## **ORIGINAL PAPER**



# Novel Composite Films Based on Acrylic Fibers Waste/Nano-chitosan for Congo Red Adsorption

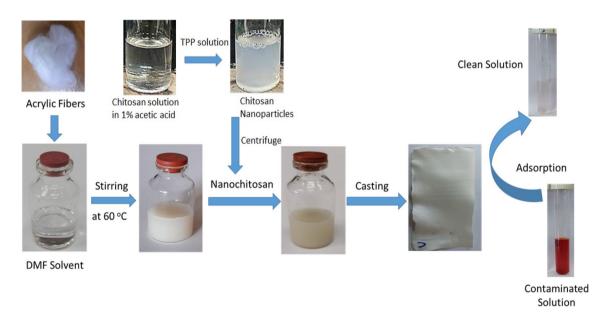
Salah E. Selim<sup>1</sup> · Gamal A. Meligi<sup>2</sup> · Ahmed E. Abdelhamid<sup>3</sup> · Mahmoud A. Mabrouk<sup>1</sup> · Ahmed I. Hussain<sup>3</sup>

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## Abstract

The current research aimed to use waste to treat waste; to recycling of acrylic fibers waste combined with nano-chitosan for use as an adsorbent to remove Congo red (CR) from wastewater. Acrylic fibers (AF) waste were mixed with nano-chitosan (NCh) with different ratios and converted into films by using phase inversion method to prepare two nanocomposites films coded, AF-NCh and AF-NCh-Epichlorohydrin. The nanocomposites films have been characterized using; Fourier transform infrared, scanning electron microscope, surface area, and thermal analysis. The results revealed successful incorporation of NCh into AF matrix with highly porous structure. Different parameters affecting adsorption efficiency such as, CR concentrations, adsorbent dose, effect of time and pH were employed. Adsorption isotherms and kinetic studies evaluations were applied to assess the adsorption mechanism and rate. Results declared that, the maximum adsorption capacities of AF-NCh and AF-NCh-Epichlorohydrin were 169 and 230 mg/g respectively. The adsorption isotherm and kinetic mechanism obey Langmuir and pseudo second order models. Regeneration of the synthesized composite films were studied for five cycles and showed relative stable reading with high efficiency.

## **Graphical Abstract**



Keywords Acrylic fiber  $\cdot$  Nanochitosan  $\cdot$  Composite film  $\cdot$  Water treatment  $\cdot$  Congo red

Salah E. Selim salah@eaeat.edu.eg

Extended author information available on the last page of the article

## Introduction

Synthetic dyes are used in a variety of industries, including leather, paper, and textiles, because of their colorgiving properties. Each year, it is estimated that 700,000 tons of various colorants are produced from approximately 100,000 commercially available dyes [1–3]. Azo dyes are complex aromatic compounds and they are a major environmental concern because the reductive cleavage of azo linkages results in the formation of amines, which are toxic and carcinogenic [4]. Congo red (CR) dye is a benzidinebased anionic diazo dye (1-naphthalenesulfonic acid, 3,3'-(4,4'-biphenylenebis(azo))-bis(4-amino) disodium salt), and it was reported as carcinogen and affect the aquatic life [5, 6]. Numerous studies are currently being conducted to determine the best dye removal process, so that dye wastewater can be recovered and reused [7–9].

Existing dye removal methods can be classified into biological, chemical, and physical processes such as; coagulation, flocculation, chemical oxidation, photochemical degradation, membrane filtration, biological degradation and adsorption are mostly techniques used for removing dyes from an aqueous medium [10]. However all of the methods mentioned above, have some disadvantages, and none of them have been effective in completely removing dye from wastewater [11]. The most economic and environmental effective method is the physical one as it didn't involve using of toxic chemicals and didn't leave toxic byproducts. Physical techniques used in the dye removal process can be divided into membrane based technique and adsorption. Adsorption process is considered one of the most favorable technique because its remarkable ability to remove most types of dyestuff in addition to its simplicity and efficiency and reusability [12–16]. Numerous types of adsorbents have been employed for water treatment. Activated carbon is one of the most widely used adsorbent for dye removal [17–21]. Biopolymers as chitosane and nanochitosane and their composites were used as a prominent adsorbent for heavy metals and CR removal [22-30]. Different nanomaterials and nanocomposites have been used in a variety of science applications such as biomedical and environmental, especially as dye's adsorbants [31–40].

Another class of materials are the fuzzes and fibers waste that produce from textile industry can cause environmental problem issues. As a result, researchers have attempted to use fibres waste in several application as concrete and soil reinforcement, as well as in the adsorption process but after chemical treatment. Acrylic fibers mainly composed of at least 85% acrylonitrile and the remaining another acrylic monomer. However, there are limited research paper dealing with the recycling of acrylic fibers waste for water remediation application. Lehia and Akbari used acrylic fibers and fuzzes wasted in carpet industries to prepare adsorption membrane for removing Persian Orange X from textile effluents [41]. Poly acrylonitrile Nanofiber materials have been recently used as CR adsorbent and heavy metal removal [42–45]. Also modified acrylic fiber waste have been recently used for removal CR, methylene blue and uranium, thorium from liquid waste solution [46, 47].

