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# A Review of Circular Economy Prospects for Stainless Steelmaking Slags

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#### Abstract

The world of stainless steel production was 52 Mt in 2019, and the annual amount of slags including electric furnace, AOD converter, ladle, and casting tundish, was estimated at 15–17 Mt. Nowadays, only a minor fraction of slags from stainless steel production is utilized and a major part goes to landfilling. These slags contain high-value elements (Cr, Ni, Mo, Ti, V...) as oxides or in metallic form, some of them being environmentally problematic if dumped. Thus, any approach toward circular economy solutions for stainless steel slags would have great economic and environmental impacts. This contribution examines the slags from different process stages, and the available and new potential means to increase internal recycling and to modify slags composition and structure by optimizing their properties for reclaiming in high-value applications. Eventual methods are, e.g., fast controlled cooling and modifying additives. Means to recover valuable metals are discussed as well as potential product applications to utilize various slags with different chemical, physical, and mechanical properties. By integrating the treatments and steering of slags' properties to the total process optimization system, the principles of circular economy could be achieved.

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#### **Graphical Abstract**



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#### Introduction

Stainless steel is the most rapidly growing metal with an annual growth rate of 5.33% (1980-2019) [1]. That number matches well with Fig. 1 which shows the recent progress from the year 2005: the production has doubled in 15 years and approached 52 Mt in 2019 belonging to the same category with aluminum and copper as to the volume and value. The overall world steel production was 1869 Mt/2019 [2]. The iron and steel production together generated a massive quantity of slags ( $\approx 600$  Mt/year). Such volumes cannot be landfilled for environmental and economic reasons, and various treatments and applications have been intensively developed. Nowadays, a high percentage is either recycled, reused, or valorized in different applications. The total amount of slags from stainless steel production was estimated as 15-17 Mt/year including slags from different process stages, EAF melting, AOD & VOD converting, ladle operations, and casting [3]. The present situation of

slags from stainless steel production is different: on average, only a minor fraction is utilized, and a major part goes to landfilling. The utilization degree varies from zero to 100% depending on the plant's course of action. An apparent reason is that stainless steel plants are small compared to carbon steel plants, and the amount of slags are minor, respectively. Hence, landfilling has been a simple means and permitted thus far, but problems may arise in the long run. Another reason is the complexity of these slags, which makes the treatment and utilization more demanding. It also needs investments in equipment. Consequently, the slag processing has not been considered economically attractive enough, and many steel plants have settled down to steel production and marginalized secondary functions. But there are several positive grounds as well which are highlighted through this article.

Differing from blast furnace and converter slags, stainless steelmaking slags contain high-value elements (Cr, Ni, Mo, Ti, V) as oxides or in metallic form. An efficient recovery



Fig.1 The growth of world stainless steel production in the years 2005–2019 [1]

of these metals is an economic driver and an environmental target for saving the use of natural resources. Another environmental aspect is that some components in slags can be environmentally problematic if dumped. Cr (VI) is a well-known risk, and its formation should be eliminated. Cr and Ni are also carcinogens [4, 5]. Fluorspar (CaF<sub>2</sub>) is commonly used as flux in stainless steel slags causing an environmental risk. Dusting is a further problem characteristic to slags with high basicity. To summarize the foregoing aspects, all actions towards circular economy solutions will have a great economic and environmental potential. The aim of this contribution is to review available and new feasible means to increase internal recycling, and to modify slags composition and structure as objectives to optimize their properties

for reclaiming in different high-value applications. Eventual methods are, e.g., modifying additives and fast controlled cooling. Different means to maximize the recovery of valuable metals are reviewed as well as potential product applications to utilize various slags.

#### **Slags from Different Unit Processes**

An overall scheme of stainless steelmaking is shown in Fig. 2. The process starts with melting stainless scrap, ordinary recycled steel charging, and alloying additions (FeCr, FeMo, FeNi) in an electric arc furnace (EAF). The aim is to prepare a liquid steel charge close to the final composition as for the main alloying elements and proper carbon and silicon contents for the subsequent AOD (Argon Oxygen Decarburization) or alternatively VOD (Vacuum Oxygen Decarburization) converter. Melting with arcs assisted by oxygen blowing results in a partial oxidation of [C] and most of [Si] to final contents about 1-1.5% C and 0.1-0.2% Si. The Cr oxidation is strived to restrict and to avoid too high  $Cr_2O_3$  content in the slag via these residual contents, especially [%Si]. In the case of direct VOD treatment (without AOD process), lower [C] is required after the EAF.

