



Dynamic Effects of a Regulating Valve in the Assessment of Water Leakages in Single Pipelines

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Abstract

Water losses in water distribution systems are typically analysed using extended period simulations, where its numerical resolution is commonly achieved using the gradient method. These models assume that adjustments to regulating valves occur, either manually or automatically, over an extended period of time, then the system inertia can be neglected. This research introduces the development of a rigid water column model for analysing water leakages in single pipelines, which can be employed to account for regulation valve adjustments in shorter time periods, thereby providing greater accuracy when assessing water losses. The application to a case study is presented to analyse pressure variations and leakage flow patterns over 30, 60, and 180 s. A comparison between the extended period simulation and rigid water column model is presented in order to note the order of magnitude on leakages when the system inertia is not considered. The results confirm that is crucial for water utilities the consideration of inertial system to simulate adequately opening and closure manoeuvres in water distribution systems, since according to the case study the extended period simulation can overestimated or underestimated the total leakage volume in percentages of 37.1 and 55.2 %, respectively.

Keywords Leakages · Rigid water column model · Pipelines · Transient flow · Water distribution system

1 Introduction

Water distribution systems (WDS) suffer from leakages causing social and economic costs (Gupta and Kulat 2018) to reduce operation and maintenance costs, water utility compa-

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nies must effectively manage water leakage in their supply systems (Ramos et al. 2023; Conejos Fuertes et al. 2020). These leaks are often caused by excessive pressure or inefficient management by utility companies (Valdez et al. 2016). Because all supply systems eventually suffer from leakages, efficient management is required to effectively identify the origin of leaks (Avila et al. 2021; Asada et al. 2021). Hence, water utility companies must establish pipe-leakage mitigation programmes aimed at improving the service efficiency and decreasing costs borne by water treatment plants, which is of the utmost important for establishing reliable digital twins in water distribution systems (Bonilla et al. 2022; Galdiero et al. 2015). According to the International Water Association (IWA) conventions (Lambert and Hirner 2000), water flow in the supply systems is divided into two types of flows: (i) the flow rate measured, which represents the authorised/billed consumption at households, industries, businesses and institutions and (ii) the uncontrolled flow rate, which is subdivided into apparent losses (customer flow meter inaccuracies, unmetered consumption, unauthorised consumption, water used for fire-fighting and water used for cleaning streets and public areas) and physical losses (leakages).

Leakage occurs in all WDS and depends on network features, the tightness obtained during the construction process, the operation practices of the corresponding water utility companies and the level of technology and expertise used for managing WDS. Water losses vary among different countries and different regions within countries; therefore, the strategy used for mitigating leakage depends largely on the understanding of each component of WDS (Germanopoulos and Jowitt 1989). Because leakage is related to energy costs of WDS, effective leakage control is necessary to ensure social, economic, and environmental sustainability (Bhaduri et al. 2015). If effective measures are not implemented to manage water losses due to leakages, drinking water supply will be insufficient to meet the basic needs of people, thereby increasing costs exponentially. Therefore, studying water-leakage patterns in WDS is necessary for utility companies globally to prevent high distribution costs (Voogd et al. 2021).

Every loss mitigation programme starts with an analysis of the water balance of the WDS being assessed. Next, implementing a mathematical model is necessary for studying the WDS. Herein, water leakage is simulated considering pressure-based consumption. Currently, water flow rates and node pressures in pipes are determined using simulation models for an extended period (quasi-static models), wherein the energy and continuity equations are solved simultaneously using the gradient method (Salgado et al. 1988). Excess water pressure can be reduced and managed by installing pressure reducing valves (PRVs) at specific points and replacing pipe sections to improve hydraulic behaviour, thus realising highly efficient water distribution management (Xue et al. 2022). PRVs help maintain an adequate service pressure throughout the day and specifically at night, reducing the water-leakage volume. Service pressure in WDS, which is indicated by the valve resistance coefficient, is directly related to PRV position. However, the continuous variations in PRV in WDS result in pressure oscillations that cannot be measured using the quasi-static model or extended period simulation (EPS) (Almandoz et al. 2005) because this model does not consider the hydraulic system inertia. The accuracy of the results obtained using the quasi-static model decreases with increasing variations in PRV opening-closure. The occurrence of transient events helps in detecting leakages in a WDS (Brunone et al. 2022). Recently, Ayedet al. (2023) proposed a transient flow model to assess the volume of water leaked from a pipe joint; however, this model failed to consider the water balance of a WDS and did not allow the measurement of water losses based on pressure-based consumption. This study proposes the development of a rigid inertial model (also known as Euler's equation) aimed at assessing water leakage in a WDS. This model can be used to effectively measure pressure pulses produced owing to PRV openings-closures; no deformations are expected to occur in the pipe walls or the