This research work was aimed to prepare novel nanocomposites films based on commercial acrylic fibers waste as a polymer matrix incorporated with a highly adsorptive nanomaterials; nanochitosane and their study in adsorption of CR from aqueous solution. Different parameters affecting the adsorption efficiency such as CR concentrations, adsorbent dose, effect of time and pH were investigated. Also kinetic study and isotherm of adsorption process were studied. Also many cycles of film reuse were investigated to assess the adsorption stability.

## **Experimental**

#### Materials

Acrylic fiber waste (AF) consisting of at least 85% polyacrylonitrile as a major constituent and the residual mainly vinyl acetate or methyl acrylate copolymer. AF waste was obtained from local textile industry. Congo red dye was supplied from Alpha Aeser, India, Commercial Chitosan of low molecular weight (150 kDa), Trisodium polyphosphate (TPP), Epichlorohydrin (EPH) and Dimethylformamide (DMF) were purchased from Sigma Aldrich, USA. Hydrochloric acid and Sodium hydroxide and other solvents were supplied from El-Nasr Company Egypt.

#### Preparation of Nanochitosan

Nanochitosan was synthesized according to ionic gelation method using TPP as crosslinking agent [48]. Briefly, one gm of chitosan was dissolved in 200 ml of 1% of acetic acid, then 0.66 of TPP was dissolved in 100 ml of distilled water and added drop wise to chitosan solution under constant stirring. The solution was turned onto turbid suspension indicating the formation of nanoparticles. The suspension was left under stirring for another one an hour after complete addition step. The nanochitosan was separated using centrifuge at a maximum of 10.000 rpm, and collected then freeze dried.

## Preparation of Acrylic Fiber-Nanochitosan Composite Films (AF-NCh)

Composite films of AF with different ratios of NCh (0, 10, 20, 30, 40, 50 and 60 wt%) were prepared as following, a

predetermined weight of AF waste is dissolved in 10 ml DMF at 70 °C under stirring for 4 h, then a definite weight of NCh was added portion wise to the PAN-DMF solution with continuing stirring till obtain a homogenous composite solution. The obtained homogenous suspension was sonicated for 1 h in ultrasonic water bath to confirm the well distribution of nanochitosan in the polymer matrix. The composite solution was casted in a glass plate using a film applicator. The casting solution was immersed in deionized water for 24 h to get a film with thickness of 0.12 mm. By adopting the same procedures, other composite film was prepared using a cross linking EPH to assure complete fixation of nanochitosan within the polymer matrix.

## Characterization

## **FTIR Studies**

To assess the reactive function groups of the composite films FT-IR was used within the range  $(400-4000 \text{ cm}^{-1})$  using Nicolet Avatar FTIR 370 CSI.

#### **SEM of Composite Film**

Surface morphology and the cross-section topography of the synthesized composite films were investigated using FESEM QUANTA 250. Prior to examination the films were dried and sputtered with gold to minimize charging effect during examination.

## **TEM of Nanochitosan**

The particle size and shape of synthesized nanochitosan were investigated using HR-TEM, (JEM-2100-TEM). The nanochitosan suspension was sonicated for half an hour and one or two drops were added to the testing grid then left for dyeing.

#### Brunauer-Emmett-Teller (BET) Measurement

The Brunauer–Emmett–Teller (BET) measurement was used to assess the surface area of the composite films based on determination of nitrogen adsorption isotherm at 77 K using the Belsorp adsorption automatic specific surface area analyzer (Microtrac-BEL, Japan).

#### Thermal Gravimetric Analysis (TGA)

Thermal stability of the new nanocomposite was investigated using TA Q500 instrument, at a heating rate 10 °C/ min in nitrogen atmosphere.

#### Adsorption and Optimization Experiments

Different concentrations of CR dye ranged from 100 to 800 mg/l have been prepared. The final concentration after adsorption and the feed solution were measured using UV–Vis (Lambda 35 Perkin Elmer) at  $\lambda$ max = 497 nm. A predetermined weight of AF-NCh and AF-NCh-EPH films were inserted into 50 ml glass round flask, then 10 ml of CR dye solution of variant concentrations were added. The flask was shaken using automatic shaker at 50 rpm for 24 h. Various parameters of adsorption study were employed such as time of shaking, CR dye concentration, adsorbent dose and solution pH.

The adsorption capacity q (mg/g) for CR dye can be calculated using the mass balance expression, Eq. (1) [49].

$$q_e = (C_0 - C_e) \times V/m, \tag{1}$$

where  $C_0$  and  $C_e$  are the initial and equilibrium concentration of the dye, respectively, expressed in (mg/l), V is the volume of the dye solution in (l) and m is the mass of the adsorbent in (g).

