



Kail sawdust charcoal: a low-cost adsorbent for removal of textile dyes from aqueous solution

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Abstract

Kail sawdust charcoal was used as an adsorbent for the removal of Torque blue, red RB and yellow M4G (textile dyes) dyes from aqueous solution. Adsorption was carried out at different concentrations of dye solution, dose of adsorbent, temperature, pH and particle size. The adsorption data were best fitted by Langmuir adsorption isotherm and pseudo-second-order kinetic models. Thermodynamic parameters (ΔG° , ΔH° and ΔS°) were determined, and the results indicated that adsorption was spontaneous, feasible and exothermic. Adsorption was better at higher pH for torque blue and at lower pH for red RB and Yellow M4G dyes. Kail sawdust charcoal (bio waste) would be quite effective and economical adsorbent for the treatment of textile dye wastewater.

Keywords Adsorption · Kail sawdust charcoal · Torque blue · Red RB · Yellow M4G

1 Introduction

Nowadays, textile industries are emerging as the most polluting industry worldwide. These industries release dyes and other chemicals, e.g., caustic soda, formic acid, organic resins, soap, softener, wetting agent, etc., into the environment which are harmful [1]. The dye is harmful as it may cause eye irritation, skin irritation and digestive tract irritation, if inhaled [2]. In aerobic conditions, it is considered mutagenic to living organisms. The treatment of textile effluents is becoming the most challenging task. In the past few years, several techniques have been adopted for removal of textile dyes from aqueous solution but adsorption method is found to be more convenient, efficient and economical [3]. Singh et al. [3] discussed in detail the use of different types of adsorbents for water purification. However, activated carbon is one of the oldest and widely used adsorbents. It is generally obtained from coal and is very costly. Due to economic reasons, agricultural

materials are the most preferred choice as the substitute of activated carbon. The basic requirement for activated carbon is that it should have porous structure with pores of different sizes. However, pore sizes depend on the source material and method of preparation. By now, many agricultural and low-cost materials have been reported for dye removal from aqueous solution [4–6].

Raw agrowastes in general have low adsorption capacity, and soluble organic matters go into solution, tending to increase its total organic carbon (TOC), and chemical/biological oxygen demands. The efficiency of adsorption by agricultural residues can be enhanced by chemical modifications [7]. Recently, activated carbons derived from various carbonaceous materials such as cocoa shell, coconut shell (H_3PO_4), pineapple waste ($ZnCl_2$), sour cherry stones ($ZnCl_2$), coconut shell (KOH), Cucumis sativus (H_2SO_4), olive-waste cake (H_3PO_4), Kenaf core fiber (H_3PO_4), date stone ($FeCl_2/ZnCl_2$), sugarcane bagasse (KOH), orange peel (K_2CO_3) and linseed deoiled cake (H_3PO_4) have been

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prepared by chemical activation for treatment of industrial wastewater [2].

Although the adsorption capacities of the above materials are very high, most of them have been used either for non-textile dyes or for those dyes which are currently not in use. So some new adsorbents, which can easily be available and have high potential for removal of currently used textile dyes, are found out.

The waste product obtained from carpenter shop (Kail sawdust) is available in plenty and can be converted to carbon, which can be used as an adsorbent for removal of dyes from water. In this paper, Kail sawdust was converted into charcoal (KSC) by carbonization and has been used as adsorbent for removal of torque blue, red RB and yellow M4G dyes from aqueous solution. These dyes are generally used for dyeing cotton, rayon, silk, wool and nylon fabrics. Torque blue is cationic (oxazine class) dye. This class of dye is very toxic to aquatic life and may cause eye irritation, vomiting, jaundice, tissue necrosis, cyanosis, shock, bladder cancer, etc. in human beings [8, 9]. Red RB and Yellow M4G are anionic (single azo) dyes. The degradation products of azo dyes such as aniline, toluene, benzidine and naphthalene have been reported to be allergenic, mutagenic, teratogenic and carcinogenic in the literature [10]. Effects of various parameters such as contact time, initial dye concentration, particle size of adsorbent, adsorbent dosage, pH and temperature have been studied for the removal of dyes by KSC. Different adsorption isotherms and kinetic models were tested, and the thermodynamic parameters were calculated.

2 Materials and methods

2.1 Materials

The Kail sawdust, obtained from the furniture market of Ghaziabad, India, was used as precursor for the synthesis of charcoal. The textile dyes, namely Torque blue, red RB and yellow M4G, were obtained from Rituraj Textile Industry, Mohan Nagar, Ghaziabad (UP), India.

2.2 Methods

2.2.1 Preparation of adsorbent

The Kail sawdust was soaked in distilled water for 2 days to remove all the impurities and color, present on the surface of sawdust and filtered. The filtered sawdust was dipped in dilute HCl to dissolve the remaining impurities. It was then filtered and dried in sunlight for 5–6 d and then in an oven for 15 h at 120 °C. The dried sawdust was ground by mechanical grinder into fine powder and

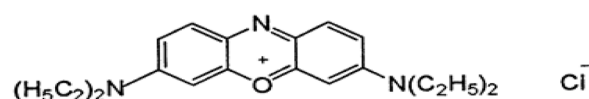
then placed in a muffle furnace at 400 °C for half an hour. After the carbonization, the sawdust was taken out from muffle furnace, cooled, washed and dried. Finally, this wood charcoal was divided into four ranges of particle sizes by sieving and getting particle size of 75–149 μm, 150–299 μm, 300–599 μm and 600–899 μm, and after that, the surface areas were determined. The obtained KSC was then kept in an airtight closed bottle and was used as an adsorbent.