fluid owing to the service pressure in WDS (Coronado-Hernández et al. 2018). The proposed model affords new in the field of water-leakage mitigation in WDS because to the best of our knowledge, no existing study measures pressure variations related to PRV in short time periods. The simulation and numerical calculation on pipeline leakage process was evaluated by Yang et al. (2010), showing the need to analyse the behaviour in other elements of the water systems (i.e., valves, derivations, control elements, among others). Xu et al. (2004) estimated the maximum leakage applied to small circuits, showing the need to analyse the behaviour of the water distribution system. In this line, the novel of this manuscript is based on developing the fundamental method to extrapolate WDS, improving the simulation and calibration of them. Moreover, the proposed model can provide a better understanding of water-leakage volumes and become a more reliable tool than the quasi-static model for utility companies to establish water loss management programmes. Because mitigating water leakage is of utmost importance for utility companies, the development of new mathematical models for leakage assessment is of great interest to the efficiency and sustainability of water companies.

Current mathematical models used for to assess water losses in WDS use quasi-static models to measure water loss volumes during a given period of time, usually 24 hours. These models neglect the system inertia generated owing to local and/or convective velocity. Nevertheless, water utility companies must constrain the service pressure at night to reduce water losses, which requires control-valve operations based on quasi-static models. When rapid variations occur in the operation of control valves, the system inertia can produce variations in the system pressure evolution and consequently in the water leakage. Pressure oscillations caused by variations in control-valve operations can be used to detect leakage and clogged pipes (Brunone et al. 2023). This study proposes algebraic differential equations using the local velocity term to assess water leaks based on the hydraulic system inertia. The proposed model can be used to evaluate water leakages considering opening and closure manoeuvres in single pipelines.

2 Materials and Methods

This section shows the methodology used in this research, which is presented in Fig. 1. The objective of this research is the development of a rigid water column model (RWCM) for computing water leakages in single pipelines, which could be extrapolated to other more complex water systems in future research. The proposal methodology is divided in five steps, as follows:

2.1 Step 1: Model Case Study

A model case study is developed, defining the parameters of the reservoir (i.e., head), pipes (i.e., roughness, length, and diameter) and valves (opening degree and dimensionless coefficient headloss). The development of the model enable the development of the different mathematical model (RWCM model) and topology model in the EPS. The model is completed considered the inputs values, which are focused on the hourly consumption patterns and the base demand of the consumption joints. The input data are required for analysing leakages in water distribution systems, which can be characterized by water utility companies through the installation of flow meters. The definition of topological characteristics of a water installation should be defined (case study).

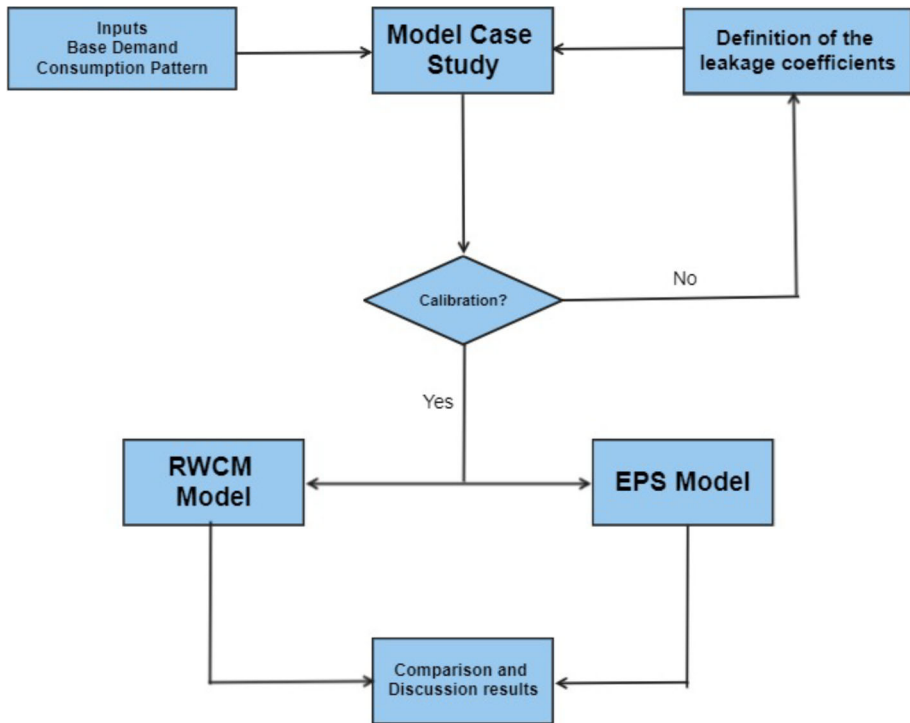


Fig. 1 Methodology

The proposed methodology can be applied to any distribution system and valve type. Therefore, the equations proposed in this research can be extrapolated to any type of valve. However, the application of these models is of interest when the opening or closing of the elements occurs abruptly and quickly.

