

Exact Solutions for an Unsteady Flow of Viscoelastic Fluid in Cylindrical Domains Using the Fractional Maxwell Model

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Abstract This paper deals with the unsteady flow of an incompressible fractional Maxwell fluid filled in the annular region between two infinite coaxial circular cylinders. The motion of the fluid is due to the inner cylinder that applies a time dependent torsional shear to the fluid and outer cylinder which is moving at a constant velocity. The velocity field and shear stress are determined by the Laplace and finite Hankel transforms. The obtained solutions are presented in terms of the generalized G and R functions. Solutions for Ordinary Maxwell fluid and Newtonian fluid are also obtained by imposing appropriate limits. Finally, the influence of different values of parameters, constants and fractional coefficient, as well as a comparison between the velocity field and shear stress are also analyzed using graphical illustration.

Keywords Velocity field · Shear stress · Fractional calculus · Hankel transform · Laplace transform

Introduction

Study of the fluid motion in cylindrical domains is not only of fundamental theoretical interest but it also has many applications in the food industry, oil exploitation, chemistry and bio-engineering.

The non-Newtonian fluids, such as lava, gums, slurries, emulsions, blood etc, are very frequently encountered in many different fields such as food industries, chemical engineering, biomedicine etc. and also are relevant to many other industrial processes. Hence, it is necessary to study the non-Newtonian fluid flows. Typical non-Newtonian characteristics include shear thinning, viscoelasticity, viscoplasticity and shear thickening behavior. Because of these complex behaviors, there are various models suggested in the literatures for non-

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Newtonian fluids such as rate type [1], differential type [2] and integral type. These fluids have non-linear relationship between shear stress and the rate of strain.

For non-Newtonian fluids, the first exact solutions corresponding to motion of second grade fluids in cylindrical domains seem to be those of [3]. Similarly, [4] and [5] proposed first exact solutions for Maxwell fluids and Oldroyd-B fluids respectively. The first exact solution for motion of non-Newtonian fluids that applies a constant shear stress to the fluid are those of [6] and [7] for second-grade fluids. Exact solutions for Taylor–Couette flow of a fractional second grade fluid in an annulus due to a time-dependent couple have been obtained by [8]. [9] worked on unsteady rotating flows of a viscoelastic fluid with the fractional Maxwell model between coaxial cylinders. The velocity field and the associated tangential stress corresponding to the rotational flow of a generalized second grade fluid within an infinite circular cylinder have been obtained by [10]. Various other studies have been done recently on non-Newtonian fluids [11–18].

Fractional calculus approach is very important in describing viscoelasticity [19–21]. The starting point of the fractional derivative model of viscoelastic fluid is usually a classical differential equation. This is being modified by replacing the time derivative of an integer order by the so-called Riemann–Liouville fractional calculus operators. Hence, many exact solutions for non-Newtonian fluids with fractional derivatives have been established [22–29] due to the importance of viscoelasticity.

The aim of this paper is to provide exact solutions for the velocity field and shear stress corresponding to the unsteady flow of an incompressible fractional Maxwell fluid in annular region between two infinitely long coaxial circular cylinders. At time $t = 0^+$, the inner cylinder applies a time dependent torsional shear to the fluid and outer cylinder is moving at a constant velocity. This solution is obtained using finite Hankel and Laplace transform methods and the result is presented in terms of the generalized-G and R functions. The solution of ordinary Maxwell fluids and Newtonian fluids are obtained by limiting cases of $\alpha \rightarrow 1$ and $\alpha \rightarrow 1, \lambda \rightarrow 0$ respectively.

Governing Equations

Let us consider an incompressible fractional Maxwell fluid with velocity V and extra stress S as in the form of

$$V = V(r, t) = w(r, t)e_\theta, \quad S = S(r, t), \quad (1)$$

where e_θ is the unit vector in the θ direction of the cylindrical coordinates.

At time $t = 0$, the fluid is at rest in an annular region between two infinite coaxial circular cylinders. At time $t = 0^+$, the inner cylinder applies a time dependent torsional shear to the fluid and outer cylinder is moving at a constant velocity. For these flows, the constraint of incompressibility is automatically satisfied. Initially the fluid is at rest, hence

$$V(r, 0) = 0, \quad S(r, 0) = 0. \quad (2)$$

For such flows the constraint of incompressibility is automatically satisfied, while the governing equations [30] are

$$(1 + \lambda D_t^\alpha) \frac{\partial w(r, t)}{\partial t} = \nu \left(\frac{\partial^2}{\partial r^2} + \frac{1}{r} \frac{\partial}{\partial r} - \frac{1}{r^2} \right) w(r, t), \quad r \in (R_1, R_2), t > 0, \quad (3)$$

$$(1 + \lambda D_t^\alpha) \tau(r, t) = \mu \left(\frac{\partial}{\partial r} - \frac{1}{r} \right) w(r, t), \quad r \in (R_1, R_2), t > 0, \quad (4)$$

where $\tau(r, t) = S_{r\theta}(r, t)$ is the non-trivial shear stress, λ is relaxation time, μ is the dynamic viscosity, ρ is the constant density of the fluid, $\nu = \frac{\mu}{\rho}$ is the kinematic viscosity and D_t^α is the Caputo fractional derivative of order α as defined by [31]

$$D_t^\alpha f(t) = \begin{cases} \frac{1}{\Gamma(1-\alpha)} \frac{d}{dt} \int_0^t \frac{f(\tau)}{(t-\tau)^\alpha} d\tau, & 0 \leq \alpha < 1; \\ \frac{d}{dt} f(t), & \alpha = 1, \end{cases} \tag{5}$$

where $\Gamma(\cdot)$ is the Gamma function.

