



Assessing the Influence of Roasting Process Parameters on Mepiquat and Chlormequat Formation in Dark Barley Malts

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Abstract

The aim of this work was to examine the effect of temperature and time on mepiquat and chlormequat pesticides' formation during the barley malt roasting process. The study was conducted for roasting of green malt and kilned malt. The barley used for the study was of the ecological type and verified by us to be free of any quaternary ammonium pesticides. In our study, we observed the formation of chlormequat (CHLM) along with mepiquat (MPQ). Both the compounds share the similarity in quaternary ammonium structure but to the best of our knowledge, it is the first report where CHLM formation has been observed during the roasting process. Additionally, we tried to study the effect of processing parameters (temperature and time) on the quantity of MPQ and CHLM formed during the process, using response surface methods. Additionally, the effect of process parameters (time and temperature) on the color parameter of luminosity (L^*) values was also studied using the response surface methodology. The key factor which determined the amount of compounds produced in the course of roasting was found to be temperature; on the other hand, duration of roasting was observed to be of lesser effect. In the process of roasting dry malt, the CHLM presence was detected at a temperature above 433 K (160 °C), while the MPQ content was found to be present at a temperature above 442 K (169 °C). In the case of green malt, the temperature at CHLM and MPQ content was detected and was found to be higher than kilned malt. We also observed that CHLM formed at lower temperatures and shorter roasting time as compared to MPQ.

Keywords Pesticides · Eco barley · Green malt · Bio beer

Introduction

Chlormequat (CHLM) and mepiquat (MPQ) are common quaternary ammonium pesticides used as plant growth regulators. Their ill-effects in humans and animals have been widely reported and studied (Jones et al. 2013; Nisse et al. 2015; Xiagedeer et al. 2016); hence, the permissible CHLM and MPQ content level in a unit of mass of a barley is 3 and 4 mg/kg, respectively (EFSA 2008; Jones et al. 2013). Some researchers suggest that CHLM introduced into a human body even below this level would affect human reproductive

systems (Torner et al. 1999). Some studies indirectly infer that exposed rats with a low dose of CHLM show an effect on their metabolism (Bonvallot et al. 2014).

Recent works established MPQ as a byproduct of the roasting process of coffee and barley grains and also correlated its presence with a change in color during roasting (Bessaire et al. 2016; Hammel et al. 2014; Wermann et al. 2014). Maillard reaction drove the MPQ formation through to the degradation of lysine (amino acid) in the presence of trigonelline (alkaloid), conjugated with a temperature of typical roasting conditions (Hammel et al. 2014). In addition to MPQ, melanoidins have also been reported to be formed by Maillard-like reactions during the roasting process of Barley and coffee (Bekedam et al. 2008; Moreira et al. 2012; Papetti et al. 2006). These melanoidins are also responsible for color changes during the roasting process (Papetti et al. 2006). Therefore, a close connection between product color changes and MPQ formation can be assumed. From these facts, we can also infer that higher roasting temperature generated higher MPQ content in roasted products as the consequence of non-enzymatic browning reaction. But during analysis of MPQ

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contents in other different cereal products, treated in typical oven conditions, it was found that the MPQ was not formed (Wermann et al. 2014). The conclusion of these observations was that MPQ formation during drying and baking conditions was correlated with baking or roasting temperature but at a temperature below 155 °C MPQ was not formed. A further literature search showed that statistical probability formation of the MPQ compounds in cereals during thermal treatment below 200 °C is extremely low. The MPQ formation process starts at the temperature above 200 °C in cereals containing free lysine (Bessaire et al. 2016). Bessaire et al. (2016) showed that levels of MPQ are not correlated with a^* (CieLab color space) color parameter and well correlated with L^* ($r^2 = 0.62$) and b^* ($r^2 = 0.76$) parameters.

Brewing process itself has been in focus for the presence of pesticides in beer (Bessaire et al. 2016). Brewery malt is one of the basic ingredients necessary for beer production. Dark

malt types are derived by heating malt at the temperatures exceeding 80 °C, generally. In the case of production of special dark malts, the roasting temperature between 160 and 240 °C (Kim et al. 1993) is also used. Two technologies in the production of dark malt can be recognized (Fig. 1a). The first consists of roasting the green malt and with this technology caramel malt is produced. Caramel malts are produced in roasters at temperatures that cause saccharification of green malt (germinated barley) with an initial moisture content of 42–45% (Gruber 2001). The green malt is then moved directly into the roasting drum (Fig. 1c). The second technology involves roasting of dry malt (after kilning) and giving brown, chocolate, and black malts (Fig. 1c). Black malt is produced from dry malt by heating up to 150 to 240 °C for 50 to 90 min. Due to safety reasons in industrial conditions, the final phase involves the injection of a small amount of water. The caramel malt (crystal malt) is produced in a different way; it begins

