### **ORIGINAL ARTICLE**



# Error analysis of adsorption isotherm models for penicillin G onto magnesium oxide nanoparticles

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#### Abstract

The adsorption of penicillin G (PC-G) from aqueous solution by magnesium oxide (MgO) nanoparticles has been investigated. This experimental study was conducted in a laboratory scale. The effects of various operating parameters such as pH (3–11), the dosage of MgO nanoparticles (0.3–1.5 g/L), contact time (20–150 min), and concentration of PC-G (50–200 mg/L) were studied. The results showed that under optimal conditions of concentration of 50 mg/L, pH 3, MgO nanoparticles dosage of 1.5 g/L and contact time of 60 min, the maximum adsorption capacity ( $q_{\rm m}$ ) of PC-G adsorption on MgO nanoparticles obtained was 25.66 mg/g. The process of penicillin G adsorption on MgO nanoparticles was found to depend on Langmuir (II) and Langmuir (III) adsorption isotherm models. It could be concluded that the MgO nanoparticles can be used for PC-G removal from its aqueous solution.

**Keywords** Penicillin G · Nanoparticles · Aqueous solution · Adsorption · Isotherm

### Introduction

Recently, the presence of pharmaceuticals and related products in the environment is proposed as a noteworthy environmental problem in the world (Richardson et al. 2005; Kord Mostafapour et al. 2017; Ahmadi and kord mostafapour 2017a). Pharmaceuticals have been used as human medicine to treat or prevent microbial infections and eliminate microorganisms, such as bacteria, virus, fungi, and parasites, for about 70 years (Gao et al. 2012; Guler and Sarioglu 2014). The annual application rate of antibiotics has been calculated to be around 100,000–200,000 tons in the world (Gulkowska et al. 2008; Kümmerer 2009).

In addition to the creation of chemical pollution, the antibiotics residue in the environment may cause the production of resistant microorganisms and dispersion of the antibiotic resistance (Aristilde et al. 2010; Zhang et al. 2016). The

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antibiotics along with the sewage, pharmaceutical industries wastewater, veterinary clinics and hospital sewages, and the agricultural products noticeably enter into the water resources and the environment (Carabineiro et al. 2012; Ahmadi et al. 2017a). If the antibiotics are not degraded or eliminated properly during the sewage treatment, in soil or in other environmental compartments, they will reach the surface water, groundwater, and, potentially, drinking water (Carabineiro et al. 2012). The presence of these contaminants in the environment is of great threat to human health (Zhang et al. 2016). Different findings have reported the presence of various kinds of antibiotics in many environmental samples (Batt et al. 2006; Ahmadi et al. 2017b).

Its density in sewage and surface water is 1  $\mu$ g/L and in hospital sewage more than 150  $\mu$ g/L (Ahmadi et al. 2017c; Liu et al. 2016). Penicillin G (PC-G) is composed of a core of 6-amino penicillanic acid with a side chain of benzyl. This antibiotic encompasses  $\beta$ -lactam loop which is very sensitive to pH, heat, and  $\beta$ -lactamase enzymes (Ahmadi and Kord Mostafapour 2017b; Peterson et al. 2012). Also, it has a biological half-life of 30–60 min (Ahmadi et al. 2017a; Peterson et al. 2012). It is soluble in aqueous solutions, and the mechanism of destruction of bacteria's cell wall is by stop production peptidoglycan layer (Gad-Allah et al. 2011). Recently, arbitrary and incorrect consumption of antibiotics has become essentially difficult in the



field of human health in Iran. Iran has been mentioned as one of the first twenty countries in the consumption of antibiotics and PC-G is the most widely used antibiotics in the country (Brown et al. 2006). Presently, the methods mostly applied to the treatment of antibiotic wastewater are coagulant sedimentation, membrane separation, activated sludge, biological contact oxidation, anaerobic sludge bed, advanced oxidation processes, ozone oxidation, electro-catalytic oxidation, dissolved air flotation and adsorption (Ahmadi et al. 2017c; Sun et al. 2014; Guo and Chen 2015). Many of these methods, such as electrochemical techniques and membrane processes, cannot be used on a large scale due to high costs of operation, repair and maintenance, high electricity consumption, production of toxic by-products, and complex operation. In contrast, adsorption process that is controlled by main physicochemical interactions, such as van der Waals forces, hydrogen bonds, polarity, and dipole-dipole interaction, is one of the most cost-effective methods for water treatment (Ren et al. 2011; Rahdar et al. 2019a, b). Particularly, the development of various nano-adsorbents, which offer unique advantages including large specific surface area, selective and abundant adsorption sites, short intraparticle diffusion distance, tunable pore size, and easy regeneration and reusability, has attracted a great deal of attentions (Tajbakhsh et al. 2014; Al-Nour 2009). Among the nanoparticles, magnesium oxide (MgO) is a basic oxide group and it has provided a large range of applications in the process of adsorption (Ghahramani et al. 2016). The most important characteristics of MgO nanoparticles are availability, cheapness, nonvolatility, non-toxicity, stability, reusability, and high absorption capability (Kermani et al. 2013). The main purpose of the research is to study the adsorption of PC-G from aqueous solution using MgO nanoparticles.