The removal efficiency at equilibrium can be calculated using the following relation, Eq. (2) [50].

$$\%R = \frac{\left(C_0 - C_e\right)}{C_0} \times 100.$$
 (2)

#### **Adsorption Isotherm Studies**

Langmuir, Freundlich and Temkin isotherm models were applied to assess the affinity between the adsorbent and adsorbate. The mathematical equations expressed the adsorption models are illustrated below by Eqs. (3), (5) and (6) respectively [28, 51].

$$\frac{C_e}{q_e} = \frac{1}{q_{max}k_l} + \frac{C_e}{q_{max}},\tag{3}$$

where  $k_l$  represents a constant related to the nanocomposites adsorption/desorption capacity, and  $q_{max}$  is the maximum adsorption capacity upon complete saturation of the nanocomposites, Ce (mg/l) is the dye concentration at equilibrium and  $q_e$  (mg/g) is the adsorption capacity at equilibrium.

The basic parameter of the Langmuir isotherm could be expressed in terms of a unitless equilibrium factor, such as the separation factor or equilibrium factor ( $R_L$ ) (Eq. (4)).

$$R_{\rm L} = 1/(1 + K_{\rm l}C_{\rm 0}),\tag{4}$$

where,  $C_0$  is the initial dye's concentration.

The Freundlich isotherm is presented using equation:

$$\log q_e = \log K + \frac{1}{n} \log C_e,\tag{5}$$

where k and n are empirical constants that can be related to the adsorption capacity and the adsorption affinity, respectively.

The linear form of Temkin equation is expressed by

$$q_e = BlnA + BlnCe, \tag{6}$$

where A  $(l g^{-1})$  and B  $(J mol^{-1})$  are the Temkin isotherm parameters relating to the equilibrium binding constant and adsorption heat, respectively.

## **Kinetic Studies**

Pseudo first order and pseudo second order are most the common kinetic models used for detect the rate of dye adsorption from the aqueous solution. The linear forms of these models can be expressed in the following equations see (7) and (8) [52].

$$\log(q_e - q_t) = \log q_e - k_1 \times \frac{t}{2.303},$$
(7)

where  $q_e$  (mg/g), is the adsorption capacity at equilibrium,  $q_t$  (mg/g) is the adsorption capacity at time t, and  $k_1$  is the first order rate constant per minute.

A plot of ln  $(q_e - q_t)$  versus time (t) indicates a straight line of slope  $(-k_1/2.303)$  and an intercept of log  $(q_e)$ .

Whereas the second order equation can be represented by Eq. (8)

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} \times t,$$
(8)

where  $K_2$  expresses the equilibrium rate constant (g/mg min), and  $q_e$  and  $q_t$  express the sorption capacities at equilibrium and at time (t), respectively. A plot  $t/q_t$  versus t shows a straight line of slope  $(1/q_e)$  and an intercept of  $(1/K_2q_e^2)$ .

## **Results and Discussion**

## **Characterization of the Synthesized Nanochitosan**

Figure 1a displayed FTIR of chitosan and nanochitosan, it showed a distinct shift of OH and NH to a lower wave number from 3437 cm<sup>-1</sup> for chitosan to 3415 cm<sup>-1</sup> for nanochitosan with large broadening indicating the physical interaction with TPP. Peaks of C=O of amide (chitin part) at 1640 cm<sup>-1</sup> and C–O at 1150 cm<sup>-1</sup> were obtained [53]. For nanochitosan a distinct peaks were appeared at 1080 and 1210 cm<sup>-1</sup> for P–O and P=O streating, respectively.

Figure 1b showed TEM images of the nanochitosan particle. The NCh had a relatively spherical shape and a narrow particle size distribution, with sizes ranging from 60 to 80 nm. The NCh exists showed some aggregates due to the highly interactive attraction force between particles [54]. Figure 1c indicated the particle size of chitosan measured using zeta Sizer (Malvern instrument Version 7.04). The figure indicated that the average particle size of the nanoparticle was 98 nm with narrow distribution. The relatively higher particles size of chitosan in DLS rather in TEM is that the measurement in DLS was performed in aqueous media and the chitosan nanoparticles were in swollen state that give relatively larger size. However in TEM measurement the particles were in dried state and selected image were obtain to confirm the particle size.

#### **Characterization of the Composite Films**

#### **FTIR Spectra**

FT-IR spectra of the prepared AF film, and nanocomposites films have been investigated as shown in Fig. 2.

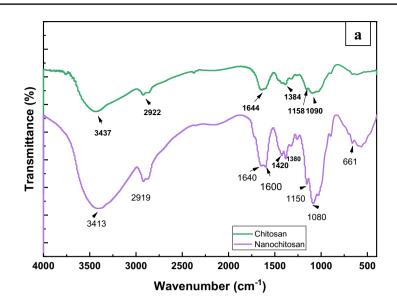
As shown in the Fig. 2, AF film have many peaks; the absorption peaks at 2928 cm<sup>-1</sup> and 2885 were related to stretching C–H bonds in CH<sub>3</sub> and CH<sub>2</sub>. Another peak is at 2245 cm<sup>-1</sup> which is assigned to presence of nitrile (C=N) groups. Peak at 3436 cm<sup>-1</sup> is may be related to –OH of adsorbed water by additives present in commercial AF [46]. The peaks at 1638 cm<sup>-1</sup> and 1738 cm<sup>-1</sup> results from presence of C=O related to comonomers like butyl acrylate and methyl acrylate and peaks at 1073 and 1237 cm<sup>-1</sup> may be related to and C–O stretching, the peaks at 1371 cm<sup>-1</sup> is related to bending motions of C–H bond [55].