2.2.2 BET surface area

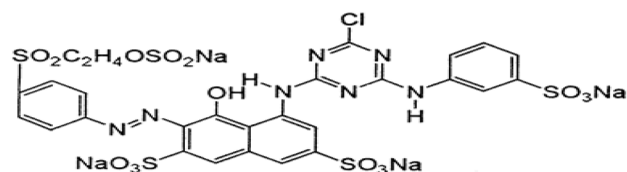
BET surface area of KSC was measured (10.762, 5.381, 2.691 and 1.6143 m²/g) using liquid nitrogen by Quantachrome Instruments version 5.0 at Banasthali Vidhyapith, Jaipur.

2.2.3 Preparation of adsorbates

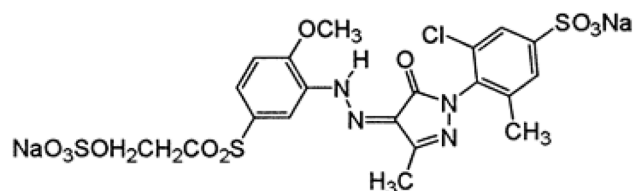
The stock solutions of 50 mg/100 mL of torque blue, red RB and yellow M4G dyes were prepared by dissolving predetermined, accurately weighed amount of dyes in double-distilled water, and experimental solutions were prepared by suitable dilution of stock solutions. The chemical structures of different dyes are given in Fig. 1a–c.



a Chemical structure of Torque Blue



b Chemical structure of Red RB



c Chemical structure of Yellow M4G

Fig. 1 a Chemical structure of torque blue, b chemical structure of red RB and c chemical structure of yellow M4G

2.2.4 SEM studies

The surface morphology of Kail sawdust, Kail sawdust charcoal and Kail sawdust charcoal after torque blue dye adsorption were examined with SEM model No Zeiss 18 EVO.

2.2.5 Spectral studies

FTIR spectra of KSC before and after adsorption of torque blue, red RB and yellow M4G dyes were recorded with Cary 630 FTIR.

2.2.6 Determination of zero point charge (pH_{zpc})

To determine the point of zero charge (pH_{zpc}) or the pH value at which the surface charge of KSC is zero, 50 mL 0.01 M solution of NaCl was taken and the pH of the solution was made 2 by adding HCl/NaOH. In a similar way, NaCl solution in five separate conical flasks was taken and the pH (pH_i) was maintained to 3, 4, 5, 6, 7, 8, 9 and 10. 0.20 g of KSC was added to each flask and left at room temperature for 48 h. When the pHs were stabilized, the solutions were filtered and the final pHs (pH_f) were measured. A graph was plotted between ΔpH ($\text{pH}_i - \text{pH}_f$) and initial pHs (pH_i). The point of intersection is the pH_{zpc} of the KSC. It was found to be 5.8 (Fig. 2).

2.2.7 Batch experiment for removal of dyes

Batch experiments were carried out by stirring 0.3–0.7 g of the KSC (adsorbent) in rotatory shaker with 100 mL aqueous solution of dyes having concentration 10–30 mg/L. KSC (surface area 5.381 m^2/g) was mixed with dye solutions. However, experiments with KSC of different surface areas were also conducted to see the effect of surface area on adsorption. All experiments were carried out by changing the temperature and pH of solutions from 300 to 330 K and 3.0–9.0, respectively. The temperature was maintained within ± 1 °C for a prescribed period of time to attain

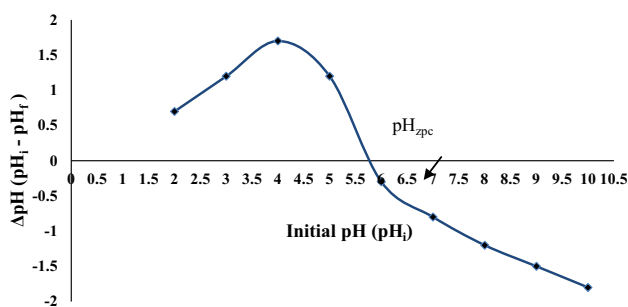


Fig. 2 Determination of pH_{zpc}

equilibrium. The required pH of the solution was adjusted by adding calculated amount of 0.1 N HCl/NaOH. The duration of each batch experiment was about 90 min. After every 15 min, the solutions were filtered through Whatman filter paper and concentrations of dyes in the solutions were determined by measuring the absorbance at a wavelength corresponding to their maximum absorbance (667, 528 and 390 nm for TB, RRB and YMG, respectively) with the help of Shimadzu UV-1800 spectrophotometer.

Calibration curves for each dye were plotted.

The amount of dyes adsorbed onto KSC and percentage removal of dye were calculated by using Eqs. 1 and 2.

$$q_e = \left(\frac{C_o - C_e}{M} \right) * V \quad (1)$$

$$\% \text{Dye removal} = \left(\frac{C_o - C_e}{C_o} \right) * 100 \quad (2)$$

where q_e is the amount of dye adsorbed at equilibrium, C_o is the initial concentration of dye in the solution, C_e is the final concentration of dye at equilibrium, M is the mass of adsorbent (g) and V is the volume of solution (L).

3 Results

3.1 Characterization of adsorbent

3.1.1 SEM studies

SEM pictures of Kail sawdust (Fig. 3a, b) show that the adsorbent surface has very rough and porous texture. It is clearly visible from the images that size of pores is between 2.1 μm and 3.3 μm .

