperature. Thus, the magnetic effects heat the fluid. The subsequent rise in D_f reduces the temperature profile as expressed by Fig. 11.

Figures set 12, 13, 14, 15, 16 and 17 display the impacts of the parameters characterizing the concentration distributions. Figure 12 reveals that, the concentration profile enhances by rising the values of S_r . According to Fig. 13,

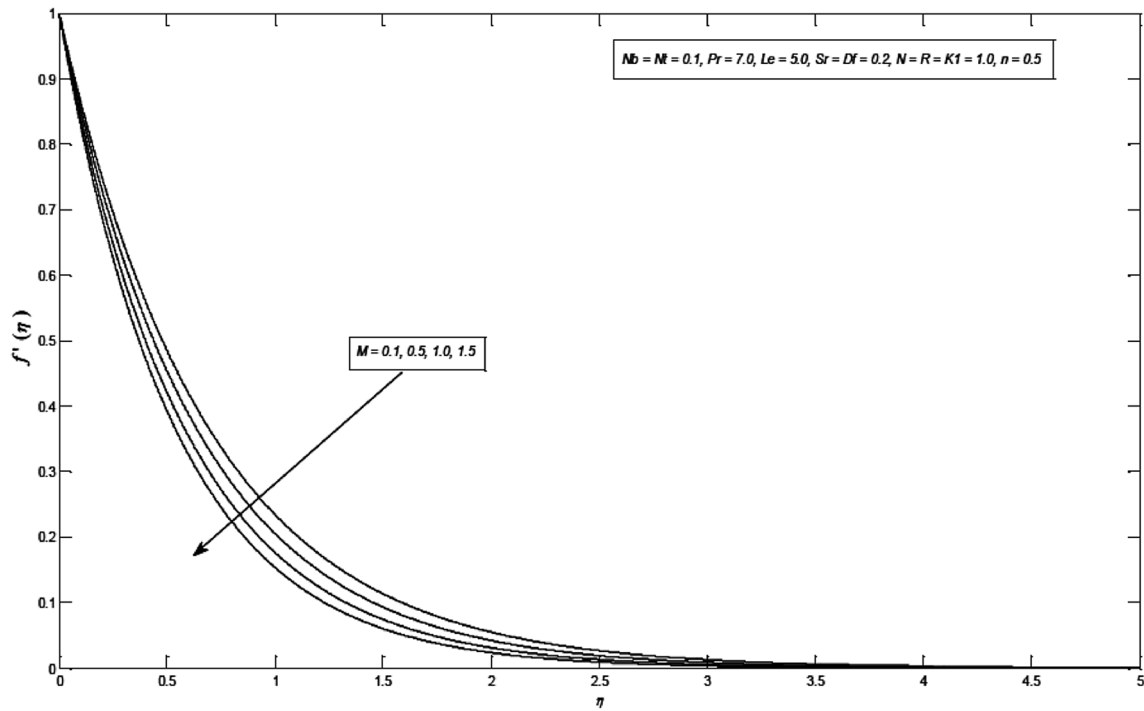


Fig. 3 The impacts of M on $f'(\eta)$

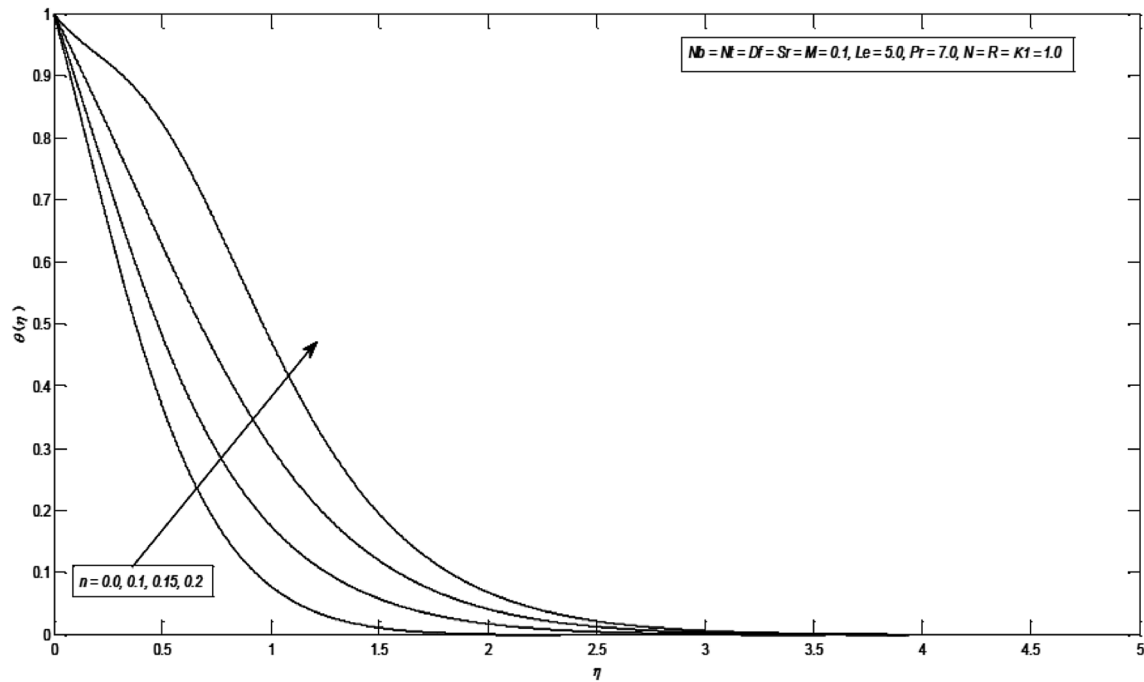


Fig. 4 The impacts of n on $\theta(\eta)$

the concentration profile shows decline by increasing the values of R . This happens due to consumption of chemicals during the flow. The concentration profile becomes smaller in relation with increment of parameter Nb in