In the AOD converter, carbon is oxidized to low contents  $(\leq 0.05\%)$  by  $O_2 + Ar (N_2)$  blowing starting with 100%  $O_2$  and by stepwise lowering  $p_{O2}$  from 100% to zero and increasing  $p_{Ar}$  from zero to 100%, in tandem. Carbon oxidation is preferred to Cr oxidation when  $p_{CO}$  is decreased by neutral gas (Ar, N<sub>2</sub>) dilution. In VOD converter,  $p_{CO}$  is reduced by



 Table 1
 Approximate compositions and amounts of slags from stainless steelmaking

Unit process	CaO	SiO <sub>2</sub>	MgO	Al <sub>2</sub> O <sub>3</sub>	Cr <sub>2</sub> O <sub>3</sub>	CaO/SiO <sub>2</sub>	$CaO + MgO/SiO_2$	Amount kg/t steel	Minor other components
EAF	40-45	25-30	5-12	5-10	3–7	1.5-1.8	1.7–2.0	100–150	Fe, Mn, Ti, V, Ni
AOD	55	25-30	5-10	$1-5^{a}$	0.5 - 1	2	2.5	100-120	CaF <sub>2</sub>
LF-CC	55-60	20-30	5-10	1-5 <sup>a</sup>	1–5	2–3	2.2–3	15-20	CaF <sub>2</sub> , Ti, Nb, V

<sup>a</sup>Even higher when the slag is reduced, and steel deoxidized with Al- or Ca-aluminate added into the slag

low pressure, i.e., vacuum. Anyway, towards very low [C], some [Cr] is oxidized, and quite high  $Cr_2O_3$  contents about 25% can be found in AOD slag after the decarburization period. Therefore, the next necessary stage is slag reduction done by adding FeSi or eventually Al into the steel melt and stirring with argon gas. After the slag reduction stage, the Cr content in the slag is aimed at low contents e.g., 0.5%  $Cr_2O_3$ . Then the slag is tapped to a slag pot, and lime and fluorspar are added into the converter to form basic liquid slag for a short desulfurization treatment with intensive Ar stirring. In addition to the composition of AOD slag in Table 1, the slag after reduction can contain several percent fluorspar.

After tapping into the ladle, CaO and CaF<sub>2</sub> are added again to form a basic slag to protect the steel from the influence of air, to absorb deoxidation products from the steel, and to improve steel cleanliness via ladle metallurgical (LM) treatments under Ar stirring. Trimming alloying is performed as well. It is common that the LM treatments take place in a ladle furnace (LF) which makes temperature adjustment easy. The LF slag follows on the ladle to continuous casting (CC), and after the cast end, the slag is poured into a slag pot. An adjunct slag used in the CC tundish is typically more acidic. Its function is thermal insulation and protecting steel during casting. The amount is minor and was not presented separately in Table 1. It can be incorporated in other slags. As a general comment, MgO (dolomitic lime) is added into slags to protect magnesia-based refractory linings. It influences the properties of the slag, e.g., basicity, Cr solubility, melting temperature, and viscosity as well as the mineralogical structure after solidification and cooling.

In Table 1, the main three types of slags are described. The figures are approximate composition ranges based on Nordic steel plants. They refer to slag compositions in situ at the end of each process stage and do not include eventual large metal lumps. Of course, slags are factory specific and can differ substantially due to various raw materials, process operation, and steel grades to be produced. In Table 1, the slags from different unit processes differ both in basicity, Cr content, and minor impurities. Except for the oxide forming components in the slag, also less-oxidizable metals like Ni and Mo can be found but mostly in metallic particles ejected from the bulk steel or endogenously formed inside the slag via the reduction process. In addition, slags can retain macroscopic metal particles, splashes, skulls, tapping remains, etc., which are not included in the slags' compositions above. Their removal and recovery in an early stage of a treatment process is essential. Nowadays, a typical slag processing route in a stainless steel plant consists of wet grinding and metal separation. It is emphasizing metal recovery but has quite restricted ability to slag recycling and productization. Depending on slag composition, cooling method (slag pit vs. intensified water cooling), and grinding,

the basic slag material is delivered to purposes such as road and infrastructure construction. Unfortunately, most slags from stainless steelmaking still go to landfilling which needs space, causes loss of valuable resources, and is hazardous to human health and the environment. As mentioned earlier, the main risk is the eventually high Cr content which can lead in contamination of soil and water in the form of leachable Cr (VI). Cr and Ni are also carcinogens. Avoiding negative impacts is a strong motivation for emphasized slags utilization, but there is also a great economic potential via improved recovery and slags valorization. In the following chapters feasible treatments for improved metals, recovery and valorized utilization of slags are surveyed. Both established methods and new innovative solutions are discussed. In many cases, the references are from carbon steel production, whereupon the special features of slags from stainless steel making should be considered when contemplating potential applications.

