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# Adsorption and corrosion inhibitive properties of P(2-aminobenzothiazole) on mild steel in hydrochloric acid media

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Abstract Corrosion inhibition of mild steel in hydrochloric acid solutions using electropolymerized Poly 2-aminobenzothiazole, P(2ABT), was evaluated using weight loss, potentiodynamic polarization and electrochemical impedance spectroscopy measurements at different temperature. Results showed that the inhibition efficiency increases with increasing the concentration of P(2ABT) up to  $12.7 \times 10^{-6}$  mol L<sup>-1</sup> and decreases with raising the temperature. Polarization curves indicate that the studied compound acts as anodic inhibitor. Thermodynamic activation parameters for both dissolution and adsorption processes are calculated and discussed as well as the adsorption isotherms are calculated. Gibbs free energy value confirms the physical nature of the adsorption, also the mechanism of inhibition is discussed. Scanning electron microscopy is used to study the surface morphology of mild steel in hydrochloric acid solution in the absence and presence of  $12.7 \times 10^{-6} \text{ mol L}^{-1}$ P(2ABT). Data obtained from all techniques are in a good agreement with each other.

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**Keywords** Polymer · Corrosion inhibition · EIS · Mild steel · Adsorption isotherms

# Introduction

The corrosion of metals, including mild steel, is a serious problem in many industries, especially during processes such as the pickling of steel, acid washing and etching [1, 2]. Corrosion inhibitors are chemical compounds that in small quantities can use in these processes to control the metal dissolutions. Most popular inhibitors are organic compound containing N, S, and O atoms. Organic compounds containing functional electronegative groups and  $\pi$  electrons in triple or conjugated double bonds are usually good inhibitors. The study of corrosion process and their inhibition by organic compounds is a very active field of research [3–5].

Benzothiazole and its derivatives are considered as one of the suitable compounds that be used as inhibitors due to it has donor atoms (N and S) via which bonding with metal ions can occur to form heterocyclic ring-metal complexes. These compounds are used as antioxidant, rust inhibitors and metal de-activators [6–9]. Aminothiazole derivatives have several useful properties like anti-corrosive [10], antimicrobial [11], antitumor activities [12] and used in sensing applications [13, 14].

Recently polymers have attracted considerable attention as corrosion inhibitors, and their inhibiting power is related structurally to the cyclic rings and hetero-atom (O, N and S) that are the major active centers of adsorption. A blanketing and protecting of the metal surface from corrosive agents present in the solution occurs via their functional groups which form complexes with metal ions [15].



2-Aminothiazole has been polymerized both electrochemically [16–18] and chemically [19]. Homopolymers [20] and copolymers [21] of 2-aminobenzothiazole had been prepared by electropolymerization method. 2ABT [21] and other thiazole derivatives [22, 23] are used as a corrosion inhibitor for mild steel (MS) in HCl using different techniques, results show the inhibiting effect is due to adsorption of thiazols on MS surface.

The goal of this work is to investigate the electropolymerized P(2ABT) as a corrosion inhibitor for the acidic dissolution of mild steel in hydrochloric solution using weight loss, potentiodynamic polarization and electrochemical impedance spectroscopy measurements at different temperatures as well as thermodynamic activation parameters for both dissolution and adsorption processes will be calculated and discussed.

#### Experimental

# Chemicals

2-Aminobenzothiazole, HCl, Na<sub>2</sub>SO<sub>4</sub>, DMF are of grade reagent obtained from (Merck-Darmstadt, Germany). Poly 2-aminobenzothiazole P(2ABT) is prepared according to our previous work [20] and its structure is represented in Scheme 1.

### Methodology

#### Weight loss measurements

Rectangular specimens of mild steel (MS), (wt%: 0.33 % C, 0.24 % Si, 0.52 % Mn, 0.04 %, Cr 0.02 % S and 98.5 % Fe) with size 3 cm × 4 cm × 0.2 cm were used as working electrode. Before each experiment, working electrodes are polished mechanically with SiC belts, 200–600 grit (Buehler, Ltd.), and 1  $\mu$ m  $\alpha$ -alumina (Buehler, Ltd.), washed with distilled water, then with acetone and dried. The weight loss, expressed in mg cm<sup>-2</sup>, was determined by weighing the cleaned MS samples before and after immersion in HCl solution for 1 h in the absence and presence of various concentrations (2.1 × 10<sup>-6</sup>: 12.7 × 10<sup>-6</sup> mol/L) (H<sub>2</sub>O/DMF 98:2, v/v) of P(2ABT).

#### Potentiodynamic polarization measurements

Potentiodynamic polarization measurements are recorded using potentiostat/galvanostat Wenking PGS 95 connected with PC computer and performed in standard three electrode cell filled with 100 ml test solution with mild steel  $(2 \text{ cm}^{-2})$  as working electrode, platinum wire as an auxiliary electrode and saturated calomel electrode as a reference electrode. Before each experiment, working electrode is polished with different emery paper in the normal way starting from coarse to fine, cleaned with distilled water, then with acetone and finally dried and *I*– *E* curves are recorded by computer software (Model ECT). For each experiment, a freshly prepared solution as well as a cleaned set of electrodes is used at constant temperature  $\pm 1^{\circ}$  C using a circular water thermostat.

#### Electrochemical impedance spectroscopy measurements

Electrochemical impedance spectroscopy measurements are carried out on the open circuit potential ( $E_{ocp}$ ), using a computer-controlled potentiostat (Voltalab). A frequency range of 100 kHz–100 MHz is used to obtain the impedance spectra after 1 h of immersion in the test solutions. A sine wave with 10 mV amplitude was used to perturb the system. The impedance diagrams are given in the Nyquist representation.

### Surface morphology

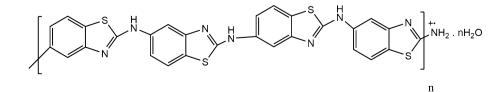
The surface morphology of mild steel after 1 h of immersion in 1 M HCl solution in the absence and presence of  $12.7 \times 10^{-6}$  mol L<sup>-1</sup> P(2ABT) at constant temperature  $\pm 1^{\circ}$  C is investigated using scanning electron microscopy model JXA-840A Electron Probe Microanalyzer (JEOL, Tokyo, Japan).

