





Research Article

Supercritical methane adsorption and storage in pores in shales and isolated kerogens

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Abstract

Shale gas is an important hydrocarbon resource in a global context. It has had a significant impact on energy resources in the US, but the worldwide development of this methane resource requires further research to increase the understanding of the relationship of shale structural characteristics to methane storage capacity. In this study a range of gas adsorption, microscopic, mercury injection capillary pressure porosimetry and pycnometry techniques were used to characterize the full range of porosity in a series of shales of different thermal maturity. Supercritical methane adsorption methods for shale under conditions which simulate geological conditions (up to 473 K and 15 MPa) were developed. These methods were used to measure the methane adsorption isotherms of Posidonia shales where the kerogen maturity ranged from immature, through oil window, to gas window. Subcritical methane and carbon dioxide adsorption studies were used for determining pore structure characteristics of the shales. Mercury injection capillary pressure porosimetry was used to characterize the meso and macro porosity of shales. The sum of the CO₂ sorption pore volume at 195 K and mercury injection capillary pressure pore volumes (1093–5.6 nm) were equal to the corresponding total pore volume (< 1093 nm) thereby giving an equation accounting for virtually all the available shale porosity. These measurements allowed quantification of all the available porosity in shales and were used for estimating the contributions of methane stored as ‘free’ compressed gas and as adsorbed gas to overall methane storage capacity of shales. Both the mineral and kerogen components of shale were studied by comparing shale and the corresponding isolated kerogens so that the relative contributions of these components could be assessed. The results show that the methane adsorption characteristics were much higher for the kerogens and represented 35–60% of the total adsorption capacity for the shales used in this study, which had total organic contents in range 5.8–10.9 wt%. Microscopy studies revealed that the pore systems in clay-rich, organic-rich and microfossil-rich parts of shale are very different, and also the importance of the inter-granular organic-mineral interface.

Keywords Shales · Kerogens · Methane · Adsorption · Mercury porosimetry · Microscopy

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1 Introduction

The development of shale gas as a methane resource started in the US and it has become an increasingly important component of natural gas supply in the past twenty years [1]. There are large potential shale gas reserves in the rest of the world, which could be exploited in the future. Compared to coal, shale only contains relatively small amounts of methane, but is economic because of very large deposits. The economics of shale gas reservoirs depends on the Gas-in-Place (GIP) and the methane extraction rate that can be achieved [2]. This depends on the properties of the shale and the fracturing of the shale matrix induced by the hydraulic fracking and horizontal drilling processes.

Shales are complex heterogeneous materials comprising of inorganic mineral and organic kerogen components, which leads to wide variations in pore structures and surface chemistry. Methane is stored as either compressed gas or physisorbed gas in porous structures in organic-rich shales and the quantities of these components are very difficult to predict. The gas filled fraction of the porosity follows known relations with pressure and temperature, but it is difficult to predict the quantity. In comparison, the adsorbed gas contribution is poorly understood, but may amount to 50–60% of the gas in some shales [3]. Shale porous structure characteristics that are particularly relevant for assessing shale reservoir potential are pore volumes, pore size distribution and adsorption characteristics under simulated geological conditions. The economic potential of the resources needs to be established unequivocally, in order to justify extraction of shale gas.

In conventional reservoirs, gas is stored in large pores as ‘free’, high pressure gas. There is very little gas adsorbed on the walls of macropores compared to free gas in the pores. In contrast, shale is a complex heterogeneous material typically consisting of > 90% minerals with < 10% organic kerogen material, in which almost all of the pores are less than a micrometre in diameter. Methane is generated from the decomposition of the organic kerogen phase in shale during geological processes over the temperature range 370–550 K. A gas rich phase is generated at temperatures > 430 K [4]. Methane is stored in pores, which range from the micropores (< 2 nm), through mesopores (2–50 nm) to larger macropores, with the adsorbed phase mainly in the micropores in equilibrium with compressed gas in larger meso and macropores through an interconnected pore structure. The adsorbed gas is slow to be released and could be an issue for shale gas exploitation. There have been only a limited number of studies of methane

adsorption on shale because of the difficulty in measuring isotherms under supercritical conditions [5–14]. At the outset, measurements were limited to 338 K, but recently these have been extended to higher temperatures [15, 16]. The amounts of methane in the adsorbed and compressed gas phases need to be quantified in order to understand the delivery mechanism of shale gas to the production well.

