# Synthesis of Pd Nanocrystals Enclosed by {100} Facets and with Sizes <10 nm for Application in CO Oxidation

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# ABSTRACT

The catalytic activity of noble-metal nanocrystals is mainly determined by their sizes and the facets exposed on the surface. For single crystals, it has been demonstrated that the Pd(100) surface is catalytically more active than both Pd(110) and Pd(111) surfaces for the CO oxidation reaction. Here we report the synthesis of Pd nanocrystals enclosed by {100} facets with controllable sizes in the range of 6–18 nm by manipulating the rate of reduction of the precursor. UV–vis spectroscopy studies indicate that the rate of reduction of Na<sub>2</sub>PdCl<sub>4</sub> can be controlled by adjusting the concentrations of Br<sup>-</sup> and Cl<sup>-</sup> ions added to the reaction mixture. Pd nanocrystals with different sizes were immobilized on ZnO nanowires and evaluated as catalysts for CO oxidation. We found that the activity of this catalytic system for CO oxidation showed a strong dependence on the nanocrystal size. When the size of the Pd nanocrystals was reduced from 18 nm to 6 nm, the maximum conversion rate was significantly enhanced by a factor of ~10 and the corresponding maximum conversion temperature was lowered by ~80 °C.

# **KEYWORDS**

Palladium, nanocubes, CO oxidation, size-dependence

Palladium (Pd) is a well-known and widely used heterogeneous and homogeneous catalyst with many industrial applications. It can catalyze a large number of reactions, including alkene hydrogenation [1–5], alcohol oxidation [6, 7], trichloroethene hydrodechlorination [8], as well as Suzuki [9, 10], Heck [11], and Stille coupling reactions [12]. Moreover, it can serve as a primary catalyst for the low-temperature reduction

<sup>§</sup> These two authors contributed equally to this work. Address correspondence to xia@biomed.wustl.edu of automobile pollutants [13], petroleum cracking [14], CO oxidation [15–18], and electro-oxidation of formic acid [19–21]. All of these applications rely on the use of Pd nanoparticles or clusters well dispersed on a catalytic support or in a solution.

Over the past decade, ways of controlling the size and shape of Pd nanocrystals have attracted much attention because these two parameters allow one to





tailor their intrinsic properties and thereby enhance their performance in various applications. For example, the conversion efficiency and selectivity of alkynes to alkenes, conjugated alkenes to monoalkenes, and hydrogenation of alkenes are all strongly dependent on the size of Pd nanocrystals [22-26], in particular, in the sub-10 nm regime. On the other hand, it has been demonstrated that the facets on the surface of Pd nanocrystals can have a strong influence on catalytic properties. So far, a wide variety of Pd nanocrystals with different shapes including cubes, bars, octahedra, plates, icosahedra, and pentagonal rods have all been prepared by carefully controlling reaction conditions such as temperature, reductants, capping agents, and concentrations of reagents and ionic species [27-38]. Nanoscale cubes and bars of Pd enclosed by {100} facets have received particular attention because these facets have been demonstrated to have a higher catalytic activity than {111} facets in some important reactions such as CO oxidation [39-45]. To this end, we and other groups have developed a simple strategy for the large-scale synthesis of Pd cubes and bars with sharp corners by introducing Br<sup>-</sup> as a capping agent and by taking advantage of its selective adsorption on {100} facets [27, 28]. Despite the early success, it still remains a great challenge to control the size of the Pd cubes and bars, particularly at scales below 10 nm.

Herein we describe a facile, aqueous approach for controlling the sizes of Pd cubes/bars in the range of 6–18 nm by adjusting the rate of reduction of Pd<sup>2+</sup> ions. The synthesis is based on a water-based process that involves injection of Na<sub>2</sub>PdCl<sub>4</sub> into an aqueous solution of ascorbic acid (AA) held at 80 °C, with Br<sup>-</sup> ions serving as a capping agent and poly(vinyl pyrrolidone) (PVP) acting as a stabilizer. Control over the size of the Pd cubes/bars was achieved by introducing different amounts of halide species such as Br<sup>-</sup> and Cl<sup>-</sup>. Besides capping the {100} facets of Pd nanocrystals, the halide species can also serve as coordination ligands to promote the formation of complexes such as [PdBr<sub>4</sub>]<sup>2-</sup> and [PdCl<sub>4</sub>]<sup>2-</sup> with Pd<sup>2+</sup> ions in aqueous solution, and thus reduce the rate of reduction of the Pd<sup>2+</sup> ions. Since the stability constant of  $[PdBr_4]^{2-}$  is nearly  $10^4$ times higher than that of [PdCl<sub>4</sub>]<sup>2-</sup>, it is clear that Br<sup>-</sup> binds Pd<sup>2+</sup> more strongly than Cl<sup>-</sup> [46, 47]. Therefore,

introducing halide species such as  $Br^-$  and  $Cl^-$  not only results in the formation of Pd cubes/bars due to their selective capping of the {100} facets, but also greatly reduces the rate of reduction of  $Pd^{2+}$  and thus the number of seeds formed in the initial stage. When the amount of the precursor is kept the same, the number of seeds and the size of the final product will be inversely proportional to each other.