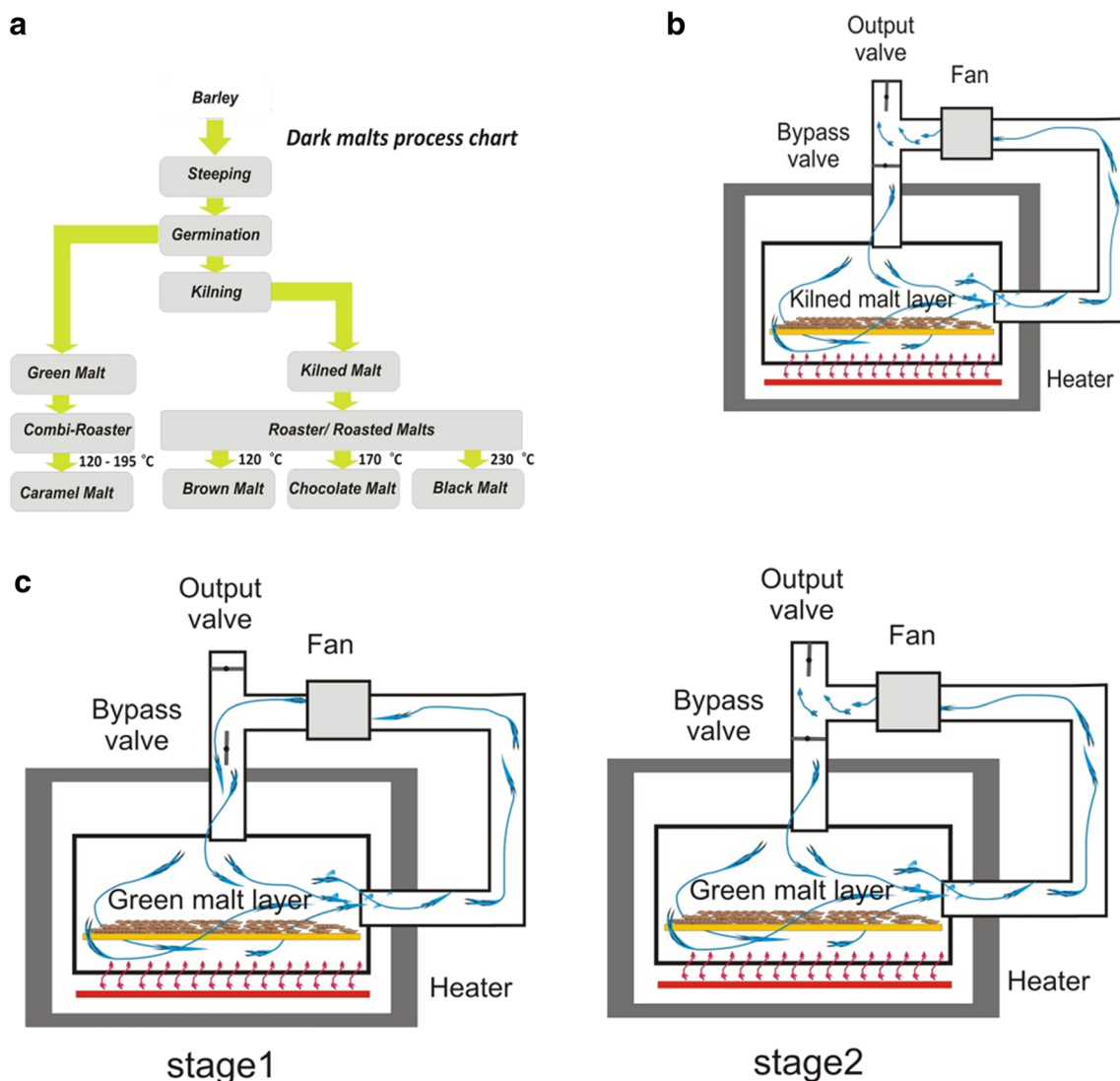


Fig. 1 Dark malt process chart (a), experimental roasted malt production chamber used during experiment (b), two-stage experimental caramel malt production chamber used during experiment (c)

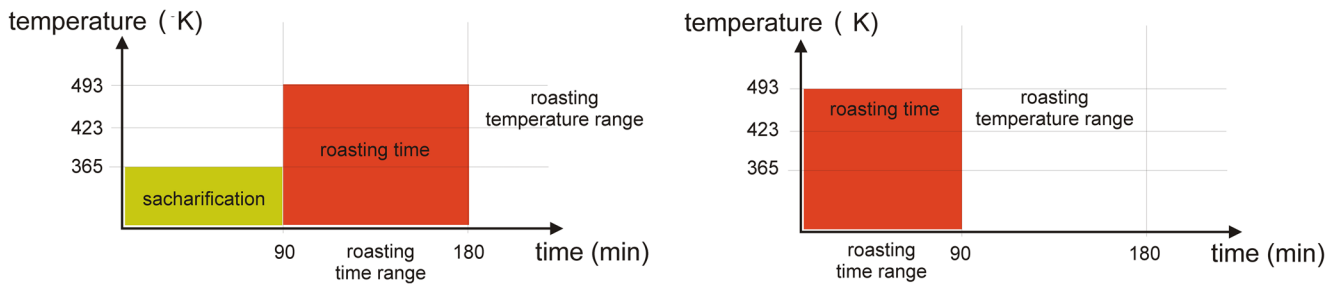


Fig. 2 Temperature and time profile during caramel (left) and roasted dry/kilned (right) malts production process