2.2 Step 2: Definition of the Leakages Coefficients

The leakages should be considered in mathematical models, therefore the different coefficients should be considered. Currently, (1) can be used to evaluate the leakage in each element (i.e., line or tap).

$$Q_{ul} = K_f (p_2 / \gamma_w)^N \quad (1)$$

where Q_{ul} is the leakage flow rate (i.e., line or consumption point), p_2 / γ_w is the pressure head (if the element is a line, the chosen pressure is the average pressure value of the line), N is the leakage exponent, and K_f is the global emitter coefficient.

The leakage volume for a single pipeline is estimated by (2)

$$V_{ul} = \sum_{i=1}^T Q_{ul,i} \Delta t \quad (2)$$

where T is the total time, ΔT is the interval time, and V_{ul} is the leakage volume.

When the flow injected is equal to measured and uncontrolled flow, the calibration is considered correct, and the methodology enable the development of the steps 3 (Section 2.3) and 4 (Section 2.4).

2.3 Step 3: Extended Period Simulation

The EPS has been used for different authors to compute water leakages in WDS (Almandoz et al. 2005; Giustolisi et al. 2008) in the last decades. Usually, EPANET software has been utilised considering the water balance proposed by the IWA (Lambert and Hirner 2000). The Bernoulli equation is used to describe the water movement along an installation. The emitter coefficient (see (1)) must be calibrated. The calibration process finishes when the injected flow rate (measured by a water utility company) gives similar values compared to the results obtained with the mathematical model.

The used emitter coefficient in EPANET is:

$$K_f = \beta l \quad (3)$$

β varies between 10^{-4} and 10^{-7} as a function of the material (cement, steel or PVC) (Maskit and Ostfeld 2014). It grows over time and this increase depends on the material. Different scenarios are defined in this case, which weighted the β value. Besides, N exponent is defined in the calibration model, estimating the value through of normalized valued, which oscillates between 0.5 and 2.5 according to published researches (Maskit and Ostfeld 2014; Van Zyl and Clayton 2007).

In this research, the EPS is modelled for a case study to quantify the water leakages in a single pipeline. For the same case study, the proposed model (RWCM) is also applied (see Section 2.4) to observe the different when manoeuvres in a regulating valve is performed in a short time period.

2.4 Step 4: Rigid Water Column Model

Currently, water leakage assessment models use the Bernoulli equation in extended periods because control-valve operations are performed in a controlled and prolonged manner. Herein, water leakage was determined using the RWCM, which is the main contribution of this research since a mathematical model is developed.

The main assumptions of the proposed model are outlined as follows:

- The mass oscillation equation is employed to monitor water movement.
- The diameter and absolute roughness of pipes remain constant along water installations.
- The friction factor for calculating losses is determined using the Swamee-Jain equation.
- Water leakages are assumed to occur such that pipe and water elasticity effects are negligible during transient events

The mathematical model used to assess leakage in a simple pipe as presented in Fig. 2 uses the water balance expressed as follows:

$$Q_{iny} = Q_m + Q_u \quad (4)$$

where Q_{iny} = injected flow rate (m^3/s), Q_m = flow rate measured (m^3/s), and Q_u = uncontrolled flow rate (m^3/s)

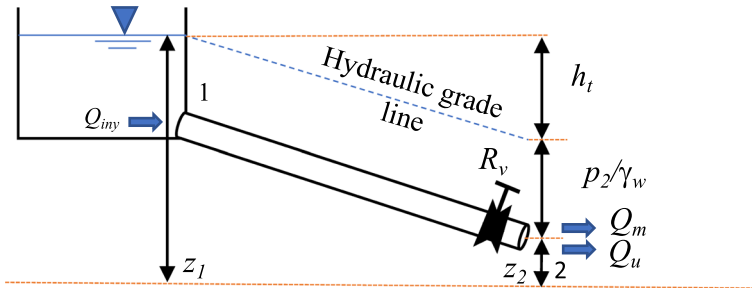


Fig. 2 Simple Pipe Scheme

Considering the main components of the water balance proposed by the International Water Association:

$$Q_{iny} = Q_{md} + Q_{mc} + Q_{mi} + Q_{mo} + Q_{uae} + Q_{uaq} + Q_{uai} + Q_{uah} + Q_{uag} + Q_{ul} \quad (5)$$

where Q_{md} = domestic consumption, Q_{mc} = commercial consumption, Q_{mi} = industrial consumption, Q_{mo} = official consumption (m^3/s), Q_{ua} = flow rate due to apparent losses, Q_{uae} = undetected flow rate due to metering errors, Q_{uaq} = flow rate billed by fixed quota users, Q_{uah} = flow rate by illegal use, Q_{uag} = flow rate used for fire hydrants, Q_{uag} = flow rate used for system flushing, and Q_{ul} = flow rate due to physical leakages.