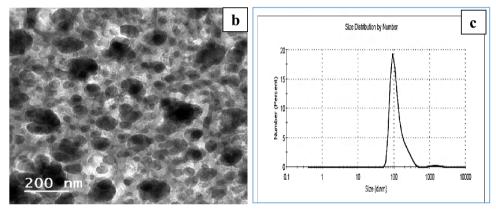
FTIR of composites films AF-NCh and AF-NCh-EPH declares that the intensity of C $\equiv$ N and C=O ester is decreased compared to pure AF and observed at 2246 cm<sup>-1</sup>, 1738 cm<sup>-1</sup> and 1735 cm<sup>-1</sup> respectively. NH and –OH peaks are observed at 3429 cm<sup>-1</sup> and 3437 cm<sup>-1</sup>, respectively.

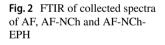
#### SEM of AF and Nanocomposites Films

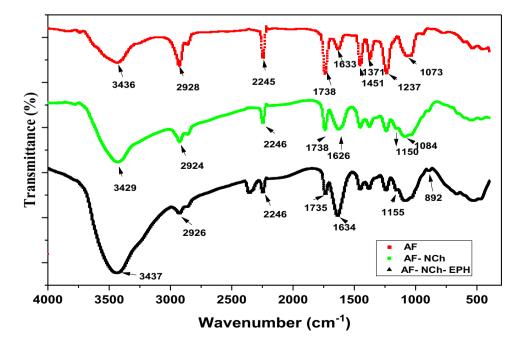
Figure 3a showed the topography of plain surface of AF film, which revealed the highly porous structure. Figure 4a displayed the cross section of AF which declared the pores and macro voids structure resulted from spontaneous demixing of solvent (DMF) and non-solvent (water) during phase inversion process. Figures 3b and 4b showed the plain and cross section of composite AF-NCh, which declared the enlarged macrovoids with more pores structure. The figures also showed the inclusion of spherical shaped nanoparticles indicating nano-chitosan incorporation into AF matrix, which resulted in increasing the active sites for dye adsorption process. For the other prepared AF-NCh-EPH

**Fig. 1** a FTIR spectra of chitosan and nanochitosan, **b** TEM of nanochitosan and **c** DLS measurement of the nanochitosan (Color figure online)









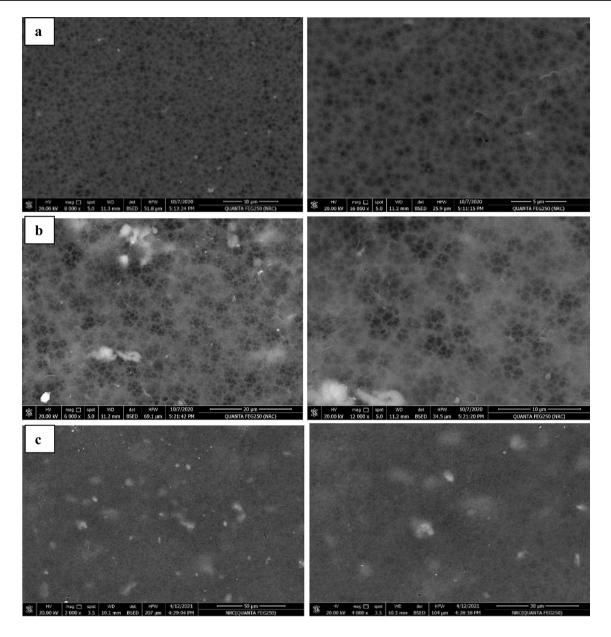


Fig. 3 SEM of film surface for **a** AF, **b** AF-NCh and **c** AF-NCh-EPH

nanocomposites; Figs. 3c and 4c displayed the surface and cross-section of the film, which revealed a significant fixation of NCh into AF matrix which leads to an enhancement in adsorption efficiency with good stability.

## Brunauer-Emmett-Teller (BET) Measurement

BET analysis of the synthesized films is illustrated in Fig. 5 and summarized in Table 1. From BET data we can noticed that surface area of AF film decreased upon addition of NCh and NCh-EPH. This may be due to the inclusion of high content of nano-chitosan with high entangled force of these particles. But in spite of decrease the surface area of nanocomposite film but they have high adsorption capacity to CR dye compared to AF film because they have hydrophilic reactive function groups as (–OH and –NH<sub>2</sub>) [56]. For AF-NCh-EPH has a larger surface area compared to AF-NCh, thus has a higher adsorption efficiency to CR removal. Also from nitrogen adsorption desorption isotherm and average pore size diameter of the synthesized films, they reveal the mesoporous structure of adsorbents films [57].