# **Materials and methods**

# **Materials**

Penicillin G (PC-G) with a molar mass of 372.48 g/mol, molecular formula  $C_{16}H_{17}KN_2O_4S$ , and wavelength of maximum absorption ( $\lambda_{max}$ ) 248 nm (Ahmadi et al. 2017a) and magnesium oxide (MgO) nanoparticles were purchased from Sigma-Aldrich Chemical Company (USA). The chemical structure of PC-G is provided in Fig. 1. The physicochemical properties of MgO nanoparticles are given in Table 1. The structural features of the MgO nanoparticles were determined using scanning electron microscopy (SEM) and Fourier transform infrared spectroscopy (FTIR). Fourier transform infrared

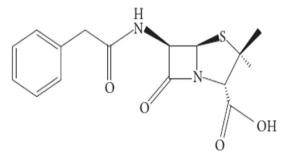


Fig. 1 Chemical structure of PC-G

Table 1 Physicochemical specifications of MgO nanoparticles

| Parameter             | Unit              | Amount            |  |  |
|-----------------------|-------------------|-------------------|--|--|
| Appearance            | _                 | White             |  |  |
| Average particle size | nm                | 20                |  |  |
| Morphology            | _                 | Multi-dimensional |  |  |
| Purity                | %                 | 99                |  |  |
| Specific surface area | $m^2/g$           | 60                |  |  |
| Density               | g/cm <sup>3</sup> | 3.58              |  |  |

spectroscopy (FTIR, JASCO 640) was done on a plus machine (4000–400 cm<sup>-1</sup>). SEM images were taken with a HITACHI Model S-3000H MgO nanoparticles.

### **Batch adsorption technique**

The effect of MgO nanoparticles (0.3–1.5 g/L), contact time (20–150 min), pH (3–11), and PC-G concentrations (50-200 mg/L) on PC-G removal was investigated. The PC-G solutions with concentrations in the range of 50 to 200 mg/L were prepared by successive dilution of the stock solution with distilled water. To work in a discontinuous system, Erlenmeyer flask was used. At each adsorption test time, the specified volume of PC-G solution with 100 mL of PC-G concentration was added into the Erlenmeyer. The desired conditions were set up, and the 0.5 g/L dose of adsorbent was added to the flask and then mixed in the magnetic stirrer at 180 rpm for 2 h. The pH of the solution was adjusted using 0.1 N HCl or 0.1 N NaOH solutions. The residual concentrations were measured using UV-visible spectrophotometer (Shimadzu Model: CE-1021). The amount of PC-G adsorbed on MgO nanoparticles,  $q_e$ , was obtained as follows (Ahmadi et al. 2017b):

$$q_{\rm e} = \frac{(C_0 - C_{\rm e})V}{M}.$$
 (1)



$$R(\%) = \frac{(C_0 - C_f)}{C_0} 100, \tag{2}$$

where  $C_0$  and  $C_e$  are the initial and equilibrium liquid-phase concentration of PC-G (mg/L), respectively,  $C_f$  is the final concentration, V is the volume of the solution (L), and M is the amount of adsorbent.

# **Adsorption isotherms study**

The equilibrium adsorption isotherm is important in the design of adsorption systems. Although several isotherm equations are available, four important isotherms including Langmuir and Freundlich isotherms were selected (Rahdar et al. 2016; Ahmadi et al. 2017c). The isotherm equations are presented in Table 2.