with the introduction of wet green malt to a sealed drum roaster (above of 38% moisture contents). The product is a long “stewed” at 65 °C for 50–90 min, during which time the drum is sealed to maintain a moist environment. Such conditions are conducive to an extent for the activity of enzymes within the malt. In a particular case, the formation of flavor happens by a prolongation of the enzymes action, which acts by degrading the starch to dextrin and simple sugars. This action increases the concentration of the precursors of the Maillard reaction. After a period of stewing, the window to outlet chamber of the roaster is opened and thereby allowing the gases and steam to pass through the malt causing it to dry and roast. The product is roasted at a temperature of 150 to 200 °C for 90–100 min. The main difference between two types of processing is at first stage, in which product is treating at a relatively high humidity during the initial phase of roasting. Many brewers have also introduced ecological beers to the market. A condition for a beer to be recognized as an ecological beer is the absence of any compound, which is not of natural origin. The processed barley and malt derived from it should not contain any MPQ and CHLM compounds at the limit of detection.

In this study, we report the formation of CHLM along with MPQ during the malt roasting process (for green and kilned malts) and tried it to find the optimal condition of processing parameters for the quantity of pesticide formed using response surface methodology. Impact of process parameters (time and

temperature) on the color lightness parameter (L^*) values were also studied using response surface methods.

Materials and Methods

Sample Preparation

Two groups of malt samples were obtained directly from malt house factory. The tests were carried out by roasting green and dry malt derived from ecological barley. The same ecological barley was used to produce green and dry malt. To recognize and trace malt production, every barley batch was signed of its own batch number. During malt production process, the malt house staff used this batch number to sample identification. Before experimenting the barley, green and dried (kilned) malt was tested for lack of pesticide contamination using the methods reported in “[Chemical Analysis of MPQ and CHLM in Examined Samples](#).” The initial green malt moisture was $42 \pm 1\%$ w/w and dry malt contained 7% w/w water. For the roasting process, the malt samples of weight (1000 g) were used. The experiments were conducted for green malt and dry malt separately with three replications of each. The test sample was placed in the steam oven used as a roaster. For the uniformity of the heat supply, the malt layer did not exceed

Table 1 Experimental design DOE, 3***(2-0), with process variables (coded and uncoded) and experimental results of kilned malt roasted

Trail code	Block	Roasting temperature T (K)		Roasting time t (min)		MPQ (mg/kg)	CHLM (mg/kg)	L^* (–)
		Coded	Uncoded	Coded	Uncoded			
6	2	0	458	–1	10	0*	0.040	27.71
3	1	–1	423	–1	10	0*	0*	74.32
9	3	0	458	0	50	0.014	0.044	18.52
2	1	1	493	0	50	0.42	0.051	1.20
5	2	1	493	1	90	0.44	0.058	1.18
7	3	1	493	–1	10	0.34	0.043	5.24
4	2	–1	423	0	50	0*	0.006	33.29
8	3	–1	423	1	90	0.009	0.009	33.13
1	1	0	458	1	90	0.089	0.051	8.96

*Results below method sensitivity (0.005 mg/kg)

Table 2 Experimental design DOE, 3^{**}(2-0), with process variables (coded and uncoded) and experimental results of green malt roasted

Trail code	Block	Roasting temperature T (K)		Roasting time t (min)		MPQ (mg/kg)	CHLM (mg/kg)	L* (–)
		Coded	Uncoded	Coded	Uncoded			
6	2	0	458	–1	10	–*	0.008	27.71
3	1	–1	423	–1	10	–*	–*	74.32
9	3	0	458	0	50	0.012	0.009	18.52
2	1	1	493	0	50	0.41	0.026	1.20
5	2	1	493	1	90	0.42	0.034	1.18
7	3	1	493	–1	10	0.25	0.022	5.24
4	2	–1	423	0	50	–*	–*	33.29
8	3	–1	423	1	90	–*	0.009	33.13
1	1	0	458	1	90	0.07	0.01	18.52

*Below method sensitivity (0.005 mg/kg)

5–6 mm. It simulated the roasting process conditions of the industrial roasting drums.

Oven temperature range and humidity could be varied between 100 to 300 °C and 0 to 100% respectively. The roasting system used in the experiment was equipped with “close mode,” allowing to carry out the process at a predetermined air humidity (Fig. 2a), or “open mode,” wherein oven working as a roaster in dry conditions (Fig. 2b). The roaster control system was able to control the temperature and air humidity inside the roaster chamber with 3% accuracy. The temperature profile during the roasting for both types of malts can be found in Fig. 2. The green malt roasting contains two stages: before high-temperature roasting, the green malts were stored at 80 °C temperature for 90 min, with 100% environmental humidity. In the next step, roasting at high temperature from 150 to 230 °C was done. Roasting of dry malt was performed at high temperature only (Fig. 2).