The challenge was to quantify the shale porosity, the methane stored in shale as ‘free’ compressed gas and the adsorbed gas phase, and the relative proportions of methane stored in both the organic and inorganic phases. Since shales contain pore structures ranging from micro to macro pores, a number of techniques must be used to quantify the different pore size ranges. These methods include high pressure supercritical gas adsorption to determine the methane adsorbed phase under simulated geological conditions, mercury injection capillary pressure (MICP) porosimetry for characterizing meso and macro pore characteristics, subcritical gas adsorption for characterizing micro and meso pore structure, helium and grain density measurements to measure the density of pore wall material and microscopy to provide ideas on the origin of kerogen and mineral particle interfaces and pore connectivity. Small-angle neutron scattering techniques may also be used to provide information on shale structure and porosity [17–19].

The porous structures of shales are affected by kerogen maturity [20], mineralogy [21], grain size [22], diagenesis and compaction [23–25]. There have been a number of studies of the relationship between total organic content (TOC) and adsorption characteristics for dry organic rich shales [5, 7, 8, 14, 26]. Gasparik et al. studied the effect of TOC on methane adsorption capacity for two suites of dry shales with a range of sources and maturity: 1) 6 shales [9] with TOC 1.0–10.5% did not show a correlation and 2) 28 shales [14] (vitrinite reflectance (V_R) = 0.7–2.4%) with TOC (0.4–14.1%) gave a positive correlation, but with some samples deviating from the trend. Wang et al. found [27] a positive correlation between methane sorption capacity and TOC for 10 Longmaxi shales (V_R = 2.7–3.68 and TOC = 1.13–3.59%). Liu et al. [28] also investigated 28 Longmaxi shales (TOC 0.25–4.45%) and found a positive correlation for methane sorption at 303 and 363 K, with TOC. The complexity of the problem of the relation between methane sorption capacity and TOC over a wide range of shale sources with varying maturities and mineral contents is lack of knowledge of the methane fraction stored in the mineral and organic structures and also, the kerogen structure changes with maturity. An additional factor that needs to be considered is the presence of moisture in shale, which has a detrimental effect on methane sorption [29, 30]. Clay mineralogy in the shale is an indicator

of potential for water adsorption [29, 31]. The decline in methane sorption capacity with increasing water content has been attributed to competitive adsorption, water cluster formation obstructing access to and occupying pore space. Therefore, methane adsorption capacities for dry shales can be regarded as maximum values whereas moisture equilibrated (relative humidity 97%) methane sorption capacities can be considered as minimum values [29].

Estimation of organic-rich shale potential for utilization as a gas resource presents major problems and challenges related to the quantification of the amounts of compressed and adsorbed gas and how this is related to shale porous structural characteristics. The aims of the study were:

1. to establish methods for the accurate measurements of supercritical methane adsorption capacity of dry shales at high temperatures and pressures, which simulate geological conditions (up to 15 MPa and 473 K);
2. to account for all the porosity (micro-, meso- and macro-) in order to estimate the amounts of sorbed gas and 'free' compressed gas stored in shale pores;
3. to determine the relative contributions of the organic kerogen and inorganic mineral phases to overall methane capacity;
4. to establish the role of kerogen content and maturity on methane capacity and
5. to integrate the porous structure characterization data with microscopic data to gain an insight into mineral and kerogen structural interfaces.

2 Experimental techniques

2.1 Shale samples

The sample of shale Alum 1 was obtained from the Skelbro-2 well in Bornholm, Denmark [32]. The Lower Toarcian Posidonia shales were obtained from the Wickensen (WIC), Harderode (HAR), and Haddessen (HAD) boreholes in Germany (see Fig. 1) [33]. These samples were core samples and the surface showed no significant evidence of contamination. The samples used were taken from the centre of the cores to avoid any possibility of surface contamination. The samples were dried at 105°, but no further treatment of the samples was considered necessary. These sampling and preparation methods were used to ensure that the samples were as far as possible representative of those in the geological formations. Two samples from each borehole were investigated in detail. The maturity of the shale samples increased progressively from the early oil-window Wickensen ($V_R=0.53\%$), through the mid oil window Harderode ($V_R=0.89\%$), to