## **Thermal Gravimetric Analysis**

The thermal stability of modified and unmodified AF-NCh was studied using thermal gravimetric analysis. Figure 6

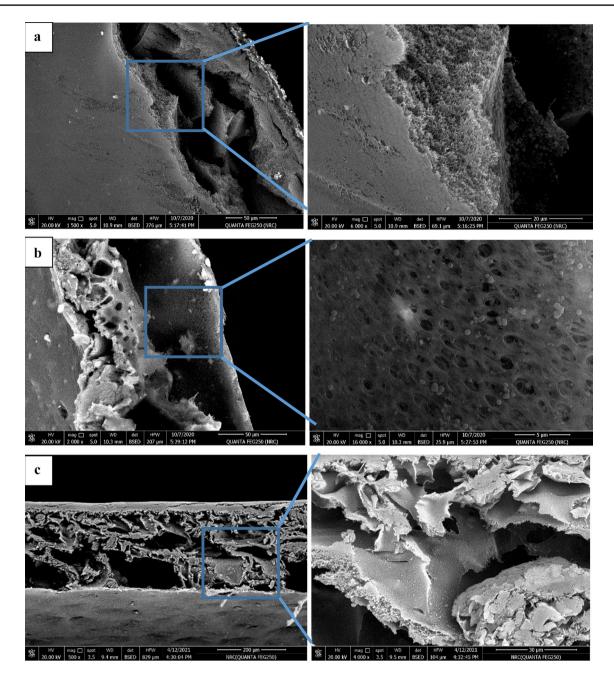


Fig. 4 SEM of film cross-section for a AF, b AF-NCh, c AF-NCh-EPH

illustrated TG and DTG curves of AF films; AF, AF-NCh and AF-NCh-EPH composites. For blank AF film there was a distinct one phase due to degradation process of the main chains. The onset degradation temperature was at 349 °C. For the prepared nanocomposites AF-NCh and AF-NCh-EPH, it was obvious a distinct two phases of degradation process, which confirmed the successful physical mixing of nanochitosan into AF film matrix. For AF-NCh the first onset degradation process was at 289 °C, attributed to nanochitosan degradation. The second onset degradation temperature was at 353 °C, for AF degradation. For AF-NCh-EPH the first onset degradation process was at 276 °C, attributed to nanochitosan degradation. The second onset degradation temperature was at 343 °C for AF chains. It was noticed that the use of crosslinking EPH decrease the thermal stability of the nanocomposites, which may be due to the decrease in oriented packing chain of AF resulted from nanochitosan [58].

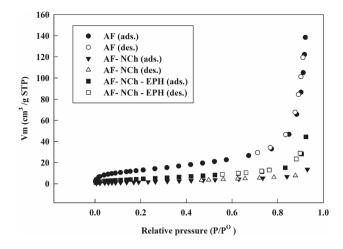


Fig. 5 BET adsorption-desorption isotherm of synthesized films

 Table 1
 BET surface area and the pore structure of the synthesized adsorbents

Sample	$S_{BET} (m^2/g)$	Pore volume (V <sub>m</sub> ) (cm <sup>3</sup> /g)	Average pore size (nm)
AF	48	11.2	17.4
AF-NCh	9.3	2.1	9
AF-NCh-EPH	19	4.3	14.4

## **Adsorption Study**

## Effect of Loading Percent of NCh on Adsorption Behavior for Congo Red Dye

The effect of loading percent of nano-chitosan into AF films was studied to measure the efficiency for CR dye removal. Weight of 0.025 g of AF-NCh with different nano-chitosan ratio (0, 10, 20, 30, 40, 50, 60 wt%) was inserted into a 10 ml of 200 mg/l CR dye. The adsorption process occurred using a mechanical shaker at 50 rpm for 24 h. Figure 7 showed the relation between loaded nanochitosan percent and adsorption removal % (%R) of CR dye. It was clear from the figure the increment of efficiency of CR dye upon increase of nanochitosan loaded percent onto AF film till 50 wt% after that it reached a plateau with no observed enhancement. The higher efficiency was due to high aspect ratio of reactive functional group (amine and hydroxyl groups) present in nanochitosan. Also the high surface area of nanoparticles may enhance the adsorption capacity [59–61]. One can see from the figure that the optimum removal efficiency (R%)was about 98% of CR for nanochitosan with 50% loading into AF film, afterword they have no significant change of %R. This can be attributed the aggregation and accumulation of the nanoparticle during the composite preparation that decrease the active surface area for the adsorption [62].