#### **Metals Losses in Slags**

Metals as dispersed fine particles or dissolved as oxides in slags are difficult to recover. Let us consider our primary interest, Cr as an example to examine which factors influence its presence in the slag. The content of oxidized Cr "Cr<sub>2</sub>O<sub>3</sub>" in the end slag of the EAF process or the slag from the AOD reduction stage depends on the oxygen potential (defined as  $p_{O2}$  or  $a_{O1}$ ), which is determined by the ambient contents (activities) of [Cr] and the controlling solutes [Si] and eventually [C] in the EAF. Hitherto, the ambient temperature as well as the slag and liquid metal compositions influence via the activity of Cr<sub>2</sub>O<sub>3</sub> and  $a_{Cr1}$ , respectively. Thermodynamic and kinetic aspects were investigated and discussed, e.g., by M. Guo et al. [6, 7]. The equilibrium Cr distribution between the slag and steel (%Cr)<sub>slag</sub>/[%Cr]<sub>steel</sub> can be derived from the reaction equation:

$$2[Cr] + 3[O] \leftrightarrow (Cr_2O_3), \tag{1}$$

$$K_{1} = \frac{a_{\rm Cr_{2}O_{3}}}{a_{\rm Cr}^{2} \cdot a_{\rm O}^{3}}.$$
(2)

Chromium oxide was simplified here as 3-valent oxide  $Cr_2O_3$ , although it is well known that in low  $p_{O2}$  conditions, also 2-valent oxide CrO exists [8, 9]. In a process with oxygen blowing,  $p_{O2}$  or  $a_{[O]}$  is controlled by carbon oxidation reaction,  $a_{[O]}$  increases, and the equilibrium is approached from left to right. The ambient top slag can become even supersaturated with oxygen via Cr oxides, especially when  $O_2$  top blowing is applied. In a reduction stage,  $a_{[O]}$  is controlled and pressed down by adding silicon or aluminum, and

the reaction should go backwards. The gross reactions can be written as follows:

$$(Cr_2O_3) + 3/2[Si] = 2[Cr] + 3/2(SiO_2),$$
 (3)

$$(Cr_2O_3) + 2[Al] = 2[Cr] + (Al_2O_3).$$
 (4)

According to several researchers, a primary reduction mechanism is the reaction between the metal bath and the emulsified slag droplets due to the large surface area of the droplets as well as efficient mass transfer due to the intensive stirring conditions in a side-blown converter [10–12]. When the reaction takes place at the slag/metal interface, the formed metal can easily merge into the bulk metal. However, when reduction occurs inside the slag-metal emulsion, the formed metal can end up in the bulk slag and remain there as fine droplets or precipitates. Then the settling rate depends on several factors like the droplet size, slag's viscosity, as well as the density difference and interfacial tension between slag and metal. In an AOD converter, the slag composition, its properties, and the process parameters, like temperature and gas flow rate, are relatively well controlled, and consequently, the reduction rate and the final reduction degree can be reasonably predicted [12]. The situation in the EAF smelting is different. As seen in Table 1, the  $Cr_2O_3$  content is much higher in the EAF slag than in the AOD reduction slag. Also, the scatter can be quite high (up to 10-15% $Cr_2O_3$  [6]), and the control of final  $Cr_2O_3$  is difficult due to the complexity of the process with varying raw materials and melting efficiency, injected additions, slag's behavior (eventual foaming), and more or less contradictory targets when trying to reconcile the final [C] and [Si] contents on the one hand and metals losses into the slag (Cr, Mn, Mo, Ni...) on the other. When optimizing the operation of the total EAF-AOD integrate, metallurgical and productivity aspects are of primary concern. In addition, maximizing metals recovery and minimizing losses and steering of slags properties for subsequent treatments and final applications should be inevitable issues as well.