The micrographs of Kail sawdust Charcoal (KSC) are shown in Fig. 4a, b; which reveal that roughness and porosity on adsorbent surface have been increased by carbonization, which would definitely enlarge surface area as compared to non-carbonized adsorbents for adsorption. Size of pores is between 4.9 μm and 6.8 μm .

SEM images of Kail sawdust charcoal after torque blue dye adsorption are shown in Fig. 5a, b. These micrographs show that the surface of KSC is slightly smoothed by dye adsorption, indicating the adsorption of dye.

3.1.2 FTIR spectral studies

FTIR spectra of KSC before adsorption and after adsorption of torque blue, red RB and yellow M4G are shown in Fig. 6. The bands appearing in anhydrous KSC at 1610 cm^{-1} , 1590 cm^{-1} may be due to amide (N–H) groups in sawdust [11]. The band at 1215 cm^{-1} shows the

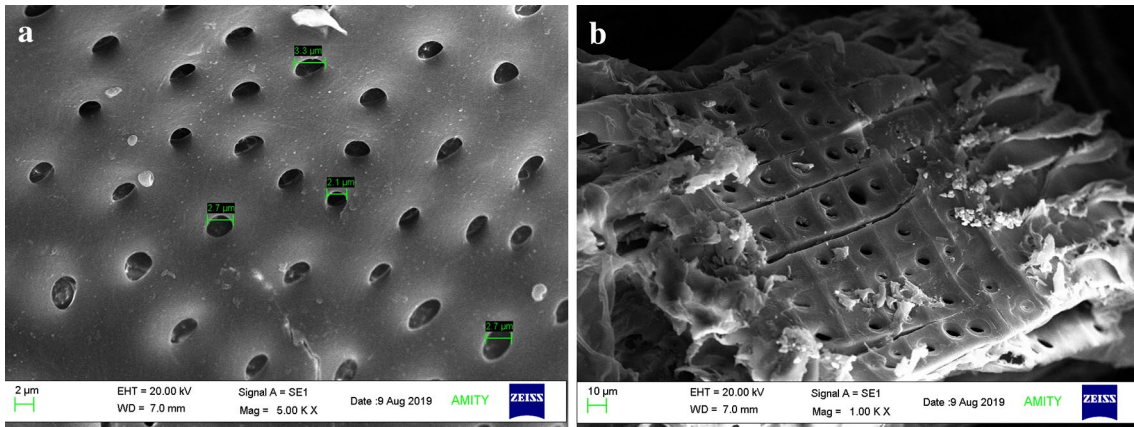


Fig. 3 a, b SEM images of Kail sawdust (KS) before carbonization

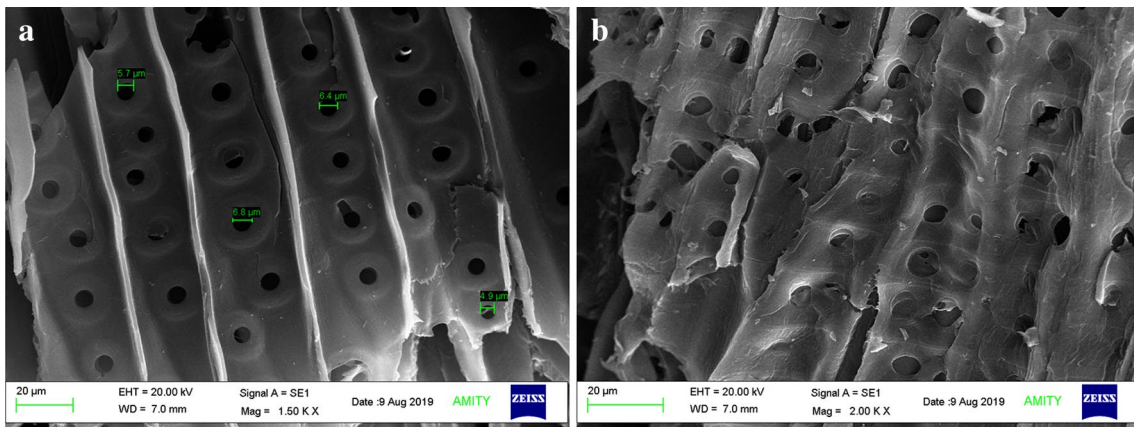


Fig. 4 a, b SEM images of Kail sawdust (KS) after carbonization

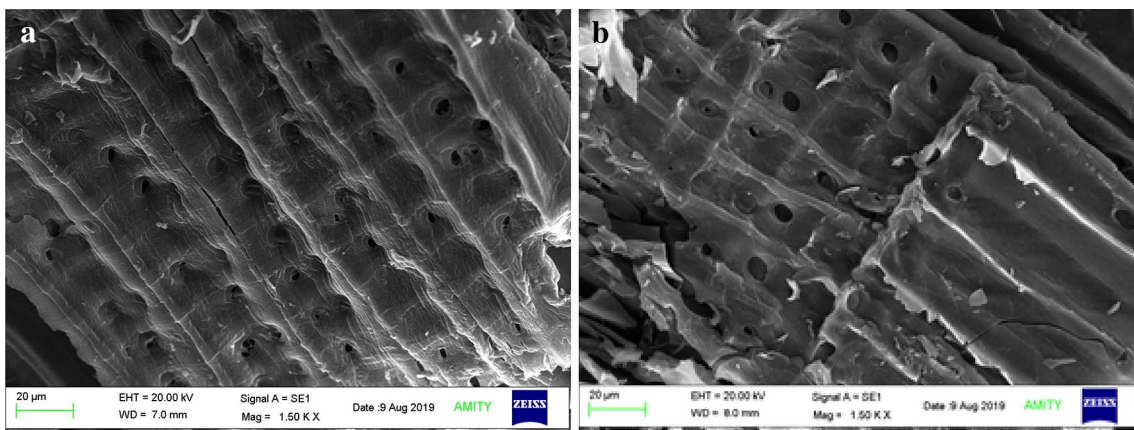


Fig. 5 a, b SEM images of Kail sawdust charcoal (KSC) after torque blue dye adsorption