#### **Effect of Dye Concentration**

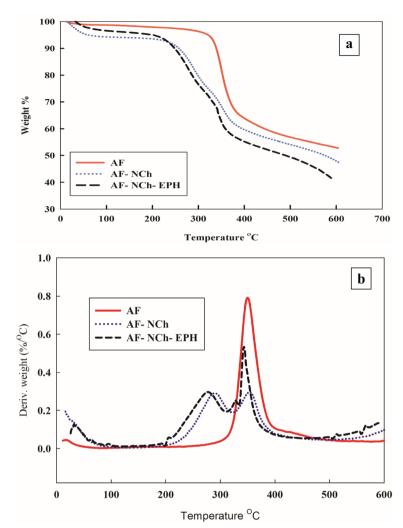
Figure 8a and b declared the effect of CR concertation on adsorption capacity within a day (24 h) with a series of CR dye ranged from 100 to 800 mg/l. From the figure, the best adsorption R% was achieved at a CR dye concentration of 400 mg/l with values 92.5% and 96.8% for AF-NCh and AF-NCh-EPH respectively. Also we can noticed that the higher concentration above 400 mg/l showed less percent removal efficiency because of the most active cites of the adsorbent was occupied and exhausted by CR dye molecules. The adsorption capacity was increased by increasing the dye concentration till 400 mg/l afterword there is no noticed increase in adsorption capacity indicating the saturation of active sites of adsorbent.

## Effect of pH

Table 2 summarize adsorption capacity for CR dye removal at different pH. It can be seen from the table that the highest adsorption capacity was achieved at pH 5.5, this due to; at relatively acidic condition pH 5.5 the amino group of nanochitosan get protonated (cationic structure), which led to an increase in the interaction to the anionic dye (CR). While at a relatively neutral condition pH 6.8 the cationic structure of nanochitosan loaded acrylic fiber waste decreased and the adsorption capacity of CR is decreased. At pH 8 adsorption capacity appears to significantly decrease for the CR dye. This due to, at slightly basic solution the negative charge of OH<sup>-</sup> groups made a repulsive force of CR dye anionic structure, thus desorption process predominates [22]. On the other hand the CR dye aromatic moiety structure is sensitive to lower below pH below 5, the color is changed to deep blue and the dye get precipitated due to the hydrophobic interaction between the dye molecules [63].

## Effect of Contact Time

Figure 9a indicated the effect of contact time on the adsorption capacity of composite films for CR dye. As it can be seen from the figure that the increase the time the increased adsorption capacity for both films (AF/NCh and AF/NCH-EPH). The increased capacity was due to the available reactive functional groups that consumed over the progress of time. The figure showed slow adsorption pattern; as it need much time for attain equilibrium, and this result may be due to the relative hydrophobic nature of the polymer matric that render the movement of the dye molecules into the bulk of polymer matrix.



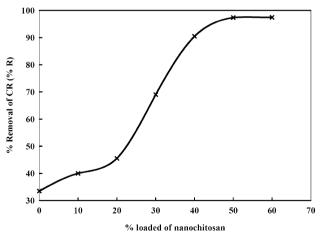


Fig.7 Effect of nanochitosan percent loaded onto AF on % removal of CR

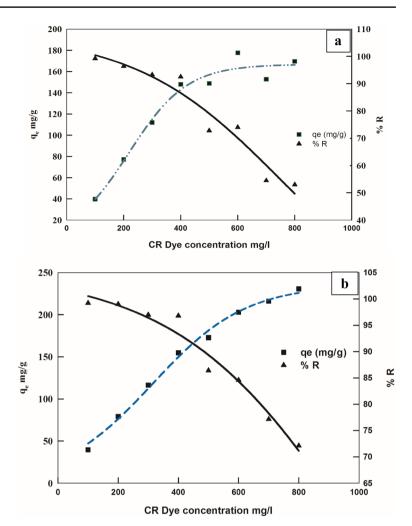
## Effect of Adsorbent Dose

In our study, different adsorbent dose, 1.25, 2.5, 5 and 7.5 g/l

of AF-NCh and AF-NCh-EPH films were used for removal of 400 ppm CR dye solution for 240 min. The %R was plotted against dose of adsorbent as shown in Fig. 9b. From the figure the dye percent removal was enhanced and increased upon increase the adsorbent dose till the dose of 5 g/l which consider the optimum dose. This was attributed to increase of surface area and active sites of adsorbent.

## **Adsorption Isotherm Study**

The linear adsorption isotherms, Langmuir Freundlich and Temkin, were used to evaluate the adsorption adsorbate affinity interaction. The Langmuir model was illustrated by a linear plot between a specific sorption (Ce/Qe) and the equilibrium concentration (Ce). We get  $1/q_{max} =$  slope and  $1/q_{max}k_l =$  intercept. For Freundlich isotherm was obtained by plotting linearized curve between  $\log q_e$  mg/g and  $\log C_e$ mg/l. We get log K = intercept and 1/n = slope. For Temkin isotherm the curve was obtained by plotting qe with ln(Ce). The Linear Langmuir, Freundlich and Temkin isotherms



plots and their calculated parameters were showed in Fig. 10 and Table 3. From figure and calculated data, the adsorption nature of CR by AF-NCh and AF-NCh-EPH were more fitted to Langmuir isotherm. This can be attributed to the high  $R^2$  value compared to Freundlich and Temkin isotherms (Table 3) and the relatively close value of qmax to the experimental one showed in Table 3. According to Langmuir isotherm the obtained adsorbent composite may have homogenous surface nature, and CR dye adsorbed completely to the synthesized films active sites via monolayer formation mechanism [64, 65]. Also equilibrium factor (R<sub>1</sub>)

