

# Surface Active Sites on $\text{Co}_3\text{O}_4$ Nanobelt and Nanocube Model Catalysts for CO Oxidation

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## ABSTRACT

CO oxidation has been performed on  $\text{Co}_3\text{O}_4$  nanobelts and nanocubes as model catalysts. The  $\text{Co}_3\text{O}_4$  nanobelts which have a predominance of exposed {011} planes are more active than  $\text{Co}_3\text{O}_4$  nanocubes with exposed {001} planes. Temperature programmed reduction of CO shows that  $\text{Co}_3\text{O}_4$  nanobelts have stronger reducing properties than  $\text{Co}_3\text{O}_4$  nanocubes. The essence of shape and crystal plane effect is revealed by the fact that turnover frequency of  $\text{Co}^{3+}$  sites of {011} planes on  $\text{Co}_3\text{O}_4$  nanobelts is far higher than that of {001} planes on  $\text{Co}_3\text{O}_4$  nanocubes.

## KEYWORDS

CO oxidation,  $\text{Co}_3\text{O}_4$ , surface active sites, turnover frequency, model catalyst

## 1. Introduction

CO oxidation is an important probe reaction in the development of many novel catalytic materials and catalytic mechanisms. A gold catalyst for CO oxidation below 0 °C was first reported by Haruta et al. in 1987 [1]. The size effect for such gold catalysts was verified by Goodman et al. in 2002 using a model catalyst of a gold cluster supported on a single crystalline surface of  $\text{TiO}_2$  {110} [2]. The shape effect for  $\text{CeO}_2$  nanocrystals in CO oxidation was reported by our group in 2005, when we showed that nanorods with exposed {110} planes prepared by a hydrothermal method are more reactive than nanoparticles with exposed {100} and {111} planes prepared by a precipitation method [3]. Si et al. subsequently prepared Au– $\text{CeO}_2$  nanocomposite catalysts with different shapes of  $\text{CeO}_2$  crystals and found a similar crystal plane effect for the water–gas

shift reaction [4]. Observation of such unexpected properties usually results from employing special techniques in the fabrication of catalytic materials [5, 6].

$\text{Co}_3\text{O}_4$ , a typical spinel-structure transition metal oxide, has attracted considerable attention for CO oxidation, and is regarded as an alternative to gold catalysts [7–10]. In 2008, our group [11] developed a hydrothermal method using cobalt hydroxide as a precursor and subsequent direct thermal decomposition to obtain  $\text{Co}_3\text{O}_4$  nanobelts with exposed {011} planes, nanosheets with exposed {112} planes, and nanocubes with exposed {001} planes. The unusually high index {112} crystal planes of  $\text{Co}_3\text{O}_4$  nanocrystals are more reactive than the more common {001} and {011} planes in the catalytic combustion of methane [11]. Xie et al. subsequently prepared  $\text{Co}_3\text{O}_4$  nanorods by a similar method which showed better catalytic properties than  $\text{Co}_3\text{O}_4$  nanoparticles for CO oxidation at

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temperatures as low as  $-77\text{ }^{\circ}\text{C}$ ; this can be attributed to the abundance of active  $\text{Co}^{3+}$  species on {110} planes in the former, assuming that the turnover frequencies (TOF) of the  $\text{Co}^{3+}$  sites are approximately the same level for the nanorods and the nanoparticles [12]. However, the shape of the nanoparticles they used for comparison is a truncated octahedron exposing {001} and {111} planes, so that the estimated TOF is an average result for {001} and {111} planes. Therefore, nanocubes with only {001} planes exposed are more suitable for investigating shape effects on CO oxidation. The  $\text{Co}^{3+}$  ions of  $\text{Co}_3\text{O}_4$  are the active sites for CO oxidation and  $\text{Co}^{2+}$  ions are almost inactive [8, 13]. From the viewpoint of traditional heterogeneous catalysts, the catalytic activity of a material depends on the number surface active sites. The relationship between the shape/crystal plane effect and the surface active sites is therefore a very important link between the structures and properties of catalysts.

In this work, we prepare  $\text{Co}_3\text{O}_4$  nanobelts and nanocubes according to Ref. [11] and investigate their behavior as model catalysts for CO oxidation. We show that the TOF of the  $\text{Co}^{3+}$  sites on  $\text{Co}_3\text{O}_4$  nanobelts is significantly higher than that of  $\text{Co}^{3+}$  sites on  $\text{Co}_3\text{O}_4$  nanocubes.