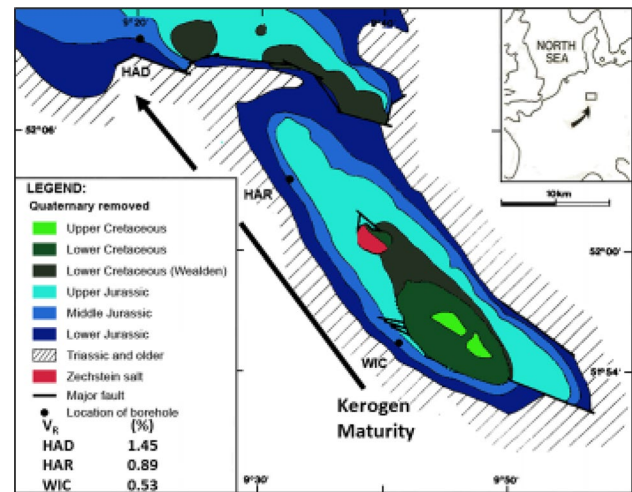


Fig. 1 Posidonia shale samples used in this study (modified from [36])

the gas-window Haddessen ($V_R=1.45\%$) samples. Characterization data for the samples are given in Tables 1 and 2. The mineralogical compositions of shales in this sample series were similar over the range of maturity with the following ranges: calcite (31–55 wt%), phyllosilicates (23–37 wt%), quartz (8–16 wt%), pyrites (4–9 wt%), dolomite (0.3–6.4%), feldspars (1–5 wt%). TOC values were in the range 5.8–10.92 wt% [34]. The shale and kerogen sample set allowed the impact of kerogen maturity on shale and kerogen pore structure on methane capacity to be studied independently of TOC and mineral composition variables.

2.2 Kerogen samples

The kerogen samples were separated from the shales. Initially the shales were treated with HCl to dissolve carbonates and then treated with acidified CrCl_2 to remove pyrite. Silicates from this sample were removed by treatment with HF [34]. Kerogen purity was checked by powder X-ray diffraction [34].

2.3 Density measurements

2.3.1 Grain density

Samples (particle size range: 500–1180 μm) were pre-dried overnight at 105 °C in air. The sample was weighed in a pre-weighed pycnometer (50 mL). 10 mL of Teepol® soap solution (concentration: 5%) was added to the pycnometer, which was then filled with degassed water and left overnight to equilibrate. The pycnometer + sample + water was weighed at 25 °C. The pycnometer was filled with

Table 1 Well depth, TOC, grain and helium densities, mercury injection pore volumes and total porosities for Alum shale and Posidonia shales and kerogens [34, 35]

Well	Shale sample	Depth (m)	TOC (wt%)	Shale grain density (g cm ⁻³)	Shale density (helium pycnometry) (g cm ⁻³)	Shale bulk vol. (MICP) (cm ³ g ⁻¹)	shale total pore vol. (%)	Kerogen TOC [†] (wt%)	Kerogen density (helium pycnometry) (g cm ⁻³)
<i>Posidonia</i>									
WIC	7145	47.4	10.92	2.331	2.321	0.497	13.8	73	1.217
WIC	7155	57.8	9.67	2.361	2.297	0.484	12.5	73	1.235
HAR	7038	44.5	7.91	2.493	2.468	0.414	3.1	97	1.168
HAR	7060	66.8	5.78	2.592	2.550	0.404	4.5	> 99	1.024
HAD	7090	40.1	7.41	2.572	2.556	0.439	11.4	83	1.342
HAD	7119	60.6	7.15	2.607	2.614	0.445	13.7	79	1.368
<i>Alum</i>									
Skelbro-2	Alum 1	9.4	6.35	2.592		n.a.	n.a.	n.a.	n.a.

n.a. not available

[†]The kerogen TOC content is corrected for the residual pyrite content, which could not be removed by the separation process

Table 2 Mineral composition of Posidonia and alum shales in wt%

	Quartz	Plagioclase	Calcite	Dolomite	Pyrite	Gypsum	Muscovite	Illite + I-S	Kaolinite	Chlorite	Other
<i>Posidonia shales</i>											
WIC7145	13.2	1.0	46.6	0.3	3.9	2.2	0.0	22.4	5.1	2.0	3.3
WIC7155	8.6	1.4	55.3	0.6	5.4	2.4	0.1	19.4	2.2	1.8	2.8
HAR7038	15.8	2.1	43.5	0.7	5.6	0.0	3.2	18.5	8.9	0.0	1.7
HAR7060	13.0	2.8	30.5	6.4	9.1	0.0	3.7	26.2	6.6	0.0	1.7
HAD7090	16.0	3.0	39.7	1.8	5.0	1.8	1.3	23.9	3.9	0.7	2.9
HAD7119	8.2	4.9	49.9	2.7	4.5	3.8	0.0	19.5	1.1	2.7	2.7
<i>Alum shale</i>											
Alum 1	44.4	1.0	0.5		1.4		9.5	35.8	0.7	4.2	2.5