 $\label{eq:table_transform} \begin{array}{l} \textbf{Table 2} & \text{Effect of } pH \text{ variation on adsorption capacity of synthesized} \\ \text{films} \end{array}$ 

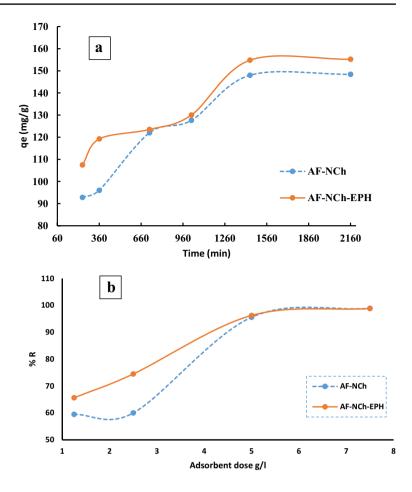
Dye conc. mg/l	рН	q mg/g (AF- NCh)	q mg/g (AF-NCh- EPH)
400	5.5	148	154.8
	6.8	128	136
	8	114.4	138.8

derived from Langmuir isotherm ranged from 0.052 to 0.0068 and 0.086 to 0.011 for AF-NCh and AF-NCh-EPH, respectively, which indicates favored CR dye to the nano-composites adsorbent materials [66].

## **Kinetic Study**

Pseudo first and second order models were adopted for our adsorption study of CR dye on AF-NCh and AF-NCh-EPH composite films. The linearized curves for the two models were represented in Fig. 11. The calculated parameters were summarized in Table 4. From these data, we can conclude that pseudo second order mechanism is most fitted for adsorption of CR dye on the two synthesized composite films. The value of  $R^2$  of pseudo second order is higher than of pseudo first order as shown in Table 4. Also the calculated values of qe were 125 and 128.2 for AF-NCh and AF-NCh-EPH, respectively.

Fig. 9 Effect of a adsorbent time and b adsorption dose on CR dye %R



## Effect of Film Regeneration

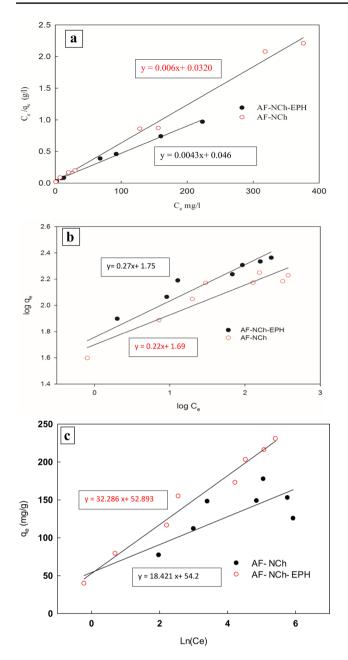
Regeneration of the adsorbent is an important step from economic point of view and practical use of an adsorbent in industries. The prepared nanocomposite films (AF-NCh and AF-NCh-EPH) were regenerated using (50:50) ethanol: water solution. Five cycles experiment were employed using 400 mg/l CR dye solution. The results were shown in Fig. 12. From the illustrated data we can state that; after five cycles of using the synthesized film the adsorption capacity decreased by approximately 30% of their initial values. Thus the synthesized AF-NCh and AF-NCh-EPH films can be used several times as an adsorbent for CR dye with relatively good stability.

## **Comparative Study**

We have also compared the maximum sorption capacity  $(q_{max})$  for the adsorption of CR dye onto the prepared nanocomposites with other nano-adsorbents and are presented in Table 5. It is observed from the table that the CR dye adsorption capacity of blended AF/nanochitosan films is higher than the previous reported nano-adsorbents based on acrylonitrile polymer or nanochitosan. Thus the prepared AF-NCh and AF-NCH-EPH have great potential for CR from aqueous media.

## Conclusion

This work was a trial for utilize waste to treat waste whereas recycling of acrylic fibers (AF) waste into adsorbent films incorporated with ecofriendly nanochitosan (NCh) with high ratio were employed. Preparation of nanocomposites films, AF-NCh and AF-NCh-EPH were performed. The nanocomposite films were well characterized via instrumental techniques and evaluated for their removal capability for anionic dye (Congo red) from aqueous solution. The results indicated the efficiency of the prepared films for removing of CR with maximum adsorption capacities of 169 and 230 mg/g for AF-NCh and AF-NCh-EPH, respectively. The adsorption was most fitted to Langmuir isotherm and pseudo second order mechanism. The prepared adsorbents showed relative stability after 5 cycles of regeneration. Finally, the prospective research on acrylic fiber waste is to be tested on other pollutants and real waste water, in addition other preparation condition can be performed as addition of pore former,



**Fig. 10** Langmuir (**a**), Freundlich (**b**) and **c** Temkin isotherms for CR dye adsorption by AF-NCh and AF-NCh-EPH

choosing another solvent and reduce thickness of the film to enhance the porosity and surface area of the adsorbent.