## 2. Experimental

### 2.1 Catalyst preparation

$\text{Co}_3\text{O}_4$  nanocubes and  $\text{Co}_3\text{O}_4$  nanobelts were prepared via a hydrothermal process using a cobalt hydroxide precursor and subsequent direct thermal decomposition [11].

#### 2.1.1 Nanocubes

$\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  (1 mmol, 0.291 g) was dissolved in 20 mL of ethanol to form a red solution, and then a mixture of 2 mL of octadecylamine and 10 mL of ethanol was added to the solution with magnetic stirring for at least 30 min. The resulting green solution was transferred into a 40-mL autoclave with a Teflon liner and heated at  $180\text{ }^{\circ}\text{C}$  for 12 h. The resulting product was filtered and washed several times with cyclohexane and ethanol, dried under vacuum at  $60\text{ }^{\circ}\text{C}$  for 2 h, and finally calcined in air at  $350\text{ }^{\circ}\text{C}$  for 3 h.

#### 2.1.2 Nanobelts

$\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  (1 mmol, 0.291 g) was dissolved in 15 mL of  $\text{H}_2\text{O}$  to form a red solution, and then 20 mL glycerol was added to the solution with magnetic stirring for at least 30 min. The resulting solution was transferred into a 40-mL autoclave with a Teflon liner and heated at  $140\text{ }^{\circ}\text{C}$  for 12 h. The resulting  $\text{Co}(\text{CO}_3)_{0.5}(\text{OH}) \cdot 0.11\text{H}_2\text{O}$  nanobelts were calcined in air at  $350\text{ }^{\circ}\text{C}$  for 3 h to produce  $\text{Co}_3\text{O}_4$  nanobelts.

### 2.2 Catalyst characterization

Powder X-ray diffraction (XRD) patterns were obtained by using a Bruker D8 Advance X-ray diffractometer with  $\text{Cu K}\alpha$  radiation ( $\lambda = 1.5418\text{ \AA}$ ). The size and morphology of all the catalysts were examined with a JEOL JEM-1200EX transmission electron microscope (TEM) and a Tecnai TF20 high-resolution transmission electron microscope (HRTEM). The catalyst powders were dispersed in ethanol to prepare samples for TEM and HRTEM. The BET surface area of the catalysts was measured by  $\text{N}_2$  adsorption using the multi-point method.

CO temperature-programmed reduction (CO-TPR) experiments were performed using a Thermo Electron Corporation TPD/R/O 1100 Series Catalytic Surfaces Analyzer equipped with an AMETEK quadrupole mass spectrometer which allowed detection of the various reaction products. In the CO-TPR experiments, a gas mixture of CO (5 vol% in He, 20 mL/min) was flowed over the sample (50 mg) [pre-treated with  $\text{O}_2$  (10 vol% in He, 20 mL/min) at  $300\text{ }^{\circ}\text{C}$  for 30 min] with heating from room temperature to  $800\text{ }^{\circ}\text{C}$  at a rate of  $10\text{ }^{\circ}\text{C}/\text{min}$ .

### 2.3 Catalytic activity

The catalytic activities for CO oxidation were evaluated in a fixed-bed quartz tubular reactor (6 mm i.d., 300 mm long) at atmospheric pressure under steady-state conditions. The catalyst particles (0.2 g) were placed in the reactor to a height of ca. 4 mm. The reactant gases (2.5% CO, 20%  $\text{O}_2$ , balanced with nitrogen) were passed through the reactor at a rate of 100 mL/min with a contact time of  $2 \times 10^{-5}$  h. The CO oxidation reaction was stabilized for 15 min, and the outlet products were then measured by gas chromatography. In every case, carbon dioxide was the only reaction