For $\alpha \rightarrow 1$ when $D_t^\alpha f(t) \rightarrow df(t)/dt$, Eqs. (3) and (4) are reduced to the governing equations for an Ordinary Maxwell fluid.

Flow Through the Annular Region

Let us consider an incompressible fractional Maxwell fluid at rest in the annular region between two infinite coaxial circular cylinders. Also, consider that radius of inner and outer cylinders are R_1 and $R_2 (> R_1)$ respectively. At time $t = 0^+$, the outer cylinder moving at a constant velocity and the inner cylinder begins to rotate about its axis with a time dependent torque per unit length $2\pi R_1 \tau(R_1, t)$ [30], where

$$\tau(R_1, t) = \frac{f_1}{\lambda} R_{\alpha,-1} \left(-\frac{1}{\lambda}, t \right); \quad 0 < \alpha < 1, \tag{6}$$

where f_1 is a constant and generalized R functions are defined by [32]

$$R_{a,b}(d, t) = L^{-1} \left\{ \frac{q^b}{q^a - d} \right\} = \sum_{n=0}^{\infty} \frac{d^n t^{(n+1)a-b-1}}{\Gamma[(n+1)a-b]};$$

$$\text{Re}(a - b) > 0, \text{ Re}(q) > 0, \left| \frac{d}{q^a} \right| < 1. \tag{7}$$

The governing equations are given by Eqs. (3) and (4), while appropriate initial and boundary conditions are

$$w(r, 0) = \frac{\partial w(r, 0)}{\partial t} = 0, \quad \tau(r, 0) = 0, \quad r \in (R_1, R_2), \tag{8}$$

and

$$(1 + \lambda D_t^\alpha) \tau(r, t) \Big|_{r=R_1} = \mu \left(\frac{\partial}{\partial r} - \frac{1}{r} \right) w(r, t) \Big|_{r=R_1} = f_1,$$

$$w(R_2, t) = f_2, \quad t > 0, \tag{9}$$

where f_2 is the constant velocity of outer cylinder. Eq. (6) is the solution of Eq. (9). To solve this problem we use Laplace and Hankel transform methods.

Calculation of the Velocity Field

Applying Laplace transform of Eq. (3) and using the initial conditions as given in Eq. (8), we obtain

$$(q + \lambda q^{\alpha+1}) \bar{w}(r, q) = \nu \left(\frac{\partial^2}{\partial r^2} + \frac{1}{r} \frac{\partial}{\partial r} - \frac{1}{r^2} \right) \bar{w}(r, q), \quad r \in (R_1, R_2). \tag{10}$$

where $\bar{w}(r, q) = \int_0^\infty e^{-qt} w(r, t) dt$ is the Laplace transform of function $w(r, t)$ and q is the transform parameter.

Applying Laplace transform of Eq. (9), we obtain

$$\begin{aligned} \left(\frac{\partial}{\partial r} - \frac{1}{r}\right) \bar{w}(r, q) \Big|_{r=R_1} &= \frac{f_1}{\mu q}; \\ \bar{w}(R_2, q) &= \frac{f_2}{q}. \end{aligned} \tag{11}$$

The Hankel transform method with respect to r is used and defined as follows

$$\bar{w}_H(r_n, q) = \int_{R_1}^{R_2} r \bar{w}(r, q) B(r, r_n) dr, \tag{12}$$

where

$$B(r, r_n) = J_1(rr_n)Y_2(R_1r_n) - J_2(R_1r_n)Y_1(rr_n), \tag{13}$$

r_n being the positive roots of the transcendental equation $B(R_2, r) = 0$. The inverse Hankel transform as defined by [30], is given below

$$\bar{w}(r, q) = \frac{\pi^2}{2} \sum_{n=1}^\infty \frac{r_n^2 J_1^2(R_2r_n) B(r, r_n)}{J_2^2(R_1r_n) - J_1^2(R_2r_n)} \bar{w}_H(r_n, q). \tag{14}$$

Multiplying both sides of Eq. (10) by $rB(r, r_n)$, then integrating with respect to r from R_1 to R_2 and taking into account the conditions Eq. (11) and the equality

$$\begin{aligned} &\int_{R_1}^{R_2} r \left(\frac{\partial^2}{\partial r^2} + \frac{1}{r} \frac{\partial}{\partial r} - \frac{1}{r^2}\right) \bar{w}(r, q) B(r, r_n) dr \\ &= -r_n^2 \bar{w}_H(r_n, q) + \frac{2}{\pi r_n} \left(\frac{\partial}{\partial r} - \frac{1}{r}\right) \bar{w}(r, q) \Big|_{r=R_1} + R_2 r_n \bar{w}(R_2, q) [Y_2(R_1r_n) J_2(R_2r_n) \\ &\quad - J_2(R_1r_n) Y_2(R_2r_n)] \\ &= -r_n^2 \bar{w}_H(r_n, q) + \frac{2}{\pi r_n} \frac{f_1}{\mu q} + \frac{R_2 r_n f_2}{q} [Y_2(R_1r_n) J_2(R_2r_n) - J_2(R_1r_n) Y_2(R_2r_n)], \end{aligned} \tag{15}$$