# **Results and discussion**

#### **Preparation and characterization**

Electrooxidation of  $1 \times 10^{-3}$  M 2ABT in 0.05 M Na<sub>2</sub>SO<sub>4</sub> and 0.3 M HCl at 309 K yield a good adhere P(2ABT) on the Pt-electrode, the obtained voltammogram is represented on Fig. 1 with two oxidation peaks (I and II) that

Scheme 1 Proposed structure of electropolymerized P(2ABT)





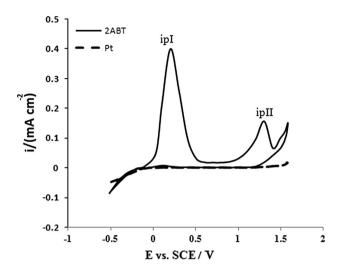


Fig. 1 Cyclic voltammogram of Pt-electrode from solution containing 0.3 M HCl and 0.05 M Na<sub>2</sub>SO<sub>4</sub> at 309 K with scan rate of  $25 \text{ mVs}^{-1}$  in absence and presence of  $1 \times 10^{-3} \text{ M 2ABT}$ 

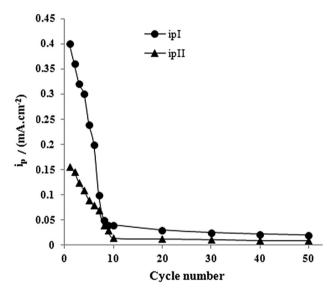


Fig. 2 Effect of number of cycles on the value of anodic current peaks I and II  $\,$ 

developed in +200 and +1322 mV vs. (SCE) and no reduction peaks.

By increasing the number of cycles, the anodic current of both peaks decrease up to 50 cycles reflect the enhances of the deposited film stability and, therefore, the peak currents (I and II) decrease with repetitive cycling [21] as shown in Fig. 2.

By changing the scan rate both  $i_{pI}$  and  $i_{pII}$  increase as in Fig. 3 with linear regression equations:

$$i_{\rm pI}({\rm mA}) = 0.149 v^{0.5} ({\rm mV s}^{-1})^{0.5} - 0.2499, r^2 = 0.991$$
  
 $i_{\rm pII}({\rm mA}) = 0.010 v^{0.5} ({\rm mV s}^{-1})^{0.5} - 0.2476, r^2 = 0.988$ 

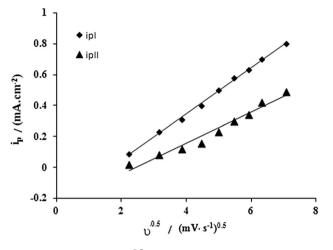


Fig. 3 Effect of (scan rate)  $^{0.5}$  on the value of anodic current peaks I and II

Both the two intercepts are small and negative which could be attributed to a decrease of the active area during the positive scan and the whole process is a partial diffusion process.

UV-vis spectra of the prepared polymer sample were measured using Shimadzu UV spectrophotometer (M160 PC) at room temperature in the range 200–900 nm using dimethyl-formamide as a solvent and reference. Spectra show the following;

- $\pi \pi^*$  transition at  $\lambda_{max}$  from 208 to 220 nm;
- polaron– $\pi^*$  transition at  $\lambda_{max} = 315$  nm and;
- $\pi$ -polaron transition at  $\lambda_{max} = 463$  nm.

IR measurements were carried out using Shimadzu FTIR-340 Jasco spectrophotometer (Japan) and show the following main bands:

- v<sub>max</sub> = 3402 cm<sup>-1</sup> for NH<sub>2</sub> stretching vibration or OH strong hydrogen bonded group of H<sub>2</sub>O molecules of hydration in P(2ABT);
- $v_{\text{max}} = 3064 \text{ cm}^{-1}$  for CH stretching vibration of aromatic amine;
- $v_{\text{max}} = 1550 \text{ cm}^{-1}$  for C=N stretching vibration;
- $v_{\text{max}} = 760 \text{ cm}^{-1}$  for C=N stretching vibration in quinonoid form;
- $v_{\text{max}} = 618 \text{ cm}^{-1}$  for C–S symmetric stretching vibration;
- $v_{\text{max}} = 721$  and 760 cm<sup>-1</sup> for C–S asymmetric stretching vibration.

From these methods, formation of P(2ABT) is confirmed [21].

The obtained P(2ABT) films were scratched from the Ptelectrode surface, washed with 0.3 M HCl to remove low molecular weight species and finally with double distilled water and left to dry at 90 C for 3 h then stored under vacuum until further studies.



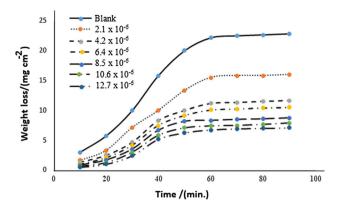


Fig. 4 Weight loss-time curves for MS in 1 M HCl in the absence and presence of different concentrations of P(2ABT) at 303 K

The solubility of the collected P(2ABT) was studied to find the suitable solvent to dissolve it, P(2ABT) did not dissolve completely in water, partially soluble in chloroform and acetone, but dissolve completely in DMF, DMSO and THF.

To prepare our inhibitor, a weighted amount of P(2ABT) was dissolved in 2 ml DMF and complete volume with water to form a mix solution [DMF:  $H_2O$  mix (2:98 v/v)]. The formed stock solution has a known concentration from which all used concentrations are taken via dilution.