All flow rate measured consumptions (Q_m) are considered independent of pressure head (p_2/γ_w). These values can be evaluated using a nodal consumption where Q_m can be simulated considering pressure-independent consumption. Downstream, pressure varies over time, so Q_m is determined using (6):

$$Q_m = C_m \overline{Q_m} \quad (6)$$

where C_m = the Q_m modulation coefficient and $\overline{Q_m}$ = the average Q_m .

However, consumption Q_{ul} is dependent on pressure (Almandoz et al. 2005; Giustolisi et al. 2008); that is, the higher the pressure, the higher the consumption and vice versa. Equation 7 demonstrates that water loss is highest at night. For assessment purposes, the emitter exponent was considered to be 0.5, which has been widely adopted by many authors (Almandoz et al. 2005 ;?).

$$Q_{ul} = K_f \sqrt{p_2/\gamma_w} \quad (7)$$

where K_f = emitter coefficient, p_2/γ_w = pressure at node 2 and γ_w = water specific weight.

Substituting (6) and (7) in (5) and disregarding the consumptions from the International Water Association, (8) is obtained:

$$Q_{iny} = C_{md} \overline{Q_{md}} + C_{mc} \overline{Q_{mc}} + C_{mi} \overline{Q_{mi}} + C_{mo} \overline{Q_{mo}} + K_f \sqrt{p_2/\gamma_w} \quad (8)$$

The continuity and momentum equations for a simple pipe are given as follows:

$$\frac{gA}{a^2} \frac{dH}{dt} + \frac{\partial Q_{iny}}{\partial x} = 0 \quad (9)$$

$$\frac{dQ_{iny}}{dt} + gA \frac{\partial H}{\partial x} + \frac{2f Q_{iny} |Q_{iny}|}{\pi d_0^3} + \frac{R_v Q_{iny} |Q_{iny}| d_0^2 \pi g}{4l} + \frac{2 \Sigma k_m Q_{iny} |Q_{iny}|}{\pi l d_0^2} = 0 \quad (10)$$

where f = friction factor, g = gravity acceleration, l = length of pipe (m), A = cross-sectional area of pipe, d_0 = internal diameter of the pipe (m), Σk_m = global coefficient of minor losses, H = hydraulic grade line, and R_v = valve resistance coefficient.

Considering that water leakages tend to reduce the increased pressure in the pipe created owing to automatic variations in PRV operations, the pipe is not expected to suffer deformations and the water column is not expected to be compressed during these variations. Therefore, a rigid pipe is considered, which implies that the wave speed tends to infinity ($a \rightarrow \infty$). Hence, $(\partial Q_{iny}/\partial x = 0)$, thereby demonstrating that the continuity equation is reduced to (11):

$$\frac{\partial Q_{iny}}{\partial x} = 0 \rightarrow Q_{iny} = Q_{iny}(t) = C_{rd}(t)\overline{Q_{rd}} + C_{rc}(t)\overline{Q_{rc}} + C_{ri}(t)\overline{Q_{ri}} + C_{rn}(t)\overline{Q_{rn}} + K_f\sqrt{p_2/\gamma_w(t)} \quad (11)$$

Upon dividing gA in the momentum equation, (12) is obtained:

$$\frac{1}{gA} \frac{dQ_{iny}}{dt} + \frac{\partial H}{\partial x} + \frac{2fQ_{iny}|Q_{iny}|}{gA\pi d_0^3} + \frac{R_v Q_{iny}|Q_{iny}|d_0^2\pi}{4lA} + \frac{2\Sigma k_m Q_{iny}|Q_{iny}|}{\pi l d_0^2 gA} = 0 \quad (12)$$

When integrating a generic t value along a pipe with an area of A between two points with a length of l , then:

$$\left(\frac{1}{gA} \frac{dQ_{iny}}{dt} + \frac{2fQ_{iny}|Q_{iny}|}{gA\pi d_0^3} + \frac{R_v Q_{iny}|Q_{iny}|d_0^2\pi}{4lA} + \frac{2\Sigma k_m Q_{iny}|Q_{iny}|}{\pi l d_0^2 gA} \right) \int_1^2 dx + H_2 - H_1 = 0 \quad (13)$$