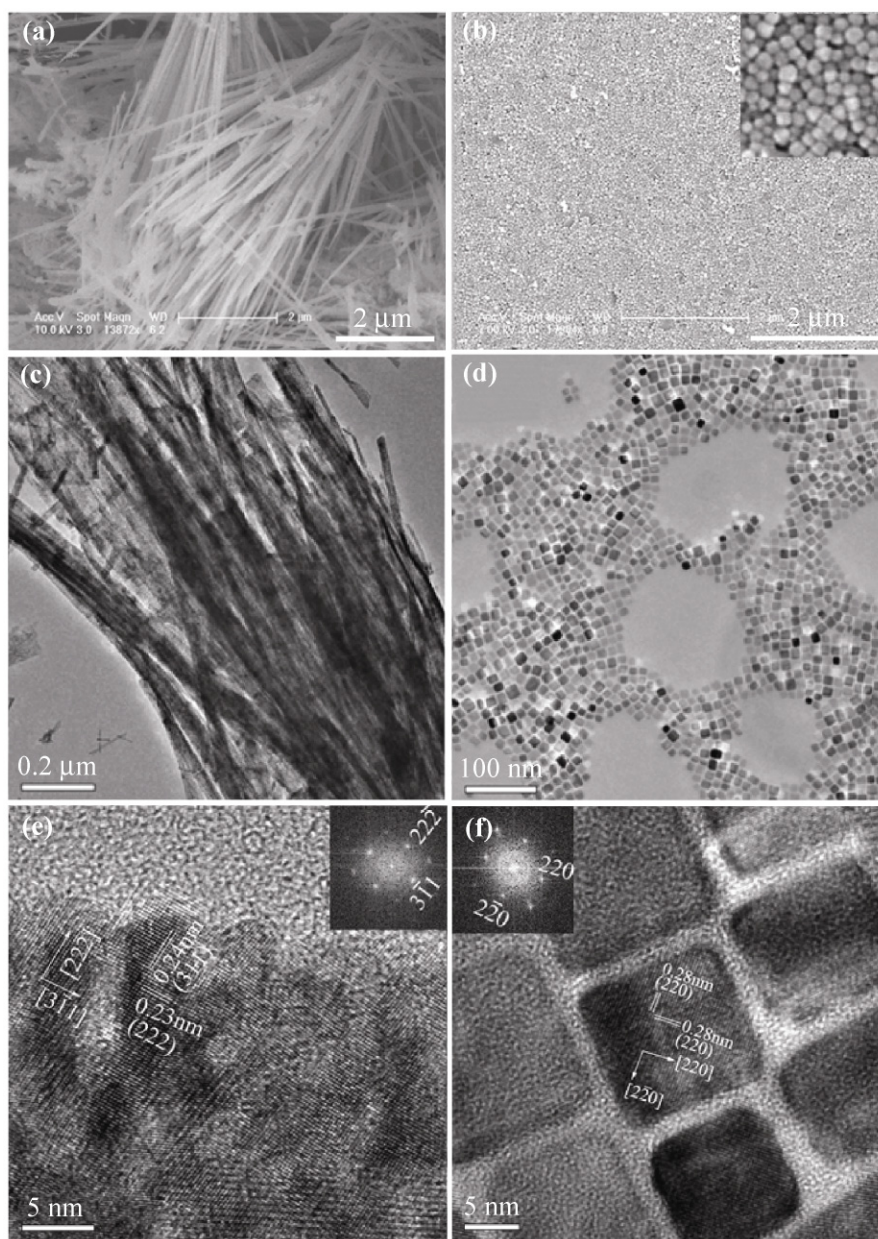
product detected throughout the whole experiment.

### 3. Result and discussion

#### 3.1 Catalyst characterization

Figure 1 shows typical scanning electron microscope (SEM), TEM, and HRTEM images of the  $\text{Co}_3\text{O}_4$  nanobelts and nanocubes. The lengths and widths of the  $\text{Co}_3\text{O}_4$  nanobelts are ca. 2–5  $\mu\text{m}$  and 50–100 nm,

respectively, while the as-prepared  $\text{Co}_3\text{O}_4$  nanocubes are monodisperse with a uniform size of ca. 15–20 nm. The average length and width of the nanobelts are 3.5  $\mu\text{m}$  and 75 nm, respectively. The average length of the nanocubes is ca. 17.5 nm. The dominant exposed planes of  $\text{Co}_3\text{O}_4$  nanobelts are  $\{011\}$ , which are the only planes normal to both the set of  $(311)$  planes with a lattice spacing of 0.24 nm and the set of  $(222)$  planes with a crossing lattice spacing of 0.23 nm. The dominant exposed planes of  $\text{Co}_3\text{O}_4$  nanocubes are



