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One-step synthesis of the PdPt bimetallic nanodendrites with controllable composition for methanol oxidation reaction

Yuan Zhang, Jinfeng Zhang, Zelin Chen, Yunwei Liu, Mengmeng Zhang, Xiaopeng Han, Cheng Zhong, Wenbin Hu and Yida Deng*

ABSTRACT This paper demonstrates a one-pot approach to produce highly dispersed dendritic palladium-platinum bimetallic nanoparticles (NPs) with small particle size, tunable composition and high catalytic activity. Herein, the PdPt bimetallic NPs have been obtained using bayberry tannin (BT) as both the reducing agent and surfactant. Additionally, the PdPt bimetallic NPs with different Pd/Pt atomic ratios can be prepared by just varying the amounts of the Pd and Pt precursors. Most importantly, the as-prepared Pd52Pt48 catalyst exhibits the optimal catalytic activities compared with the other compositional PdPt NPs (Pd₈₂Pt₁₈, Pd₆₉Pt₃₁, and Pd₃₆ Pt₆₄) and commercial Pt/C (20 wt.%) catalyst for the methanol oxidation reaction (MOR). Meanwhile, Pd₅₂Pt₄₈ also shows better CO tolerance, which can be attributed to the unique dendritic structure and the synergistic effect between Pd and Pt. With evident advantages of the facile preparation and enhanced catalytic performance, it holds great promise as a high-performance catalyst for electrochemical energy conversion.

Keywords: one-pot approach, bayberry tannin, dendritic nanoparticles, controllable composition, methanol oxidation electrocatalysis

INTRODUCTION

With the world's growing demand for new resources that can be used as substitutes for the traditional fossil fuels, much attention has recently been given to proton exchange membrane fuel cells (PEMFCs). This is because they are ideal candidates for use in portable devices and are excellent alternatives that offer clean energy [1–3]. As we all know, Pt is the best catalyst of all pure metals for the PEMFCs [4]. However, it is hindered by the limited

reserves, high cost, and its poor resistance to CO poisoning despite the high activity [5]. One of the most effective strategies to solve this problem is to produce bimetallic Pt nanocrystals containing low-cost transition metals, which can effectively reduce the loading amount of Pt and improve catalytic activities ascribed to the synergistic effect between the two metals.

Based on this case, various structures have been successfully generated for Pt-based bimetallic nanostructures in a wide range of elements, such as PtPd [6-11], PtCu [12,13], PtAg [14], PtCo [15,16], PtAu [17,18], PtNi [19 -21], PtRu [22-25], and PtFe [26]. By comparison, given that Pd and Pt have nearly the same structures (the same group of the periodic table, the face-centered cubic (fcc) crystal structure and the similar lattice constants) [27,28], the PdPt bimetallic nanoparticles (NPs) are especially attractive for catalyzing multiple reactions due to the presence of the powerful catalytic components of Pd and Pt. Meanwhile, the incorporation of Pd into Pt-based bimetals can not only significantly reduce the cost of the catalysts by decreasing the amount of Pt, but also enhance the catalytic properties while reducing the CO poisoning effect due to a strong coupling between these two metals [8,29].

In order to develop PdPt catalysts with the enhanced Pd utilization and catalytic activity and durability, PdPt catalysts with a variety of morphologies were prepared, especially for the dendritic nanostructures, which have attracted increasing interest [6,7,9–11,30–32]. This special nanostructure can give rise to more catalytically active sites, such as boundaries and corner atoms, providing a high surface area in catalytic reactions. For example, the PdPt nanodendrites were acquired by following a facile

Tianjin Key Laboratory of Composite and Functional Materials, School of Materials Science and Engineering, Tianjin University, Tianjin 300372, China

^{*} Corresponding author (email: yida.deng@tju.edu.cn)

aqueous synthetic method reported by Zhou et al. [6], Yamauchi et al. [11], and Zhang et al. [30]. Regretfully, the catalytic performance toward methanol oxidation reaction (MOR) is far from meeting the application demands owing to the inapparent dendritic structure [6] and relatively large particle size [30]. Later, Lu et al. [7] synthesized the hollow Pt-on-Pd nanodendrites via a template approach, which employed a complicated preparation process. Moreover, the mass activity of the asobtained PtPd catalysts for MOR in the case was $275.2 \text{ mA mg}_{Pt}^{-1}$. This was too low to meet the current requirement due to the larger particle size although a hollow interior was successfully prepared. Meanwhile, the PtPd nanodendrites were usually prepared by a seedmediated growth strategy, in which the produced Pd nanoparticles first served as the seeds [9,10]. So undoubtedly, the main challenge in the synthesis of the PdPt nanoparticles with higher activity and stability is the difficulty involved in designing an economical and rational approach.