#### Weight loss measurements

### Effect of time

The variation of weight loss per area  $(mg \text{ cm}^{-2})$  of MS immersed in different time intervals up to 90 min in 1 M HCl solution at 303 K in the absence and presence of P(2ABT) is shown in Fig. 4. From the Figure, we notice that, the corrosion rate of MS coupons in free inhibitor solution increases with increasing the time up to 60 min, then begin to be mostly stable. By increasing the inhibitor concentrations, weight loss of MS in case of inhibitor solutions is lower that of free inhibitor solution in the same period of time. This behavior may be explained by the ability of the investigated compound to be used as an inhibitor through adsorption on MS surface and forming a barrier against the corrosive medium.

#### Effect of HCl concentration

The variety of weight loss (mg) and the corrosion rate, CR, (mg cm<sup>-2</sup> h<sup>-1</sup>) of MS immersed for 1 h in 0.5, 1.0 and 2.0 M HCl aerated stagnant solutions with and without various concentrations (from  $2.1 \times 10^{-6}$  to  $12.7 \times 10^{-6}$  M) of P(2ABT) at 303 K are calculated. The inhibition efficiency (%IE) values are calculated using Eq. (1) for MS in HCl acid solutions containing various concentrations of the P(2ABT). The calculated values of %IE are given in Table 1 and graphically represented in Fig. 5.

$$\text{IE\%} = \left(1 - \frac{W}{W^\circ}\right) \times 100\tag{1}$$

where  $W^{\circ}$  and W are the weight losses (g) for MS in the absence and presence of inhibitor.

From these data, the weight loss and the corrosion rate of MS electrode enhance with increasing the acid concentrations. On the other hand, addition of different concentrations of P(2ABT) inhibits the corrosion rate of MS in these solutions. This is clearly seen from the decrease in weight loss corresponding to a noticeable decrease in the corrosion rate in each acid concentration with an increase in the polymer concentrations. This trend may result from the fact that adsorption and surface coverage,  $\theta$ , increases with the increase in P(2ABT) concentration; thus the MS surface is separated from the corrosive medium.

The use of P(2ABT) gives %IE  $\approx 65$  to 71 % for concentration 15 ppm (12.7  $\times 10^{-6}$  mol L<sup>-1</sup>), which is better than that of the monomer (2ABT) which gives %IE  $\approx 67$  % for concentration of 50 ppm [22].

Figure 5 shows the variation of the calculated inhibition efficiency (%IE), values as a function of logarithmic concentration of the inhibitor. It is obvious from the data of Fig. 5

**Table 1** Weight loss, corrosion rate of MS and inhibition efficiency %IE of various concentrations of P(2ABT) in 0.5, 1.0 and 2.0 M HCl at303 K

P(2ABT) conc. $\times 10^{-6}$ (M)	Weight loss (mg)			Corrosion rate (mg cm <sup><math>-2</math></sup> h <sup><math>-1</math></sup> )			%IE		
	0.5 M	1.0 M	2.0 M	0.5 M	1.0 M	2.0 M	0.5 M	1.0 M	2.0 M
Blank	229.62	266.34	296.40	20.32	23.57	26.23	_	_	_
2.1	154.69	186.58	216.63	13.81	16.66	19.34	32.03	29.32	26.26
4.2	110.70	134.55	157.70	9.888	12.014	14.08	51.36	49.03	46.32
6.4	101.98	121.11	143.54	9.10	10.814	12.81	55.19	54.12	51.14
8.5	81.72	100.23	129.32	7.30	8.95	11.55	64.09	62.03	55.98
10.6	72.034	89.62	111.60	6.43	8.00	9.96	68.35	66.05	62.01
12.7	65.70	81.52	102.47	5.874	7.28	9.15	71.13	69.12	65.12



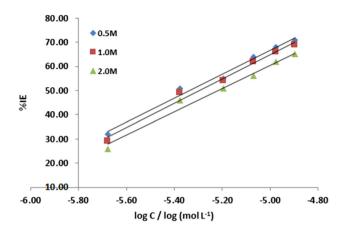


Fig. 5 The relation between %IE and log the concentration of P(2ABT) in different HCl concentrations at 303 K from weight loss technique

that, the inhibition efficiency increases with increasing the concentrations of the inhibitor. Moreover, it is found that at a given inhibitor concentration, the inhibition efficiency decreases in general with increasing the acid concentration.

# Effect of temperature

The influence of solution temperature (298, 303 and 308 K) on the weight loss and consequently the corrosion rate, CR, of the MS electrode in 1.0 M HCl solution in the absence and presence of different concentrations of P(2ABT) were investigated. The immersion time of each experiment is 1 h. The values of weight loss (mg) and corrosion rate (mg cm<sup>-2</sup> h<sup>-1</sup>) are given in Table 2.

It is clear from the data that in the absence of the P(2ABT), the weight loss and consequently the corrosion rate of MS increase by raising the temperature, and decrease with increasing P(2ABT) concentrations.

The inhibition efficiencies (%IE) are calculated using Eq. (1) and are listed in Table 2.

Figure 6 represents the dependence of the inhibition efficiency (%IE) versus logarithmic the P(2ABT) concentrations in the three tested temperatures. According to

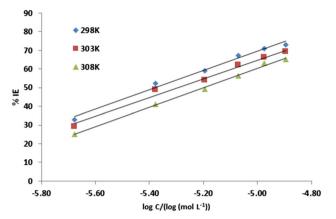


Fig. 6 The relation between %IE and log the concentration of P(2ABT) in 1.0 M HCl at 298, 303 and 308 K from weight loss technique

these data, it is seen that the inhibition efficiencies decrease with increasing the solution temperature. Such behavior could be due to the increases in the corrosion rate of MS and/or increasing the rate of desorption of P(2ABT) from the surface of MS with increasing temperature indicating that the inhibitor species are mainly physically adsorbed on the MS electrode surface.

#### Potentiodynamic polarization measurements

The potentiodynamic polarization behavior of MS electrode in 1.0 M HCl in the absence and presence of different concentrations of P(2ABT) with a scan rate of 10 mVs<sup>-1</sup> at 298, 303 and 308 K is illustrated in Fig. 7.