we obtain

$$\begin{aligned} &\bar{w}_H(r_n, q) \\ &= \frac{2 f_1 v}{\pi \mu r_n} \frac{1}{q(q + \lambda q^{\alpha+1} + \nu r_n^2)} \\ &\quad + \nu R_2 r_n f_2 [Y_2(R_1r_n) J_2(R_2r_n) - J_2(R_1r_n) Y_2(R_2r_n)] \frac{1}{q(q + \lambda q^{\alpha+1} + \nu r_n^2)}. \end{aligned} \tag{16}$$

Rewriting Eq. (16) into a suitable equivalent form, we obtain below

$$\begin{aligned} &\bar{w}_H(r_n, q) \\ &= \frac{2f_1}{\pi\mu r_n^3} \frac{1}{q} - \frac{2f_1(1 + \lambda q^\alpha)}{\pi\mu r_n^3(q + \lambda q^{\alpha+1} + \nu r_n^2)} \\ &\quad + \frac{f_2 R_2}{r_n} [Y_2(R_1 r_n) J_2(R_2 r_n) - J_2(R_1 r_n) Y_2(R_2 r_n)] \left[\frac{1}{q} - \frac{(1 + \lambda q^\alpha)}{(q + \lambda q^{\alpha+1} + \nu r_n^2)} \right]. \end{aligned} \tag{17}$$

Applying inverse Hankel transform to Eq. (17) and taking into account the following result

$$\int_{R_1}^{R_2} (r^2 - R_2^2) B(r, r_n) dr = \frac{4}{\pi r_n^3} \left(\frac{R_2}{R_1} \right)^2, \tag{18}$$

we obtain

$$\begin{aligned} &\bar{w}(r, q) \\ &= \frac{f_1}{2\mu} \left(\frac{R_1}{R_2} \right)^2 \left(r - \frac{R_2^2}{r} \right) \frac{1}{q} - \frac{\pi f_1}{\mu} \sum_{n=1}^{\infty} \frac{J_1^2(R_2 r_n) B(r, r_n)}{r_n [J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} \frac{(1 + \lambda q^\alpha)}{(q + \lambda q^{\alpha+1} + \nu r_n^2)} \\ &\quad + \frac{\pi^2}{2} R_2 f_2 \sum_{n=1}^{\infty} \frac{r_n J_1^2(R_2 r_n) B(r, r_n)}{[J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} [Y_2(R_1 r_n) J_2(R_2 r_n) - J_2(R_1 r_n) Y_2(R_2 r_n)] \\ &\quad \times \left[\frac{1}{q} - \frac{(1 + \lambda q^\alpha)}{(q + \lambda q^{\alpha+1} + \nu r_n^2)} \right]. \end{aligned} \tag{19}$$

Applying Inverse-Laplace transform of Eq. (19) and taking into account the following result [32]

$$\begin{aligned} G_{a,b,c}(d, t) &= L^{-1} \left\{ \frac{q^b}{(q^a - d)^c} \right\} \\ &= \sum_{j=0}^{\infty} \frac{d^j \Gamma(c + j)}{\Gamma(c) \Gamma(j + 1)} \frac{t^{(c+j)a-b-1}}{\Gamma[(c + j)a - b]}; \\ &\quad \text{Re}(ac - b) > 0, \text{Re}(q) > 0, \left| \frac{d}{q^a} \right| < 1, \end{aligned} \tag{20}$$

we obtain

$$\begin{aligned} &w(r, t) \\ &= \frac{f_1}{2\mu} \left(\frac{R_1}{R_2} \right)^2 \left(r - \frac{R_2^2}{r} \right) - \frac{\pi f_1}{\mu \lambda} \sum_{n=1}^{\infty} \frac{J_1^2(R_2 r_n) B(r, r_n)}{r_n [J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} \sum_{k=0}^{\infty} \left(\frac{-\nu r_n^2}{\lambda} \right)^k \\ &\quad \times [G_{\alpha, -k-1, k+1}(-\lambda^{-1}, t) + \lambda G_{\alpha, \alpha-k-1, k+1}(-\lambda^{-1}, t)] \\ &\quad + \frac{\pi^2}{2} R_2 f_2 \sum_{n=1}^{\infty} \frac{r_n J_1^2(R_2 r_n) B(r, r_n)}{[J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} [Y_2(R_1 r_n) J_2(R_2 r_n) - J_2(R_1 r_n) Y_2(R_2 r_n)] \\ &\quad \times \left[1 - \frac{1}{\lambda} \sum_{k=0}^{\infty} \left(\frac{-\nu r_n^2}{\lambda} \right)^k \{ G_{\alpha, -k-1, k+1}(-\lambda^{-1}, t) + \lambda G_{\alpha, \alpha-k-1, k+1}(-\lambda^{-1}, t) \} \right]. \end{aligned} \tag{21}$$