Chemical Analysis of MPQ and CHLM in Examined Samples

The analysis of MPQ and CHLM content of unroasted and roasted samples was performed at Research Institute of Horticulture in Skierniewice, Department of Food Safety Research (Accredited laboratory in the Food Safety Research Department, <http://www.pca.gov.pl>), Poland. All

experiments were done using an Agilent 1260 Series LC/MS system (details in Tables 9 and 10). Chlormequat chloride and mepiquat chloride were purchased from Sigma-Aldrich, while mepiquat iodide D3 and chlormequat D4 were obtained from Dr. Ehrenstorfer GmbH (Augsburg, Germany). Other reagents used were acetonitrile LC/MS grade (Merck), formic acid LC/MS grade (Fluka), water LC/MS grade (Merck (Direct-Q)), methanol LC/MS grade (Merck), and ammonium formate (Fluka). The limit of quantification (LOQ) of MPQ and CHLM content was 0.005 mg/kg. The accuracy of the measured values was determined at the 95% confidence level. Individual pesticides' stock solutions containing 1000 µg/mL of the target analytes were prepared by dissolving 25 mg reference standards in 25 mL of methanol and stored in a freezer (≤ -20 °C) and all dilutions were also stored in the refrigerator. Working stock standard mixture in methanol containing 10 µg/mL of each compound was prepared by mixing appropriate quantities of the individual stock solutions. For sample extraction, 5 g of the sample was weighed into a 50-mL Teflon centrifuge tube and 10 mL of water was added to it. The tube was closed and shaken vigorously by a Vortex-type shaker for 5 min. To the same tube, 10 mL of methanol (+1% vol. formic acid) and 50 µL of the internal standard solution were added; the tube was closed and shaken vigorously by a Vortex-type shaker for 30 min. The sample was centrifuged using laboratory centrifuge for 5 min at 7200 rpm.

Table 3 Results of variance analysis of empirical model for MPQ content, determination, and corrected determination coefficients obtained during experiment of kilned malt: $r^2 = 0.82253$. SS sum of squares, *df* degree of freedom, *MS* sum of mean squares, *F* *F* statistics, *p* value of test probability

Source of variation	SS	Df	MS	<i>F</i>	<i>P</i>
Time (t)	0.051698	1	0.051698	6.82699	0.030993
Temperature (T)	0.186963	1	0.186963	24.68960	0.001095
Interaction	0.047556	1	0.047556	6.28010	0.036598
Pure error	0.060580	8	0.007573		
Total sum of squares	0.341359	11			

Table 4 Results of variance analysis of empirical model for CHLM content, determination, and corrected determination coefficients obtained during experiment of kilned malt: $R^2 = 0.7125$ i $R_p^2 = 0.6047$. *SS* sum of squares, *df* degree of freedom, *MS* sum of mean squares, *F* *F* statistics, *p* value of test probability

Source of variation	SS	Df	MS	<i>F</i>	<i>P</i>
Time (t)	0.001988	1	0.001988	12.41666	0.007803
Temperature (T)	0.001018	1	0.001018	6.35965	0.035707
Interaction	0.000241	1	0.000241	1.50655	0.254556
Pure error	0.001281	8	0.000160		
Total sum of squares	0.004456	11			

An aliquot of 0.5 mL of the extract was transferred to a new Eppendorf safe-lock tube and subsequently diluted with 0.4 mL of methanol (+ 1% vol. formic acid) and 100 μ L methanol. The content was vortexed gently and filtered through the 0.22- μ m Teflon filter attached to a syringe directly into amber HPLC vial. Final determination was performed using LC-MS/MS.

For chromatographic and mass spectrometry conditions, please refer to Tables 9 and 10.

Measurement of Color Space Parameter (L^*)

All samples for color space parameters measurement were milled (Bosch MKM 6000 impact mill) and subsequently sieved (sieve size # 0.05, 0.01, 0.15, 0.25, 0.5 mm, DIN ISO 3310-1, vibration amplitude 6 mm, and vibration frequency 2.0 Hz) for 10 min to obtain an average particle size of 100 μ m. Color space parameters were measured using the CIE $L^*a^*b^*$ (CIELAB) color description system of the CIE-Commission Internationale de l'Eclairage (International Commission on Illumination) which is one of the most often used standards for color evaluation (Bessaire et al. 2016; Lee et al. 2013; Ohta and Robertson 2005). The advantage of this method lies in the fact that it utilizes three independent coordinate axes viz. color luminosity (L^*), a^* -(redness-greenness) and b^* -(yellowness-blueness) (Ohta and Robertson 2005).

All measurements were done using a self-fabricated instrument assembly (80 \times 40 \times 40 cm, with inside matte black walls, illuminated with 15 fluorescent lights TL-D De Luxe Pro (Philips), with a color temperature 6500 K). The

colorimeter has undergone the validation process by using the Minolta calibration plate and is approved for this use. The samples were spread on black paper and then photographed in a light chamber equipped with D65 fluorescent lamps using the CCD color camera ac A2500–14uc (5 Mpx, Basler, Ahrensburg, Germany). The visual analysis was done using NI Visio Assistance software, produced by National Instruments. In our research, color changes' parameter (L^*) was used in the range from 0 (pure black) to 100 (pure white).