#### Metals Separation and Recovery: Pyroand Hydrometallurgical Treatments

Metals recovery from slags can be done via physical and chemical means. Physical separation is applicable for large metallic particles; the slag should be first properly comminuted to liberate the metals after which metal is removed by gravimetric and/or magnetic methods [13–16]. EAF slags have the best potential in good metal recovery due to the highest metal content. Conventionally, slags are merged for treatments, but it would be possible to handle each slag type

independently, even by considering slags from production of different steel grades (e.g., Ni, Mo, Ti, V). Then each slag type could get its own specific post-treatment without getting blended into the big bulk. The recovered metals can be recycled as reverts to process. The quantity is typically several percent of the slag weight. In the case of stainless steel, the value of Cr is the leading factor; its content is high in all stainless grades throughout the process stages. The comparison of unit prices of valuable elements ( $\ell/kg$ ) gives an order: Cr < <Ni < <Mo < V. In special cases , when high Ni or Mo steels are produced, their value in the steel and in metallic inclusions in slag can be even higher than the value of Cr, respectively. For an efficient recovery, it is important to keep each special type of slag as its own lot and not to mix and dilute the valuable element into the big bulk of slags. As to other minor but valuable elements, vanadium contents are typically max tenths of a percent, but its recovery can be worth an inquiry. The same concerns titanium although it is less expensive.

For more quantitative recovery a pyrometallurgical treatment is an option. It might be a separate "reduction furnace" in which valuable metals could be reduced from the slag to very low contents in a properly stirred reactor under highly reducing conditions, e.g., in the presence of a Fe-C or Fe-C-Cr melt. Also, other reductants like Si and Al are possible [15–21]. Cr bound is most difficult to reduce in spinels like MgCr<sub>2</sub>O<sub>4</sub>. Liquid slag and high temperature  $\geq$  1873 K make beneficial conditions to achieve over 95% Cr recovery. Any ready industrial applications are not on the record, but such approaches have been examined. Both electric furnaces with electrodes and induction furnaces are feasible reactors. The product is liquid Fe-C-Cr alloy containing also other valuable metals depending on the initial slag composition. When a pyrometallurgical slag treatment furnace can be installed on-site in the steel plant, direct charging of the liquid slags can be applied. Then a much faster process and significant energy saving are achieved. Also, the metallic product is possible to use in situ. Depending on the unit processes inside a steel plant integrate, it can be possible to combine slags from stainless steelmaking with other industrial byproducts like blast furnace slag, slag from FeCr process, mill scales, pickling sludges, etc. [21–25].

Also, hydrometallurgical treatments afford means for recovery of valuable metals from stainless steelmaking slags. In a European CHROMIC project (Efficient mineral processing and hydrometallurgical recovery of by-product metals from low-grade metal-containing secondary raw materials), a comprehensive characterization of slags and a survey of different potential methods for metals recovery were performed [13, 14, 25–28]. Extraction of Cr has been promoted, e.g., via mechanical or microwave activation, alkaline roasting/leaching, and acid leaching. Other metals like V, Mo and Ni are possible to leach and recover selectively [25, 29, 30].

On the other hand, leaching tests can be used to determine the stability/instability of metals like Cr and V in the slag's mineral structure [31]. As pointed out earlier, the risk of leachable Cr and its oxidation to Cr(VI) is a potential risk in landfilled slag as well as in certain applications like fertilizer and soil conditioner. Therefore, the "residual chromium" in the slag should be stabilized as strongly as possible. For that purpose, binding Cr in spinel structure is a firm solution [31–37]. Low basicity and high  $Al_2O_3$  and MgO favor spinel formation. A "spinel factor" was developed to define the dependency:

Factor sp = 0.2MgO + 1.0Al<sub>2</sub>O<sub>3</sub> + nFeO<sub>x</sub> - 0.5Cr<sub>2</sub>O<sub>3</sub>(wt%). (5)

The coefficient n gets values from 1 to 4 depending on the oxidation state of iron (FeO<sub>x</sub>  $\rightarrow$  Fe<sub>2</sub>O<sub>3</sub>). A strong spinel formation is attained with factor sp > 5 [32–35].