In order to clarify the role of Br<sup>-</sup> in controlling the size of Pd nanocrystals, we conducted a set of experiments with different amounts of Br<sup>-</sup> being introduced. Figure 1(a) shows a typical transmission electron microscopy (TEM) image of the product obtained when 300 mg of KBr was added. The cubes/bars were 5 to 14 nm in size as measured by the width. The size distribution derived from the TEM image by counting ca. 150-200 cubes/bars is also plotted in Fig. 1(b). From this plot, the mean size of the Pd cubes/bars was found to be ~10 nm (width =  $9.5 \text{ nm} \pm 4.5 \text{ nm}$ , average aspect ratio = 1.2). When the amount of KBr was increased to 600 mg, we obtained Pd cubes/bars of ~18 nm (width =  $18.0 \text{ nm} \pm 4.3 \text{ nm}$ , average aspect ratio = 1.2) in size, as shown in Figs. 1(c) and 1(d). It is worth pointing out that the formation of Pd cubes/bars was also accompanied by a color change from reddish brown to black. The reaction rate can be estimated from the color change. In the case of 300 mg of KBr, the color change was observed at  $t = 2 \min$ . Further increasing the amount of KBr retarded the color change. With the addition of 600 mg KBr, the color of the solution remained unchanged for 5 min. It is clear that Pd cubes/bars with different sizes can be obtained by simply varying the amount of KBr introduced into the reaction system. As two additional examples, Pd cubes/bars of ~13 nm (width =  $12.6 \text{ nm} \pm 4.3 \text{ nm}$ , average aspect ratio = 1.2) and ~15 nm (width =  $15.4 \text{ nm} \pm 3.7 \text{ nm}$ , average aspect ratio = 1.2) in size were produced when 400 mg and 500 mg of KBr were introduced, respectively (Fig. S-1 in the Electronic Supplementary Material (ESM)).

In general, nanocrystal growth can be separated into two stages: nucleation and growth. The rate of reduction is one of the most important parameters in controlling the nucleation events. When the rate of reduction is high, more seeds will be formed in the nucleation stage. Obviously, more seeds will lead to



**Figure 1** TEM images of samples prepared in aqueous solutions containing 57 mg of  $Na_2PdCl_4$ , 105 mg of PVP, 60 mg of ascorbic acid, and (a) 300 mg of KBr and (c) 600 mg of KBr, and (b, d) the corresponding histograms of particle size distribution. For the cubes/bars, both width and average aspect ratio are used to describe their sizes

the formation of nanocrystals with smaller sizes when the amount of the precursor is kept the same. In this case, reducing the amount of KBr speeded up the rate of reduction of the precursor, and hence reduced the size of the Pd cubes/bars. As a result, one should be able to obtain Pd cubes/bars with smaller sizes (e.g., sub-10 nm) by further reducing the amount of KBr added. When only 5 mg KBr was introduced into the solution, the color changed very quickly, and Pd nanocrystals with a size of ~4 nm were obtained. Unfortunately, the cubic shape of the Pd nanocrystals was not maintained, as shown in Fig. S-2 (in the ESM). The product was dominated by irregularly shaped nanocrystals and a very small amount of cubes/bars, because there were not enough shape-directing ions (i.e.,  $Br^{-}$  ions) to cap the {100} facets. To overcome this problem, we introduced Cl<sup>-</sup> ions into the reaction mixture because Cl<sup>-</sup> can also act as a capping agent for Pd nanocrystals while showing weaker coordination ability for Pd<sup>2+</sup>. In the synthesis of sub-10 nm Pd cubes/bars, the total molar concentration of halide ions was maintained the same as that with 300 mg of KBr, while different ratios of Br<sup>-</sup>/Cl<sup>-</sup> were employed. Figure 2(a) shows a TEM image of the product obtained with the addition of 5 mg of KBr and 185 mg of KCl. In this case, we obtained sub-10 nm Pd cubes/ bars with sharp corners. From the corresponding size distribution histogram (Fig. 2(b)), the average size of the Pd cubes/bars was reduced to ~6 nm (width =  $5.8 \text{ nm} \pm$ 2.2 nm, average aspect ratio = 1.4). The color of the solution started to change at t = 30 s, indicating that the reduction in this case was much faster than the synthesis in which 300 mg KBr was introduced. When the Br<sup>-</sup>/Cl<sup>-</sup> ratio was slightly increased (75 mg of KBr and 141 mg of KCl), the size of the resulting Pd cubes/ bars increased, as shown in Fig. 2(c). According to the size distribution histogram (Fig. 2(d)), the average size of the Pd cubes/bars was 7 nm (width =  $7.3 \text{ nm} \pm 2.8 \text{ nm}$ , average aspect ratio = 1.3). This work represents the first synthesis of sub-10 nm Pd cubes/bars, and this