In order to validate the adsorption isotherm models used in the study, in addition to  $R^2$ , the parameters of Marquardt's percent standard deviation (MPSD)and hybrid error function (HYBRID) were also evaluated, which can be described as Eqs. (3) and (4):

MPSD = 
$$100\sqrt{\frac{1}{n-p}\sum_{i=1}^{n} \left(\frac{q_{e,exp} - q_{e,calc}}{q_{e,exp}}\right)_{i}^{2}}$$
 (3)

HYBRID = 
$$\frac{100}{n-p} \sum_{i=1}^{n} \left[ \frac{(q_{e,exp} - q_{e,calc})^2}{q_{e,exp}} \right]_i$$
 (4)

**Table 2** Equations of isotherms

| Isotherm type  | Main equation  | Linear form   |
|----------------|--|---|
| Freundlich     | $q_e = K_{\rm f} C_{\rm e}^{\frac{1}{n}}$                    | $\log (x/m) = \log \left(K_{\rm f}\right) + \frac{1}{n}\log \left(C_{\rm e}\right)$                               |
| Langmuir (I)   |  | $\frac{c_{\rm e}}{q_{\rm e}} = \frac{1}{q_{\rm m}} + \frac{1}{q_{\rm m}K_{\rm l}}$                                |
| Langmuir (II)  | $q_{\rm e} = \frac{q_{\rm m}K_1C_{\rm e}}{1 + K_1C_{\rm e}}$ | $\frac{1}{q_{\rm e}} = \frac{1}{q_{\rm m}} + \left(\frac{1}{q_{\rm m}K_{\rm l}}\right) \frac{1}{C_{\rm e}}$       |
| Langmuir (III) |  | $q_{\mathrm{e}} = q_{\mathrm{m}} - \left(\frac{1}{K_{\mathrm{L}}}\right) - \frac{q_{\mathrm{e}}}{C_{\mathrm{e}}}$ |
| Langmuir (IV)  |  | $\frac{q_{\rm e}}{C_{\rm e}} = k_{\rm L} q_{\rm m} - k_{\rm L} q_{\rm e}$   |

**Table 3** Isotherm model constants for the adsorption of PC-G ( $C_0$ =50 mg/L and Tem=298 K)

| Isotherm       | q <sub>e exp</sub> | $K_{ m L}$ | $q_{ m m}$ | $\Delta q$ (%) | HYBRID | MPSD  | $R^2$ |
|----------------|--------------------|------------|------------|----------------|--------|-------|-------|
| Freundlich     | 23                 | 6.56       | 0.47       | 10.3           | 9.6    | 20.1  | 0.962 |
| Langmuir (I)   | 23                 | 0.5        | 4.4        | 92.4           | 4.2    | 19.49 | 0.973 |
| Langmuir (II)  | 23                 | 0.094      | 0.086      | 16.73          | 2.97   | 17.02 | 0.995 |
| Langmuir (III) | 23                 | 0.59       | 25.66      | 6.32           | 0.4259 | 6.48  | 0.976 |
| Langmuir (IV)  | 23                 | 0.038      | 1.56       | 33.9           | 12     | 34.6  | 0.976 |

The isotherm parameters with the various error functions used in the present study are given in Table 3. In order to determine the goodness of fit of the isotherm models for the adsorption system, it is necessary to analyze the data set using  $\Delta q$  (%) combined with the values of the determined coefficient  $R^2$  (Ahmadabadi et al. 2016; Igwegbe et al. 2018; Ahmadi et al. 2018):

$$\Delta q \,(\%) = 100 \sqrt{\frac{\sum \left| \left( q_{\text{exp}} - q_{cal} \right) / q_{\text{exp}} \right|^2}{N - 1}},\tag{5}$$

where  $q_{\rm exp}$  and  $q_{\rm cal}$  (mg/g) are the experimental and calculated amount of PC-G adsorbed, respectively, and N is the number of measurements made, respectively.

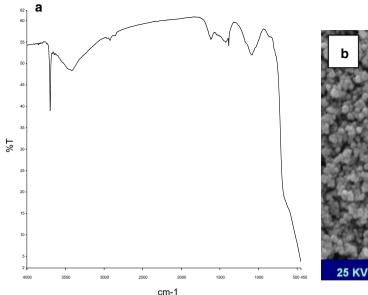
## **Results and discussion**

# FTIR and SEM analysis on MgO nanoparticles

Figure 2a shows the FTIR spectrum (% transmittance vs. wave number) for MgO nanoparticles. The functional groups present in the MgO nanoparticles were identified. Peaks 3419.46 cm<sup>-1</sup> (O–H stretch, H-bonded) assigned to alcohols and phenols are very strong. SEM was used to show the surface morphology, size, and location of the individual MgO nanoparticles. The SEM image of MgO nanoparticles is shown in Fig. 2b. The MgO nanoparticles were also found to consist of lamellar- or platelike structures.