After integrating and rearranging the terms:

$$H_1 = H_2 + \frac{l}{gA} \frac{dQ_{iny}}{dt} + \frac{2flQ_{iny}|Q_{iny}|}{gA\pi d_0^3} + \frac{R_v Q_{iny}|Q_{iny}|d_0^2\pi}{4A} + \frac{2\Sigma k_m Q_{iny}|Q_{iny}|}{\pi d_0^2 gA} \quad (14)$$

Finally, when assessing energies at points 1 and 2, thus:

$$z_1 = z_2 + \frac{p_2}{\gamma_w} + \frac{4l}{g\pi d_0^2} \frac{dQ_{iny}}{dt} + \frac{8flQ_{iny}|Q_{iny}|}{g\pi^2 d_0^5} + R_v Q_{iny}|Q_{iny}| + \frac{8\Sigma k_m Q_{iny}|Q_{iny}|}{g\pi^2 d_0^4} \quad (15)$$

where z = corresponds to an elevation of the pipe profile.

This equation simulates water behaviour based on the RWCM (Coronado-Hernández et al. 2018). By replacing the terms and solving (15):

$$\frac{dQ_{iny}}{dt} = \frac{(z_1 - z_2 - \frac{p_2}{\gamma_w})g\pi d_0^2}{4l} - \frac{2fQ_{iny}|Q_{iny}|}{\pi d_0^3} - \frac{R_v Q_{iny}|Q_{iny}|g\pi d_0^2}{4l} - \frac{2\Sigma k_m Q_{iny}|Q_{iny}|}{\pi l d_0^2} \quad (16)$$

The friction factor can be determined using the Swamee-Jain formula.

$$f = \frac{0.25}{\left[\log\left(\frac{k_s}{3.7d_0}\right) + \frac{5.74}{Re^{0.9}} \right]^2} \quad (17)$$

where k_s = absolute roughness of a pipe and Re = Reynolds number.

The Reynolds number is defined by relationship $\frac{v_w d_0}{\nu}$, where v_w = water velocity (injected flow rate) and ν = kinematic viscosity.

2.5 Step 5: Comparison and Discussion Results

This step considers the assessment of water leakages using different typical behaviours and applications of the EPS and RWCM. The RWCM surpasses EPS by incorporating the system inertia term ($\frac{dQ_{iny}}{dt}$), essential for accurately simulating rapid maneuvers induced by regulating valves. Conversely, the EPS overlooks this crucial term. The analysis shows the discrepancies on the estimation of volume leakages for a case study considering domestic and industrial consumption patterns.

The next section presents the application of the used methodology to a case study.

3 Analysis of Results

In order to assess changes in water leakage, the following characteristics of a simple pipe has been considered: $l = 1300$ m, $d_0 = 300$ mm, $k_s = 0.0015$ mm, $\Delta z = z_1 - z_2 = 45$ m, $\Sigma k_m = 5$, and $R_v = 210$ ms²/m⁶. For this analysis, a kinematic viscosity (ν) of 1×10^{-6} m²/s was considered. To perform the water balance, the following data were obtained: $\bar{Q}_{iny} = 140.0$ l/s and $\bar{Q}_r = 91.0$ l/s (with $\bar{Q}_{md} = 75.5$ l/s and $\bar{Q}_{mi} = 15.5$ l/s). Figure 3 shows the modulation coefficients for domestic and industrial consumption. For the domestic consumption, the peak coefficient is found from 9:00 to 10:00 h, while the minimum coefficient of 0.1 is detected between 4:00 to 6:00 h. For the industrial consumption, the maximum and minimum values

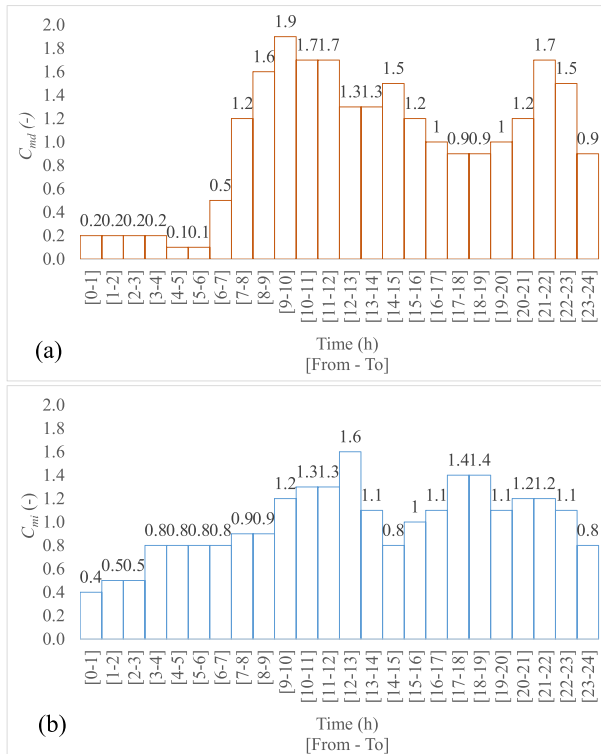


Fig. 3 Modulation Coefficients: (a) Domestic consumption; and (b) Industrial consumption