Fig. 14. It is also clear in Fig. 15 that larger the values of Nt causes enhancement in concentration profile. Figure 16 exhibits that the concentration profile enhances by rising

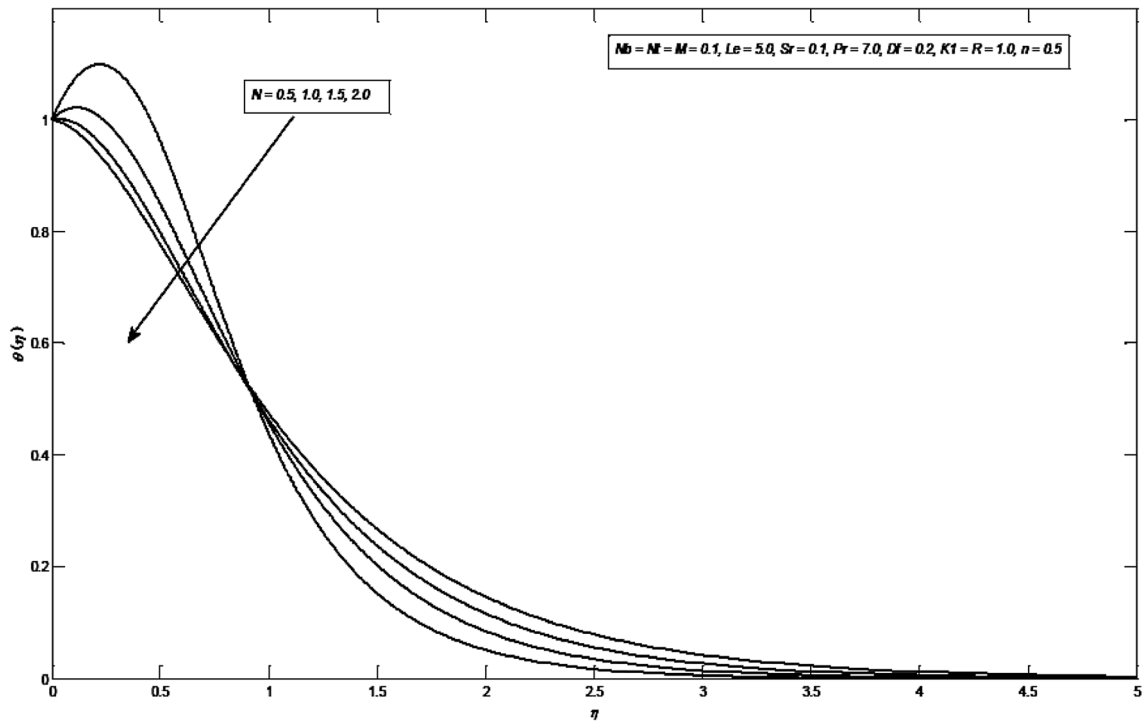


Fig. 5 The impacts of N on $\theta(\eta)$

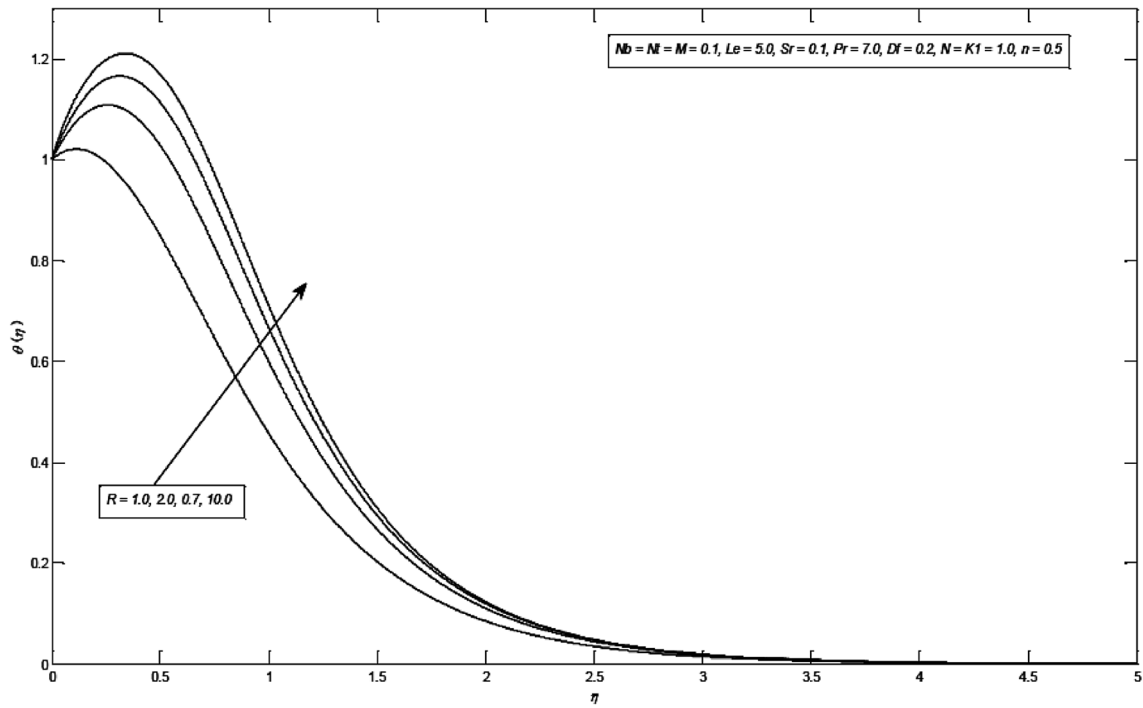


Fig. 6 The impacts of R on $\theta(\eta)$

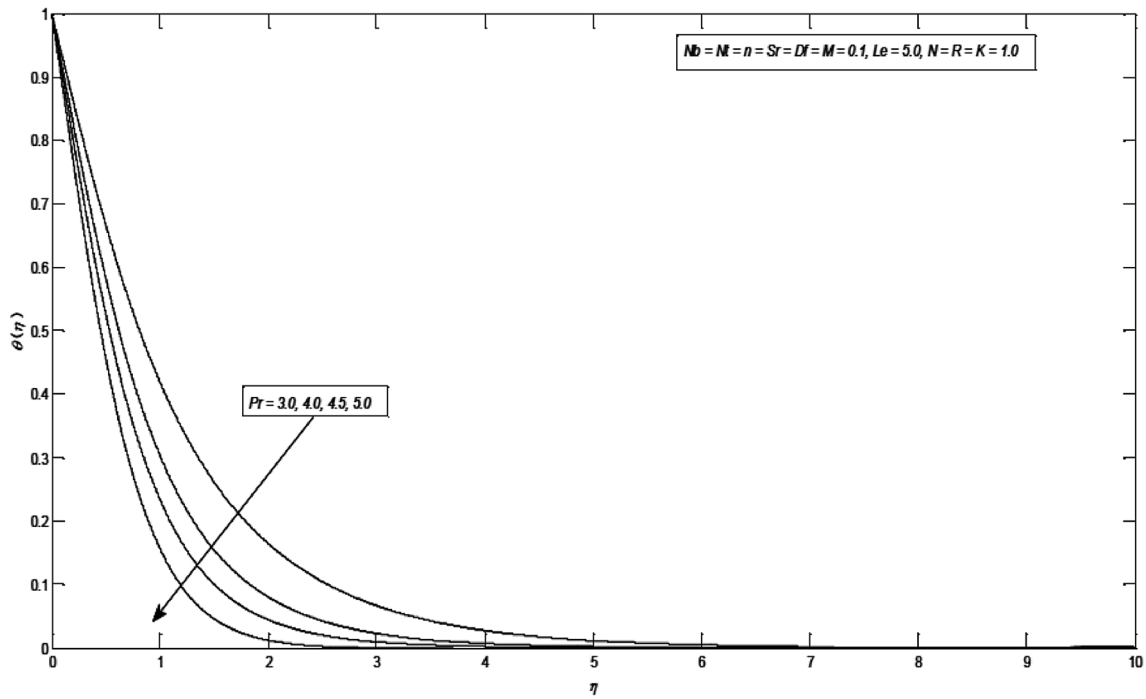


Fig. 7 The impacts of Pr on $\theta(\eta)$

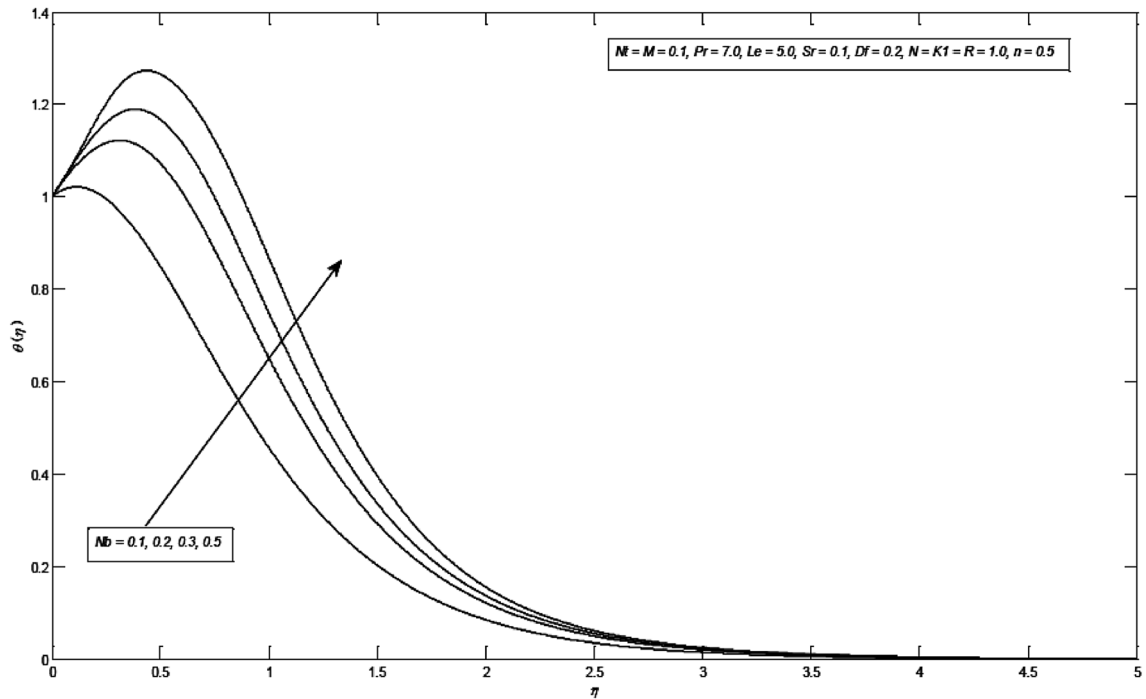