**Figure 2** TEM images of samples prepared in aqueous solutions containing 57 mg of Na<sub>2</sub>PdCl<sub>4</sub>, 105 mg of PVP, 60 mg of ascorbic acid, and different amounts of KCl and KBr: (a) 5 mg of KBr and 185 mg of KCl, and (c) 75 mg of KBr and141 mg of KCl. (b, d) The corresponding histograms of particle size distribution. The mixtures of halide salts contain the same total number of moles as that of 300 mg of KBr

approach may allow us to reduce the Pd cubes/bars down to even smaller sizes (e.g., 2 nm).

Based on the above observations, it can be concluded that the size of Pd cubes/bars can be easily controlled by varying the rate of reduction of Pd<sup>2+</sup> ions. To better account for the rates of reduction of Pd<sup>2+</sup> ions, UV-vis spectroscopy was employed to monitor the absorbance of the solution at different stages of the reactions for the syntheses of 6-, 10-, and 18-nm cubes/bars. As shown in Figs. 3(a)–3(c), there was an adsorption peak at ~245 nm, which can be attributed to  $[PdCl_xBr_{4-x}]^{2-}$  [48, 49]. The concentration of the Pd precursor can be followed by plotting the change in absorbance at ~245 nm as a function of time (Fig. 3(d)). For the synthesis of 6-nm Pd cubes/bars, the consumption of the Pd precursor was much faster than in the syntheses of larger Pd nanocrystals, confirming that formation of smaller Pd cubes/bars results from a faster reduction rate, and vice versa. This result is also consistent with the observations of color changes. We

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can conclude that the number of seeds formed in the nucleation step can be experimentally controlled by introducing different amounts of halide ions.

The Pd cubes/bars having different sizes were then immobilized onto ZnO nanowires and used for catalytic studies. It was found that the Pd nanocrystals with different sizes showed a similar, well-dispersed distribution on ZnO nanowires (Fig. S-3 in the ESM). The catalytic oxidation of CO was used as a model reaction to examine the catalytic properties of Pd cubes/bars with different sizes. This system is ideal for the study of size-dependent effects in Pd catalysts as the effect of facets can be excluded here. The catalytic test was performed in a fixed-bed reactor (reaction conditions: flow rate 60 mL/min; 100 mg of Pd/ZnO catalyst; 2 wt% of Pd;  $1.01 \times 10^5$  Pa pressure, 1% CO, 20% O<sub>2</sub>, and He balance). Before catalytic testing, all the catalysts were pretreated at 100 °C for 2 h under 10% O<sub>2</sub>/He (60 mL/min) [50]. Figure 4 summarizes the dependence of the CO conversion rate on the reaction



**Figure 3** UV-vis spectra of solutions taken at different reaction stages for the synthesis of: (a) 6-nm, (b) 10-nm, and (c) 18-nm Pd cubes/bars. (d) Time dependence of the absorbance at the peak position (~245 nm), which is directly proportional to the concentration of the [PdCl<sub>x</sub>Br<sub>4-x</sub>]<sup>2-</sup> species in the reaction solution



**Figure 4** CO conversion as a function of temperature for Pd cubes/bars with different sizes supported on ZnO nanowires. Reaction conditions: Pd/ZnO catalyst (100 mg); weight loading of Pd (2%); pressure  $(1.01 \times 10^5 \text{ Pa})$ ; reaction gas (1% CO, 20% O<sub>2</sub>, and He balance)

temperature. The CO conversion over the 6-nm Pd cubes/bars was much higher than that over the 10and 18-nm Pd cubes/bars. Decreasing the size of the Pd cubes/bars enhanced the conversion rate dramatically. The maximum conversion temperature also depends strongly on the sizes of the Pd cubes/bars. For example, for the 6-nm Pd cubes/bars, the maximum conversion temperature was 160 °C, much lower than those for larger Pd nanocrystals. The intrinsic turnover frequency (TOF, defined here as CO conversion per surface Pd atom per second) was also dependent on the size of the Pd cubes/bars (Fig. 5). At a reaction temperature of 140 °C, the TOF of the 6-nm Pd cubes/bars was approximately 3 and 10 times higher, respectively, than those of the 10- and 18-nm Pd cubes/bars. Since the TOF reflects the intrinsic activity of the surface sites, Fig. 5 clearly demonstrates that the size of the Pd cubes/bars strongly influences the nature of the catalytically active sites on the nanocrystals, which is consistent with the previous studies of CO oxidation on a Pd/MgO (100) model catalyst [51]. The dependence of CO oxidation on particle size can also be possibly attributed to other factors, including structural effects,