Response Surface Analysis

In setting up the research plan, the DOE (design of experiment) central composite plan was used. These techniques when applied to experiment design help to reduce the number of trials and save time. The DOE plan is adopted in our experiment to estimate response surface and further to optimize the process parameters in the roaster. In the formation of the central plan, the roasting temperature (RT) limit values of $T_1 = 423$ K (150 $^{\circ}$ C) and $T_2 = 493$ K (230 $^{\circ}$ C) and the roasting time lower time limit $t_1 = 10$ min and an upper limit of $t_2 = 90$ min were adopted. The DOE experiment plan 3**-(2-0) was used; the generated coded data have been presented in Tables 1 and 2.

The generation of response surface plots and statistical analysis was carried out using DOE module in statistical software (Statistica v.2016, StatSoft, USA).

The coded and real values of the independent process variables with design matrix are given in Tables 1 and 2. The

Table 5 Results of variance analysis of empirical model for color parameter (L^*), determination, and corrected determination coefficients obtained during experiment of kilned malt: $r^2 = 0.74542$. *SS* sum of squares, *df* degree of freedom, *MS* sum of mean squares, *F* *F* statistics, *p* value of test probability

Source of variation	SS	Df	MS	<i>F</i>	<i>P</i>
Time (t)	17.176,34	1	17.176,34	20.83619	0.001839
Temperature (T)	2131.56	1	2131.56	2.58574	0.064497
Interaction	80.46	1	80.46	0.09760	0.076271
Pure error	6594.81	8	824.35		
Total square error	25.904,59	11			

Table 6 Results of variance analysis of empirical model for MPQ content, determination, and corrected determination coefficients obtained during experiment of green malt: $r^2 = 0.80615$. *SS* sum of squares, *df* degree of freedom, *MS* sum of mean squares, *F* *F* statistics, *p* value of test probability

Source of variation	SS	Df	MS	<i>F</i>	<i>P</i>
Time (t)	0.0096	1	0.0096	0.945033	0.375634
Temperature (T)	0.1944	1	0.1944	19.13691	0.007191
Interaction	0.007225	1	0.007225	0.711236	0.437508
Pure error	0.050792	5	0.010158		
Total sum of squares	0.262017	8			

Table 7 Results of variance analysis of empirical model for chlomequat content (CHLM), determination, and corrected determination coefficients obtained during experiment of green malt: $r^2 = 0.89377$. *SS* sum of squares, *df* degree of freedom, *MS* sum of mean squares, *F* *F* statistics, *p* value of test probability

Source of variation	SS	df	MS	<i>F</i>	<i>P</i>
Time (t)	0.000088	1	0.000088	3.790303	0.109107
Temperature (T)	0.000888	1	0.000888	38.18246	0.001618
Interaction	0.000002	1	0.000002	0.096728	0.768340
Pure error	0.000116	5	0.000023		
Total sum of squares	0.001094	8			

levels of each independent variable were found according to declared ranges of process parameters.

Results and Discussion

MPQ and CHLM both belong to the quaternary ammonium compound category. For the MPQ formation during roasting processes, two different routes have been proposed in literature. First, in the presence of free lysine, reducing sugar and alkylating agent, a maillard-like reaction leads to the formation of MPQ (Bessaire et al. 2016; Hammel et al. 2014; Wermann et al. 2014). The second route includes the temperature-assisted direct decarboxylation of pipercolic acid and pipercolic acid betaine leading to direct formation of MPQ and piperidine. Piperidine is later converted to MPQ with the help of a methylating agent (Yuan et al. 2017a, b). The color

change during the roasting process (coffee and barley) has also been studied and explained by the formation of melanoidins. The melanoidins are final products of Maillard reaction along with a complex mix of various compounds of different molecular weights and advanced glycation endproducts (AGEs). These chromophores (alone and conjugated) are responsible for the coloration of roasted products. They absorb light at wavelengths as high as 420 nm and are predominantly responsible for the characteristic brown color of roasted food products (Wang et al. 2011). Melanoidins were also reported to be formed by Maillard-like reaction, leading to the color change (Bekedam et al. 2008; Moreira et al. 2012; Papetti et al. 2006). *L** color parameter of roasted products has already been correlated with the quantity of acrylamide and MPQ and results have already been reported, where these products were proposed to be formed via Maillard reaction (Bessaire et al. 2016; Mizukami et al. 2016, 2014).

Table 8 Results of variance analysis of empirical model for color lightness parameter (*L**), determination, and corrected determination coefficients obtained during experiment of green malt: $r^2 = 0.90453$. *SS* sum of squares, *df* degree of freedom, *MS* sum of mean squares, *F* *F* statistics, *p* value of test probability

Source of variation	SS	Df	MS	<i>F</i>	<i>P</i>
Time (t)	539.032817	1	539.032817	6.490359	0.051415
Temperature (T)	2969.93002	1	2969.93002	35.760183	0.001874
Interaction	425.390625	1	425.390625	5.122022	0.073059
Pure error	415.256542	5	83.051308		
Total square error	4349.61	8			