are 1.6 (12:00 to 13:00) and 0.4 (0:00 to 1:00), respectively. The case study considered is a classical urban supply model that considers flow variations over time with an urban consumption pattern used in different journal publications. This implies its representativeness in the analysis of results for real cases.

The water balance has been addressed considering a domestic and industrial consumptions and the water leakage. In this sense, (8) can be reduced as:

$$Q_{iny} = 75.5C_{md} + 15.5C_{mi} + K_f\sqrt{15} \quad (18)$$

The EPS was run to know the water behaviour over 1 day. The input parameters were determined by solving (8), (16) and (17) considering a zero local velocity ($dQ_{iny}/dt=0$). An emitter coefficient (K_f) of 9.29 l/s/wmc^{0.5} was previously calibrated. The water flow in the entrance of the single pipeline was at $t = 0$ h for 79 l/s, which were considered as the initial conditions for the mathematical model. Figure 4 shows the results obtained from applying the EPS. The maximum pressure is 39.5 m, occurring from 4:00 to 6:00 a.m. For this period, the highest water leakage of 59.1 l/s is reported. The highest flow in the water treatment plant is 197.3 l/s (from 9 to 10 am) and the minimum is 79 l/s (from 4 to 6 am). The EPS represents leaked flow patterns effectively.

Since water utilities need to control downstream pressure head, then a value of 15 m was imposed in the pressure reducing valve (PRV). The EPS was run using a PRV, which is named as EPS-PRV. If $\frac{p_2}{\gamma_w} = 15$ m, then the resistance coefficient (R_v) can be computed using (19):

$$R_v = \frac{z_1 - z_2 - \frac{p_2}{\gamma_w}}{Q_{iny}|Q_{iny}|} - \frac{8fl}{g\pi^2d_0^5} - \frac{dQ}{dt} \frac{4l}{Q_{iny}|Q_{iny}|g\pi d_0^2} - \frac{8\Sigma k_m}{g\pi^2d_0^4} \quad (19)$$

The RWCM was simulated using formulations 8, 16, and 17. A regulating valve is manipulated for two scenarios: (i) considering an opening manoeuvre (RWCM-Opening) with a minimum R_v value of 9000 ms²/m⁶ (at 30 s); and (ii) a closure manoeuvre (RWCM-Closure) with a maximum value of 210 ms²/m⁶ (at 30 s). Figure 5 presents the simulation during the first 180 s for the EPS, EPS-PRV, RWCM-Opening, and RWCM-Closure. Figure 5a shows