In this study, we described a one-step route to synthesize the PdPt bimetallic NPs with the assistance of bayberry tannin (BT) as reducing agent and surfactant. We provided a convenient and environmentally friendly approach without organic solvent and premade seeds. The dendritic PdPt bimetallic NPs with different compositions (Pd₈₂Pt₁₈, Pd₆₉Pt₃₁, Pd₅₂Pt₄₈, and Pd₃₆Pt₆₄) were prepared by adjusting the molar ratio between the Pd and Pt precursors (Table S1). The electrocatalytic results revealed that these dendritic PdPt catalysts exhibited higher catalytic property than that of commercial Pt/C catalyst toward the MOR. This result can be attributed to the high surface area with greatly promising active sites and to the synergistic effect of the two metals. Particularly, the Pd₅₂Pt₄₈ catalysts showed the optimal catalytic performance and an enhanced CO tolerance compared with other compositional PdPt catalysts.

EXPERIMENTAL SECTION

Chemicals and materials

Chloroplatinic acid hexahydrate (H₂PtCl₆·6H₂O, analytical grade) and perchloric acid (HClO₄, 70%) were purchased from Sinopharm Chemical Reagent Co., Ltd. Palladium (II) chloride (PdCl₂, analytical grade) was bought from Alfa Aesar. Bayberry tannin (BT, 99%) was purchased from Adamas Reagent Co., Ltd. Nafion perfluorinated resin solution (5 wt.% in a mixture of lower aliphatic alcohols and water, contains 45% water) was prepared from Sigma Aldrich, Co., Ltd. The commercial

Pt/C (20 wt.%) catalyst was purchased from Shanghai Hesen Electric Co., Ltd., and the commercial PtRu/C (20 wt.% Pt, 10 wt.% Ru) catalyst was obtained from Sigma Aldrich. The isopropanol alcohol was bought from Tianjin Commie Chemical Reagent Co., Ltd. Methanol (CH₃OH, 99.5%) was purchased from Aladdin Industrial Corporation. All reagents were used without further purification. Deionized water (Milli-Q) was used for the synthesis of nanocrystals and during the centrifugal process.

Preparation of PdPt catalysts

To prepare the dendritic PdPt bimetallic nanoparticles, 3 mL of 5 mmol L⁻¹ H₂PtCl₆·6H₂O, 1 mL of 10 mmol L⁻¹ Pd precursor (0.5 mmol L⁻¹ PdCl₂ dissolved into HCl with mole ratio of 1:2 to obtain Pd precursor solution), and 0.085 g BT were dissolved in 26 mL deionized water, after which the mixture was continuously stirred for 15 min at room temperature. Afterwards, the resultant homogeneous brown-yellow solution was transferred into a 50 mL Teflon-lined stainless steel autoclave, which was treated at 120°C for 6 h and then cooled down to room temperature by furnace cooling. Finally, the resulting product was collected by centrifugation at 18,000 rpm for 15 min, and washed five times with the mixture of deionized water and ethanol. The composition of PdPt NPs can be rationally adjusted by changing the volume of the different precursors added in the synthesis (Table S1).

Materials characterization

Transmission electron microscope (TEM) images, elemental analysis mapping, and line-scanning were recorded by a JEOL JEM-2100F with an acceleration voltage of 200 kV. Samples for TEM were prepared by dropping one drop of the NPs in water dispersion on a carboncoated copper grid (200 mesh). The crystal structure of the samples was characterized using a D8 Advanced Xray diffraction equipment (XRD, Cu K α , radiation, λ = 1.5406 Å). The inductively coupled plasma-mass spectrometry (ICP-MS) and energy-dispersive spectrometer (EDS) were used to measure the composition of the nanocrystals. The surface composition and electronic structure of the samples were characterized by X-ray photo electron spectroscopy (XPS, Kratos AXIS Ultra DLD). The plasma cleaner (PDC-002-HP (230V)) were used to clean the surface of the particles.

Electrocatalytic measurements

The methanol oxidation experiments were carried out using a conventional three-electrode system, which con-

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tained a glassy carbon electrode with a diameter of 5 mm as the working electrode for electrochemical measurements. The counter and reference electrodes were a Pt plate and an Ag/AgCl (3 mol L⁻¹ KCl) electrode, respectively. To prepare a catalyst-coated working electrode, the suspension in isopropyl alcohol and water (1:1) was dropcoated onto the polished electrode surface, followed by drying at room temperature. Afterward, the catalyst was covered with 8 µL of Nafion solution (0.2 wt.%) to ensure that the catalyst was tightly attached to the electrode surface during the electrochemical measurements. Then, the electrode was dried at room temperature. The electrode was cleaned by a plasma cleaner before the characterization. The metal loading of the prepared PdPt and commercial Pt/C, PtRu/C catalysts on the working electrode were both 35.7 µg cm⁻² according to the ICP data.