0.06 0.05 0.04 TOF (s<sup>-1</sup>) 0.03 0.02 0.01 0.00 8 10 12 14 16 18 6 Particles size (nm)

**Figure 5** Turnover frequencies (TOFs) of CO conversion at 140 °C over ZnO-supported Pd cubes/bars with different sizes. The TOF was calculated on the basis of CO molecule per surface Pd atom. Reaction conditions: Pd/ZnO catalyst (100 mg); weight loading of Pd (2%); pressure  $(1.01 \times 10^5 \text{ Pa})$ ; reaction gas (1% CO, 20% O<sub>2</sub>, and He balance)

electronic effects, metal-support interaction, and formation of an active surface oxide layer. Although we need to further investigate the origin of the sizedependent TOF of the Pd cubes/bars for CO oxidation, our results showed unambiguously, for the first time, that the size of the shape-controlled Pd cubes/bars determines their TOF for catalytic CO oxidation reaction.

In summary, we have succeeded in preparing sub-10 nm Pd cubes/bars by controlling the rate of reduction. Using this kinetic approach, the sizes of Pd nanocrystals can be tuned in the range of 6 to 18 nm. We then immobilized the Pd cubes/bars with different sizes onto ZnO nanowires and evaluated their catalytic performance in the CO oxidation reaction. Compared with the 18-nm Pd cubes/bars, the maximum conversion temperature for CO oxidation was 80 °C lower and the TOF was about 10 times higher for the 6-nm Pd cubes/bars, suggesting that smaller Pd cubes/bars may be better for low temperature CO oxidation reactions. Our results clearly show that the size of the Pd cubes/bars enclosed by {100} facets determines the TOF for CO oxidation reactions.

## Experimental

**Synthesis of Pd cubes/bars.** In a typical synthesis of Pd cubes/bars with different sizes, 8.0 mL of an aqueous solution containing poly(vinyl pyrrolidone) (PVP,

 $M_{\rm W} \approx 55\ 000$ , 105 mg, Aldrich), *L*-ascorbic acid (AA, 60 mg, Aldrich), and different amounts of KBr and KCl were placed in a 20 mL vial, and pre-heated in air under magnetic stirring at 80 °C for 10 min. Then, 3.0 mL of an aqueous solution containing Na<sub>2</sub>PdCl<sub>4</sub> (57 mg, Aldrich) was added using a pipette. After the vial had been capped, the reaction was allowed to proceed at 80 °C for 3 h. The product was collected by centrifugation and washed 10 times with water to remove excess PVP.

**Synthesis of the ZnO nanowire support.** We followed the protocol developed by Wang and co-workers for the preparation of ZnO nanowires [52]. In a typical procedure, a mixture of ZnO and carbon powder was placed in a ceramic boat inside a tube furnace, and a Si substrate was placed downstream to collect the ZnO nanowires. The horizontal distance between the source and the substrate was about 2–3 cm. Prior to heating, the quartz tube was purged with Ar gas (99.9%) for 30 min. The tube furnace was heated to 1000 °C for 60 min. After cooling the tube furnace to room temperature, ZnO nanowires were collected from the Si substrate.

**Preparation of Pd on ZnO catalysts.** The preparation of each Pd/ZnO catalyst involved three steps: (1) the ZnO nanowires were dispersed in ethanol by sonication; (2) the as-prepared Pd nanocrystals were added into the solution with vigorous magnetic stirring; and (3) the Pd/ZnO catalyst was collected by filtration, washed with ethanol, and kept in an oven overnight at 100 °C.

**Evaluation of catalytic activity.** The activities of the Pd/ZnO catalysts for CO oxidation were evaluated in a home-made, fixed-bed quartz tubular reactor [53]. The Pd/ZnO catalysts (100 mg, 2 wt% of Pd) were placed in the reactor. The reactant gases (1.0% CO, 20%  $O_2$ , and He balance) were passed through the reactor at a rate of 60 mL/min. The composition of the reaction products exiting the reactor was monitored by a gas chromatography.

**Characterization.** For TEM, the nanocrystals were dispersed in ethanol and then dropped on carbon-coated copper grids. TEM images were obtained using



a Philips 420 transmission electron microscope operated at 120 kV. The concentrations of the catalyst samples were determined using inductively coupled plasma mass spectrometry (ICP-MS) (PerkinElmer Elan DRC II ICP-MS) measurements. For UV–vis characterization, 25  $\mu$ L of reaction solution was diluted with 3 mL 18 M $\Omega$ water, and spectra recorded with a Cary 50 spectrometer (Varian).

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