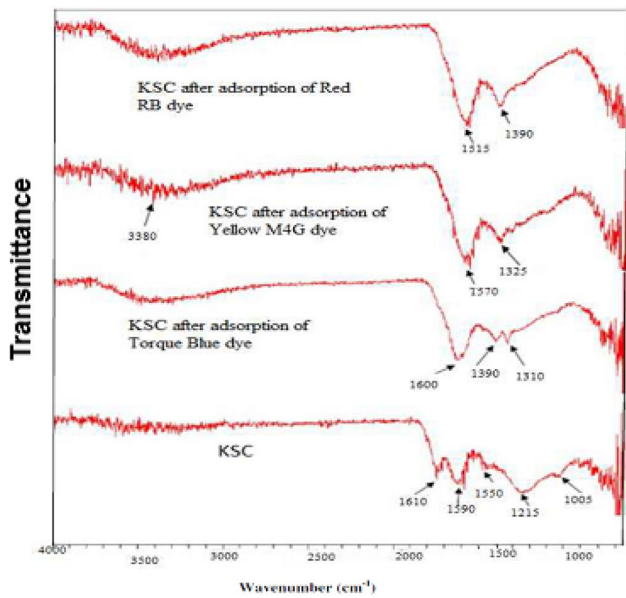


Fig. 6 FTIR spectra of KSC before and after adsorption of torque blue, red RB and yellow M4G dyes

crystalline cellulose, and the band at 1005 cm^{-1} shows C–O–C symmetric stretching. The FTIR spectra of Kail sawdust charcoal after adsorption of dyes show shifting of bands and appearance of new bands. This indicated some sort of weak interactions between dye molecules and the surface of KSC. A broad peak at about 3400 cm^{-1} after dye adsorption may be due to OH group coming from water solution of dye.

3.2 Removal of torque blue, red RB and yellow M4G dyes from aqueous solution

The removal of textile dyes torque blue, red RB and yellow M4G from aqueous solutions by Kail sawdust charcoal (*Pinus wallichiana*) was examined at different concentrations (10–30 mg/L) of dye solutions, surface areas of KSC, adsorbent doses (0.3–1.0 g), pH (3.0–9.0) and temperatures (300–330 K). The percentage removal of dye under different conditions is shown in Figs. 7, 8, 9, 10 and 11. Figure 7 shows that as the concentration of dye increased, percent removal is decreased. As the surface area increased, adsorption increased (Fig. 8). With the increase in adsorbent dose, percent removal increased (Fig. 9). Figure 10 shows that percent removal of red RB and yellow M4G dyes decreased with increase in pH, whereas in the case of torque blue dye it increased with increase in pH. Further with increase in temperature, the percent removal of dyes decreased (Fig. 11).

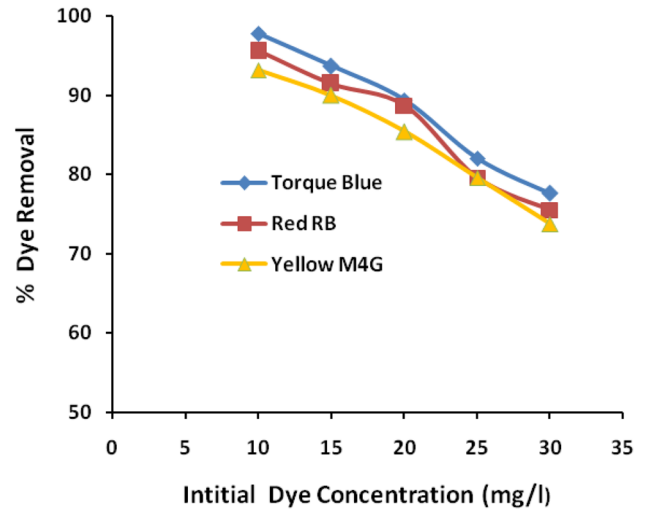


Fig. 7 Effect of initial dye concentration 10–30 mg/L on adsorption of dyes on KSC