**Figure 1** (a) SEM image of typical  $\text{Co}_3\text{O}_4$  nanobelts. (b) SEM image of typical  $\text{Co}_3\text{O}_4$  nanocubes. (c) TEM image of typical  $\text{Co}_3\text{O}_4$  nanobelts. (d) TEM image of typical  $\text{Co}_3\text{O}_4$  nanocubes. (e) HRTEM image of a typical nanobelt and (f) HRTEM image of a typical nanocube

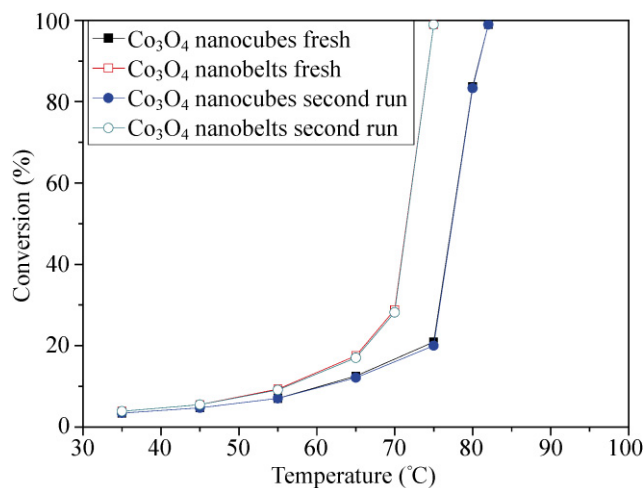
{001}, which are the only planes normal to the set of (220) planes with a lattice spacing of 0.28 nm.

The XRD patterns (Fig. S-1 in the Electronic Supplementary Material (ESM)) show that  $\text{Co}_3\text{O}_4$  nanobelts and nanocubes can be indexed as the fcc phase (space group  $Fd\bar{3}m$ ) with a lattice constant  $a = 8.065 \text{ \AA}$ , which is consistent with the values in the literature (JCPDS# 74-1657).

For the nanobelts, the estimated crystal size of the thickness ( $h$ ) normal to the {011} surface is ca. 17.3 nm according to Scherrer equation. Therefore, the calculated surface area of the nanobelts is ca.  $23.6 \text{ m}^2\cdot\text{g}^{-1}$ , which is close to the experimental BET surface area of  $20.1 \text{ m}^2\cdot\text{g}^{-1}$ . For the nanocubes, the estimated crystal size of the thickness ( $h$ ) normal to the {001} surface is ca. 21 nm according to the Scherrer equation, which is consistent with the size of 20 nm given by HRTEM. The calculated surface area of the nanocubes is  $56.5 \text{ m}^2\cdot\text{g}^{-1}$ , which is higher than the experimental BET surface area of  $22.6 \text{ m}^2\cdot\text{g}^{-1}$ . These results indicate that the nanocubes are probably aggregated, and that there is almost no influence of the cracks and interspaces within the nanobelts.

### 3.2 Catalytic activity

Figure 2 shows the catalytic properties of differently shaped  $\text{Co}_3\text{O}_4$  nanocrystals. For a gas hourly space velocity (GHSV) of  $50\,000 \text{ h}^{-1}$ , the values of  $T_{10}$  (the temperature which gives a 10% CO conversion) for  $\text{Co}_3\text{O}_4$  nanocubes and nanobelts are  $61 \text{ }^\circ\text{C}$  and  $56 \text{ }^\circ\text{C}$ , respectively. The CO conversion is 10% over  $\text{Co}_3\text{O}_4$  nanobelts and 7% over  $\text{Co}_3\text{O}_4$  nanocubes at  $56 \text{ }^\circ\text{C}$ , with the corresponding mass specific rates of conversion of CO being  $0.85$  and  $0.62 \text{ } \mu\text{mol}\cdot\text{g}^{-1}\cdot\text{s}^{-1}$ , respectively, as shown in Table 1. The specific rate of conversion over  $\text{Co}_3\text{O}_4$  nanobelts at  $56 \text{ }^\circ\text{C}$  is therefore 1.37 times higher than that over the nanocubes, indicating that the  $\text{Co}_3\text{O}_4$  nanobelts are significantly more active than  $\text{Co}_3\text{O}_4$  nanocubes. At  $56 \text{ }^\circ\text{C}$ , the TOF of  $\text{Co}^{3+}$  sites on the nanobelts is  $7.4\times 10^{-3} \text{ s}^{-1}$ , whilst it is only  $2.7\times 10^{-3} \text{ s}^{-1}$  for the nanocubes, indicating that the TOF of  $\text{Co}^{3+}$  sites on {011} planes is 2.7 times higher than those on {001} planes. Details of the calculations of the TOF values are given in the ESM. The  $\text{Co}^{3+}$  sites on the nanobelts are far more reactive than those at the nanocubes. No