Other minerals includes Feldspar, Siderite, Anatase, Marcasite, Aragonite and Dickite [34, 35]

de-gassed water and weighed at 25 °C to determine the volume of the pycnometer. The particle grain density was calculated from the above weights and the known density of water at 25 °C.

2.3.2 Helium density

Helium density measurements were carried out as part of the high pressure adsorption measurements since the information is necessary for calculating the surface excess values. Pre-dried kerogen and shale samples were loaded into a Hiden Isochema Intelligent Manometric Instrument (IMI). The samples were outgassed typically for ~4 h, at < 10⁻⁴ Pa, at 110 °C in the IMI instrument before helium pycnometry. Helium dosing at a pressure of 2 MPa at 40 °C from a reference cell was used with successive evacuation and helium dosing cycles with the skeletal volume and sample density being determined each time. The mean of 3 repeats was used. A stainless steel cylinder was used

as a volume calibration standard under matching conditions. The volume of gas injected into the sample cell was calculated using the NIST Standard Reference database 23 by using the REFPROP Version 9.0 software [37]. Helium density measurements were repeatable to ±0.01 g cm⁻³.

2.4 Adsorption studies

2.4.1 Low-pressure adsorption

An Intelligent Gravimetric Analyzer (IGA), supplied by Hiden Isochema Ltd., Warrington, UK; was used for low temperature nitrogen, carbon dioxide and methane adsorption studies of shales and kerogens. Samples of shales (500–1180 μm) and kerogens were out-gassed under ultra-high vacuum at 383 K until constant weight. Liquid nitrogen (77 K) and solid carbon dioxide/acetone cryogenic baths (195 K) were used for temperature control. Methane adsorption measurements at 112 K were

achieved using a Hiden Isochema cryostat system cooled by gaseous nitrogen generated from liquid nitrogen. A computer controlled recirculating bath of water/ethylene glycol was used for adsorption measurements at 273 K.

Isotherm repeatabilities were typically $\pm 1.5\%$ for CO_2 adsorption at both 196 and 273 K at 100 kPa and $\pm 1.1\%$ for N_2 uptakes at 77 K and 99 kPa.

2.4.2 High-pressure supercritical methane sorption

A Hiden Isochema Intelligent Manometric Instrument (IMI) was used for high pressure CH_4 adsorption. Shales and kerogen samples were pre-dried at 383 K in a vacuum oven and loaded typically with ~ 10 g shale (particle size range: 500–1180 μm), 0.8–1.3 g kerogen (particle size range as produced from demineralization process) into the IMI sample cell. Displacers were employed to reduce the void volume, because only relatively small quantities of kerogen samples were available. The skeletal volumes of the samples were determined, which also allowed calculation of the corresponding helium densities. Methane isotherms were measured at 318, 338 and 358 K. Isotherm experimental repeatabilities were typically $\pm 5.0\%$ for both shale and kerogens at 10 MPa. Helium isotherms were measured at all temperatures as blank determinations for no adsorption to monitor skeletal densities and leak-test the instrument.

Saturated vapor pressures (p_0) and gas densities were calculated from the NIST Standard Reference database 23 by using the REFPROP Version 9.0 software [37]. The following equations of state (EOS) were used: CO_2 (Span et al.) [38], N_2 (Span et al.) [39], CH_4 (Setzmann et al.) [40] and helium (Lemmon et al.) [37].