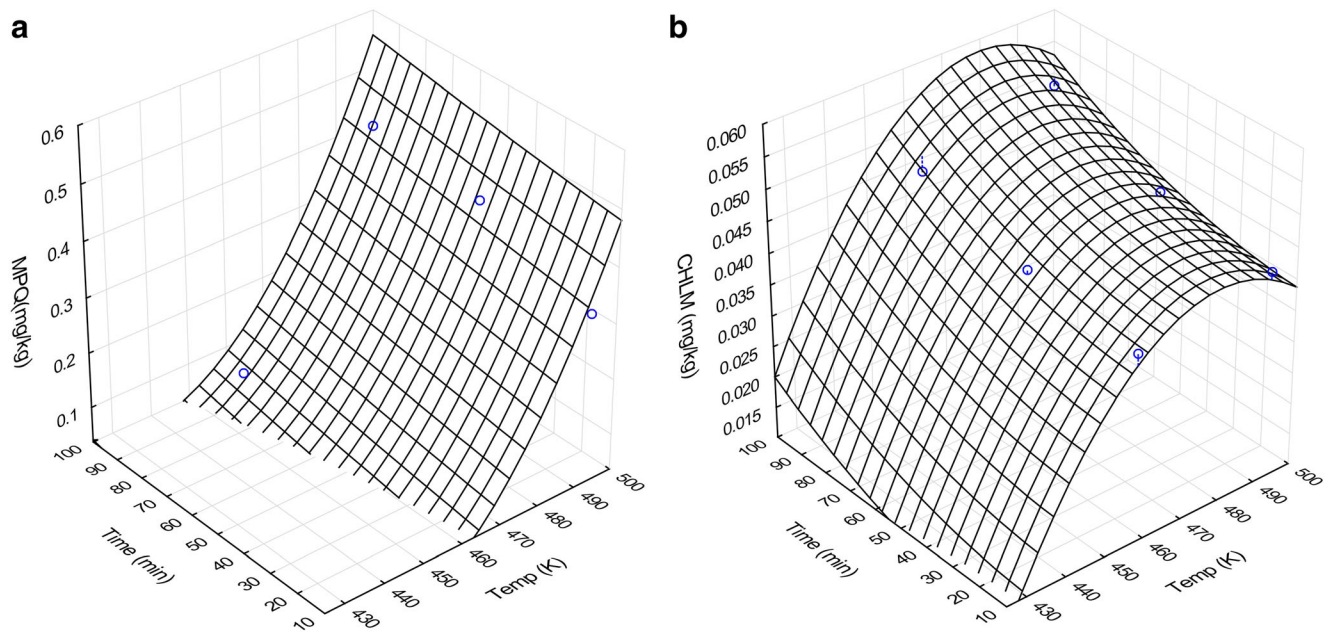


Fig. 3 Response surface diagrams illustrating the effect of temperature and process time on mepiquat (a) and chlormequat (b) contents during roasting the kilned malt

However, in this study, we observed the formation of CHLM along with MPQ. The effect of process parameters has been tried to study for change in L* color parameter. Having said that, though we have tried to understand the effect of process parameters on browning, considering a number of possible chromophore byproducts from Maillard like reaction, it is difficult to conclude anything about quantity of pesticides formed and color parameter (L*). The mechanism of formation of CHLM in the barley roasting process is not the target of

this study, but along with Maillard-like reaction or thermal-assisted direct decarboxylation-like reaction can be hypothesized to be responsible for the CHLM formation. Considering the structural similarity of choline, betaine, and trigonelline with the CHLM, which is in addition to the quaternary amine nature of these compounds, the possibility of Maillard-like reaction to be involved is likely, which is, in addition, the fact that choline, betaine, and trigonelline are commonly found in barley (Corol et al. 2012). The moisture content plays a key