Fig. 8 The impacts of Nb on $\theta(\eta)$

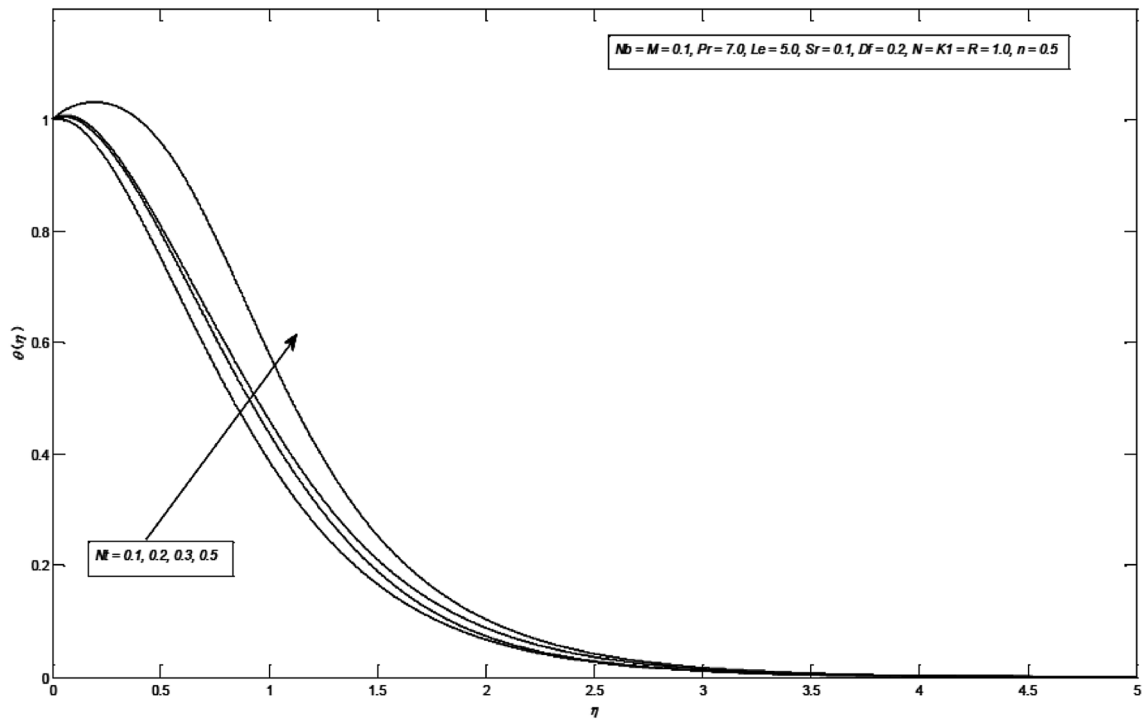


Fig. 9 The impacts of Nt on $\theta(\eta)$

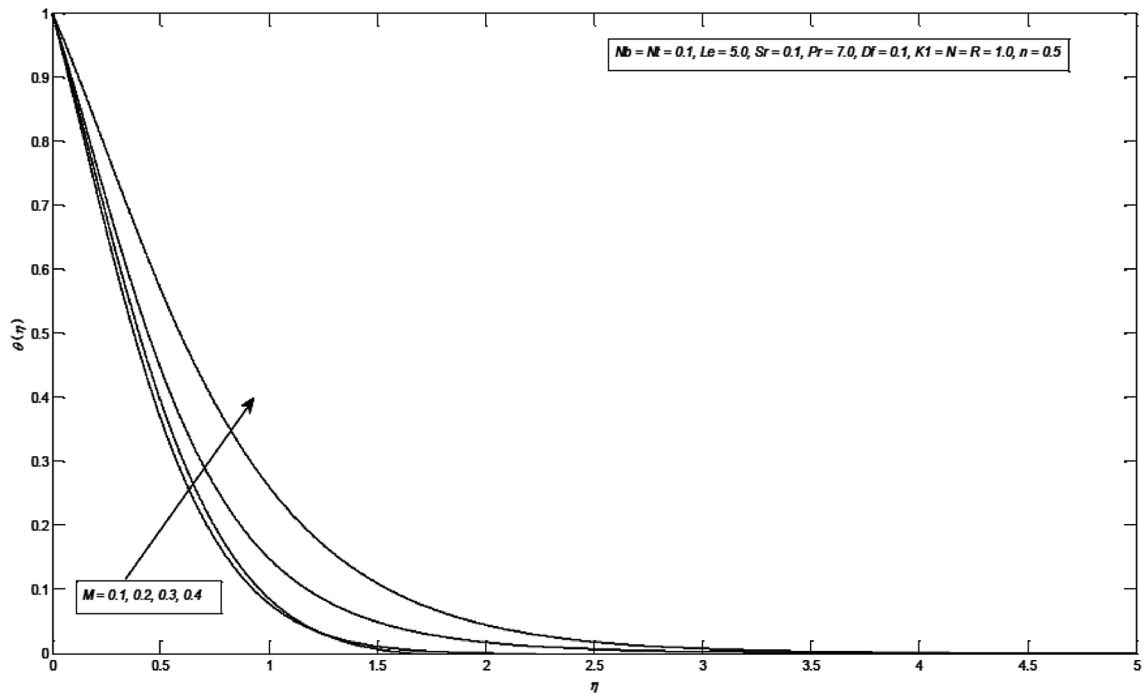


Fig. 10 The impacts of M on $\theta(\eta)$

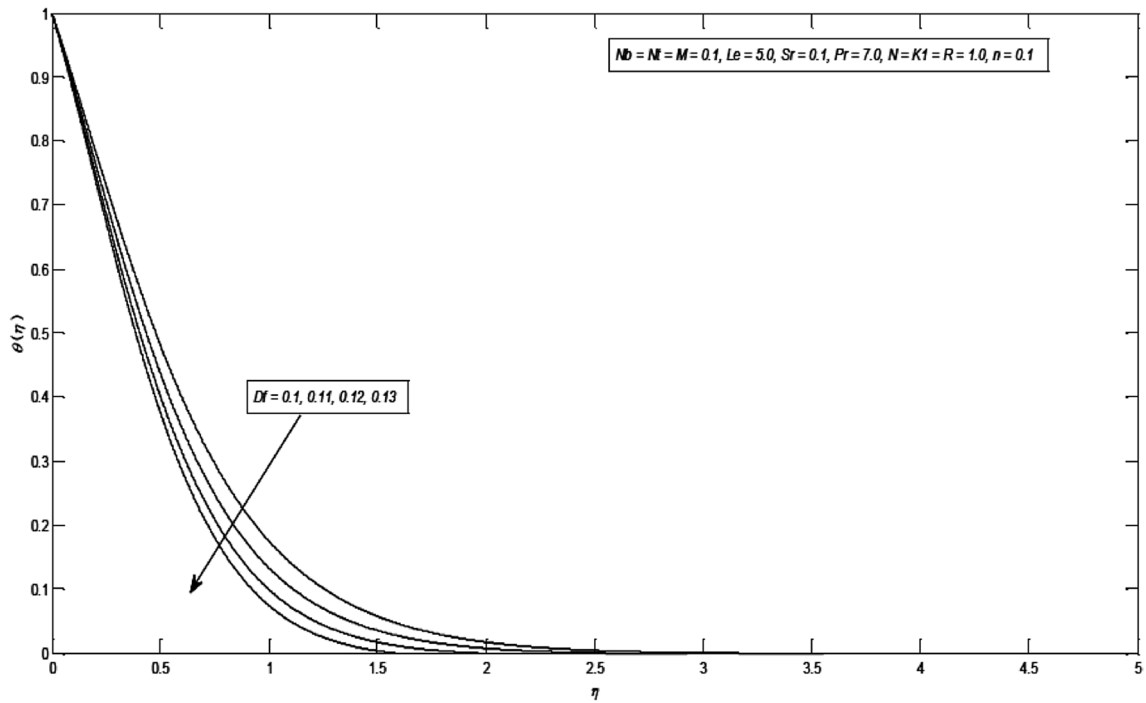


Fig. 11 The impacts of D_f on $\theta(\eta)$

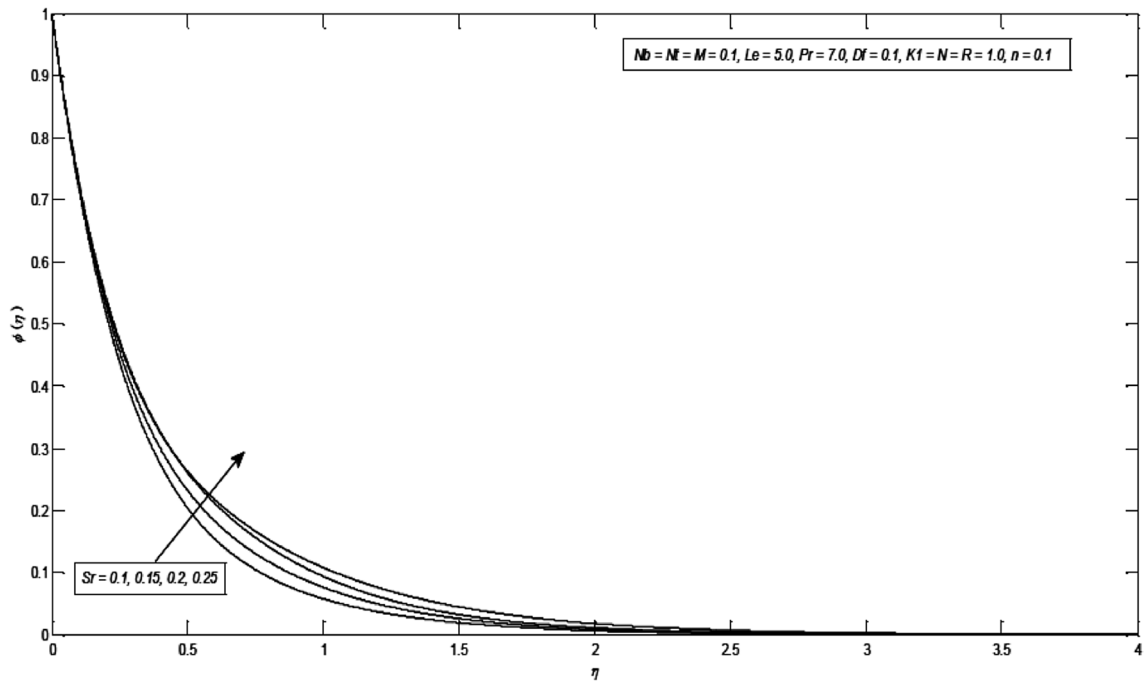


Fig. 12 The impacts of S_r on $\phi(\eta)$

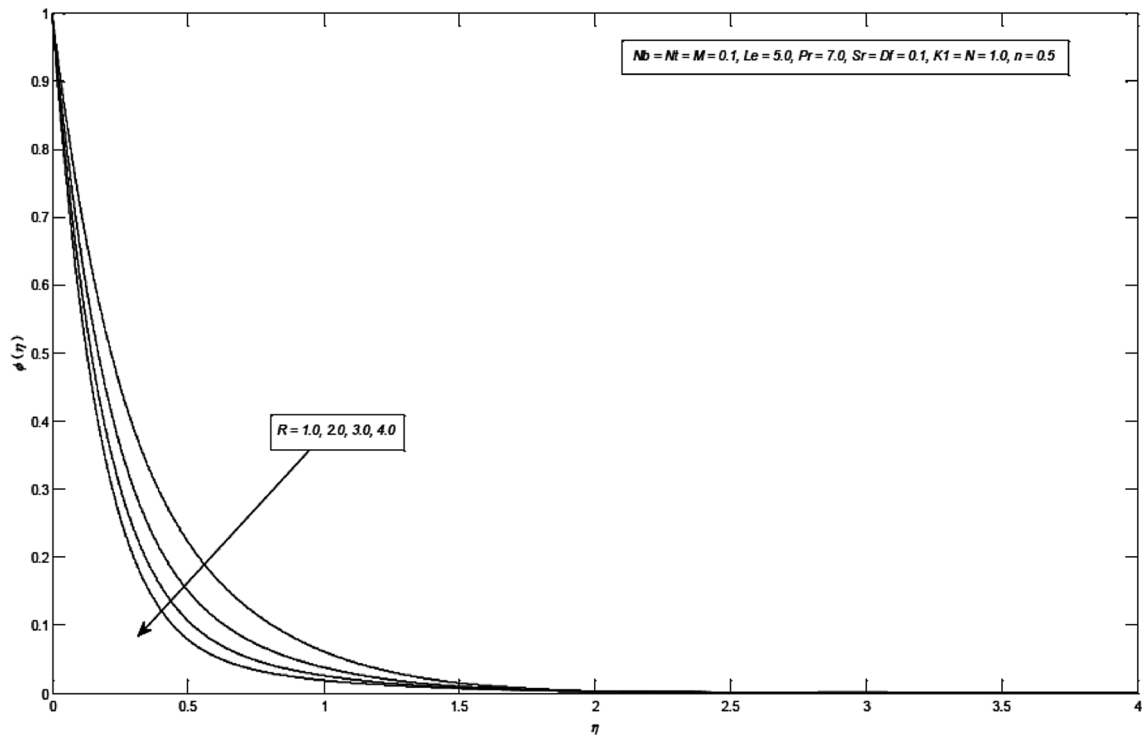


Fig. 13 The impacts of R on $\phi(\eta)$