As can be seen from the figure, the anodic and cathodic overpotentials are increased (mainly the anodic) in the presence of P(2ABT), meaning that the addition of P(2ABT) to HCl solution mainly reduces the anodic dissolution of MS and slightly retards the cathodic hydrogen evolution reaction. Based on this result, P(2ABT) is considerable, mainly acting as anodic inhibitor. The values of the corrosion current density,  $i_{corr}$ , and corrosion potential,

**Table 2** Weight loss, corrosion rate of MS in 1.0 M HCl containing various concentrations of P(2ABT) and inhibition efficiency %IE at 298,303 and 308 K

P(2ABT) conc. $\times 10^{-6}$ (M)	Weight loss (mg)			Corrosion rate (mg cm <sup><math>-2</math></sup> h <sup><math>-1</math></sup> )			%IE			
	298 K	303 K	308 K	298 K	303 K	308 K	298 K	303 K	308 K	
Blank	240.92	266.34	283.86	21.32	23.57	25.12	_	_	_	
2.1	159.96	186.58	210.98	14.28	16.66	18.84	33.01	29.32	25.01	
4.2	159.96	186.58	210.98	10.21	12.01	14.79	52.12	49.03	41.12	
6.4	114.34	134.55	165.65	8.73	10.81	12.73	59.03	54.12	49.32	
8.5	97.83	121.11	142.58	7.01	8.96	11.01	67.12	62.03	56.18	
10.6	78.51	100.23	123.28	6.18	8.00	9.27	71.02	66.05	63.08	
12.7	69.20	89.62	103.87	5.73	7.28	8.76	73.12	69.12	65.13	



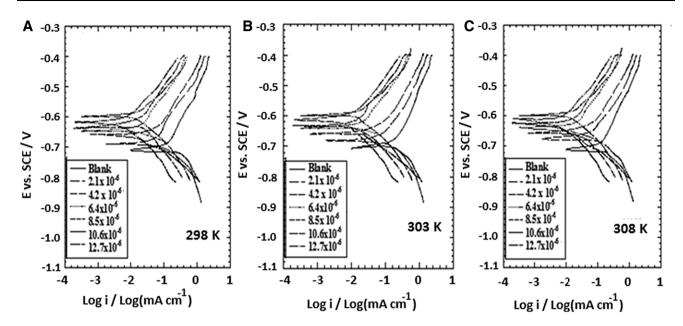


Fig. 7 Effect of P(2ABT) concentration on the potentiodynamic polarization curves of MS electrode in 1.0 M HCl at a 298 K, b 303 K and c 308 K

**Table 3** The electrochemical kinetic parameters ( $i_{corr}$ ,  $E_{corr}$ ,  $\beta_c$  and  $\beta_a$ ) and inhibition efficiency (%IE) obtained from polarization curves of MS electrode in 1.0 M HCl at 298, 303 and 308 K

P(2ABT)	i <sub>corr</sub> (n	$hA cm^{-2}$	)	$-E_{\rm corr}$	(mV)		$\beta_{\rm c}$ (mV	$dec^{-1}$		$\beta_{\rm a}$ (mV	$V dec^{-1}$ )		%IE		
conc. $\times 10^{-6}$ (M)	298 K	303 K	308 K	298 K	303 K	308 K	298 K	303 K	308 K	298 K	303 K	308 K	298 K	303 K	308 K
Blank	400	473.20	500	692	708	680	1.36	1.43	1.48	0.300	0.306	0.309	_	_	_
2.1	276	340.00	386	690	681	676	0.96	0.99	1.06	0.302	0.302	0.302	31.00	28.15	22.80
4.2	216	288.00	320	664	659	657	0.86	0.90	0.82	0.280	0.280	0.280	46.00	39.14	36.00
6.4	170	236.50	273	642	640	638	0.76	0.81	0.71	0.274	0.270	0.270	57.50	50.02	45.40
8.5	146	200.00	245	638	633	627	0.62	0.65	0.61	0.256	0.250	0.250	63.50	57.73	51.00
10.6	94	170.02	215.5	618	613	636	0.60	0.64	0.59	0.235	0.230	0.230	67.50	64.07	56.90
12.7	116.4	153.32	193.0	615	619	621	0.96	0.98	0.56	0.232	0.240	0.240	70.90	67.60	61.40

 $E_{\text{corr}}$ , for MS electrode in 1.0 M HCl solution in the absence and presence of P(2ABT) are determined by extrapolation of the cathodic and anodic Tafel lines to the point of intersection.

Table 3 represents the influence of P(2ABT) concentrations and temperatures on the corrosion parameters of MS electrode in 1.0 M HCl solution in the potential range  $\pm 50$  mV from the corrosion potential.

The inhibition efficiency (%IE) at different P(2ABT) concentrations and temperatures for MS electrode in 1.0 M HCl solution is calculated using Eq. (2). The values of %IE are given in Table 3.

$$\% \text{ IE} = \left(1 - \frac{i_{\text{corr}}}{i_{\text{corr}}^{\circ}}\right) \times 100 \tag{2}$$

According to these data, it is observed that at a given temperature, %IE increases with increasing the inhibitor concentration and decreases by raising the temperature. This behavior can be illustrated due to the desorption of some P(2ABT) species at higher temperatures. This suggests that physical adsorption may be the type of adsorption of the inhibitor on the metal surface. It is clear that the %IE values obtained from weight loss and polarization measurements are parallel in a good agreement.