The electrochemically active surface areas (ECSAs) were measured by cyclic voltammograms (CVs) in an N₂saturated 0.1 mol L⁻¹ HClO₄ solution at a scan rate of 50 mV s⁻¹ by cycling the potential between 0.076 and 1.1 V (vs. reversible hydrogen electrode (RHE)). The ECSAs were calculated by the following equation: ECSA $=Q_{\rm H}$ / $m \times 210$, where $Q_{\rm H}$ is the charge in the $H_{\rm und}$ (underpotential deposited hydrogen) adsorption-desorption area obtained after the double layer correction region between 0.151 and 0.351 V (vs. RHE), m is the Pt loading amount on the electrode, and 210 µC cm⁻² is the charge required for the monolayer adsorption of hydrogen on the Pt surface. For methanol oxidation, the CVs and chronoamperometry curves were recorded in a mixture solution of 0.1 mol L^{-1} HClO₄ and 1 mol L^{-1} CH₃OH solution at a sweep rate of 50 mV s⁻¹. The CVs were obtained with the potential range of 0.256-1.256 V (vs. RHE). For the CO stripping measurements, high-purity CO (99.99% v/v in purity) was purged into the 0.1 mol L⁻ HClO₄ electrolyte for 20 min to obtain a maximum coverage of CO on the Pt active sites. Then, the dissolved CO was excluded by bubbling Ar gas (99.99% v/v in purity) for 20 min. Three consecutive CVs were recorded between 0.076 and 1.1 V (vs. RHE) at 50 mV s⁻¹.

RESULTS AND DISCUSSION

The dendritic PdPt catalysts were synthesized in an aqueous solution at 120°C for 6 h. The TEM image of the as-obtained PdPt nanoparticles with the $Pd_{52}Pt_{48}$ composition is illustrated in Fig. 1a. As can be seen, these PdPt NPs are distributed uniformly with the dendritic shape. High resolution TEM (HRTEM) images (Fig. 1b, c) taken from several subunits clearly show the well-resolved fringes with lattice spacing of 0.225 nm (①),

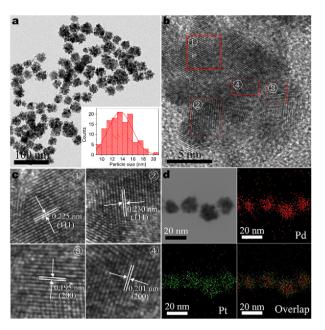


Figure 1 (a) TEM image and the size distribution (inset) of the $Pd_{52}Pt_{48}$ NPs. (b) and (c) HRTEM images of the $Pd_{52}Pt_{48}$ NPs. (d) EDX mapping images of Pd and Pt elements.

0.230 nm (②) and 0.195 nm (③), 0.201 nm (④), which can be indexed to the {111} and {200} crystal facets of the fcc PdPt NPs. Moreover, the lattice distances are slightly different from an individual metal Pd or Pt due to the production of the bimetallic NPs [33,34]. As seen in Fig. 1d, the energy-dispersive X-ray (EDX) elemental mapping images of Pd and Pt elements indicate the formation of a Pt-on-Pd structure consisting of Pd-rich core and Pt shell. Based on the dendritic morphology and small size, the NPs can present a high surface area, which is beneficial for improving the catalytic mass activity.

In order to determine the formation mechanism of the dendritic PdPt NPs, the effect of time on the morphology was investigated (Fig. 2 and Scheme 1). A large number of tiny irregular nanocrystals (4.8 nm) (Fig. 2a and Fig. S1) formed in the initial stage of the reaction (15 min). The BT (Fig. S2) served as the reductant which chelated with Pd(II) and Pt(IV) ions through its adjacent phenolic hydroxyl groups (Fig. S2b). Then, the Pd(II) and Pt(IV) ions are reduced to Pd and Pt atoms, while the phenolic hydroxyl groups are inductively oxidized to the corresponding quinones (Fig. S2c) [35-37]. Due to the excessive BT, Pd(II) and Pt(IV) ions can be reduced as much as possible although tannin may partially be oxidized to quinones under air atmosphere. However, because of the relatively faster reduction rate of Pd precursor compared with that of Pt [38], the preferential

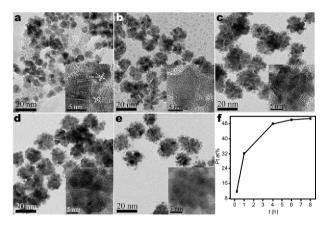
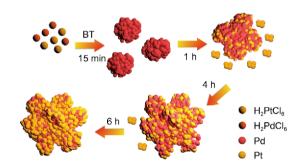


Figure 2 TEM and HRTEM images (inset) of the $Pd_{52}Pt_{48}$ NPs collected at different growth stages: (a)15 min, (b) 1 h, (c) 4 h, (d) 6 h and (e) 8 h. (f) The content of Pt varies with the reaction time.