#### **Steering Slags Properties for Applications**

As described afore and presented in Table 1, several slags are generated in stainless steel smelting and refining and each slag type has its own chemical and mineralogical characteristics. They are mainly defined by the metallurgical demands of the targeted steel grade and eventual specific requirements (ferritic, austenitic, other high steel grades). The first one, i.e., EAF slag (black slag, EAFS) is mainly formed by calcium silicates, and it is rich in metallic oxides (Cr<sub>2</sub>O<sub>3</sub>, FeO, MnO), in some cases up to 10% or even more. The minerals observed in the EAFS are  $\beta$ -Dicalcium-silicate (Ca<sub>2</sub>SiO<sub>4</sub>), Bredigite (Ca<sub>17</sub>Mg<sub>03</sub>SiO<sub>4</sub>), Merwinite (Ca<sub>3</sub>MgSiO<sub>8</sub>), Melilite (Ca<sub>2</sub>Al<sub>2</sub>SiO<sub>7</sub>—Ca<sub>2</sub>MgSi<sub>2</sub>O<sub>7</sub>), and Spinels ((Fe,Mg)  $(Cr,Fe)_2O_4$ ). This slag is compact and has a good volume stability. Characteristic to these slags is a wide composition variety owing to the batch process and heterogeneity of charge materials.

In the AOD process, the primary decarburization slag is reduced and adjusted to higher basicity for desulfurization and after this treatment tapped into a slag pot (single slag practice). In the case of demanding final sulfur target, the reduction slag can be tapped and an additional slag with higher basicity can be formed (2-slag practice). AOD reduction slag (AODS) is typically more basic than the EAFS and has a white color due to its low Fe, Mn, and Cr oxides. Mineral composition is not very divergent from EAFS consisting of calcium silicates and occasionally free lime (CaO<sub>free</sub>) and cuspidine (Ca<sub>4</sub>F<sub>2</sub>Si<sub>2</sub>O<sub>7</sub>) originating from fluorspar additions for slag's fluxing, and no spinels. It is collected in slag pots in which also the desulfurization slag is poured in the case of 2-slag practice. AODS is composed mainly by crystals of  $\beta$ - and  $\gamma$ -dicalcium silicate (Ca<sub>2</sub>SiO<sub>4</sub>). These slags tend to disintegrate by the phase transition from  $\beta$ - to  $\gamma$ -dicalcium silicate during cooling, causing dust generation. Another instability problem comes from hydration of free lime (CaO<sub>free</sub>) and periclase (MgO<sub>free</sub>) which are typically present in basic slags (AODS, LFS). Conventional "hot modification" of slag can be performed during slag tapping/pouring or in the slag pot by adding a "stabilizer" (borate, MgO, Al<sub>2</sub>O<sub>3</sub>) which prevents the dust-forming  $\beta$ -C<sub>2</sub>S to  $\gamma$ -C<sub>2</sub>S transition [36–41].

A portion of the AODS slag is accompanying steel to the Ladle furnace where slag's composition is further adjusted by suitable additions (CaO, MgO, CaF<sub>2</sub>, Ca-aluminate slag) depending on the steel grade. The main functions and requirements of the ladle furnace slag (LFS) are to protect steel from contamination with air, to minimize heat losses, to improve cleanliness by absorbing inclusions from steel, and to minimize the wear of refractory lining [42]. This slag has a similar elemental and mineral composition as that one coming from AOD desulfurization, and thus, it is practical to incorporate them together. After all, in the stainless steel production, two basic types of slag can be distinguished: black EAFS with higher contents of metallic oxides and low basicity (C/S  $\approx$  1.5), and white slags from AOD, VOD, and LF, which are more basic  $(C/S \ge 2.0)$  and with lower contents of metallic oxides.

### Effects and Potential Applications of Controlled Cooling

Apart from slag chemistry, cooling rate is another way to control the mineralogical structure of the solidified slag. Slag's "journey" from the process conditions  $\geq 1600$  °C to outdoors temperature is, thus, extremely crucial, and it is strongly connected to utilization of slags in different applications. For different controlled cooling rates, several methods are available from slower to faster cooling: free air cooling in slag pot or bed < the same with water spraying < air granulation < water quenching < pouring thin layer on metal substrate or corresponding rapid cooling technique [43-50]. Rapid cooling can prevent crystallization in accordance with the phase diagram resulting in an amorphous glassy structure, encapsulating eventual metal particulates and solid oxides, and thereby lowering the solubility of heavy metals. Such a slag can be used for road construction. The tendency for glass formation is characteristic for acid viscous silicate slags and, thus, depends on both the chemical composition and the cooling conditions. Glasses, such as granulated slags, can be regarded as supercooled liquids with very high viscosity. By enhancing the fraction of amorphous material in a slag, the potential hydrating properties are improved, and the slag can be used in cement and concrete products for high-quality construction applications. Controlled cooling conditions can be a means to affect minerals formation and transformation and, consequently, the solubility of elements such as Cr, Mo, and V. Their leachability depends on the distribution between glassy and crystalline phases which is influenced by the whole cooling curve including the high-temperature liquid and liquid–solid stages too [48–50].