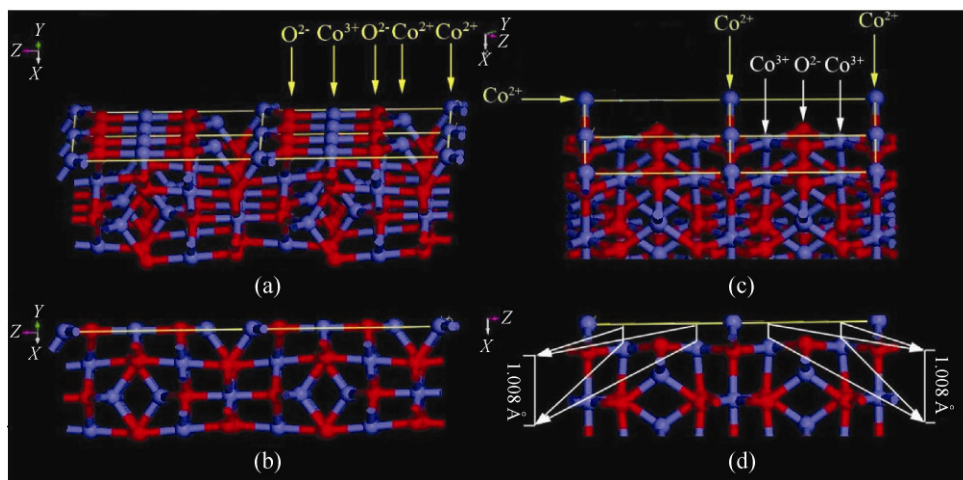
**Figure 2** CO conversion as a function of reaction temperature over  $\text{Co}_3\text{O}_4$  nanobelts and nanocubes at GHSV =  $50\,000 \text{ h}^{-1}$  (reactants are oxygen and CO)

**Table 1** Catalytic properties of  $\text{Co}_3\text{O}_4$  nanobelts and nanocubes

$T_{10}$ ( $^\circ\text{C}$ )	Reaction rate ( $\mu\text{mol}\cdot\text{g}^{-1}\cdot\text{s}^{-1}$ )		TOF ( $\text{s}^{-1}$ )	
	Nanobelts	Nanocubes	Nanobelts	Nanocubes
56	0.85	0.62	$7.4\times 10^{-3}$	$2.7\times 10^{-3}$

deactivation was observed when the  $\text{Co}_3\text{O}_4$  nanocubes and nanobelts were reused in a second run.

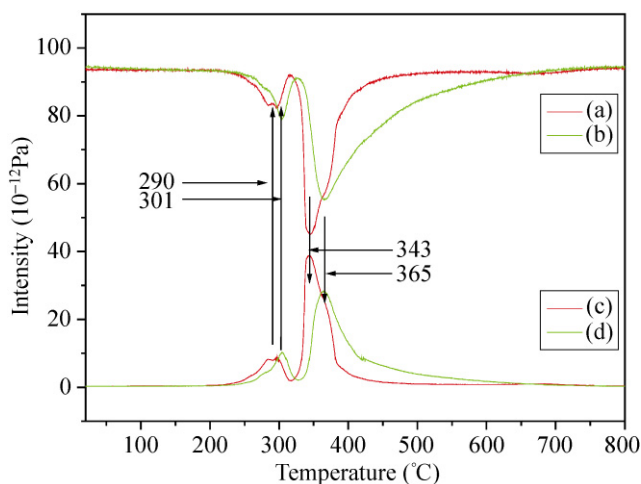
The TOF of the nanoparticles might be an overestimate since the calculations assume that the only active sites are those exposed at the corners and edges of spherical particles with 5%–10% defects [12]. In fact, there are six equivalent {001} planes on nanocubes without defects which expose the first sub-layer of  $\text{Co}^{3+}$  sites to reactant oxygen and CO. The different locations of  $\text{Co}^{3+}$  sites on {011} and {001} planes are expected to lead to a difference in catalytic activity. The active  $\text{Co}^{3+}$  sites in the nanobelts are located on the surface layer of the {011} planes as shown in Figs. 3(a) and 3(b), whereas those in the nanocubes are on the first sub-layer of the {001} plane with a distance of  $1.008 \text{ \AA}$  to the topmost surface layer as shown in Figs. 3(c) and 3(d). In the presence of CO and  $\text{O}_2$ , CO is adsorbed on the  $\text{Co}^{3+}$  sites of  $\text{Co}_3\text{O}_4$ , and surface lattice oxygen is transferred from  $\text{Co}^{2+}$  to  $\text{Co}^{3+}$  leading to the production of  $\text{CO}_2$ , and the resulting oxygen vacancy is subsequently filled by reaction with  $\text{O}_2$  [14]. The adsorption of CO on the first sub-layer of  $\text{Co}^{3+}$  sites is expected to be more