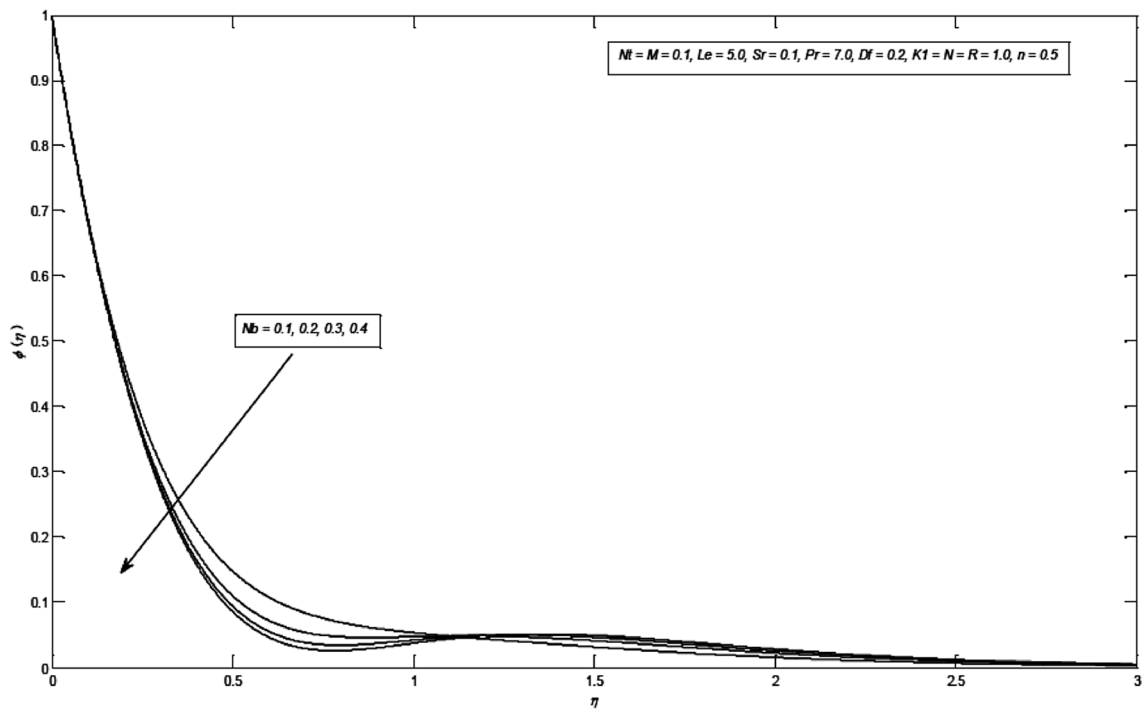


Fig. 14 The impacts of Nb on $\phi(\eta)$

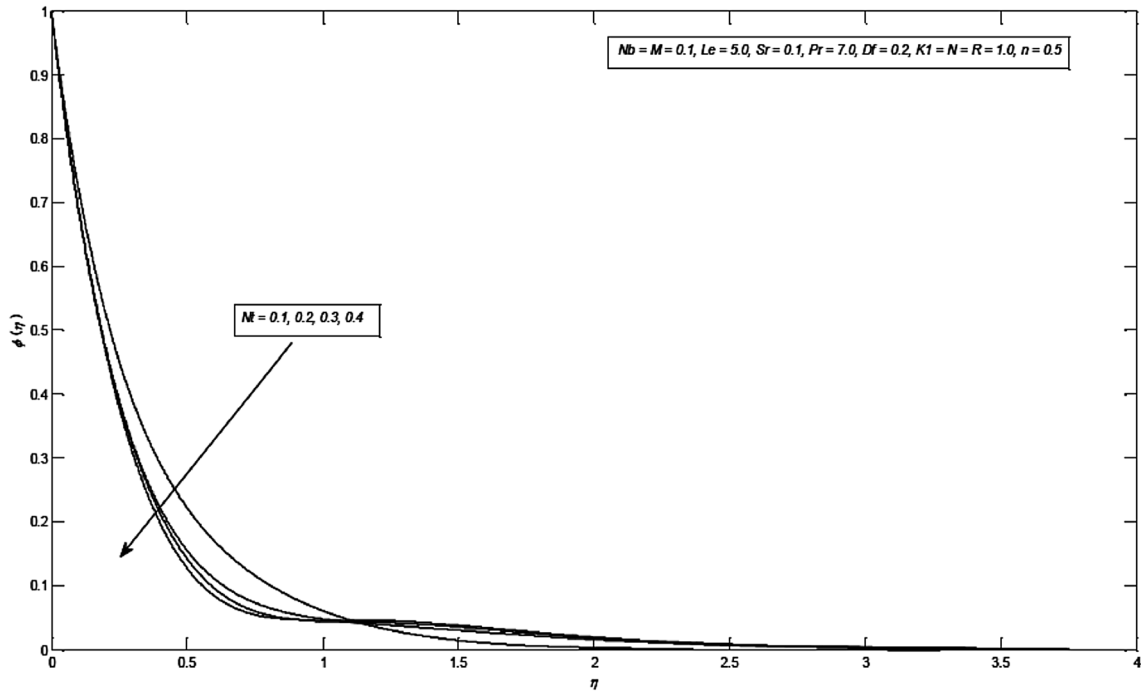


Fig. 15 The impacts of Nt on $\phi(\eta)$

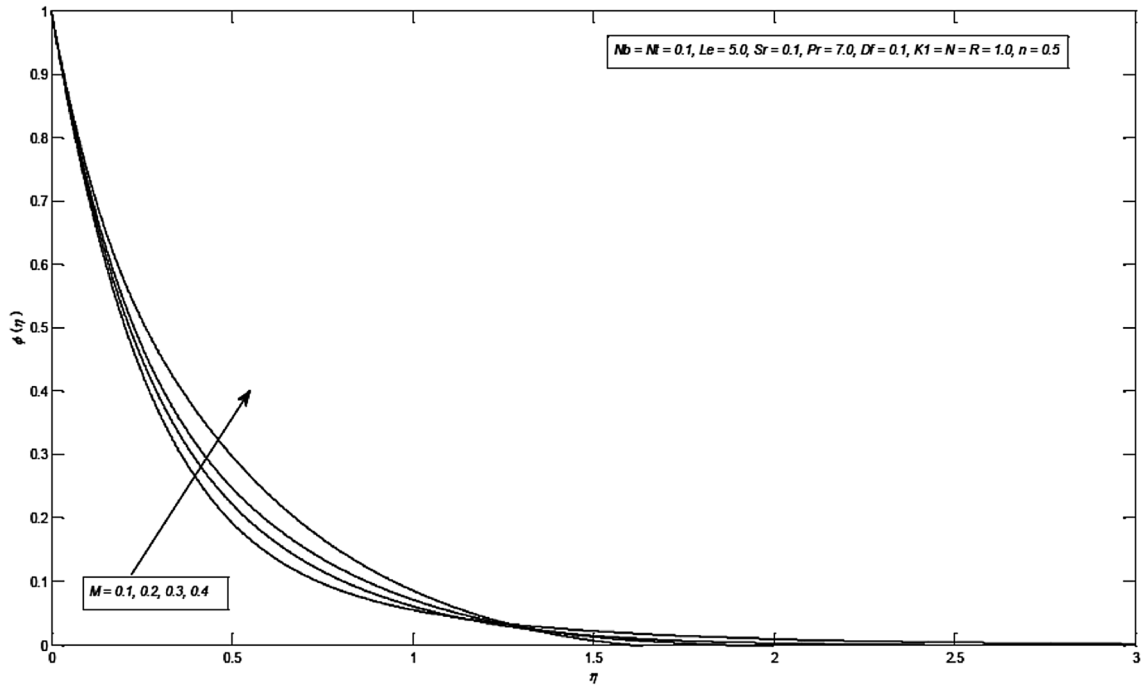


Fig. 16 The impacts of M on $\phi(\eta)$

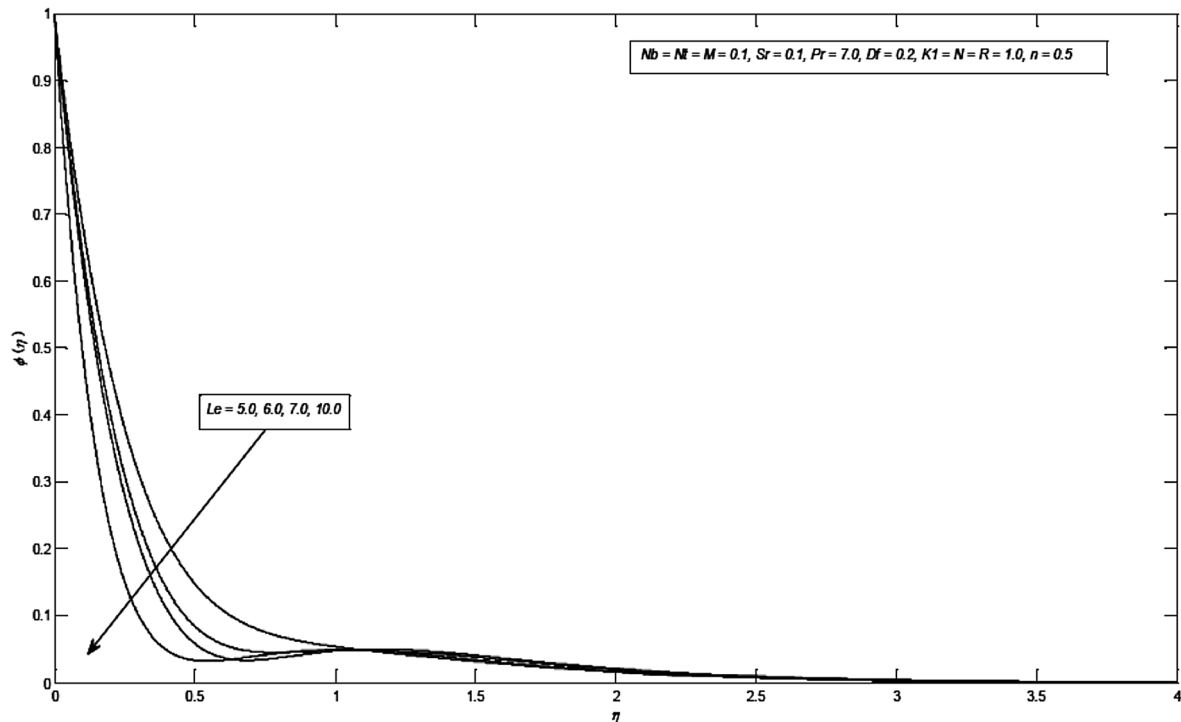


Fig. 17 The impacts of Le on $\phi(\eta)$

the values of M . Whereas this profile reduces in case of increasing the values of Le , which is depicted by Fig. 17.

4 Conclusions