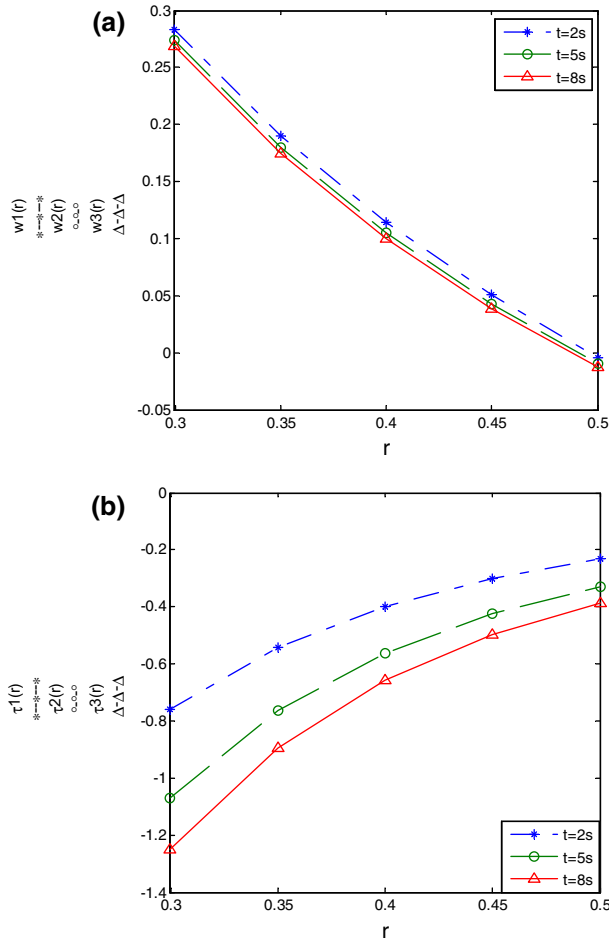


Fig. 1 Profiles of the velocity $w(r,t)$ and shear stress $\tau(r,t)$ given by Eqs. (21) and (25) for $R_1 = 0.3, R_2 = 0.5, f_1 = -3, f_2 = -2, \nu = 0.015, \mu = 1.01, \lambda = 5, \alpha = 0.5$ and different values of t

Calculation of the shear stress

Applying Laplace transform to Eq. (4), we obtain

$$\bar{\tau}(r, q) = \mu \frac{1}{(1 + \lambda q^\alpha)} \left(\frac{\partial}{\partial r} - \frac{1}{r} \right) \bar{w}(r, q). \tag{22}$$

Substitute Eq. (19) in Eq. (22), we obtain

$$\begin{aligned} \bar{\tau}(r, q) = & f_1 \left(\frac{R_1}{r} \right)^2 \frac{1}{q(1 + \lambda q^\alpha)} + \pi f_1 \sum_{n=1}^{\infty} \frac{J_1^2(R_2 r_n) \bar{B}(r, r_n)}{[J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} \frac{1}{(q + \lambda q^{\alpha+1} + \nu r_n^2)} \\ & - \frac{\pi^2}{2} \mu R_2 f_2 \sum_{n=1}^{\infty} \frac{r_n^2 J_1^2(R_2 r_n) \bar{B}(r, r_n)}{[J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} [Y_2(R_1 r_n) J_2(R_2 r_n)] \end{aligned}$$

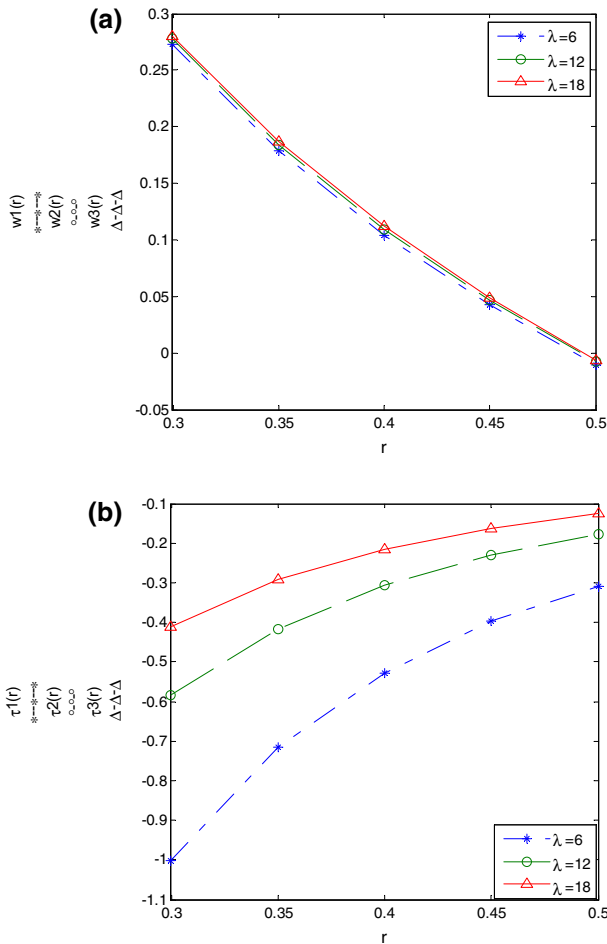


Fig. 2 Profiles of the velocity $w(r,t)$ and shear stress $\tau(r,t)$ given by Eqs. (21) and (25) for $R_1 = 0.3, R_2 = 0.5, f_1 = -3, f_2 = -2, t = 6s, \nu = 0.015, \mu = 1.01, \alpha = 0.5$ and different values of λ