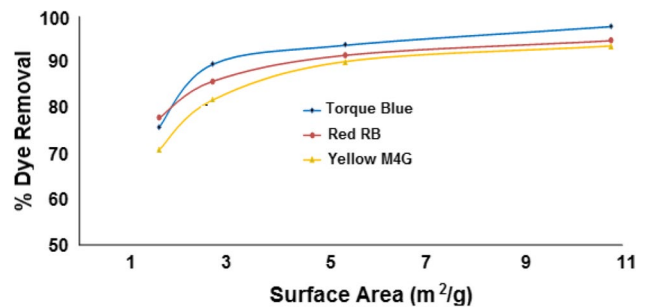


Fig. 8 Effect of surface area on adsorption of dyes on KSC

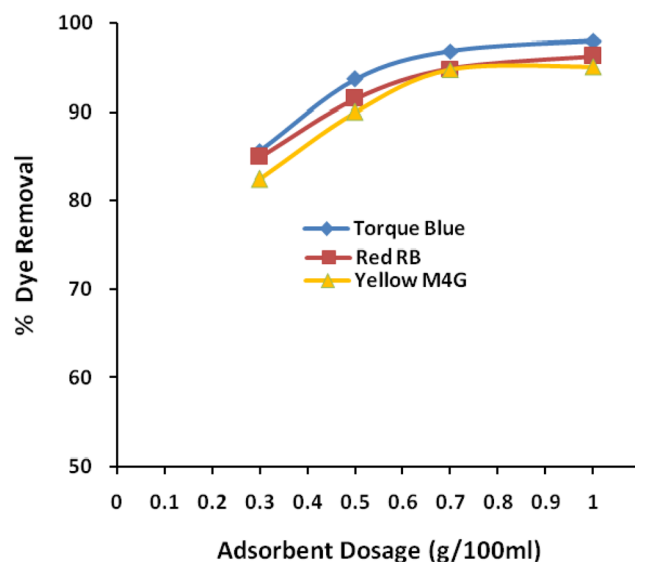


Fig. 9 Effect of adsorbent dosage (0.3–1.0 g) on adsorption of torque blue, red RB and yellow M4G dyes

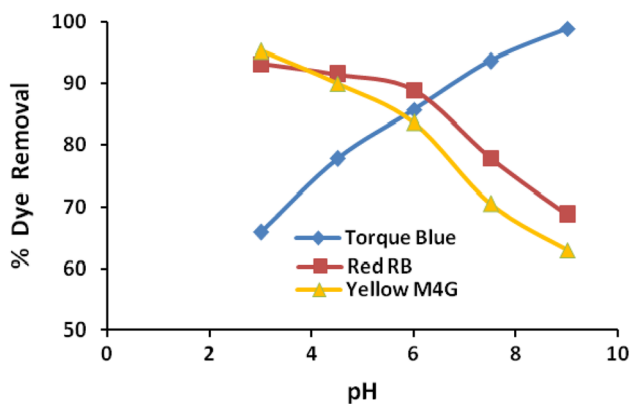


Fig. 10 Effect of pH (3.0–9.0) on adsorption of torque blue, red RB and yellow M4G dyes on KSC

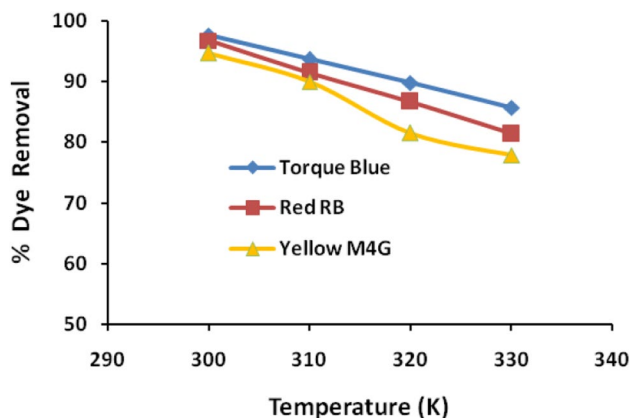


Fig. 11 Effect of temperature (300–330 K) on adsorption of torque blue, red RB and yellow M4G dyes on KSC

3.3 Thermodynamic parameters

Thermodynamic parameters, e.g., Gibbs free energy change (ΔG°), enthalpy change (ΔH°) and entropy change (ΔS°), were estimated by using Eqs. 3–6.

$$\Delta G^\circ = -RT \ln K \tag{3}$$

where R is the gas constant and K is the equilibrium constant at temperature T .

The equilibrium constants (K_1, K_2, K_3 and K_4) at temperatures 300, 310, 320 and 330 K were calculated according to the relation:

$$K_{\text{equ}} = \frac{C_{\text{ads}}}{C_{\text{sol}}} \tag{4}$$

where C_{ads} and C_{sol} are the concentrations of dye on the adsorbent surface and in solution, respectively.

Entropy change (ΔS°) is determined by Eq. 5.

$$\Delta S^\circ = \left[\frac{\Delta H^\circ - \Delta G^\circ}{T} \right] \tag{5}$$

The enthalpy change (ΔH°) refers to the amount of energy released or absorbed in a chemical reaction, and it can be calculated by combining Eqs. 3 and 5:

$$\ln K = \frac{\Delta S^\circ}{R} - \frac{\Delta H^\circ}{RT} \tag{6}$$

Equation (6) is used to calculate the change in enthalpy (ΔH°) and the change in entropy (ΔS°) by plotting $\ln K$ versus $1000/T$. The slopes and intercepts of the graphs were used to determine the values of ΔH° and ΔS° , respectively. The calculated values of thermodynamic parameters are given in Table 1.

Table 1 Thermodynamic parameters of torque blue, red RB and yellow M4G dyes at different temperatures

Adsorbent	Dyes	Temperature (K)	Parameters		
			$-\Delta G^\circ$ (kJ/mol)	$-\Delta H^\circ$ (kJ/mol)	$-\Delta S^\circ$ (J/(K mol))
<i>Thermodynamic parameters</i>					
Kail sawdust charcoal	Torque blue	300	9.350	52.985	146.740
		310	6.957		
		320	5.787		
		330	4.912		
	Red RB	300	8.503	52.170	146.830
		310	6.124		
		320	4.987		
		330	4.049		
	Yellow M4G	300	7.190	46.176	130.450
		310	5.662		
		320	3.945		
		330	3.456		

3.4 Adsorption isotherms

The adsorption isotherms of torque blue, red RB and yellow M4G dyes at different concentrations were analyzed by applying Langmuir, Freundlich and Temkin adsorption isotherm models to understand the extent and degree of favorability of adsorption [3].