Scheme 1 The schematic illustration of the Pd₅₂Pt₄₈ NP formation.

nucleation and growth of Pd lead to the prospective initial generation of the Pd-rich NPs, which is consistent well with the TEM-EDS results showing the atomic percentage of Pd is almost 88 at.% in the early stage (Table S2 and Fig. 2f). The interplanar spacings with 0.223 and 0.198 nm are observed in the inset at the bottom right in Fig. 2a, which are close to the {111} and {200} lattice spacing of the fcc Pd crystal, respectively, further demonstrating the formation of the Pd-rich nanoparticles. When the reaction time was increased to 1 h (Fig. 2b), Pd core was preferentially formed, and then Pt atoms deposited on the outer surface of Pd core due to the intrinsic high surface free energy and interatomic bond energy [39]. As a result, the dendritic PdPt structure with increasing particle size (15.2 nm) and Pt content (Fig. 2f) was formed due to the deposition of newly formed Pt atoms in an island growth mode on the Pd core surface (Scheme 1).

After 4 h, the particle size increased to 19 nm along with the Pt content (Fig. 2c and Fig. S1, respectively), which can be ascribed to the growth of the Pd core and

the deposition of Pt atoms side from the reduction of Pt precursors by BT via a chemical reaction that induced Pt atoms to form in an island pattern. With a further increase in reaction time to 6 h (Fig. 2d), Pt atoms can also be achieved by the galvanic displacement reaction between Pd atoms and Pt precursors (2Pd + 2Cl⁻+ PtCl₆²⁻ \rightarrow Pt + 2PdCl₄²⁻). This phenomenon contributes to a decrease in size (18.2 nm) with increasing Pt content due to the similar size of the Pd and Pt atoms [27,28]. After 8 h, no significant changes can be observed in the size, composition, and shape of the PdPt NPs (Fig. 2e), confirming the complete reaction within 6 h. The XRD patterns of the products obtained at different reaction stages are shown in Fig. S3, revealing an obvious shift of the pure Pt with the increased reaction time, which is also in agreement with the EDS composition analysis and the previous description (Fig. 2f).

The crystal structure, chemical composition, and electronic properties of the Pd₅₂Pt₄₈ catalyst were further characterized by XRD, TEM-EDS, and XPS. Fig. 3a shows four diffraction peaks corresponding to (111), (200), (220), and (311), respectively, which are positioned between the pure Pt (JCPDS No. 87-640) and Pd (JCPDS No. 87-637) crystal phases, thereby suggesting the generation of PdPt NPs. The Pd/Pt atomic ratio was confirmed as about 52:48 by both TEM-EDS (49.8:50.2, Fig. 3b) and ICP-MS (51.9:48.1, Table S3). Fig. 3c, d display the respective XPS spectra of Pd 3d and Pt 4f for the asobtained Pd₅₂Pt₄₈ and commercial Pt/C catalysts. The binding energies (BE) of Pd52Pt48 NPs are located at 335.21 and 340.76 eV for the $3d_{5/2}$ and $3d_{3/2}$, respectively, whereas those peaks are located at 335.01 and 340.31 eV for the pure Pd sample, respectively (Fig. 3c). Such positively shifted values indicate that the Pd in Pd₅₂Pt₄₈ catalyst is present in a different electronic environment, possibly due to the charge transfer of the PdPt catalyst [6,34]. Likewise, this change in the electronic structure of Pd and Pt is also responsible for the negative shift of Pt 4f BEs (Fig. 3d) compared with that of Pt/C catalyst. Specifically, Pt would draw electrons from Pd due to the larger electronegativity of Pt (2.28) compared with that of Pd (2.20) [40]. The change would then cause partial filling of the Pt 5d bands, resulting in a downshift of the d-band center [41].

In addition, the similar PdPt NPs with other Pd/Pt atomic ratios were prepared by simply tuning the molar ratio of the Pd and Pt precursors (Table S1). In the present synthesis system, the amount of Pt precursors plays an important role in the formation of the dendritic PdPt nanocrystals. When the composition was Pd₈₂Pt₁₈ ac-

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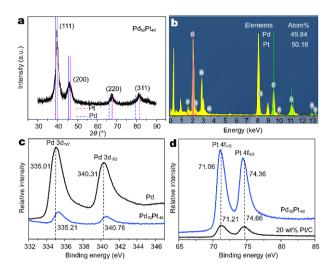


Figure 3 (a) XRD patterns of the as-prepared $Pd_{52}Pt_{48}$ catalyst. The drop-lines are the standard peaks for Pt (pink) and Pd (blue) from the JCPDS. (b) TEM-EDS pattern of the $Pd_{52}Pt_{48}$ catalyst. (c) Pd 3d XPS spectrum of the $Pd_{52}Pt_{48}$ NPs and bulk Pd. (d) Pt 4f XPS spectrum of the $Pd_{52}Pt_{48}$ and commercial Pt/C catalysts.

cording to both EDS and ICP-MS (Table S3), the monodisperse NPs with an average size of 13.6 nm were observed, as presented in Fig. 4a and Fig. S4.