$$-J_2(R_1 r_n) Y_2(R_2 r_n)] \times \left[\frac{1}{q(1 + \lambda q^\alpha)} - \frac{1}{(q + \lambda q^{\alpha+1} + \nu r_n^2)} \right], \tag{23}$$

where

$$\bar{B}(r, r_n) = J_2(r r_n) Y_2(R_1 r_n) - J_2(R_1 r_n) Y_2(r r_n). \tag{24}$$

Applying inverse Laplace transform to Eq. (23) and using Eq. (20), we obtain

$$\tau(r, t) = f_1 \left(\frac{R_1}{r} \right)^2 \frac{1}{\lambda} R_{\alpha, -1}(-\lambda^{-1}, t) + \frac{\pi f_1}{\lambda} \sum_{n=1}^{\infty} \frac{J_1^2(R_2 r_n) \bar{B}(r, r_n)}{[J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} \sum_{k=0}^{\infty} \left(\frac{-\nu r_n^2}{\lambda} \right)^k G_{\alpha, -k-1, k+1}(-\lambda^{-1}, t)$$

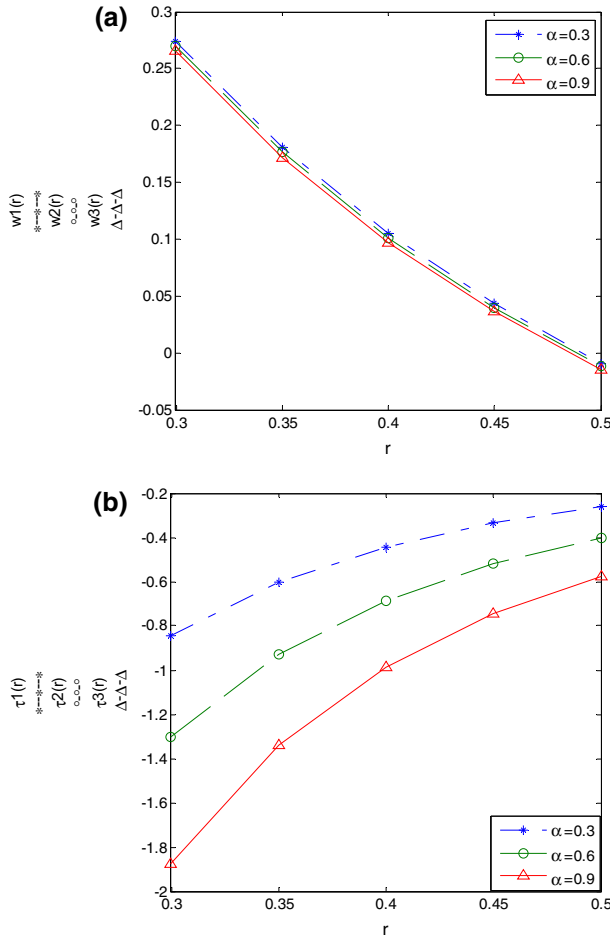


Fig. 3 Profiles of the velocity $w(r,t)$ and shear stress $\tau(r,t)$ given by Eqs. (21) and (25) for $R_1 = 0.3, R_2 = 0.5, f_1 = -3, f_2 = -2, t = 6s, \nu = 0.015, \mu = 1.01, \lambda = 5$ and different values of α

$$\begin{aligned}
 & -\frac{\pi^2}{2} \frac{\mu R_2 f_2}{\lambda} \sum_{n=1}^{\infty} \frac{r_n^2 J_1^2(R_2 r_n) \bar{B}(r, r_n)}{[J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} \\
 & [Y_2(R_1 r_n) J_2(R_2 r_n) - J_2(R_1 r_n) Y_2(R_2 r_n)] \\
 & \times \left[R_{\alpha, -1}(-\lambda^{-1}, t) - \sum_{k=0}^{\infty} \left(\frac{-\nu r_n^2}{\lambda} \right)^k G_{\alpha, -k-1, k+1}(-\lambda^{-1}, t) \right]. \tag{25}
 \end{aligned}$$

Limiting Cases

Ordinary Maxwell Fluid

Applying $\alpha \rightarrow 1$ into Eqs. (21) and (25), we obtain the velocity field