# Determination of point of zero charge ( $pH_{pzc}$ )

To determine the  $pH_{zpc}$ , 50 mL nitrite potassium (0.01 M) was added to glass plates and the pH was adjusted in 2–14 using HCl and NaOH. Then, 0.2 g of magnesium oxide nanoparticles (MgO nanoparticles) was added and mixed in a shaker with a velocity of 180 rpm. After 24 h, the final pH was measured. The graph of  $pH_{i(initial)}$  against  $pH_{f(final)}$  was drawn, and the intersection point was isoelectric pH. The  $pH_{zpc}$  for MgO nanoparticles was 12.4 (Rahdar et al. 2018).



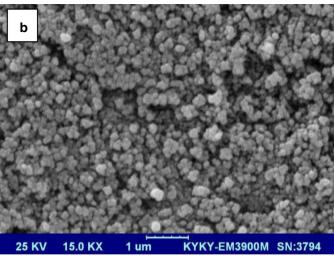
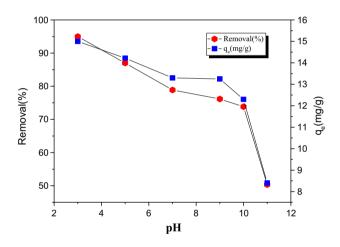


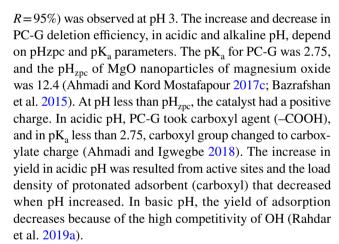
Fig. 2 a FTIR pattern and b SEM image of the MgO nanoparticles



**Fig. 3** Effect of pH on PC-G removal efficiency on MgO nanoparticles ( $C_0$  = 50 mg/L, dosage of 0.5 g/L, and time = 60 min)

# The effect of pH

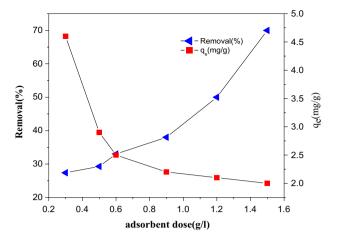
The pH is an important parameter that influences the surface charge of adsorbent, ionization degree of different pollutants, and separation of functional groups on absorbent active sites (Ahmadi and Kord Mostafapour 2017c). To obtain the optimal pH value, experiments were carried out by varying initial solution pH from 3 to 11, and under the condition of 50 mg/L of initial penicillin G (PC-G) concentration, 0.5 g/L of MgO nanoparticles dose, and 60 min of contact time. It can be seen from Fig. 3 that the adsorption of PC-G was highly dependent on the pH of the solution, and the maximum amount of removal of the PC-G ( $q_m$ =14.75 mg/g,



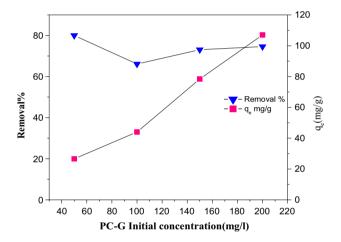
### The effect of adsorbent dosage

The adsorbent dosage is an important parameter to study the removal of PC-G from water by adsorption process, because this parameter determines the adsorption capacity of the adsorbent. To evaluate the effect of adsorbent dose on the adsorption of PC-G, 0.3 to 1.5 g/L of MgO nanoparticles was used for adsorption experiments at the fixed conditions of pH 3, 50 mg/L of initial PC-G concentration, and 60 min of contact time. As it can be seen from Fig. 4, the removal efficiency of PC-G increased rapidly with an increase in the adsorbent dosage from 0.3 to 1.5 g/L. A maximum removal of PC-G ( $q_{\rm m}$ =2 mg/g, R=70%) was achieved at an adsorbent concentration of 1.5 g/L. This is because an increase in the number of available adsorption sites will result in an





**Fig. 4** Effect of adsorbent dosage on removal efficiency of PC-G on MgO nanoparticles. ( $C_0$ =50 mg/L, pH=3, and contact time=60 min)



**Fig. 5** Effect of PC-G initial concentration on removal efficiency of PC-G on MgO nanoparticles. (Adsorbent dosage= $1.5\,$  g/L, pH=3, and contact time= $60\,$ min)

increase in adsorption capacity (Ahmadi and Kord Mostafapour 2017c; Ahmadi et al. 2017b).