2.5 Mercury injection capillary pressure (MICP) porosimetry

A Micromeritics Autopore IV Mercury Injection Porosimeter was used in the study [34]. MICP could only be used for the shales since kerogens only occur as very small particles in shale. Also, kerogens are plastic and deform under the very high pressures used in the technique. Initially shale samples were freeze-dried for 48 h. Samples with a volume of $\sim 1 \text{ cm}^3$ were then outgassed under vacuum prior to MICP porosimetry studies. The mercury pressure was increased stepwise from 1.379 up to 268.9 MPa in order to characterize the meso/macroporosity. MICP bulk volumes/densities of shale were calculated from the known sample mass and the grain or helium density of the sample. The difference of the volume of mercury injected at 1.379 MPa and 268.9 MPa was used to calculate MICP pore volumes. Surface topography and micro fractures related to the de-stressing and drying of geological samples were

excluded (see Table 1). The Washburn equation [41, 42] is derived for cylindrical pores and calculations were carried out assuming a contact angle 141° between mercury and the particle surface, and a surface tension of 0.485 N m^{-1} [24, 43, 44]. The mercury pressures were used to predict pore throats (constrictions) with equivalent diameters between 1093 nm at 1.379 MPa and 5.6 nm at 268.9 MPa. These diameters should be regarded as equivalent pore diameters because of the variation in pore shape in the heterogeneous shale materials.

2.6 Microscopy studies

Scanning electron microscopy (SEM) was carried out using a Hitachi SU-70 High Resolution Analytical instrument equipped with an Oxford Instrument Energy Dispersive X-ray (EDX) microanalysis system (INCA Energy 700). Samples were prepared as carbon-coated polished thin sections. Back Scattered Electron (BSE) mode used a YAG detector. Some samples (3 mm diameter) were polished with an argon broad ion beam (BIB) in a GATAN 691 Precision Ion Polishing System (PIPSTM) to reduce shale topography. Secondary Electron (SE) images were obtained using a through-the-lens detector (TLD) at magnifications of up to 10,000 \times . EDX analysis was used to generate elemental and phase distributions of selected areas.

3 Results and discussion

3.1 Supercritical methane adsorption on shale

Initially it was necessary to provide information on supercritical methane adsorption characteristics under simulated geological conditions in order to gain an insight into the variation of sorption capacity with temperature and pressure.

3.1.1 Isotherms

At the start of the study it was apparent that the accuracy of supercritical gas adsorption measurements at high pressures was not established. Subsequently, an investigation of the accuracy of high pressure supercritical CO_2 adsorption measurements on highly porous activated carbons was reported [45]. Similar studies have been reported recently for CO_2 adsorption on zeolite ZSM-5 [46]. Initial validation of isotherm reproducibility successfully used a small sample (~ 500 mg) of F400 activated carbon. The development and validation of high pressure adsorption techniques for measuring supercritical adsorption isotherms for shales is much more challenging than for activated carbon since the adsorption is two orders of

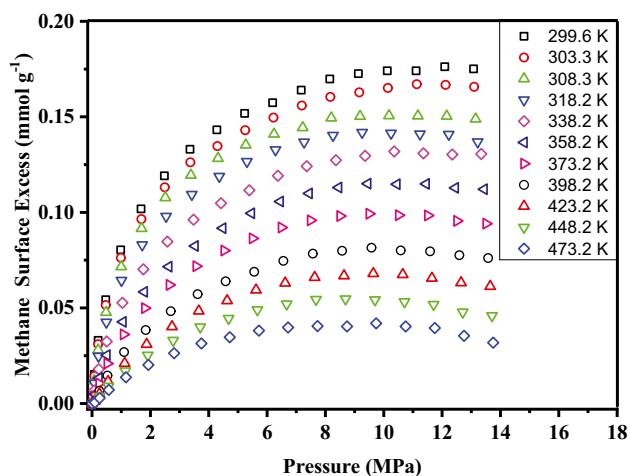


Fig. 2 Supercritical methane adsorption isotherms for Alum 1 shale for temperatures in the range 299.6–473.2 K (data from [35])

magnitude lower. This led to the use of larger sample amounts (typically 10 g of shale and ~ 1 g of kerogen) being used to obtain the required accuracy. These techniques were used to investigate the variation of isotherms under a range of simulated geological pressure and temperature conditions and validate the consistency of the data. Figure 2 shows methane adsorption isotherms for shale Alum 1 over the temperature range 299.6–473.2 K and pressures up to ~ 140 bar [35]. These conditions cover the temperature and pressure range that simulate geological conditions. The reproducibility of the measurements were confirmed in a ‘round robin’ study of an immature Posidonia shale and an over-mature Upper Chokier formation shale [47]. The Newcastle results were in the middle of the set of results confirming reasonable agreement.