3.4.1 Langmuir adsorption isotherm

The basis of Langmuir equation is a saturated monolayer adsorption of adsorbate onto the homogeneous surface of adsorbent. It assumes that sorption energy remains constant during the process, and there is no transmigration of the

adsorbate in the plane of surface. The Langmuir equation is given by Eq. 7.

$$\frac{C_e}{q_e} = \frac{1}{Q^0 b} + \frac{C_e}{Q^0} \tag{7}$$

where C_e is the remaining concentration of dye (mg/L) in solution at equilibrium; q_e is the amount of dye adsorbed at equilibrium (mg/g); Q^0 is the adsorption capacity of adsorbent, i.e., amount of dye adsorbed per unit weight of adsorbent in forming a complete monolayer on the surface (mg/g) and b (L/mg) is the Langmuir constant related to energy of adsorption. The plots of C_e/q_e versus C_e (Fig. 12) for all the dyes gave straight lines over the entire concentration range studied with very high regression coefficients (0.991–0.998). The values of Q^0 (mg/g) and b are calculated from the slope and intercept of the linear plots. The Langmuir parameters are given in Table 2. The results of Langmuir parameters showed that maximum adsorption capacity of KSC at 310 K was 5.102 mg/g for adsorption of Yellow M4G dye.

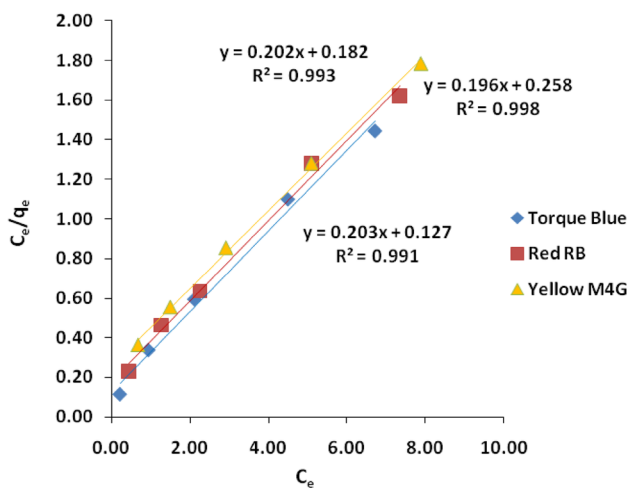


Fig. 12 Langmuir adsorption isotherm for torque blue, red RB and yellow M4G dyes

3.4.2 Freundlich adsorption isotherm

The Freundlich adsorption isotherm model was used to determine the adsorption intensity of the adsorbate onto the adsorbent surface [3]. It assumes non-ideal adsorption on the heterogeneous surface of adsorbent. The linearized equation of Freundlich isotherm model is given by Eq. 8.

$$\log q_e = \log K_f + \frac{1}{n} \log C_e \tag{8}$$

Table 2 Langmuir, Freundlich and Temkin adsorption constants of torque blue, red RB and yellow M4G dyes on KSC

Isotherms	Dyes	Parameters		
		Q^0 (mg/g)	b (L/mg)	R^2
Adsorption isotherm constants				
Langmuir	Torque blue	4.926	1.598	0.991
	Red RB	4.95	1.110	0.993
	Yellow M4G	5.102	0.760	0.998
Isotherms	Dyes	N	K_f (L/mg)	R^2
		Freundlich		
Freundlich	Torque blue	3.984	2.871	0.982
	Red RB	3.333	2.535	0.978
	Yellow M4G	2.857	2.239	0.996
Isotherms	Dyes	B	A (L/g)	R^2
		Temkin		
Temkin	Torque blue	0.775	49.116	0.984
	Red RB	0.911	18.116	0.999
	Yellow M4G	1.045	8.820	0.983

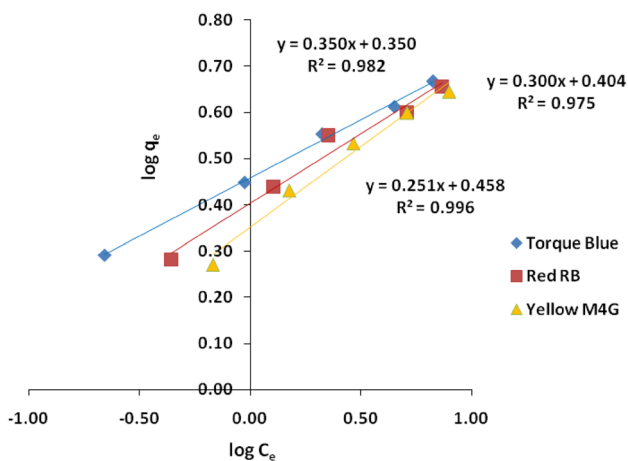


Fig. 13 Freundlich adsorption isotherm for torque blue, red RB and yellow M4G dyes

where k_f (L/mg) is the adsorption or distribution coefficient, i.e., quantity of dye adsorbed onto adsorbent per unit equilibrium concentration [3] and n is the Freundlich constant related to adsorption intensity, which is used to know the deviation from linearity of adsorption. The Freundlich parameters calculated from the plots of $\log q_e$ against $\log C_e$ (Fig. 13) are presented in Table 2. The values of n were found between 1 and 10, supporting that adsorption is favorable.