Nevertheless, only small irregular particles with no obvious dendritic structure in this case were obtained, which resulted from less Pt atoms deposited onto the preferential nucleated Pd core surface due to the insufficient amount of the Pt precursors. With the increasing amount of the Pt precursors, the dendritic Pd₆₉Pt₃₁ NPs were formed (Fig. 4b), and the size of the nanocrystals ranged narrowly from 10 to 26 nm, with an average diameter of 19.2 nm (Fig. S4). This result is due to the subsequently direct nucleation and growth of Pt atoms on the central Pd core surface as mentioned previously. When the ratio of the Pd and Pt precursors changed to 2:3 (Fig. 4c), the overall atom percentage of Pt in the nanocrystals was 48.2%, as measured by ICP-MS, corresponding to a composition of Pd₅₂Pt₄₈. Furthermore, the obtained dendritic morphology which can provide more active sites were barely changed compared with Pd₆₉Pt₃₁ NPs. As illustrated in Fig. 4d, the dendritic Pd₃₆Pt₆₄ catalysts with an average size of 17.7 nm were obtained, and the sufficient Pt precursors more thoroughly facilitated the galvanic replacement reaction between Pd atoms and PtCl₆²⁻. This result will contribute greatly to the understanding of the decrease of PdPt particle size. Nonetheless, owing to the balance of the replacement reaction, Pd atoms cannot be replaced by Pt

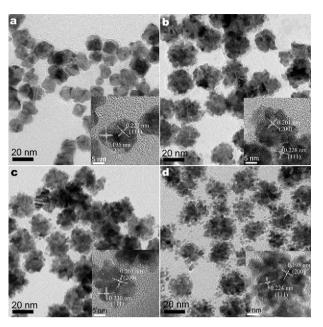


Figure 4 TEM and HRTEM (inset) images of the (a) $Pd_{82}Pt_{18}$, (b) $Pd_{69}Pt_{31}$, (c) $Pd_{52}Pt_{48}$, and (d) $Pd_{36}Pt_{64}$ NPs.

atoms absolutely. It can also be seen that some small particles distribute around the PdPt NPs, which can be ascribed to the spontaneous self-nucleation and growth of Pt atoms partially due to the increased content of the Pt precursors. In order to further reveal the detailed structure of these NPs, the corresponding HRTEM images are shown in the inset, indicating the growth of Pt branches at multiple sites on the Pd core. The measured interplanar spacing suggests the formation of PdPt NPs, which are mainly exposed by the {111} and {200} planes of the fcc PdPt nanostructure.

The XRD patterns were used to characterize the structure of these PdPt NPs, as presented in Fig. 5. All catalysts show four diffraction peaks corresponding to the fcc structure. Specifically, the peaks corresponding to the (111) plane of different PdPt NPs with increasing ratio of Pt are located at approximately 39.2°, 39.4°, 39.6°, and 39.8° respectively, showing a small shift to higher 2θ values. This shift results from the lattice expansion due to the incorporation of the larger Pt atoms into the Pd lattice [42].

To measure the ECSA of the PdPt NPs with different Pd/Pt atomic ratios, their CVs in an N_2 -saturated 0.1 mol L^{-1} HClO₄ solution at a scan rate of 50 mV s⁻¹ were conducted, as illustrated in Fig. 6a and Fig. S5a. From the hydrogen adsorption/desorption charges in the CV curves, the ECSA of the catalysts were calculated (Fig. 6b) to be 37.8, 31.3, 40.1, 21.3, 52.1 and 50.7 m² g_{pt}^{-1} for

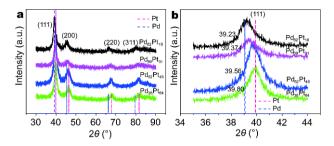


Figure 5 (a) XRD patterns of the $Pd_{82}Pt_{18}$, $Pd_{69}Pt_{31}$, $Pd_{52}Pt_{48}$, and $Pd_{36}Pt_{64}$ NPs. The drop-lines are the standard peaks for Pt (pink) and Pd (blue). (b) Enlarged XRD patterns in the range of $2\theta = 35^{\circ}-44^{\circ}$.