# Electrochemical impedance spectroscopy measurements

The impedance of the MS electrode in 1 M HCl solution at 298 K in the absence and presence of different





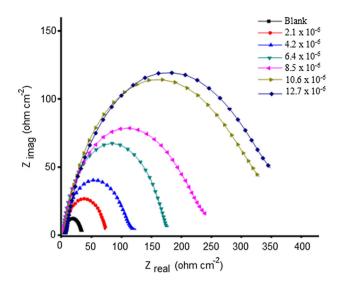


Fig. 8 Nyquist plots for MS in 1 M HCl at different concentrations of P(2ABT) at 298 K

concentrations P(2ABT) is shown in Fig. 8 as a Nyquist plot. Data show that, the presence of single semi-circle curves in all cases is attributed to the presence of single charge transfer process during dissolution of MS which is unaffected by the presence of inhibitor molecules. Deviations from perfect circular shape are referred to the frequency dispersion of interfacial impedance that arises due to surface roughness, impurities, dislocations, grain boundaries, adsorption of inhibitors, and formation of porous layers and in homogenates of the electrode surface [24]. EIS data show that, the  $R_{\rm ct}$  values increase and the  $C_{\rm dl}$ values decrease with increasing the inhibitor concentrations. This is due to adsorption of the inhibitor molecules on the MS and gradual replacement of water molecules, decreasing the extent of dissolution reaction of MS. The higher  $(R_{ct})$  values are associated with slower corroding system [25]. The decrease in the  $C_{dl}$  can result from the decrease of the local dielectric constant and/or from the increase of the thickness of the electrical double layer suggested that the inhibitor molecules function by adsorption at the metal/solution interface [26]. The %IE obtained from EIS measurements is close to those deduced from polarization measurements.

# Thermodynamic activation functions of the corrosion process

It has been reported elsewhere that, for the acid corrosion of MS, the logarithm of the corrosion rate given in mg cm<sup>-2</sup> h<sup>-1</sup> (from weight loss data) and  $i_{corr}$  (from polarization data) is a linear function with 1/*T* where *T* is the absolute temperature [following Arrhenius Eq. (3) and the transition state Eq. (4)] [27].

$$\log(CR) = -\frac{E_a^0}{2.303RT} + A$$
(3)

$$CR = \frac{RT}{Nh} e^{\left(\frac{\Delta S^*}{R}\right)} e^{\left(-\frac{\Delta H^*}{RT}\right)}$$
(4)

where  $E_a^{\circ}$  is the apparent activation energy,  $\Delta S^{\circ}$  is the entropy of activation,  $\Delta H^{\circ}$  is the enthalpy of activation, h is Planck's constant and N is the Avogadro number. According to Eq. 3,  $E_{a}^{\circ}$  could be obtained by plotting log (CR) against 1/T as in Fig. 9. Moreover, from Eq. 4, a plot of log (CR/T) against 1/T should give a straight line with a slope of  $(-\Delta H^{\circ}/2.33 R)$  and an intercept of  $(\log R/Nh - \Delta S/R)$ 2.303 R) as in Fig. 10. The calculated parameters are given in Table 4. Inspection of these data reveals that the apparent activation energy E<sub>a</sub> in HCl solution in the absence of P(2ABT) is 12.53 kJ mol<sup>-1</sup>. The addition of a P(2ABT) to the acid solution increases  $E_a^{\circ}$  and the extent of the increase is proportional to the inhibitor concentration, indicating that the energy barrier for the corrosion reaction increases with P(2ABT) concentration. This means that the corrosion reaction will be further pushed to surface sites that are characterized by progressively higher values of  $E_{a}^{\circ}$ as the concentration of the P(2ABT) in the acid solution becomes larger. The entropy of activation  $\Delta S^{\circ}$  in the absence and presence of P(2ABT) is large and negative. This implies that the activated complex in the rate determining step represents an association rather than a dissociation step, meaning that a decreases in disordering takes place on going from reactants to the activated complex. The positive signs of  $\Delta H^{\circ}$  reflect the endothermic nature of the steel dissolution process. The data infer that the values of  $E_a^{\circ}$  of the corrosion of MS in 1.0 M HCl solution in the presence of P(2ABT) are higher than that in the uninhibited acid solution. The thermodynamic functions  $E_{a}^{\circ}$ ,  $\Delta H^{\circ}$  and  $\Delta S^{\circ}$  enhance with increasing the inhibitor concentration, implying that more energy barrier for the corrosion in the presence of inhibitor is attained. Large and negative values of  $\Delta S^{\circ}$  imply that the activated complex in the rate determining step represents an association rather than dissociation step, meaning that the decrease in disordering takes place on going from reactants to the activated complex.

#### Adsorption considerations

Adsorption depends mainly on different parameters as; the charge, nature and electronic characteristics of the metal surface, adsorption of solvent and other ionic species, temperature of corrosion reaction and on the electrochemical potential at solution interface [28, 29].

Adsorption isotherms are usually used to describe the adsorption process, the most frequently used isotherms include; Langmuir, Frumkin, Hill de Boer, Parsons, Temkin, Flory–Huggins, Dhar-Flory–Huggins, Bockris-



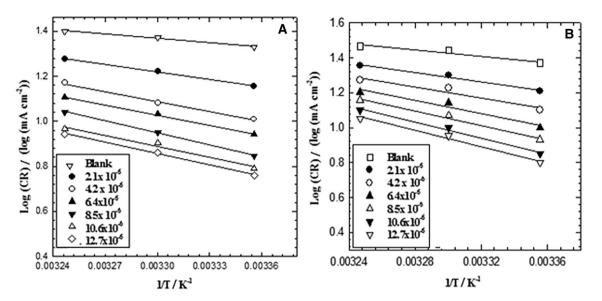


Fig. 9 Arrhenius plot of corrosion rate of MS in 1.0 M HCl containing various concentrations of P(2ABT) **a** from weight loss and **b** from polarization measurements

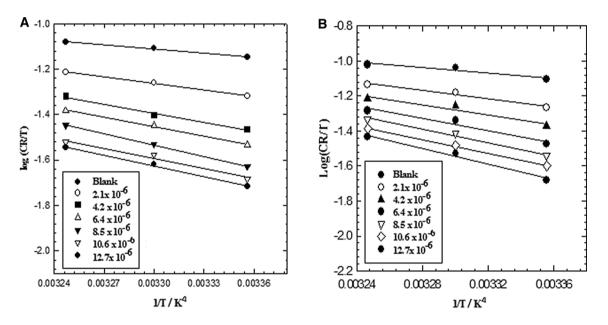


Fig. 10 Transition state plot of corrosion rate of MS in 1.0 M HCl containing various concentrations of P(2ABT) **a** from weight loss and **b** from polarization measurements

Swinkels and the recently formulated thermodynamic/kinetic model of El-Awady et al. [30–32] Adsorption isotherms can provide important information about the nature of the metal/inhibitor interaction. Adsorption of the organic molecules occurs as the interaction energy between inhibitor and metal surface is higher than that between the  $H_2O$  molecule and the metal surface [33].