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 Table 3
 Langmuir & Freundlich isotherms parameters for CR dye adsorption by AF-NCh and AF-NCh-EPH adsorbents

Isotherm model	Parameter	AF-NCh	AF-NCh-EPH
Langmuir	R <sup>2</sup>	0.992	0.997
	Kl	0.18	0.106
	q <sub>max</sub>	166.6	232.5
	qmax (experimental)	169	230
Freundlich	$\mathbb{R}^2$	88	91
	K <sub>f</sub>	48.9	56.2
	n	4.5	63.7
Temkin	$\mathbb{R}^2$	0.74	0.97
	В	18.4	32.2
	А	18.5	4.8

## **Declarations**

**Conflict of interest** The authors confirm that there is no conflict of interest.

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**Fig. 11** Pseudo first order (**a**) and second order (**b**) for CR dye adsorption by AF-NCh and AF-NCh-EPH

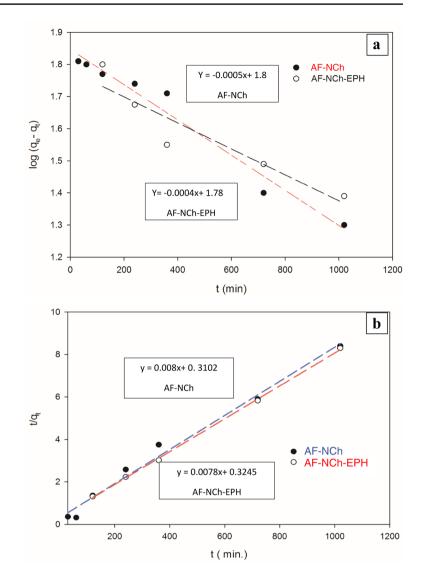


 
 Table 4
 Pseudo first order and pseudo second order parameters for CR dye adsorption by AF-NCh and AF-NCh-EPH

	Parameter	AF-NCh	AF-NCh-EPH
1st order	$\mathbb{R}^2$	0.97	0.88
	K1	$1.15 \times 10^{-3}$	$9.2 \times 10^{-4}$
	q <sub>e</sub>	70.8	60.25
2nd order	$q_e R^2$	98	99
	K2	$2.06 \times 10^{-4}$	$1.87 \times 10^{-4}$
	q <sub>e</sub>	125	128.2

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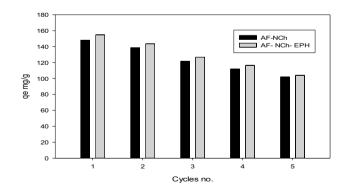


Fig. 12 Effect of cycles on adsorption capacity for CR dye by AF-NCh and AF-NCh-EPH

 Wang J, Qin L, Lin J et al (2017) Enzymatic construction of antibacterial ultrathin membranes for dyes removal. Chem Eng J 323:56–63. https://doi.org/10.1016/j.cej.2017.04.089 Table 5Comparison of<br/>adsorption capacities of various<br/>adsorbents for removal of CR<br/>dye

Adsorbent	q <sub>max</sub> mg/g	Adsorption iso- therm model	Adsorbate (Dye)	References
PAN-PEI 2D nano fibrous mat	77.5	Lang.	CR	[67]
Functionalized PAN-EDA nanofibers	130	Lang.	CR	[68]
PAN/Fe <sub>2</sub> O <sub>3</sub> nanocomposite fibers	52	Lang.	CR	[69]
Chitosan/montmorillonite nanocomposite	54.2	Lang.	CR	[ <b>70</b> ]
AF-NCh	166.6	Lang.	CR	Our study
AF- NCh-EPH	232.5	Lang.	CR	Our study

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# **Authors and Affiliations**

# Salah E. Selim<sup>1</sup> Salah A. Meligi<sup>2</sup> · Ahmed E. Abdelhamid<sup>3</sup> · Mahmoud A. Mabrouk<sup>1</sup> · Ahmed I. Hussain<sup>3</sup>

- <sup>1</sup> Egyptian Academy for Engineering and Advanced Technology Affiliated To Ministry of Military Production, Al Salam City, Egypt
- <sup>2</sup> Chemistry Department, Faculty of Science, Ain Sham University, Cairo, Egypt
- <sup>3</sup> Polymers and Pigments Department, National Research Center, 33 El-Buhouth St., Dokki, Cairo 12622, Egypt

 Wang L, Wang A (2007) Adsorption characteristics of Congo Red onto the chitosan/montmorillonite nanocomposite. J Hazard Mater 147:979–985. https://doi.org/10.1016/j.jhazmat.2007.01.145

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