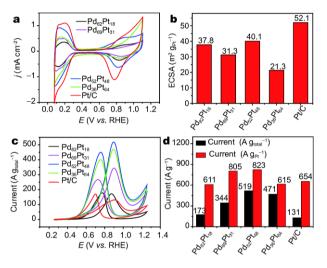


Figure 6 (a) CV curves in N_2 -saturated 0.1 mol L^{-1} HClO₄ solution at a scanning rate of 50 mV s⁻¹. (b) The ECSA of the catalysts. (c) CV curves in the 0.1 mol L^{-1} HClO₄ + 1 mol L^{-1} CH₃OH solution at a scan rate of 50 mV s⁻¹. (d) The MOR activity per unit mass of Pt (red bars) and per unit mass of metals (black bars).

 $Pd_{82}Pt_{18}$, $Pd_{69}Pt_{31}$, $Pd_{52}Pt_{48}$, $Pd_{36}Pt_{64}$, Pt/C, and PtRu/C, respectively. As for the PtRu/C catalyst, due to the surface dilution effect by Ru [43,44], it has relatively lower ECSA than that of Pt/C catalyst.

The catalytic activities of the samples toward MOR compared with commercial Pt/C and PtRu/C catalyst were investigated in the solution of 0.1 mol L⁻¹ HClO₄ + 1 mol L⁻¹ CH₃OH at a scan rate of 50 mV s⁻¹ (Fig. 6c and Fig. S5b, respectively). For the Pd₈₂Pt₁₈ catalyst, the relatively small size of these NPs is beneficial for the increase of the MOR activity, but the irregular structure without dendritic morphology is unfavorable. Therefore, these two factors make the activity of 173 A g_{total}^{-1} , which is relatively low. For the Pd₆₉Pt₃₁ catalyst, the activity was estimated to be 344 A g_{total}^{-1} . The higher value relative to the former can be attributed to the dendritic structure

providing larger surface area as well as high Pt content. It should be noted that the Pd52Pt48 catalyst displays the maximum peak current of 519 A g_{total}⁻¹, which is almost 4 and 1.3 times higher than those of commercial Pt/C (131 A g_{total}⁻¹) and PtRu/C (403 A g_{metal}⁻¹) catalysts, respectively. Additionally, the Pd₅₂Pt₄₈ catalyst has the largest specific ECSA, which can be attributed to the electronic coupling between the two metals. The Pd₅₂Pt₄₈ catalyst also has a large dendritic structure that provides a larger surface area, further confirming that the electrocatalytic activity can be optimized when the atomic percentage of Pt is about 50% in our case. Compared with the commercial Pt/C catalyst, the enhanced activity arises from the synergistic effect with Pd as well as its high surface area. With a further increased content of the Pt precursors (Pd36Pt64), the MOR activity was calculated to be 471 A g_{total}⁻¹, resulting from the branched structure with the highly exposed surface and active sites that was beneficial to MOR. In brief, the arrangement difference of the surface atoms for the bimetallic PdPt nanocrystals can readily lead to the activity change for MOR, although they have the similar shape and size. This observation is consistent with the structure-sensitive reaction [21,45] for MOR. Similarly, based on the per unit mass of Pt, the MOR activity increases with Pd/Pt ratio and then declines (Fig. 6d, red bars).

The Pd₅₂Pt₄₈ catalyst shows the highest activity (823.4 A g_{Pt}^{-1}), which is almost 1.26 and 1.36 times larger than that of the commercial Pt/C (654 A g_{Pt}⁻¹) and PtRu/C (604.1 A g_{Pt}⁻¹) catalysts, respectively. In methanol oxidation, Pd and Pt are mainly responsible for the water dehydrogenation (Pd-OH formation) and methanol dehydrogenation (Pt-CO formation), respectively. The reaction between Pd-OH and Pt-CO produces CO2 and regains the active metal surface, which is favorable for reducing the electronic binding energy in Pt and improving catalytic activity. This is also significantly co-affected by both the Pt/Pd ratio and their reaction dynamics. In the case of the lack of Pd, the water dehydrogenation on Pt occurs at a higher potential, making the overall oxidation process on pure Pt sluggish [34]. Thus, the activity of the Pd₃₆Pt₆₄ NPs is lower than that of the Pd₅₂Pt₄₈ catalyst despite the high Pt content. The activity also decreases with the presence of the excessive Pd on account of the lack of Pt for methanol dehydrogenation, as seen in the MOR catalysis of the Pd₈₂Pt₁₈ NPs. Moreover, according to XPS data for the Pd₅₂Pt₄₈ catalyst, the negative shift for the binding energy of Pt occurred. As is well known, the shift in binding energies is associated with the variation in the d-band center [41]. The

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resulting downshift d-band center of Pt can be ascribed to the electronic interactions of Pt and Pd, as well as the larger electronegativity of Pt than that of Pd [40], which is beneficial for the higher electrocatalytic activity. Thus, it is expected that the $Pd_{52}Pt_{48}$ catalyst exhibits the highest activity among all the samples due to the optimized composition in this study. Furthermore, unlike the reported bimetallic catalysts listed in Table S4, the MOR activity of the dendritic $Pd_{52}Pt_{48}$ nanoparticle is comparable to that of several state-of-the-art electrocatalysts, such as the nanoporous twinned $Pd_{75}Pt_{25}$ [46] and PtRu nanodendrites [22], but higher than those of many reported electrocatalysts [6–8,11,14,24,25,20,31,34].