To obtain the adsorption isotherm, the degree of surface coverage ( $\theta$ ) for various concentrations of the P(2ABT) is calculated according to ( $\theta = \%$ IE/100).

Because, the data of weight loss and polarization are close to each other, we use the data obtained from weight loss to study the adsorption of P(2ABT) on MS electrode in hydrochloric acid solution, different isotherms are studied as follows:

Langmuir adsorption isotherm is expressed according to Eq. (5) or its related one (6) [34, 35].

$$\frac{C}{\theta} = \frac{1}{K_{\text{ads}}} + C \tag{5}$$



$P(2ABT)$ conc. $\times 10^{-6}$ (M)	Weight loss			Polarization				
	$\frac{E_{\rm a}^{\circ}}{(\rm kJ\ mol^{-1})}$	$\Delta H^{\rm o}  ({\rm kJ}  {\rm mol}^{-1})$	$\Delta S^{\rm o} ({\rm J \ mol}^{-1} {\rm \ K}^{-1})$	$\frac{E_{\rm a}^{\circ}}{\rm (kJ\ mol^{-1})}$	$\Delta H^{\rm o} \ (\rm kJ \ mol^{-1})$	$\Delta S^{\rm o} ({\rm J \ mol}^{-1} \ {\rm K}^{-1})$		
Blank	12.53	11.24	-182.07	17.08	14.55	-187.81		
2.1	21.08	18.61	-160.43	25.62	23.11	-144.16		
4.2	28.28	25.71	-139.37	30.06	27.55	-131.14		
6.4	28.76	26.23	-138.80	36.23	33.70	-112.56		
8.5	30.62	27.92	-133.82	39.54	37.03	-102.80		
10.6	31.04	28.53	-131.52	42.68	38.41	-100.42		
12.7	32.40	29.87	-130.18	25.62	43.08	-84.99		

**Table 4** The thermodynamic activation functions of MS dissolution in 10 M HCl in the absence and presence of different concentrations ofP(2ABT) obtained from weight loss and polarization data by applying Arrhenius and transition state plots

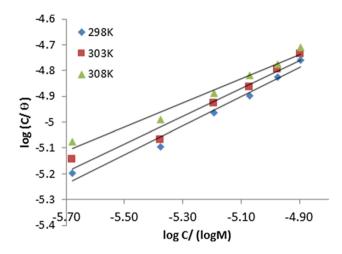


Fig. 11 Langmuir adsorption isotherm of P(2ABT) based on weight loss data at different temperatures

$$\log\left(\frac{C}{\theta}\right) = \log C - \log K_{\rm ads} \tag{6}$$

where *C* is the concentration of the inhibitor,  $K_{ads}$  is the adsorption equilibrium constant and  $\theta$  is degree of surface coverage of the inhibitor. Plotting log (*C*/ $\theta$ ) against log *C* gives a linear relationship as shown in Fig. 11. The parameters of Langmuir isotherm are listed in Table 5. The  $r^2$  values >0.96 indicate fitting to Langmuir adsorption isotherm [36], so the adsorption of P(2ABT) on the MS surface show no interaction between them [37].

For Temkin adsorption isotherm, the degree of surface coverage  $(\theta)$  is related to inhibitor concentration (*C*) according to Eq. (7) and its log form (8) [34].

$$\exp(-2a\theta) = K_{\rm ads}C\tag{7}$$

$$\theta = \frac{-2.303 \log K_{\text{ads}}}{2a} - \frac{2.303 \log C}{2a} \tag{8}$$

where  $K_{ads}$  is the adsorption equilibrium constant and *a*, is the attractive parameter. Temkin plots are presented in Fig. 12, linear relationship, which shows that adsorption data fitted Temkin adsorption isotherm. Adsorption parameters obtained from Temkin adsorption isotherms are recorded in Table 5. The values of attractive parameter (a) are negative in all cases, indicating that repulsion exists in the adsorption layer.

Flory–Huggins adsorption isotherm can be expressed according to Eq. (9) [36]. and is shown in Fig. 13.

$$\log\left(\frac{\theta}{C}\right) = \log K_{\text{ads}} + x \log(1-\theta) \tag{9}$$

where the size parameter is x (the number of adsorbed water molecules substituted by a given inhibitor molecule). The value of the size parameter x is positive as shown in Table 5, indicating a bulky adsorption of P(2ABT) species which displace more than one water molecule from the MS surface.

Frumkin adsorption isotherm is given by Eq. (10) [34].

$$\log\left\{ [C] \times \left(\frac{\theta}{1-\theta}\right) \right\} = 2.303 \log K_{\text{ads}} + 2\alpha\theta \tag{10}$$

where  $K_{ads}$  is the adsorption–desorption constant and  $\alpha$  is the lateral interaction term describing the interaction in adsorbed layer. A linear plot is seen (see Fig. 14) which show the applicability of Frumkin isotherm. The values for Frumkin adsorption parameters were recorded in Table 5. From which the value of the adsorption parameter  $\alpha$  is positive, suggesting the attractive behavior of the inhibitor on the surface of mild steel. The characteristics of the El-Wady's kinetic/thermodynamic isotherm model are given by Eq. (11).

$$\log\left(\frac{\theta}{1-\theta}\right) = \log K + y \log C \tag{11}$$

where *C* is the concentration of the P(2ABT),  $\theta$  is the degree of surface coverage,  $K_{ads}$  is the equilibrium constant of adsorption process and  $K_{ads} = K^{1/y}$ . The values for the