The surface excess isotherm can be converted to the isotherm for the absolute amount using the equation below

$$n_{abs} = n_{ex} + \rho_b * V_{ad} \tag{1}$$

where n_{abs} is the absolute amount adsorbed, n_{ex} is the surface excess determined experimentally, ρ_b is the bulk gas phase density and V_{ad} is the adsorption pore volume. This equation has been used for crystalline materials, where the structure has been determined from crystallographic studies [48–51]. There is good agreement between crystallographic and adsorption pore volumes. However, shales are heterogeneous materials with a wide pore size distribution and not all larger pores have significant gas adsorption. The issue for shales is to identify the pore size ranges and volumes associated with both adsorption and high pressure compressed gas, which are the phases in equilibrium for methane storage in shale.

3.1.1.1 Isosteric enthalpy of adsorption The isotherm data were used to calculate the isosteric enthalpy of adsorption using the Clausius–Clapeyron equation and to validate the consistency of the data [35]. The derivation of this equation assumes that the gas is ideal and the adsorbed phase volume is neglected. These two assumptions may lead to errors at high pressures [52], which can be examined using graphs $\ln(\text{Fugacity})$ versus $1/T$ at various surface coverages for the set of data shown in Fig. 3. The linearity of the graphs demonstrate the consistency of the data over simulated geological conditions.

The determination of isosteric enthalpy of adsorption (Q_{st}) graph is limited by the availability of data at constant surface coverage. The Clausius–Clapeyron graph for the lowest 5 temperatures and 2.85–7.62 MPa and ~ 70% of maximum surface excess ($0.125 \text{ mmol g}^{-1}$) gives Q_{st} of $20.5 \pm 1.3 \text{ kJ mol}^{-1}$. This compares with a Q_{st} of $19.0 \pm 0.2 \text{ kJ mol}^{-1}$ for a surface excess of 0.01 mmol g^{-1} . Graphs of $\ln(\text{Pressure})$ versus $1/T$ gave very similar values for Q_{st} . These values are typical for adsorption of CH_4 on shales [8], activated carbon [53–55], coal [56] and metal organic framework materials [57]. There is no evidence for any significant variation in isosteric enthalpy of adsorption even though shale is heterogeneous with a variety of inorganic mineral and organic kerogen components.

3.1.2 Isobars

The variation of CH_4 surface excess with temperature at constant pressure is important in assessing shale adsorption characteristics under simulated geological conditions. The adsorption isotherm data in Fig. 2 provides information from which the dependence of surface excess

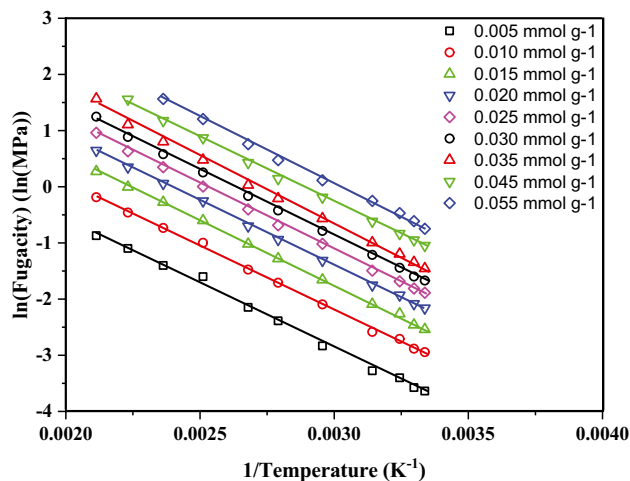


Fig. 3 Clausius–Clapeyron graphs of $\ln(\text{Fugacity})$ versus $1/\text{temperature}$ for the supercritical adsorption of methane on Alum 1 shale (data from Ref. [35])

adsorption on temperature can be determined. Figure 4 shows a comparison of surface excess (SE) isobars for a phenomenological model [$SE = k/T$ where k is a constant and T is temperature (K)] and the equation proposed by Illin ($SE = k_1 \exp(-k_2 T^{0.5})$) where k_1 and k_2 are constants and T is the temperature (K) [58, 59]. Comparison of the model over the pressure range 0.5–13.5 MPa shows that both equations fit the data, but the simple phenomenological model provides the slightly better fit to the data. Previous studies of supercritical methane adsorption on a metal organic framework have shown that these isobar equations provide good descriptions of the data [57].