The stability of the electrocatalysts with different Pd/Pt ratios was also evaluated by continuous CV cycling in the 0.1 mol L⁻¹ HClO₄ + 1 mol L⁻¹ CH₃OH solution. As shown in Fig. S6, it can be observed that the peak currents initially increase as a result of their exposed surface, which can adsorb impurities, then the currents gradually decrease with successive scans resulting from poisoning the electrode surface. To better evaluate the durability of these catalysts, the CV curves of all the catalysts after 500 cycles were determined. As illustrated in Fig. 7a and Fig. S5c, the $Pd_{82}Pt_{18}$, $Pd_{69}Pt_{31}$, $Pd_{52}Pt_{48}$, $Pd_{36}Pt_{64}$, and commercial Pt/C and PtRu/C catalysts show losses of 86%, 41%, 38%, 65%, 60% and 39% after 500 cycles, respectively. Strikingly, the Pd₅₂Pt₄₈ and Pd₆₉Pt₃₁ NPs retain a higher methanol oxidation current than the rest of the catalysts tested as well as that of Pt/C catalyst due to the well-developed synergistic effect under this composition in this paper. In detail, on the basis of the previous work [28], Pd is more easily dissolved compared with Pt. With the continuous removal of Pd in the core through pinholes, the particles gradually shrink, and the rearrangement of Pt atoms on the surface forms a more uniform and thin Pt layer, which can then improve the stability of the core-shell structure. This finding is also in agreement with the one mentioned above. Then, the stability of all samples was also evaluated by chronoamperometry. The results are descripted in Fig. 7b and Fig. S5d. After a sharp drop in the initial period of about 100s, the current decays at a slow speed, and then approaches a flat line. This phenomenon is attributed to the intermediate carbonaceous residues, which can be effectively oxidized and removed leading to a sustainable electro-oxidation process.

Impressively, the Pd₅₂Pt₄₈ and Pd₆₉Pt₃₁ catalysts maintained the higher current within 1,000 s when compared with the other catalysts tested in consistency (Fig. 7a and Fig. S5c). The morphologies of the Pd₅₂Pt₄₈ and Pt/C

catalysts after durability tests were also examined by TEM, as shown in Fig. S7. The results reveal that the dendritic nanostructures of $Pd_{52}Pt_{48}$ samples are well maintained after 500 cycles, whereas the Pt/C catalyst show significant aggregations, further confirming that $Pd_{52}Pt_{48}$ NPs has better stability compared with the Pt/C catalyst.

Given that CO poisoning tolerance is a significant indicator to further evaluate the performance toward MOR, three consecutive CVs were recorded for the Pd₅₂Pt₄₈ NPs (Fig. 8a), Pt/C catalyst (Fig. 8b), and other PdPt catalysts (Fig. S8), respectively. As shown in Fig. 8 and Fig. S8, a sharp peak appears during the first scan, and then disappears in the subsequent scan, indicating that the adsorbed CO is completely oxidized during the first forward scan. The onset potential of CO oxidation is indicated by the dashed line on the left for these catalysts. As can be seen, the Pd₈₂Pt₁₈ (0.492 V), Pd₆₉Pt₃₁ (0.463 V), Pd₅₂Pt₄₈ (0.451 V), and Pd₃₆Pt₆₄ (0.482 V) catalysts are much more negative than that of commercial Pt/C (0.507 V) catalyst, indicating the easier removal of CO from the surface of the dendritic PdPt catalysts. Additionally, the CO oxidation peak potentials are 0.887, 0.809, 0.823, 0.803, and 0.831 V for the $Pd_{82}Pt_{18}$, $Pd_{69}Pt_{31}$, $Pd_{52}Pt_{48}$, $Pd_{36}Pt_{64}$, and Pt/C catalysts, respectively. The lower CO oxidation potential implies the better CO-tolerance capability of the

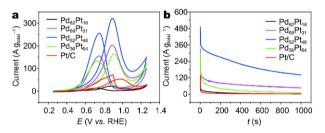


Figure 7 (a) CV curves of all the catalysts after 500 cycles in the solution of 0.1 mol L^{-1} HClO₄ + 1 mol L^{-1} CH₃OH acquired at a scan rate of 50 mV s⁻¹. (b) Chronoamperometry curves for all the catalysts in the 0.1 mol L^{-1} HClO₄ + 1 mol L^{-1} CH₃OH at 0.816 V (ν s. RHE) for 1,000 s.