Isotherm	Temperature (K)	$r^2$	Log K	$\Delta G_{\rm ads} \ ({\rm kJ} \ {\rm mol}^{-1})$	а	α	x	1/y
Langmuir	298	0.97	-2.037	-21.58				
	303	0.96	-2.132	-22.49				
	308	0.97	-2.443	-24.69				
Frumkin	298	0.99	-0.000357189	-9.95		1.88		
	303	0.97	-0.00044949	-10.12		3.03		
	308	0.96	-0.000453775	-10.28		3.24		
Tempkin	298	0.99	1.28	-17.54	-0.45			
	303	0.99	1.19	-17.03	-0.44			
	308	0.99	1.26	-17.43	-0.45			
Flory-Huggin	298	0.99	5.30	-30.71			1.15	
	303	0.99	5.50	-31.91			1.47	
	308	0.98	5.37	-31.15			1.47	
EL-Awady	298	0.92	1.05	-15.95				1.05
	303	0.985	1.09	-16.45				1.09
	308	0.996	1.04	-16.41				1.04

Table 5 Isotherms parameter from different models for adsorption of P(2ABT) based on weight loss data at different temperatures

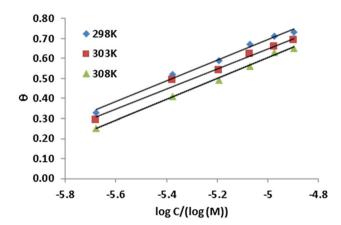


Fig. 12 Timkin adsorption isotherm of P(2ABT) based on weight loss data at different temperatures

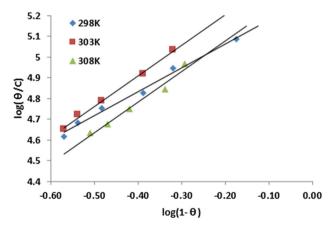


Fig. 13 Flory-Huggins adsorption isotherm of P(2ABT) based on weight loss data at different temperatures

El-Awady's kinetic/thermodynamic model parameters were recorded in Table 5. This model is plotted in Fig. 15.

Gibb's free energy, enthalpy of adsorption and entropy of adsorption can be calculated from the adsorption isotherm [36–40] Standard Gibb's free energy ( $\Delta G_{ads}^{\circ}$ ) can be calculated using Eq. (12):

$$\Delta G_{\rm ads}^{\circ} = -RT \ln \left( K_{\rm eq} \right) \tag{12}$$

where  $K_{eq}$  is an equilibrium adsorption constant which is calculated from the adsorption isotherm to be followed and it has been calculated with reference to its molars of water, 55.5 M, under standard condition. Data are inserted into Table 5.

A negative  $\Delta G_{
m ads}^\circ$  suggest that the adsorption of P(2ABT) onto the MS surface is a spontaneous process [41] and strongly attracted to MS [42]. Generally, values of

 $\Delta G_{\rm ads}^{\circ}$  up to  $-20 \text{ kJ mol}^{-1}$  are consistent with physisorption, while those around  $-40 \text{ kJ mol}^{-1}$  or higher are associated with chemisorptions [43]. So, we suggest from the data in Table 5 that the adsorption is physically in natures.

From standard free energy, enthalpy and entropy of adsorption can be calculated using the following Eq. (13)or its log form (14):

$$\Delta G_{\rm ads}^{\circ} = \Delta H_{\rm ads}^{\circ} - T \Delta S_{\rm ads}^{\circ} \tag{13}$$

$$\log K_{\rm eq} = \frac{-\Delta H_{\rm ads}^{\circ}}{2.303RT} + \frac{\Delta S_{\rm ads}^{\circ}}{2.303RT} - \log 55.5$$
(14)

Values of  $\Delta H_{ads}^{\circ}$  and  $\Delta S_{ads}^{\circ}$  are obtained and illustrated in Table 6. The magnitude of the values of  $\Delta H_{ads}^{\circ}$  and  $\Delta S_{ads}^{\circ}$  is characteristic of the occurrence of the replacement process during adsorption process



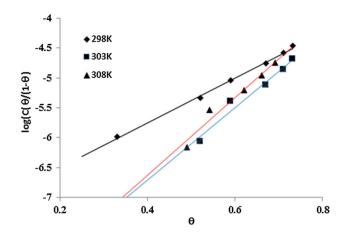


Fig. 14 Frumkin adsorption isotherm of P(2ABT) based on weight loss data at different temperatures

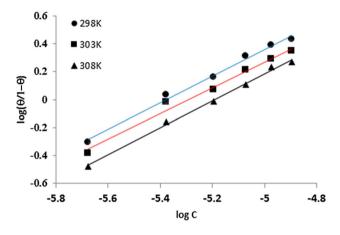


Fig. 15 El-Awady adsorption isotherm of P(2ABT) based on weight loss data at different temperatures

### Surface morphology

SEM photographs of mild steel after 1 h of immersion in 1 M HCl solution in the absence and presence of  $12.7 \times 10^{-6}$  mol L<sup>-1</sup> P(2ABT) at constant temperature  $\pm 1^{\circ}$  C are shown in Fig. 16a–c. Data show that, the Polished lines of the steel surface are observed before exposure to the corrosive medium (Fig. 16a) while the damage of its surface after immersion in 1 M HCl due to the dissolution is seen in Fig. 16b. SEM image (Fig. 16c) of mild steel surface after immersion in 1 M HCl in the presence of P(2ABT) shows the smooth surface indicating that the inhibitor molecules hinders the dissolution of MS by forming the protective film on its surface and thereby reduce the corrosion rate.