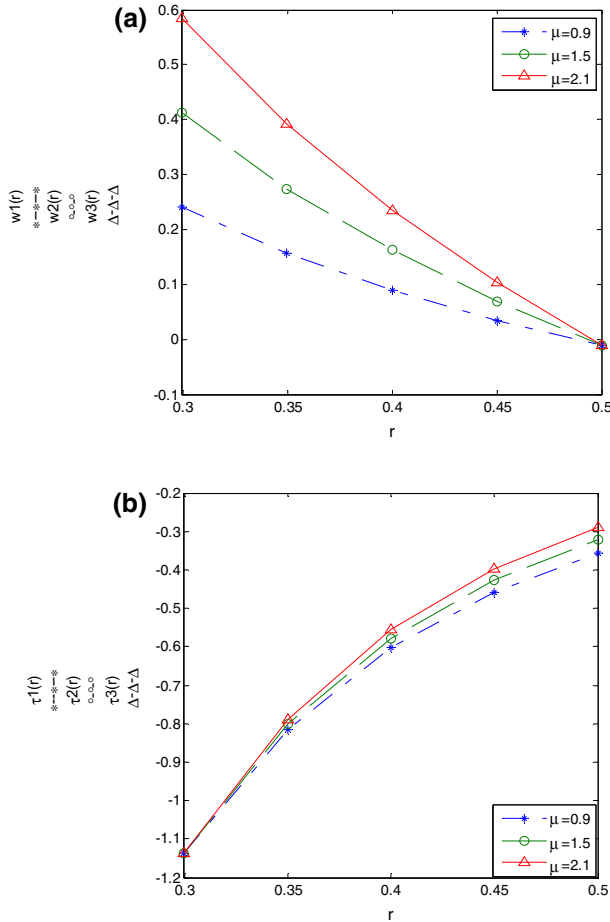


Fig. 4 Profiles of the velocity $w(r,t)$ and shear stress $\tau(r, t)$ given by Eqs. (21) and (25) for $R_1 = 0.3, R_2 = 0.5, f_1 = -3, f_2 = -2, t = 6s, \nu = 0.015, \lambda = 5, \alpha = 0.5$ and different values of μ

$$\begin{aligned}
 &w_M(r, t) \\
 &= \frac{f_1}{2\mu} \left(\frac{R_1}{R_2}\right)^2 \left(r - \frac{R_2^2}{r}\right) - \frac{\pi f_1}{\mu\lambda} \sum_{n=1}^{\infty} \frac{J_1^2(R_2 r_n) B(r, r_n)}{r_n [J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} \sum_{k=0}^{\infty} \left(\frac{-\nu r_n^2}{\lambda}\right)^k \\
 &\quad \times [G_{1,-k-1,k+1}(-\lambda^{-1}, t) + \lambda G_{1,-k,k+1}(-\lambda^{-1}, t)] \\
 &\quad + \frac{\pi^2}{2} R_2 f_2 \sum_{n=1}^{\infty} \frac{r_n J_1^2(R_2 r_n) B(r, r_n)}{[J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} [Y_2(R_1 r_n) J_2(R_2 r_n) - J_2(R_1 r_n) Y_2(R_2 r_n)] \\
 &\quad \times \left[1 - \frac{1}{\lambda} \sum_{k=0}^{\infty} \left(\frac{-\nu r_n^2}{\lambda}\right)^k \{G_{1,-k-1,k+1}(-\lambda^{-1}, t) + \lambda G_{1,-k,k+1}(-\lambda^{-1}, t)\}\right], \quad (26)
 \end{aligned}$$

and its associated shear stress corresponding to ordinary Maxwell fluid performing the same motion

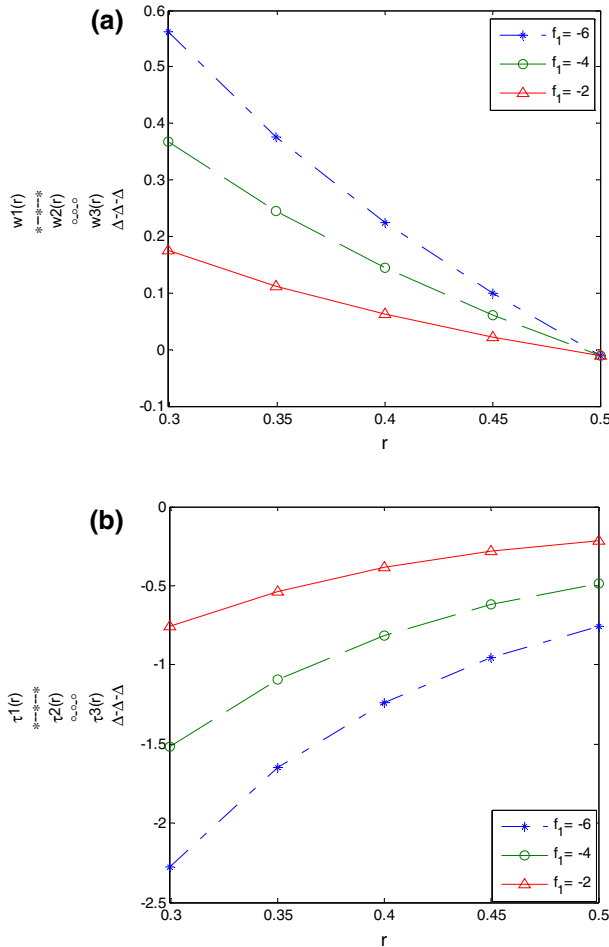


Fig. 5 Profiles of the velocity $w(r,t)$ and shear stress $\tau(r,t)$ given by Eqs. (21) and (25) for $R_1 = 0.3, R_2 = 0.5, f_2 = -2, t = 6s, v = 0.015, \mu = 1.01, \lambda = 5, \alpha = 0.5$ and different values of f_1