Controlled slag cooling process gives a good opportunity for heat recovery as hot air or steam [51-57]. When producing amorphous slag as a substitute to cement dry granulation by air is the best choice. Such methods like rotary drum, spinning disks, and rotary cups are potential methods, offering the advantage of generating uniform and small grains at a lower energy consumption rate [52]. Better heat exchange is attained with smaller droplets resulting in better heat recovery and higher temperature, and the slag is quenched faster with less coolant. A two-step heat recovery system consisting of a fluidized bed, followed by a packed bed has been proposed to get maximal energy recovery efficiency, as both high outlet gas temperature and low slag discharge temperature are achieved [52]. In this form, the heat recovery is, however, only for energy storage before its final utilization. Better total energy efficiency could be achieved via chemical energy recovery methods which afford high energy density and zero loss when applied on-site without any transportation. Examples of processes under investigation are methane reforming and coal gasification [55, 56]. Hydrogen production by decomposition of CO<sub>2</sub>-CH<sub>4</sub> over hot-granulated slag in a packed bed has been studied. The slag acted not only as thermal media but also as a catalyst promoting the decomposition process [58, 59]. Thermoelectric power generation appears to be an emerging technology in the future with many applications. Combined with an appropriate phase change material (PCM) as energy storage to solve the current mismatch between the high slag temperature and much lower operating range of thermoelectric materials, this technology might suit to the recovery of slag waste heat energy as well [52, 60].

#### **Current and Novel Slag Products and Applications**

In general, several steel slags have beneficial properties such as good strength, durability, and latent pozzolanic (cementitious) properties that make them attractive and potentially suitable for engineering applications, such as infrastructure construction, soil stabilization, neutralizer, as filler or binder in concrete or as drainage or low-permeability barrier layers [61–67]. Slags from stainless steelmaking are potential as well provided that the best suitable slag type is selected and modified by appropriate additions, cooling method, or other pre-treatments, i.e., tailoring for each specific application. Electric arc furnace slags (EAFS) have physical properties comparable to natural aggregates such as granite, e.g., high compressive strength and resistance to abrasion and, thus, fitted as landfill construction material. More basic slags (AODS, LFS) are potential substitutes as cementitious binders, thus, cutting CO<sub>2</sub> emissions of the cement production [64–69]. Alkali activation is used to improve cementitious properties and to form hardening matrix, geopolymer [69, 70].

Different product applications of metallurgical slags in general and potential for stainless steel slags are collected in Fig. 3 by completing the previous process scheme. An essential stage is slags' treatment, which can be specific for each slag type and dependent on the target product. Recovery of metals and direct return to the in-plant processes or eventual external use are performed in this stage. Internal recycling of slag is possible as well, e.g., a part of AODS/ LFS could be returned to EAF as a CaO+MgO source and slag forming agent. Thereafter, the slag lots continue to their final purposes, products, and uses. Some of these were



**Fig. 3** The scheme of different unit processes in stainless steelmaking, slags formation, treatment, and product applications already discussed above. The use in fillers for instance as an ingredient in asphalt concrete has been studied [71, 72]. Precipitated calcium carbonate (PCC) is a relatively valuable product as a filler and pigment for paper industry. The conversion of slag to PCC means carbonization of CaO (MgO) in the slag to form CaCO<sub>3</sub>. Such decarbonization processes have been intensively studied; few examples are in references [73-77]. As a measure to mitigate CO<sub>2</sub> emissions, it was estimated that utilization of one ton of EAFS for carbon capture could mineralize 0.38 tons of CO<sub>2</sub> in the flue gas, via an accelerated carbonation process. The carbonated EAFS product could be used in cement mortar, with additional benefits. The whole global CO<sub>2</sub> reduction potential by applying mineralization for iron and steelmaking slags was approximated as 0.137 Gt CO<sub>2</sub>, per annum [57]. All these applications are substitutes for virgin materials and thus save natural resources and reduce CO2 emissions. Two dashed arrows between the "slag line" and "product line" describe the interactive relation slag's steering/treatment ↔ application/

2000

1500

product. By integrating the treatments of slags and steering of their properties to the total process optimization system, the targets of circular economy could be attained, and the portion of landfilling minimized and even reset to zero.