## Mechanism of inhibition

Corrosion of iron and steel [44, 45] in HCl solution follows the following proposed mechanism

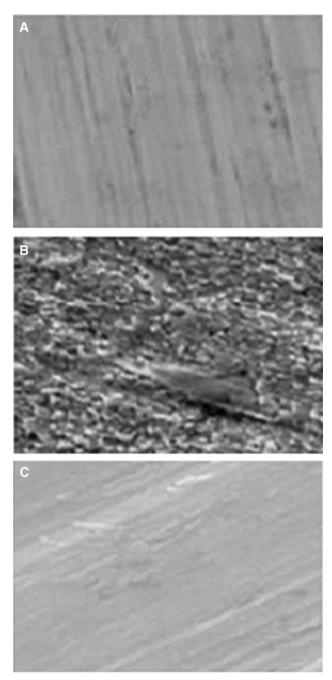


Fig. 16 SEM micrographs of mild steel samples at 28 K a only surface polishing, b after immersion in 1 M HCl without inhibitor, c after immersion in 1 M HCl in presence of  $12.7 \times 10^{-6}$  M P(2ABT)

1. Anodic dissolution of iron is as follows:

$$Fe + Cl^{-} \rightleftharpoons (FeCl^{-})_{ads} \rightleftharpoons (FeCl)_{ads} + e^{-}$$
$$(FeCl) \rightarrow (FeCl)^{+} + e^{+}$$
$$(FeCl)^{+} \rightleftharpoons Fe^{+2} + Cl^{-}$$

2. Cathodic hydrogen evolution is as follows:



Isotherm	$\Delta H_{\rm ads} \ ({\rm kJ} \ {\rm mol}^{-1})$	$\Delta S_{\rm ads} \ ({\rm JK}^{-1} \ {\rm mol}^{-1})$
Langmuir	71.13	38.29
Frumkin	3.68	73.01
Temkin	1.67	73.38
Flory-Huggin	-12.64	89.01
EL-Awady	1.67	73.38

**Table 6** Values of  $\Delta H^{\circ}_{ads}$  and  $\Delta S^{\circ}_{ads}$  from different isotherm models of P(2ABT) based on weight loss data

$$\begin{split} Fe + H^+ \rightleftharpoons (FeH^+)_{ads} \\ (FeH^+)_{ads} + e^- &\rightarrow (FeH)_{ads} \\ (FeH)_{ads} + H^+ + e^- &\rightarrow Fe + H_2 \end{split}$$

Accumulated ions at the metal/solution interface replace solvent molecules from the metal surface and their centers reside at the inner Helmholtz plane. The anions are adsorbed when the metal surface has an excess positive charge in an amount greater than that required to balance the charge corresponding to the applied potential [46]. The exact nature of this interaction depends on the relative coordinating strength towards the given metal of the particular groups present [46]. Due to the well accepted model, the adsorption of organic inhibitor molecules is often a displacement reaction involving removal of adsorbed water molecules from the metal surface [43].

$$Org_{(sol)} + xH_2O_{ads} \leftrightarrow Org_{(ads)} + xH_2O_{sol}$$

In general, the proceeding of physical adsorption requires the presence of both electrically charged metal surface and charged species in the bulk of the solution. Chemisorption process involves sharing or transfer of charge from the inhibitor molecules to the metal surface to form a coordinate type of a bond. This is a possible in case of a positive as well as a negative charge on the surface [47].

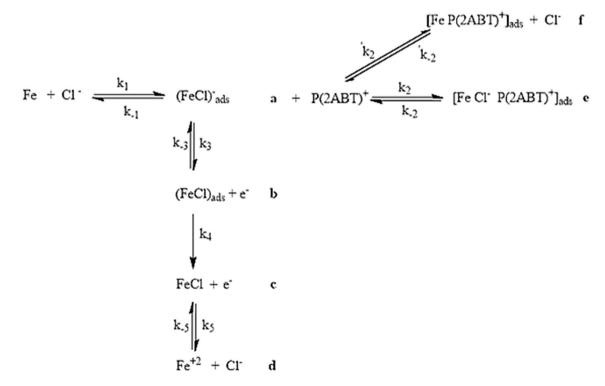
When mild steel immersed in the HCl solution, in the presence of P(2ABT),  $Cl^-$  ions are firstly adsorbed to the MS surface create an excess negative charge towards the solution (step a), and favor more adsorption of the cations [41, 44]. After that Two assumptions are proposed;

I.

 $P(2ABT)^+$  are adsorbed on (Fe–Cl)<sup>-</sup> surface (step e). So it can be proposed that, reaction, pathway of P(2ABT) seems to be through (a  $\rightarrow$  e). The equilibrium constant  $k_2$  must be much bigger than  $k_3(k_2 \gg k_3)$  and reaction (a  $\rightarrow$  e) should be more favoured than (a  $\rightarrow$  d). Thus, the P(2ABT) may act as a barrier against corrosion of MS (see Scheme 2).

II.

 $P(2ABT)^+$  replaces with Cl<sup>-</sup>. Thus, Cl<sup>-</sup> ion is removed from the metal surface towards a solution (Scheme 2). As a result of this, a new double layer is formed so MS is



Scheme 2 Proposed adsorption mechanism of P(2ABT) onto MS surface in HCl solution

loaded negative charge against positive charged P(2ABT) to form (Fe P(2ABT)<sup>+</sup>)<sub>ads</sub>.

Depending on this explanation, the equilibrium constant of the related step  $k'_2$  is expected higher than both  $k_2$  and  $k_3$ . Consequently, P(2ABT) interacts with the MS surface other than electrostatic interactions, it can be suggested that the reaction pathway is from step  $(a \rightarrow f)$  instead of  $(a \rightarrow e)$ .

### Conclusions

From the overall experimental results the following conclusions can be deduced:

- 1. P(2ABT) is a good inhibitor for MS corrosion and acts as anodic type inhibitor in HCl solutions.
- 2. Gravimetric and electrochemical measurements show that the inhibiting action increases with increasing the inhibitor concentration and decreases with raising the temperature.
- 3. Gibbs free energy value confirms the spontaneous physical adsorption.
- 4. The energy barrier for the corrosion reaction increases with the addition of P(2ABT).
- 5. The adsorption of P(2ABT) on the MS surface in HCl solutions follows the tested isotherms.

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