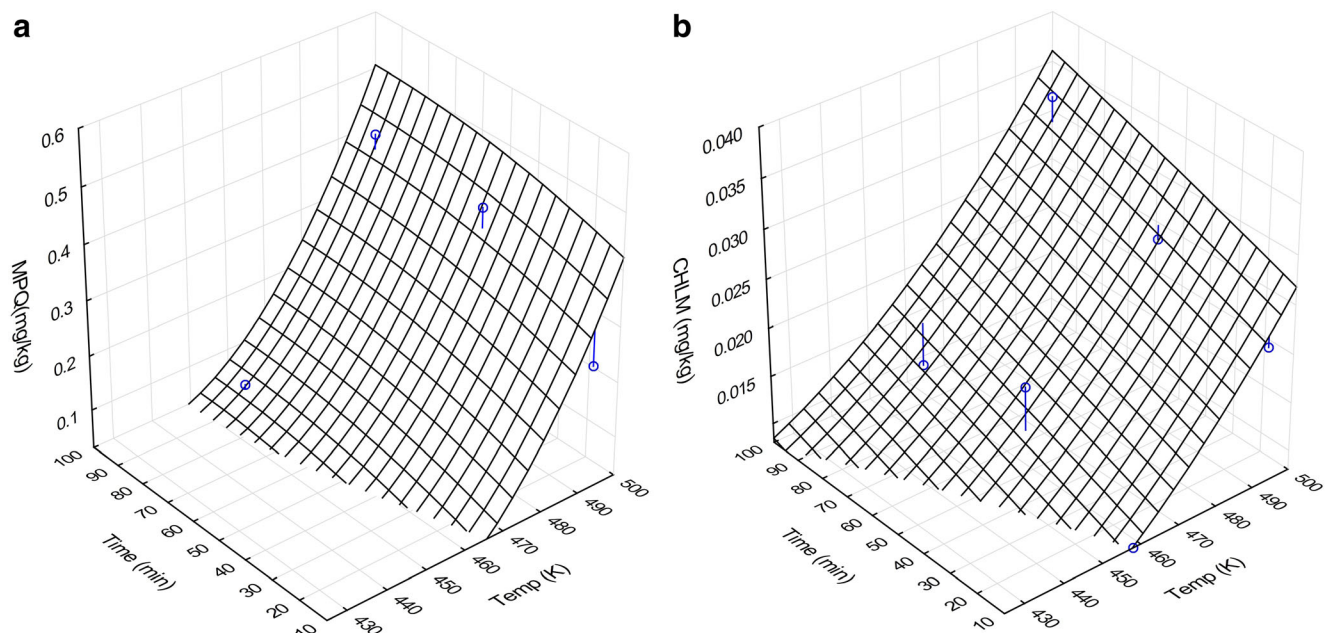


Fig. 4 Response surface diagrams illustrating the effect of temperature and process time on MPQ (a) and CHLM (b), contents during roasting the green malt

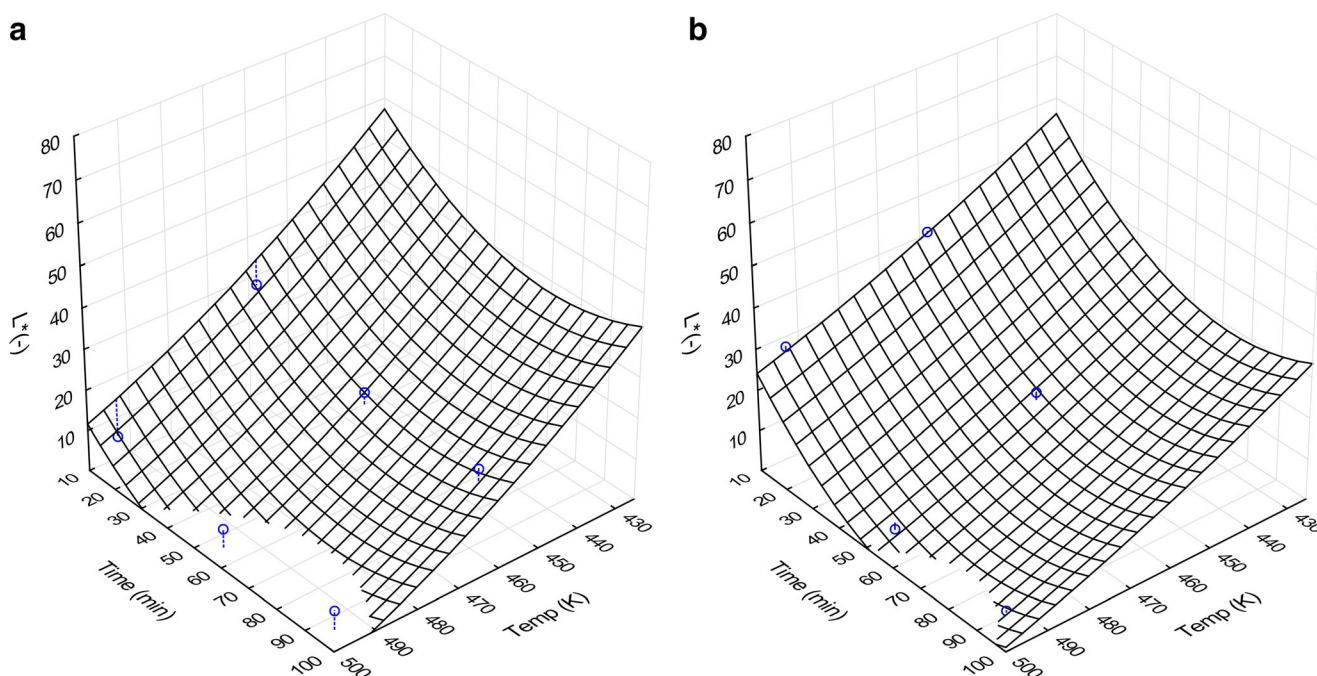


Fig. 5 Color parameter value L^* of milled roasted kilned malt (**a**) and green malt (**b**) with respect to process parameters

role in the expansion of Maillard reaction because water is a major factor during the flavor formation, additionally acting as a solvent and thereby affecting the mobility of the basic compounds taking part in chemical reactions. Therefore, the

roasting of green malt follows a different course of Maillard reaction assisted by water as a solvent as compared to the dry malt, wherein malt roasting at a lower moisture content is dominated by non-enzymatic browning reactions in