#### **Economic Viewpoint**

The foregoing survey mainly started from environmental and metallurgical standpoints. For more advanced development and industrial exploitation, there must also be an explicit economic incentive. Figure 4 strives to outline the economic driver for slags treatment and productization. In the current situation, when most of stainless slags are landfilled, it means expenses (from tens to few hundreds €/t depending on the disposal tax and handling costs.

Anyway, the value is negative: large amounts and high total cost. By refining waste to resource and final useful products, the value turn to positive to tens/hundreds/thousands  $\notin$ /t. The highest value Ca-based products might be

**Fig. 4** Schematic illustration of the economic driver for slags' productization and reclaiming in high-value applications. The relative amounts of different products were approximated by the width of each box



Fig. 5 Estimated relative values of cash flow for different slag products (columns) and respective segments of slags (symbols blue square, red triangle) (Color figure online) such products like food additives. Along with the valueadded production, the treatment expenses tend to grow and the quantities to decrease. As an offshoot of a large integrate, it can utilize the ready infrastructure which means low investment costs and raises its attractiveness. In Fig. 4, the conceivable volumes are presented by the width of each box. The fraction of "Landfilling" corresponds to the remaining landfilled amount after full productization.

Another economic approach is presented in Fig. 5 in which the cash flow of each slag product group was estimated. The cash flow values were calculated based on the approximated fraction of each product (as well as of land-filled slag) and its market price. It is seen that high-value Ca-based products with a volume of 5% might yield of the order of 2/3 of the total cash flow. For the total economic value estimation also, the production costs should be approximated, respectively.

## **Concluding Remarks**

The world of stainless steel production is strongly growing. As a consequence, the amount of produced slags increase rapidly. Today, most of these slags go to landfilling, although there are varying practices in different companies. The utilization degree has been low due to their small amounts and complexity. Slags landfilling can cause environmental and health risks due to metal and fluoride contents. Tightening environmental requirements and demands for circularity are pressing for reassessment and corrective actions. On the positive side, the slags have a great economic, technical, and ecologic potential, when properly recycled, recovered, and productized. The main results of the survey can be condensed into a few remarks.

- Optimized running of the unit processes (EAF-AOD/ VOD-LF-CC) is a central issue considering slags' properties as for the function of the slag in the primary process and for the subsequent slag processing for specific products.
- 2. For the steelmaking process, it is crucial to minimize metal losses into the process slags, and to obtain efficient metals recovery from the slags.
- As the slags, however, always contain valuable alloying metals (Cr, Ni, Mo), their efficient recovery is a key economic issue. Also, minor elements (V, Ti) should be considered. In addition to mechanical separation, chemical treatments, leaching, and extraction are attractive. Via selective individual processing of different slag types, the recovery of metals could be maximized.
- 4. The composition and mineralogical structure of the slags can be steered by modifying additions and controlled

cooling. Heat recovery from molten slag is a potential option too.

- 5. Slag granulation equipped with heat recovery as hot air could produce significant amounts of high-quality material to construction purposes with minimal energy and low carbon footprint.
- 6. High total energy efficiency could be achieved via chemical energy recovery methods for production of synthesis gas, hydrogen, or even direct conversion to electricity. Such techniques are under development.
- 7. Concerning slags, utilization and productization, stainless steel slags are suitable to special high-value products due to relatively small quantities with well-specified chemistry and properties. An economic assessment was performed exhibiting the potential to minimize landfilling costs and turn to positive cash flow by developing a group of low and medium to high-value products. Precipitated Calcium Carbonate PCC is an example of a valuable product for paper industry. As a bonus, it binds  $CO_2$  and mitigates the carbon footprint of steel production.
- 8. Furthermore, on a wider scope, slags' comprehensive utilization results in significant energy saving and direct and indirect reduction of  $CO_2$  emissions. These issues, as well as the elimination of environmental and health risks, can be summarized by the phrase "turning threats into opportunities."

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#### Declarations

**Conflict of interest** The authors declared that they have no conflict of interest.

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