**Figure 3** (a) Surface atoms of the  $\text{Co}_3\text{O}_4$  {011} plane. (b) Horizontal view of the  $\text{Co}_3\text{O}_4$  {011} plane. (c) Surface atoms of the  $\text{Co}_3\text{O}_4$  {001} plane. (d) Horizontal view of the  $\text{Co}_3\text{O}_4$  {001} plane. Atoms highlighted with yellow arrows are located on the surface layer of the plane, and those with white arrows on the first sub-layer of the plane

difficult than on the topmost surface layer of  $\text{Co}^{3+}$  sites, which is consistent with the relative catalytic activities of the nanobelts and nanocubes. Therefore, the location of  $\text{Co}^{3+}$  sites on different planes is the major influence on the catalytic activity to CO.

Figure 4 compares the CO-TPR profiles of  $\text{Co}_3\text{O}_4$  nanobelts and nanocubes obtained by simultaneously monitoring the signals of CO consumption and  $\text{CO}_2$  formation by mass spectroscopy. For  $\text{Co}_3\text{O}_4$  nanobelts, the broader peak centered at 290 °C and the narrower peak centered at 343 °C can be attributed to the reduction of  $\text{Co}^{3+}$  to  $\text{Co}^{2+}$  (step I) and  $\text{Co}^{2+}$  to  $\text{Co}^0$  (step II) [15, 16], respectively. For the reduction of the  $\text{Co}_3\text{O}_4$  cubes, the corresponding peaks shift to 301 °C and 365 °C, respectively. This indicates that the  $\text{Co}_3\text{O}_4$  nanobelts show a higher reducibility than their nanocube counterparts. Surface lattice oxygen is regarded as playing an important role in the reduction reactions [17, 18]. For the nanobelts, there is only one kind of surface layer lattice oxygen in the {011} planes which has a coordination number of three (one  $\text{Co}^{2+}\text{-O}^{2-}$  and two  $\text{Co}^{3+}\text{-O}^{2-}$ ) bonds. For the nanocubes, the first sub-layer lattice oxygen in the {001} planes has the three same bonds in its coordination shell. In the absence of gaseous oxygen, the reduction requires breaking of the lattice oxygen bonds and subsequent reaction with CO. The surface layer lattice oxygen is more easily activated by CO than the first sub-layer



**Figure 4** CO-TPR profiles of  $\text{Co}_3\text{O}_4$  nanocrystals. (a) and (b) are the traces of the CO consumption signals for the  $\text{Co}_3\text{O}_4$  nanobelts and nanocubes, respectively. (c) and (d) are the traces of the  $\text{CO}_2$  formation signals for the  $\text{Co}_3\text{O}_4$  nanobelts and nanocubes, respectively

lattice oxygen, which is a possible reason for the stronger reducing properties of {011} planes compared with {001} planes.

#### 4. Conclusions

CO oxidation has been performed on  $\text{Co}_3\text{O}_4$  nanobelts exposing primarily {011} planes and nanocubes exposing primarily {001} planes. The {011} planes show a higher catalytic activity for CO oxidation than the



{001} planes. The importance of shape and crystal plane effects is highlighted by the fact that the  $\text{Co}^{3+}$  sites on {011} planes are more reactive than those on {001} planes. These findings are of importance in the development of shape-controllable nanocrystal model catalysts and provide guidance for practical heterogeneous catalysis.

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**Electronic Supplementary Material:** XRD patterns of  $\text{Co}_3\text{O}_4$  nanobelts and nanocubes, together with details of the calculations of surface areas and TOF values are available in the online version of this article at <http://dx.doi.org/10.1007/s12274-010-1040-2> and accessible free of charge.

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