3.1.3 Subcritical CH₄ adsorption studies

Since physisorption increases with decreasing temperature, assessment of the maximum amount of methane that can be adsorbed on a shale was obtained using low temperature subcritical adsorption isotherm. A comparison of the subcritical isotherms for nitrogen, methane and

carbon dioxide on a relative pressure basis for the Alum 1 shale are shown in Fig. 5. The total sorption pore volume obtained from subcritical CH₄ adsorption at 112 K represents the maximum pore volume available for methane adsorption since the low temperature allows measurements with a relative pressure close to 1, where condensation occurs. There is an experimental difficulty in measuring subcritical CH₄ adsorption because of the lack of a suitable cryogenic fluid. The measurement was carried out using a special cell with circulation of cooled gaseous nitrogen, but this is experimentally challenging. The Dubinin-Radushkevich (DR) ultramicropore volume obtained for the Alum 1 shale from CO₂ adsorption at 273 K was 12.9 mm³ g⁻¹. The sorption pore volumes for subcritical CO₂ at 195 K (16.8 mm³ g⁻¹) and CH₄ at 112 K (18.0 mm³ g⁻¹) are similar as expected from the Gurvitch Rule [60]. This rule states that the adsorption uptakes at relative pressure ≈ 1 on a given adsorbent when expressed as a volume of liquid, using the liquid density, are similar for all adsorptives. Therefore, the CO₂ sorption pore volume was used as a substitute for the CH₄ total pore volume in subsequent studies of shale maturity, since it is much easier to use solid CO₂/acetone as the cryogenic liquid [34, 35]. Therefore, when studying the effect of shale and kerogen maturity on supercritical methane adsorption, correlations between subcritical CO₂ sorption pore volume and high pressure supercritical methane adsorption were examined to validate this approach.

3.2 Porosity characterization

Porosity characterization methods are well developed with the exception of the measurements of supercritical methane adsorption capacities for shales and kerogens

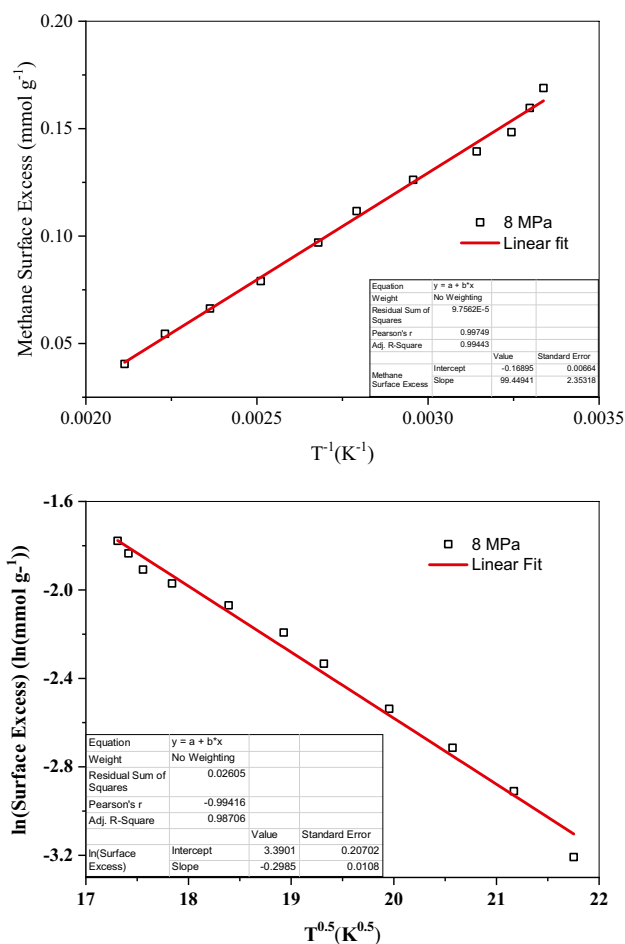


Fig. 4 Isobars for supercritical CH₄ adsorption on Alum 1 shale **a** phenomenological model [35] and **b** Illin equation [58]

