## ERRATUM

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## PARTIAL HYDROGENATION OF PHENYLACETYLENE ON COPPER-PROMOTED IRON CATALYST

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Unfortunately both tables 1 and 2 were omitted in the original version.

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|--|---|--|--|--|--|--|--|
| D <sub>c</sub> <sup>c</sup><br>(nm)  | $\frac{R_0^{d}}{(\mathrm{mmol}\cdot\mathrm{min}^{-1}\mathrm{g}^{-1})}$                    | S <sub>50</sub><br>(%)   |  |  |  |  |  |
| 16   | $1.1 \times 10^{-2}$  | 95.7   |  |  |  |  |  |
| 12   | $5.5 \times 10^{-2}$  | 95.1   |  |  |  |  |  |
| 16   | $1.2 \times 10^{-2}$  | 96.0   |  |  |  |  |  |
| 17   | $4.9 \times 10^{-2}$  | 97.6   |  |  |  |  |  |
| 17   | $1.0 \times 10^{-3}$  | 91.0 <sup>f</sup>  |  |  |  |  |  |
| 18   | $2.1 \times 10^{-3}$  | 94.0   |  |  |  |  |  |
| 20   | $2.7 \times 10^{-3}$  | 92.0   |  |  |  |  |  |
| 32   | $1.1 \times 10^{-3}$  | 91.5 <sup>f</sup>  |  |  |  |  |  |
|  | D <sub>c</sub> <sup>c</sup><br>(nm)<br>16<br>12<br>16<br>17<br>17<br>17<br>18<br>20<br>32 | $\begin{array}{c c} D_{\rm c}^{\rm c} & R_0^{\rm d} \\ \hline ({\rm nm}) & ({\rm mmol} \cdot {\rm min}^{-1} {\rm g}^{-1}) \\ \hline 16 & 1.1 \times 10^{-2} \\ 12 & 5.5 \times 10^{-2} \\ 16 & 1.2 \times 10^{-2} \\ 16 & 1.2 \times 10^{-2} \\ 17 & 4.9 \times 10^{-2} \\ 17 & 1.0 \times 10^{-3} \\ 18 & 2.1 \times 10^{-3} \\ 20 & 2.7 \times 10^{-3} \\ 32 & 1.1 \times 10^{-3} \end{array}$ |  |  |  |  |  |

Table 1 Hydrogenation of phenylacetylene<sup>a</sup> on various Fe-M/SiO<sub>2</sub> catalysts<sup>b</sup>

<sup>a</sup> Carried out in ethanol at 60 °C under 1 MPa of hydrogen.

<sup>b</sup> Fe: M = 9:1 in atomic ratio.

<sup>c</sup> Mean crystallite size of Fe measured by X-ray line broadening.

<sup>d</sup> Initial reaction rate.

Table 2

<sup>e</sup> Selectivity in styrene at 50% conversion.

<sup>f</sup> Measured at 20% conversion.

| ruore 2              |               |     |            |    |                             |
|----------------------|---------------|-----|------------|----|-----------------------------|
| Effects of reduction | conditions on | the | properties | of | $Fe-Cu(7:3)/SiO_2$ catalyst |

| No.            | Heating rate <sup>a</sup><br>(°C $\cdot$ min <sup>-1</sup> ) | $H_2$ flow rate<br>$(1 \cdot h^{-1})$ | D <sub>c</sub><br>(nm) | $\frac{R_0}{(\text{mmol} \cdot \text{min}^{-1}\text{g}^{-1})}$ | S <sub>50</sub><br>(%) | - |
|----------------|--|---------------------------------------|------------------------|--|------------------------|---|
| <br>1          | 10   |                                       | 12                     | 1.9×10 <sup>-1</sup>   | 99.5                   | - |
| 2              | 5  | 8                                     | 11                     | $3.1 \times 10^{-1}$   | 99.5                   |   |
| 3              | 10   | 16                                    | 11                     | $2.9 \times 10^{-1}$   | 99.5                   |   |
| 4              | 5  | 16                                    | 10                     | $3.7 \times 10^{-1}$   | 99.5                   |   |
| 5 <sup>b</sup> | 10   | 16                                    | 12                     | $2.0 \times 10^{-1}$   | 99.6                   |   |

<sup>a</sup> Heated up to 500 °C and held as such for 1 h.

<sup>b</sup> Reduced after heating at 300 °C for 1 h in a flow of nitrogen.

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