$$\begin{aligned}
 \tau_M(r, t) &= f_1 \left(\frac{R_1}{r} \right)^2 (1 - e^{-t/\lambda}) \\
 &+ \frac{\pi f_1}{\lambda} \sum_{n=1}^{\infty} \frac{J_1^2(R_2 r_n) \bar{B}(r, r_n)}{[J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} \sum_{k=0}^{\infty} \left(\frac{-v r_n^2}{\lambda} \right)^k G_{1,-k-1,k+1}(-\lambda^{-1}, t) \\
 &- \frac{\pi^2}{2} \frac{\mu R_2 f_2}{\lambda} \sum_{n=1}^{\infty} \frac{r_n^2 J_1^2(R_2 r_n) \bar{B}(r, r_n)}{[J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} [Y_2(R_1 r_n) J_2(R_2 r_n) \\
 &- J_2(R_1 r_n) Y_2(R_2 r_n)] \\
 &\times \left[\lambda (1 - e^{-t/\lambda}) - \sum_{k=0}^{\infty} \left(\frac{-v r_n^2}{\lambda} \right)^k G_{1,-k-1,k+1}(-\lambda^{-1}, t) \right]. \tag{27}
 \end{aligned}$$

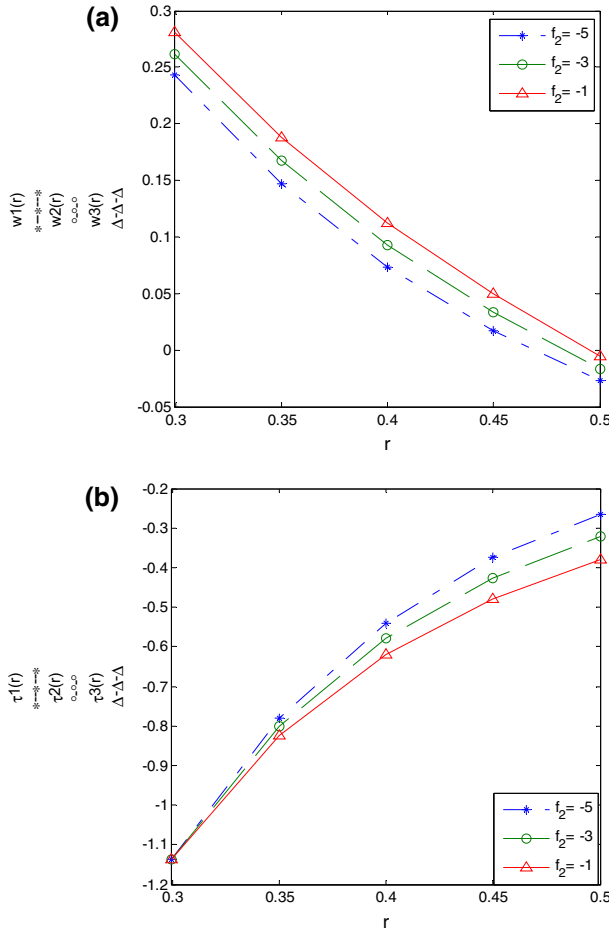


Fig. 6 Profiles of the velocity $w(r,t)$ and shear stress $\tau(r,t)$ given by Eqs. (21) and (25) for $R_1 = 0.3, R_2 = 0.5, f_1 = -3, t = 6s, \nu = 0.015, \mu = 1.01, \lambda = 5, \alpha = 0.5$ and different values of f_2

Newtonian Fluid

Applying $\lambda \rightarrow 0$ into Eqs. (26) and (27) and taking into account the following result

$$\lim_{\lambda \rightarrow 0} \frac{1}{\lambda^m} G_{1,b,m}(-\lambda^{-1}, t) = \frac{t^{-b-1}}{\Gamma(-b)}, \quad b < 0,$$

we obtain the corresponding solutions for the Newtonian fluid, as follows

$$\begin{aligned} w_N(r, t) = & \frac{f_1}{2\mu} \left(\frac{R_1}{R_2} \right)^2 \left(r - \frac{R_2}{r} \right) - \frac{\pi f_1}{\mu} \sum_{n=1}^{\infty} \frac{J_1^2(R_2 r_n) B(r, r_n)}{r_n [J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} e^{-\nu r_n^2 t} \\ & + \frac{\pi^2}{2} R_2 f_2 \sum_{n=1}^{\infty} \frac{r_n J_1^2(R_2 r_n) B(r, r_n)}{[J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} [Y_2(R_1 r_n) J_2(R_2 r_n) \\ & - J_2(R_1 r_n) Y_2(R_2 r_n)] \left(1 - e^{-\nu r_n^2 t} \right), \end{aligned} \tag{28}$$