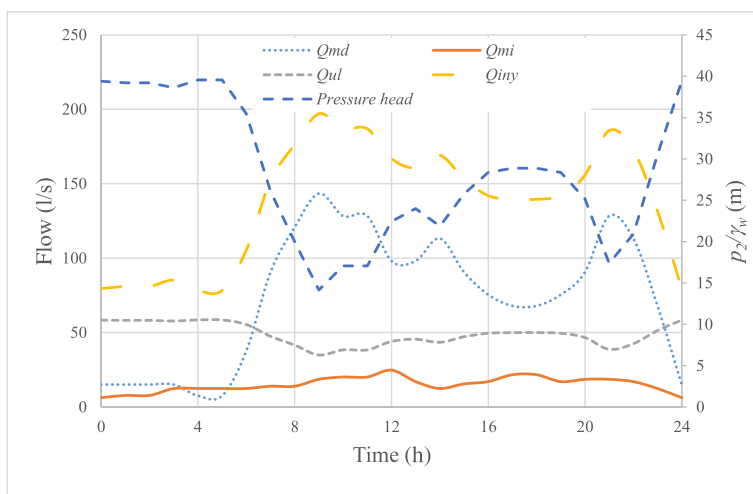


Fig. 4 Analysis of the water balance under an EPS

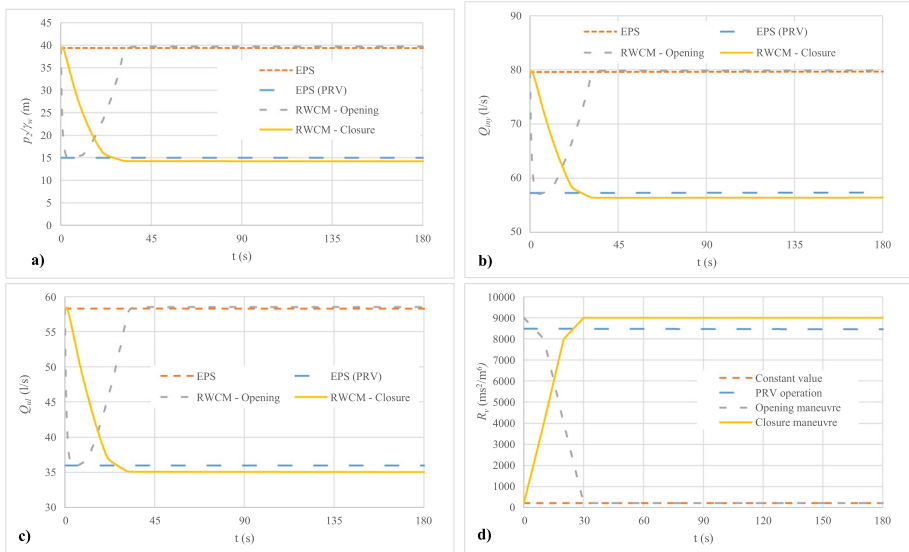


Fig. 5 Comparison between EPS, EPS-PRV, RWCM-opening, and RWCM-Closure models: (a) Pressure head; (b) Injected flow rate (Q_{iny}); (c) Physical leakages (Q_{ul}); and (d) Resistance coefficient (R_v)

the behaviour of pressure head for the different simulations, where the EPS trends to a constant value of 39.4 m for the analysed period. Similarly, the EPS-PRV provides a constant value of 15 m, as expected for the function imposed by the valve. The RWCM-Opening starts at 39.7 m ($t = 0$ s), but after the opening of the regulating valve, the pressure head reaches a constant value of 38.68 m at $t = 38.5$ s. For the RWCM-Closure, the pressure head attains its minimum value after the closure manoeuvre (30 s) with a value of 14.26 m. The injected flow has also different patterns considering the analysed simulations (Fig. 5b). The total flow presents a constant value of 79.6 l/s for the first 180 s (EPS), while the EPS-PRV shows a reduction of 22.3 l/s in comparison to the EPS, since a constant value of 57.3 l/s is detected by the model. Considering the results of the RWCM-opening, the minimum injected flow is reached at 5 s with a flow of 57.1 l/s. After 38.5 s, the injected flow trends to a constant value of 79.8 l/s. The injected flow attains a minimum value of 56.4 l/s (at $t = 35.5$ s) for the RWCM-Closure. The behaviour of water leakage (Q_{ul}) is similar to the behaviour of injected flow (Q_{iny}) since domestic and industrial consumption are not varying for this period, as shown in Fig. 5c. Figure 5d presents the variation of the resistance coefficients (R_v) analysed for the current simulations. The proposed model and the EPS trend to give similar results after the total opening or closure of the regulating valve (at $t = 38.5$ s).

Table 1 presents the leakage volumes computed for periods of 30, 60, and 180 s. As expected, the EPS gives the greatest leakage water volume compared to the other simulations. Considering the first 30 s (see Fig. 5) the leakage volume computed for the EPS is 1.75 m³. The minimum values of leakage volume are obtained with the EPS-PRV, where for a total time of 180 s, a leakage water volume of 6.49 m³ is computed. The EPS and EPS-PRV cannot detect opening and closure manoeuvres of regulating valves, which are represented as RWCM-Opening and RWCM-Closure, respectively. For time periods of 60 and 180 s, the RWCM-Opening provides higher leakage water volume compared to the RWCM-Closure. The RWCM-Opening underestimated the total water volume of leakages in percentages ranging from 4.0 to 25.7 % from the EPS, while RWCM-Closure presents values from

Table 1 Analysis of leakage volume for different periods

Simulation type	TV(m ³)			Percentage of EPS (%) ¹			Percentage of EPS-PRV (%) ²		
	30 s	60 s	180 s	30 s	60 s	180 s	30 s	60 s	180 s
EPS	1.75	3.50	10.49	-	-	-	-	-	-
EPS-PRV	1.10	2.18	6.49	-	-	-	-	-	-
RWCM-Opening	1.30	3.05	10.07	25.7	12.9	4.0	-18.2	-39.9	-55.2
RWCM-Closure	1.34	2.39	6.60	23.4	31.7	37.1	-21.8	-9.6	-1.7

where TV represents the total water volume for leakages for the analysed simulation type

¹ Percentages regarding the RWCM are calculated based on the EPS

² Percentages regarding the RWCM are calculated based on the EPS-PRV

23.4 to 37.1 %. When the PRV is acting, under EPS-PRV, the RWCM-Opening showed an overestimation of the total water volume varying from 18.2 to 55.2 %. The RWCM-Closure provided values with percentages from 1.7 to 21.8 % from the EPS-PRV. When the inertia system is not considered, then the EPS does not estimate accuracy the total water leakages when regulating valve are acting for short time periods. Thus, the RWCM plays an important role to quantify the total water leakages for these kind of manoeuvres.