3.4.3 Temkin adsorption isotherm

The basis of Temkin isotherm model is adsorbate–adsorbent interaction on adsorption sites [3] and is given by Eq. 9.

$$q_e = B \ln A + B \ln C_e \tag{9}$$

where $B = \frac{RT}{b}$, A (L/g) and b (J/mol) are Temkin constants related to maximum binding energy and heat of sorption, respectively; R is the gas constant (8.314 J/mol K), and T is the absolute temperature (K). The plots of q_e against $\ln C_e$

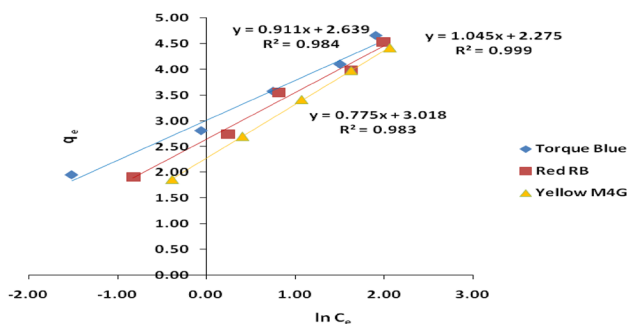


Fig. 14 Temkin adsorption isotherms for torque blue, red RB and yellow M4G dyes

C_e for various dyes are shown in Fig. 14, and the obtained parameters are given in Table 2.

3.5 Kinetics of adsorption

The kinetic studies of adsorption are important for the adsorbents in the dye removal from aqueous solution. Kinetic studies are helpful to describe the solute uptake rate by which the residence time of adsorption process can be determined. The efficiency of KSC for removal of dyes (torque blue, red RB and yellow M4G) at 310 K can be determined with the help of adsorption kinetics. To know the mechanism of adsorption phenomenon, the dynamical data were fitted into pseudo-first-order and pseudo-second-order kinetic equations.

3.5.1 Pseudo-first-order kinetics

The pseudo-first-order kinetic model was applied for the adsorption of solid/liquid system. The integrated linear equation is given by Eq. 10.

$$\log (q_e - q) = \log q_e - \frac{k_1}{2.303} t \tag{10}$$

where q_e and q are the amounts of adsorbate (mg/g) at equilibrium and at any time t , respectively, and k_1 is the pseudo-first-order rate constant (min^{-1}). The plots of $\log (q_e - q)$ versus t for different dyes at temperature 310 K are depicted in Fig. 15. The values of k_1 and q_e were determined from the slopes and intercepts of the lines, and the values are given in Table 3.

3.5.2 Pseudo-second-order kinetics

The linear form of pseudo-second-order rate equation is expressed by Eq. 11.

$$\frac{t}{q} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \tag{11}$$

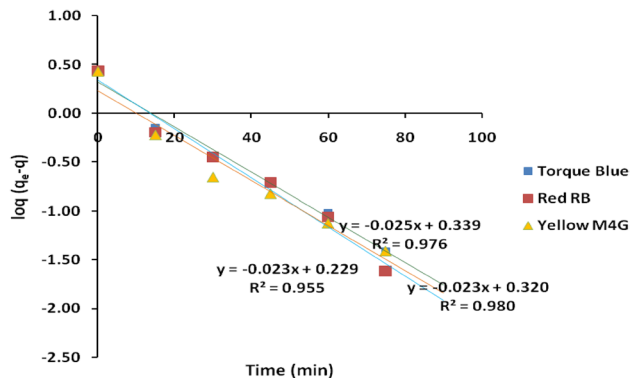
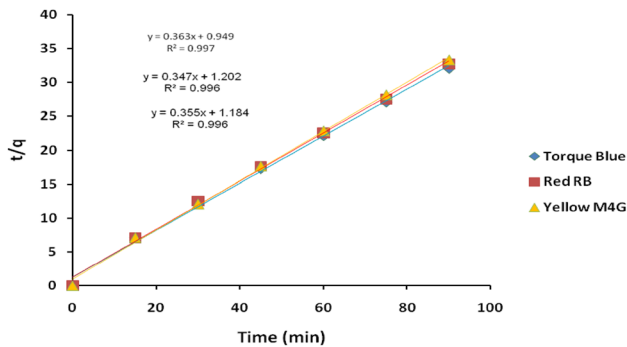


Fig. 15 Pseudo-first-order plots for the adsorption of torque blue, red RB and yellow M4G dyes on KSC

Table 3 Kinetic parameters for adsorption of torque blue, red RB and yellow M4G dyes on KSC

Dyes	Pseudo-first order			Pseudo-second order			Experimental q_e (mg/g)
	Calculated q_e (mg/g)	k_1 (min^{-1})	R_1^2	Calculated q_e (mg/g)	k_2 (g/mg/min)	R^2	
Torque blue	2.089	0.053	0.980	2.882	0.100	0.996	2.811
Red RB	2.183	0.058	0.976	2.817	0.106	0.996	2.750
Yellow M4G	1.694	0.053	0.955	2.755	0.139	0.997	2.701

**Fig. 16** Pseudo-second-order plots for the adsorption of torque blue, red RB and yellow M4G dyes on KSC

where q_e and q are the amounts of adsorbate (mg/g) at equilibrium and at any time t , respectively, and k_2 is the pseudo-second-order rate constant (g/mg/min). The plots of t/q versus t for different dyes at temperature 310 K are presented in Fig. 16. The values of k_2 and q_e were calculated from the intercept and slope and are given in Table 3.