# The effect of the initial concentration

Figure 5 shows that the effect of PC-G initial concentration (50–200 mg/L) on PC-G removal on MgO nanoparticles at optimum pH of 3 and adsorbent dosage of 1.5 g/L and contact time of 60 min at 298 ± 2 K. As the initial concentration of PC-G was increased from 50 to 200 mg/L, the removal efficiency decreased from 58 to 74.97% (Fig. 5). The effect of PC-G concentration showed that the adsorbent possesses finite adsorption sites, and in less concentrations of PC-G, more adsorbent sites are present. This is the cause for the increase in adsorption of PC-G (Samadi et al. 2013; Rahdar

et al. 2017). The reason for the decreasing removal efficiency by enhancement of antibiotic density is the saturation of active places of adsorption (Ahmadi and Kord Mostafapour 2017d; Rahdar et al. 2019b).

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### The effect of contact time

The effect of contact time on the PC-G adsorption capacity of MgO nanoparticles was investigated at different contact time (20, 40, 60, 80, 120 and 150 min) at PC-G initial concentration of 50 mg/L, pH of 3, and adsorbent dosage of 1.5 g/L at different temperatures (298 and 313 K). Figure 6 shows the effect of contact time on PC-G removal. The efficiency of antibiotic removal was increased by increasing the contact time. The reason for an increase in the removal efficiency at the early hours is that, as time passes, the made cavity and corrosion on the MgO nanoparticles level will be expanded and so increase in the cross section of adsorption (Bazrafshan et al. 2015). The amount of PC-G desorbed is proportional to the amount of PC-G on the adsorbent, which infers dynamic equilibrium (Bazrafshan and Ahmadi 2017; Ahmadi et al. 2017c). The time required to attain this state of equilibrium is referred to as equilibrium time (Bazrafshan and Ahmadi 2017; Rahdar et al. 2017).

# **Adsorption isotherms**

The estimated isotherm parameters, fixed correlation coefficient,  $R^2$ , and error analysis functions (MPSD, HYBRID, and  $\Delta q$ ) for the studied isotherms are presented in Table 3. PC-G adsorption on MgO nanoparticles conformed more to the Langmuir isotherms compared to the Freundlich isotherm with regards to their correlation coefficient,  $R^2$  (Table 3).

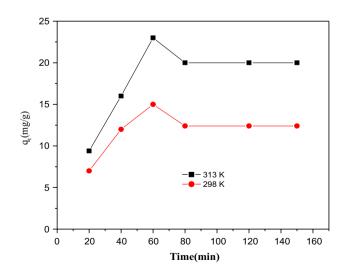


Fig. 6 Effect of contact time on PC-G removal efficiency on MgO nanoparticles. ( $C_0 = 50 \text{ mg/L}$ , dosage = 1.5 g/L, and pH = 3)



From the equilibrium data of the four Langmuir models, the results showed that the highest adsorptive capacity of PC-G on MgO nanoparticles was 25.66 mg/g based on Langmuir isotherm (III). Considering the error range for each model, it was deduced that Langmuir model (II) and Langmuir model (III) were the most proper models for describing the adsorption process. In fact, the highest amount of  $R^2$  and the lowest amounts of MPSD and HYBRID  $\Delta q$  showed better consistency with Langmuir model (II) and Langmuir model (III) (Rahdar and Ahmadi 2017; Watkinson et al. 2007).

### **Conclusions**

The general results of the study showed that MgO nanoparticles could lead to surface adsorption of PC-G from aqueous solutions with a maximum adsorption capacity and removal efficiency of 25.66 mg/g and 80%, respectively, under the optimal adsorption conditions of pH 3, initial concentration of 50 mg/L, and adsorbent dosage of 1.5 g/L. As a result, PC-G adsorption by MgO nanoparticles followed the Langmuir linear models. Among the four linear models, Langmuir (II) model showed the highest correlation coefficient. It was also documented that the Langmuir (II) and Langmuir (III) isotherm models had the best fit with the experimental data.

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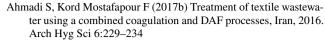
# Compliance with ethical standards

Conflict of interest All authors declare that they have no conflict of interest.

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