Addressing more accurate modelling of leakage when regulating elements act in distribution systems will allow network managers to improve real technical indicators of operation, energy efficiency and address economic evaluations with greater rigour that can provide a rigorous assessment and can establish implications with the evaluation of the different targets of the sustainable development goals.

This research introduces a pioneering method for analysing water leakages in single pipes, offering valuable insights for decision-making concerning the operation of regulating valves during opening and closure manoeuvres, an aspect currently overlooked in the existing model. The proposed model is based on physical formulations, then it holds relevance across diverse installations. Future investigations should focus on mathematically formulating water volume leakages utilizing the RWCM for series, parallel, and more intricate network configurations.

4 Conclusions

In this study, a mathematical model to simulate the behaviour of water-leakage flow considering the RWCM was developed. The proposed model is more effective compared to the EPS since it is suitable to represent rapid manoeuvres in regulating valves. The proposed model was applied to a case study where domestic and industrial consumptions were reported. The initial condition of the mathematical model is the one obtained from the EPS. For the assessment, the emitter coefficient was calculated using the results of the quasi-static model. The numerical resolution of the algebraic-differential system provides a satisfactory solution to the water-leakage flow problem because the resolution satisfies the condition that states the water-leakage flow increases with pressure and vice versa. The proposed model can represent pressure head and leakages flow rate pulses for short and large time periods, which could be applied in more complex water systems. This study confirmed that the system inertial will have substantial influence on the water-leakage flow, thus yielding results that can be substantially different from those obtained using the EPS. When opening and closure manoeuvres are performed, then discrepancies between 4.0 to 25.7 % and 23.4 to 37.1 % are found regarding the EPS for the analysed case study. The implementation of the proposed

model can be considered for developing digital twins approaches in water improving the sustainability management of the water systems.

It is crucial to highlight that the proposed model holds significant importance for water utilities, enabling the computation of water volume leakages under specified scenarios where system inertia resulting from the operation of regulating valves occurs, a capability absent in the EPS. Accurately determining water volume leakages is essential for comprehending the interplay between water and energy in water distribution systems.

5 Notation

The following symbols are used in this paper:

A	cross-sectional area of pipe (m^2);
C_m	modulation coefficient (-);
C_{md}	modulation coefficient for a domestic consumption (-);
C_{mi}	modulation coefficient for an industrial consumption (-);
d_0	internal pipe diameter (m);
f	pipe wall friction coefficient (-);
Σk_m	global coefficient of minor-loss (-);
K_f	emitter coefficient ($\text{m}^3/\text{s}/\text{m}^{0.5}$);
k_s	absolute roughness (m);
g	gravity acceleration (m/s^2);
H	hydraulic grade line (m);
l	pipe length (m);
N	leakage exponent (-);
p_2	downstream pressure head (Pa);
Q_{iny}	injected flow rate (m^3/s);
Q_m	flow rate measured (m^3/s);
Q_u	uncontrolled flow rate (m^3/s);
Q_{md}	domestic consumption (m^3/s);
Q_{mc}	commercial consumption (m^3/s);
Q_{mi}	industrial consumption (m^3/s);
Q_{mo}	official consumption (m^3/s);
Q_{ua}	flow rate due to apparent losses (m^3/s);
Q_{ul}	flow rate due to physical leakages (m^3/s);
Q_{uae}	undetected flow rate due to metering errors (m^3/s);
Q_{uaq}	flow rate billed by fixed quota users (m^3/s);
Q_{uag}	flow rate by illegal use (m^3/s);
Q_{uah}	flow rate used for fire hydrants (m^3/s);
Q_{uaf}	flow rate used for system flushing (m^3/s);
R_v	resistance coefficient of a regulating valve (m^2/s^6);
R_e	Reynolds number (-);
t	time (s);
T	simulation time (s);
x	distance along a pipeline (m);
V_{ul}	leakage volume (m^3);
z	elevation (m);
γ_w	water unit weight (N/m^3);

v_w water velocity (injected flow rate) (m/s);
 ν kinematic viscosity (m^2/s);
 ΔT interval time (s);

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Declarations

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