The present study provides Soret–Dufours and thermal stratification effects on hydromagnetics nanofluid flow engendered by stretched surface in exponential manner inserted inside the porous medium. The transformation equations lead to transform the equations showing flow behavior of nanofluid into differential equations in ordinary form. Then the Keller box method is applied on resultant equations to get clear insight of governing parameters by numerical computations. Although, a number of studies are available in the literature on nanofluid flow with different geometries but in the light of growing applications of the nanofluids in industry and engineering. We considered the nanofluid along with Soret and Dufour impacts in the stratified porous medium. A couple of instances such as atomic surplus disposal, hydrology and thermal vigour are notable. Results derived from this investigation can be summarized as

1. Increase of the magnetic parameter tends to enhance the temperature and concentration profiles as well.

2. Due to increase in Dufour parameters, temperature profile reduces. On contrast, larger the Soret parameter results increase in concentration profile.
3. Radiative and chemical reactive constraints show converse behaviour on temperature profile. The temperature profile increases in relation with enhancement of chemical reaction parameter whereas this profile displays reduction by rising radiation parameter.
4. The temperature profile decreases by rising the Prandtl number whereas the concentration profile declines by enhancing the Lewis number.
5. The temperature profile enhances by increasing both parameters signifying Brownian motion and thermophoresis effects whereas concentration profile expresses reverse behaviour in case of these parameters.

Compliance with ethical standards

Conflict of interest The authors declare that they have no conflict of interest.

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