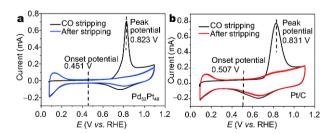


Figure 8 The CO stripping measurements of the (a) $Pd_{52}Pt_{48}$ and (b) commercial Pt/C catalysts in 0.1 mol L^{-1} $HClO_4$ at 50 mV s⁻¹.

catalyst, which arises from the dendritic structure and the synergistic effect due to the doping of the Pd atoms [27]. For the $Pd_{82}Pt_{18}$ catalyst, the larger peak potential may be due to the inapparent dendritic structure. Interestingly, although the $Pd_{52}Pt_{48}$ catalyst shows lower onset potential for CO removal than those of the $Pd_{69}Pt_{31}$ and $Pd_{36}Pt_{64}$ catalysts, it shows a slightly larger peak potential than those of the latter.

CONCLUSIONS

In summary, the as-made dendritic PdPt nanoparticles with tunable composition were fabricated by a one-step method, in which BT was used as both the reducing agent and surfactant. The binary compositions of these PdPt catalysts were controlled by simply adjusting the molar ratio of the Pd and Pt precursors. For MOR, these PdPt nanoparticles exhibited enhanced electrocatalytic performance. Especially, the Pd₅₂Pt₄₈ catalyst displayed the highest activities and much better durability, along with improved CO-resistance, making it superior to other PdPt samples and commercial Pt/C catalysts. This is due to the dendritic PdPt catalysts having a highly open structure that allows accessible active sites at the surfaces as well as good electrical connection across the entire surface. On the other hand, the incorporation of Pd in Pt can modify the electronic structure of Pt due to the charge transfer from Pd to Pt resulting in a lower CO adsorption on the PdPt surface. The synergistic effect can be well-developed under the composition of Pd₅₂Pt₄₈ in this report. This context develops a simple and feasible route, which may be extended to the preparation of other bimetallic nanocrystals, thus making it possible to design highly active catalysts for fuel cells.

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Author contributions Zhang Y and Zhang J designed and conceived the research framework; Zhang Y prepared and engineered the samples as well as conducted the performance investigation and so on; Chen Z designed the Scheme 1; Zhang Y wrote the paper with support from Zhang J and Deng Y. All authors discussed the results and commented on the manuscript.

Conflict of interest The authors declare that they have no conflict of interest.

Supplementary information Supporting data are available in the online version of this paper, including additional TEM, HRTEM images, XRD patterns, the molecular structure and chemical properties of BT, CV curves of the current change for all the catalysts with the continuous cycling from the $1^{\rm st}$ to $500^{\rm th}$ cycle, EDX, ICP data, and the MOR activities of various catalysts, and so on.



Yuan Zhang was born in 1992. She received her bachelor's degree from the School of Material Science and Engineering, Yanshan University, in 2015. She is now a graduate student at Tianjin University. Her research interests focus on the synthesis and characterization of platinum (Pt)-based nanomaterials for electrocatalytic applications.



Jinfeng Zhang received her PhD from the Department of Materials Science and Engineering, Shanghai Jiao Tong University, in 2016. She joined the Department of Materials Science and Engineering, Tianjin University in 2016. Her recent research interests focus on the design, synthesis, and characterization of nanostructured materials for electrocatalytic applications.



Yida Deng is a professor at the School of Materials Science and Engineering, Tianjin University. He received his PhD from Shanghai Jiao Tong University in 2006. His research interests include metal and metal oxide nanostructures for electrochemical and energy applications.

具有枝状形貌的PdPt双金属纳米颗粒的甲醇氧化活性增强研究

张媛, 张金凤, 陈泽霖, 刘赟威, 张萌萌, 韩晓鹏, 钟澄, 胡文彬, 邓意达*

摘要 本文利用一步法制备了具有小粒径、 组成可控和高催化活性的高度分散的枝状PdPt双金属纳米颗粒. PdPt双金属纳米颗粒通过单宁酸(BT)作为还原剂和表面活性剂得到,起到了简化工艺的作用. 此外,具有不同Pd/Pt原子比的PdPt双金属纳米颗粒可以通过改变Pd和 Pt前躯体的量来获得. 与其他成分PdPt纳米颗粒($Pd_{s2}Pt_{1s}$, $Pd_{s9}Pt_{31}$, $Pd_{36}Pt_{44}$)和商业Pt/C(20 wt.%)催化剂相比, $Pd_{52}Pt_{4s}$ 催化剂具有最高的甲醇氧化电催化活性,这归因于其独特的树枝状结构以及Pd和Pt之间的协同效应. 该研究具有易于制备和高催化性能的优点,在电化学能量转换高性能催化剂方面具有巨大的应用前景.