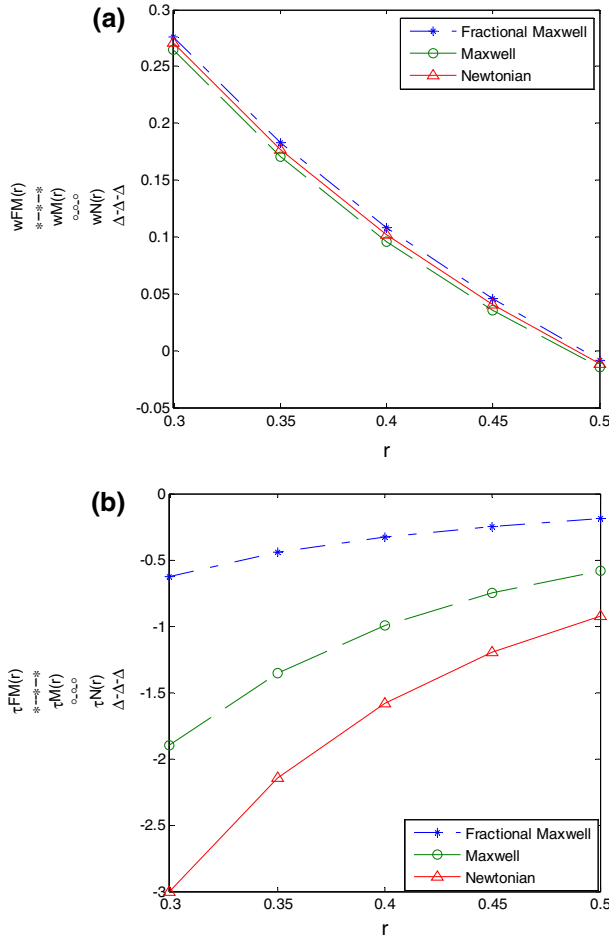


Fig. 7 Profiles of the velocity $w(r,t)$ and shear stress $\tau(r,t)$ corresponding to the Fractional Maxwell , ordinary Maxwell and Newtonian fluids, for $R_1 = 0.3, R_2 = 0.5, f_1 = -3, f_2 = -2, t = 6 \text{ s}, \nu = 0.015, \mu = 1.01, \lambda = 6$ and $\alpha = 0.2$

and

$$\begin{aligned}
 \tau_N(r, t) = & f_1 \left(\frac{R_1}{r} \right)^2 + \pi f_1 \sum_{n=1}^{\infty} \frac{J_1^2(R_2 r_n) \bar{B}(r, r_n)}{[J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} e^{-\nu r_n^2 t} \\
 & - \frac{\pi^2}{2} \mu R_2 f_2 \sum_{n=1}^{\infty} \frac{r_n^2 J_1^2(R_2 r_n) \bar{B}(r, r_n)}{[J_2^2(R_1 r_n) - J_1^2(R_2 r_n)]} [Y_2(R_1 r_n) J_2(R_2 r_n) \\
 & - J_2(R_1 r_n) Y_2(R_2 r_n)] \left(1 - e^{-\nu r_n^2 t} \right). \tag{29}
 \end{aligned}$$

Conclusions and Numerical Results

The purpose of this paper is to establish exact solutions for the velocity field and shear stress corresponding to the unsteady flow of an incompressible fractional Maxwell fluid flow

in the annular region. Where, the motion is produced by the inner cylinder that applies a time dependent torsional shear to the fluid and outer cylinder which is moving at a constant velocity. The solution is obtained by finite Hankel and Laplace transform methods and the result is presented under series form in terms of the generalized G and R functions. The similar solutions for Ordinary Maxwell and Newtonian fluids are also obtained as limiting cases of the solution for fractional Maxwell fluid. The velocity field and shear stress are also analyzed using graphical illustration for various parameters, constants and fractional coefficients and a comparison between models of the velocity field and shear stress are also analyzed using graphical illustration.

As shown in below diagrams, the velocity $w(r, t)$ and the shear stress $\tau(r, t)$ given by Eqs. (21) and (25) have been drawn against r for different values of the time t , f_1 , f_2 and other relevant parameters. It can be clearly seen from the figures that the velocity component w is decreasing function of r and the shear stress component τ is increasing function of r . The motion of the fluid is relatively higher and shear stress lower in the neighborhood of the inner cylinder for given boundary conditions and $f_1 < 0$, $f_2 < 0$. Figures 1a and b are showing the effect of different values of time on the fluid motion. It can be seen that the velocity and the shear stress are the decreasing function of time t . The influence of relaxation time λ and fractional parameter α on the fluid motion is shown in Figs. 2 and 3. Both parameters have opposite effect on the fluid motion. The velocity and the shear stress are increasing function of λ and decreasing function of α . Figures 4a and b are showing the effect of different values of dynamic viscosity on the fluid motion. The results indicate that the velocity and the shear stress are increasing function of dynamic viscosity. Figures 5 and 6 are showing the behavior of f_1 and f_2 on the fluid motion for their different values. Figure 7 is showing a comparison diagram of the velocity $w(r, t)$ and the shear stress $\tau(r, t)$ among three models (Fractional Maxwell fluid, Ordinary Maxwell fluid and Newtonian fluid) for same values of the common material constants and time t . The velocity in the neighborhood of inner cylinders is swiftest for fractional Maxwell fluid while it is slowest for the Ordinary Maxwell fluid. Similarly, shear stress on the whole flow domains highest for fractional Maxwell fluid while it is slowest for the Newtonian fluid.

In all of above, the root r_n has been approximated by $\frac{(2n-1)\pi}{2(R_2-R_1)}$.

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