Table 9 Chromatographic conditions

Chromatographic conditions				
HPLC system	Series 1200/1260 HPLC (Agilent Technologies) Degasser (G1322A) Binary pump (G1312B) High-performance autosampler (G1367E) Thermostatted column compartment (G1316A)			
Pre-column	Agilent 1290 infinity in-line filter (PN: 5067-4368) with 0.3- μm frit ring installed (PN: 5023-0271)			
Column	HILIC Plus RRHD (Agilent), 100 mm \times 2.1 mm i.d., 1.8- μm particle size			
Column oven temperature	45 $^{\circ}\text{C}$			
Injection volume	2 μL			
Mobile phase	Eluent A: H ₂ O w/20 mM ammonium formate + 0.2% formic acid Eluent B: acetonitrile			
Gradient	Time [min]	% eluent A	% eluent B	Flow [mL/min]
	0	3	97	0.3
	0.3	3	97	0.3
	4	30	70	0.3
	5	60	40	0.3
	7	60	40	0.3
	7.10	3	97	0.3
	15	3	97	0.3
Total analysis time	15 min, post time 3 min			

Table 10 Mass spectrometry conditions

Mass Spectrometry Conditions				
MS system	Agilent Technologies 6460A Triple Quad LC/MS			
Ionisation type	Electrospray (ESI, Agilent Jet Stream, G1958-65138)			
Polarity	Positive ion mode			
Drying Gas Temperature	325 °C			
Drying gas flow	9 (l/min)			
Sheath Gas Heater	350 °C			
Sheath Gas Flow	11 (l/min)			
Nebulizer pressure	40 (psi)			
Capillary voltage	2500 (V)			
Nozzle voltage	0 (V)			
Scan type	MS/MS, Multiple Reaction Monitoring (MRM)			
Time segments	Index	Start Time (min)	Divert Valve	Delta EMV
	1	0	To Waste	0
	2	5.6	To MS	0
	3	7.8	To Waste	0
Scan resolution	MS1- Wide (1.2 amu)/MS2- Unit (0.7 amu)			
Analyte monitored	Ion mass transition monitored (m/z)	Fragmentor (V)	Collision energy (V)	Cell Accelerator Voltage
Mepiquat	114.1→98.2	106	28	4
	114.1→58.2	106	28	4
Chlormequat	122.1→63.1	116	20	4
	122.1→58.1	116	32	4
ISTD Chlormequat-D4	126.1→58.2	108	20	4
	126.1→67.1	108	36	4
ISTD Mepiquat-D3	117.1→101.2	112	28	4
	117.1→61.2	112	28	4

combination to the phenomenon of pyrolysis. The direct decarboxylation without the role of Maillard-like reaction can also be postulated for the formation of MPQ and CHLM in the case of kilned malt.

Quantitative results of the amount of MPQ, CHLM formed, and observed L^* values are presented in Tables 1 and 2. The first order polynomial model was used for two-

factor design. The coded and real value of the independent variables with design matrix is presented in Tables 1 and 2. The values below the minimum limit of quantification/method sensitivity (0.005 mg/kg) are presented as zero. Results of variance analysis of an empirical model for MPQ and CHLM content in green and dried malt are shown in Tables 3 and 4 and Tables 5 and 6 respectively. Results of

variance analysis of ground malt color parameter (*L) in green and dried malt are shown in Tables 7 and 8 respectively.

From Figs. 3a and 4a, it can be seen that the MPQ content increases with increase in temperature from 0 to 0.5 mg/kg. Effect of roasting time is visible at higher process temperatures while there is a very less or even negligible effect of roasting at lower temperatures. The effects of process variables on the CHLM content of roasted malt are presented in Fig. 4b; CHLM was found to be present at lower roasting temperature. Process temperature was the most important factor that affected the CHLM formation, but at higher temperatures, the treatment time starts to be the significant factor. This indicates that the formation of CHLM and MPQ is dependent on the heat supply, not temperature only. As shown in Fig. 5a, b, L* values of milled malt quickly decrease with the increase of process temperature and process time. Higher roasting temperature above 480 K is able to produce the deep dark malt. In the process of roasting dry malt, the CHLM presence was detected at a temperature above 160 °C, while the MPQ content was measurable at a temperature above 170 °C. The roasting of green malt caused an increase in the process temperature at which CHLM and MPQ content was detected (Tables 9 and 10).

Conclusion

This study reports the formation of CHLM and MPQ in barley malt roasting process, although the presence and mechanism of MPQ formation are already reported. It is the first report where CHLM has been identified to be formed during the roasting process. The investigations on the mechanism of CHLM formation are not targeted in this study. The hypothesized mechanism could be Maillard-like reaction or direct decarboxylation reaction similar to MPQ formation. The partial support for this hypothesis arises from structure similarity of trigonelline, choline, betaine, and CHLM and MPQ. This mechanism of CHLM formation certainly needs more investigation to prove the hypothesis. The key factor, which determined the amount of compounds produced in the course of roasting, is temperature; duration of roasting is of lesser effect. A reduction of the duration of roasting at low temperatures may result in incomplete browning of malt grains. It was found that CHLM is a compound, which is synthesized at lower temperatures with a shorter roasting time. In the process of roasting dry malt, the CHLM presence was detected at a temperature above 433 K (160 °C), while the MPQ content was measurable only at a temperature above 442 K (169 °C). Roasting of green malt caused an increase in the process temperature at which CHLM and MPQ content was detected. In the case of roasting green malt, the CHLM content was detected above the roasting temperature of 435 K (162 °C) and roasting time of 30 min. The MPQ content increased above

the detection level in the course of treatment at a temperature of 450 K (177 °C).

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