4 Discussion

Figure 7 shows that % removal of torque blue by KSC decreased from 97.8 to 77.6%, red RB from 95.6 to 75.5% and Yellow M4G from 93.2 to 73.7% with increase in initial dye concentration from 10 to 30 mg/L. The optimum adsorption took place at 15 mg/L. At higher concentrations of dye, the active adsorbent sites were insufficient for the same mass of the adsorbent, so adsorption decreased. This is similar to the adsorption of methylene blue and crystal violet on treated orange peel [12] and that of acridine orange and Azure B on activated carbon prepared from brown linseed deoiled cake [13].

The percent removal of dyes by KSC increased with surface area of KSC (Fig. 8). Maximum removal was in the case of torque blue dye.

As shown in Fig. 9, adsorption efficiency of KSC increased with increasing the quantity of adsorbent up to optimal amount beyond which adsorption attained equilibrium. At constant initial dye concentration, increasing the amount of adsorbent increased the number of

unsaturated adsorbent sites, and as a consequence, more surface area was provided for adsorption [14]. The percent removal of torque blue increased from 85.6 to 98.0%, red RB from 84.9 to 96.3% and Yellow M4G from 82.4 to 95.1%, respectively, with increase in the amount of adsorbent from 0.3 to 1.0 g. The optimum adsorption took place at adsorbent dosage of 0.5 g.

The effect of pH was evaluated at varying pH from 3 to 9 (Fig. 10). At pH above pH_{zpc} (5.8), surface attained a negative charge which favoured the adsorption of torque blue. The optimum value of pH for torque blue dye is 7.5. At pH below pH_{zpc} (5.8), surface attained positive charge which favoured the adsorption of red RB and Yellow M4G. The optimum value of pH for red RB and Yellow M4G dyes is 4.0. It can be seen from Fig. 10 that on increasing the pH of solution from 3 to 9, percentage removal for torque blue dye was increased from 65.8 to 98.9%, while for red RB and Yellow M4G dyes it was decreased from 93.2 to 68.7% and 95.3 to 62.5%, respectively. Each dye has different characteristics. Torque blue is a cationic dye, so its ions in the solution exist as positively charged species. Increase in the pH (above pH_{zpc}) of solution increased the negative charge on adsorbent surface. Subsequently, the negative adsorption sites were favorable for adsorption of cationic dye, but on the other hand, red RB and Yellow M4G dyes are anionic dyes, dispersed in solution as negatively charged species. On increasing the pH, adsorbent surface also became negative which retarded the adsorption of negatively charged dye ions onto KSC due to electrostatic repulsion. Similar observations were reported in the literature for other anionic dyes [15].

The effect of temperature on percentage dye removal of torque blue, red RB and yellow M4g by KSC is shown in Fig. 11. It was observed that uptake capacity of KSC was decreased by increasing the temperature. This may occur due to the weakening of residual forces on the active sites of surface, so percent removal of torque blue decreased from 97.7 to 85.7%, red RB from 96.8% to 81.4% and Yellow M4G from 94.7% to 77.9% with increase in temperature from 300 K to 330 K. The optimum adsorption took place at a temperature of 310 K. Similar results have already been reported [16].

The values of thermodynamic parameters (ΔG° , ΔH° and ΔS°) for torque blue, red RB and yellow M4G dyes at

different temperatures are given in Table 1. The Gibbs free energy changes (ΔG°) were found to be negative in all the cases, indicating that adsorption is spontaneous. The values of enthalpy changes (ΔH°) were found negative for all the processes, suggesting exothermic nature of adsorption. Further the negative values of entropy changes (ΔS°) indicated decreased disorder and randomness.

From Table 2, it can be concluded that Langmuir adsorption isotherm model fits the data better than Freundlich and Temkin adsorption isotherms models. The suitability of Langmuir model suggested the monolayer formation of dye molecules on the adsorbent surface.

Table 3 shows that the correlation coefficients for all the dyes by using pseudo-second-order kinetic model were very high (0.996–0.997). Furthermore, the theoretical q_e values were found very near to the experimental q_e values for second-order kinetics. Therefore, the adsorption kinetics was more dominated by pseudo-second-order kinetic equation.

KSC may be considered as a better adsorbent for removal of red RB and Yellow M4G dyes as compared to some other adsorbents. Belpatra removed red RB dye 94% [6], whereas activated carbon removed Yellow M4G dye only 84% [17].

5 Conclusion

Results have shown that KSC acts as an effective adsorbent for removal of torque blue, red RB and yellow M4G dyes from aqueous solutions. The overall experimental results suggested that KSC has the maximum adsorption for torque blue (98.9%) followed by red RB (96.8%) and yellow M4G (95.3%) dyes. It was found that adsorption increased with increase in surface area of KSC. pH played an important role during adsorption. Percentage removal of red RB and yellow M4G dyes decreased with increase in pH, whereas in the case of torque blue dye it increased with increase in pH. The adsorption phenomenon was spontaneous, exothermic and favorable. Langmuir adsorption isotherm explained the monolayer coverage of adsorbates on KSC. The pseudo-second-order kinetics described the mechanism of adsorption.

Compliance with ethical standards

Conflict of interest The authors have no conflict of interest.

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