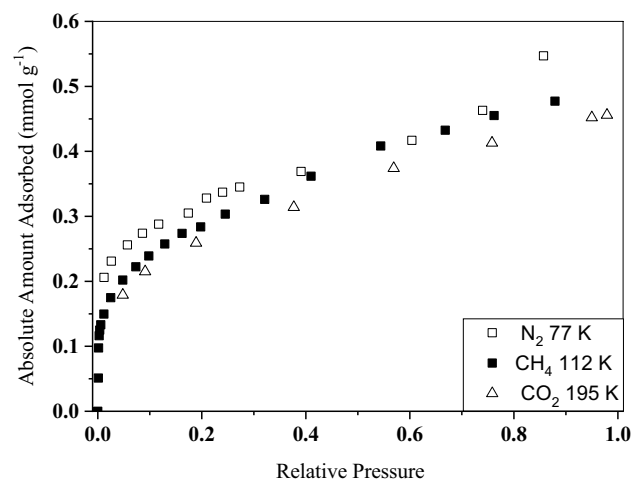


Fig. 5 Subcritical adsorption isotherms for CH₄ (112 K), N₂ (77 K) and CO₂ (195 K) for Alum 1 shale [35]

under a range of conditions, which simulate geological conditions of high pressure and temperature. The methane adsorbed phase is expected to be almost exclusively stored in the smallest pores of shales and kerogens. The porosity in which compressed gas is stored in equilibrium with the adsorbed phase mainly involves the larger pores. The strategy for the characterization of shale porosity was to quantify all the porosity from macro- through meso- to micropores to complement the supercritical methane adsorption studies. A range of microscopy, gas adsorption, mercury injection and pycnometry techniques were used in order to explore the full pore size range in shales so that the relative amounts of adsorbed and compressed CH₄ could be established. Small-angle neutron scattering techniques may also be used to characterize shale structure and porosity [17–19] but these techniques were not available for this study. The measurements techniques available and size ranges covered are shown in Fig. 6.

Mercury injection capillary pressure (MICP) porosimetry is an established technique for assessing porosity in minerals and it was important in providing measurements of macro and meso (> 5 nm) porosity in shales. MICP porosimetry measures pore throats (smaller passages or constrictions in the pore structure), which are connections between larger pore bodies. The pore throats are obvious restrictions in the pore structure and are typically a fraction of the pore size. The Washburn equation [42] was used to calculate the equivalent pore diameters for mercury entering pores at specific pressures [24, 41, 43, 44]. At a pressure of 1.379 MPa mercury enters pores of > 1093 nm diameter and this allows the shale bulk density (ρ_{HgBulk}) to be determined. Therefore $1/\rho_{HgBulk}$ is the volume of shale and pores < 1093 nm. Helium is not adsorbed to any significant extent under ambient conditions and enters all accessible pores. Therefore, the volume of shale is $1/\rho_{He}$ where ρ_{He} is the helium density measured by pycnometry

[34]. As expected grain density and helium density have a strong linear correlation and therefore ρ_{Grain} can be used in place of ρ_{He} . Therefore, the shale total pore volume (TPV) for equivalent pore diameters < 1093 nm and Total Porosity are given by the equations below

$$Total\ pore\ volume (< 1093\ nm) = \frac{1}{\rho_{HgBulk}} - \frac{1}{\rho_{He}} \tag{2}$$

$$Total\ porosity (< 1093\ nm) = 1 - \frac{\rho_{HgBulk}}{\rho_{He}} \tag{3}$$

The Washburn equation indicates that a capillary pressure of 1.379 MPa fills pore throats up to 1093 nm and 268.9 MPa fills up to 5.6 nm. Therefore, the MICP pore volume provides a measure of the macro + mesopore volume between equivalent pore diameters of 1093 and 5.6 nm from the amounts injected at pressure of 1.379 and 268.9 MPa.

Subcritical gas adsorption studies are routinely used for characterizing micro and mesoporous structures of porous materials using a variety of isotherm equations [61]. Adsorption occurs in micropores (< 2 nm) and some mesopores (> 2 nm). The Brunauer Emmett and Teller (BET) equation [62] accounts for multilayer adsorption and is usually applied to N₂ adsorption isotherm data at 77 K. N₂ adsorption isotherm data at 77 K has also been used to determine pore size distributions in order to gain insights into organic matter in coal and shales [63, 64]. However, characterization parameters such as surface areas, obtained from N₂ adsorption at 77 K may have issues due to activated diffusion effects in ultramicroporous materials at very low temperatures [65–67] and may overestimate surface areas in microporous materials. In this case CO₂ adsorption is commonly used to characterize activated carbons [61, 68] because of the higher adsorption temperature. CO₂ adsorption on shale is also of interest in relation to storage of CO₂ in depleted shales for sequestration applications [64]. The Dubinin–Radushkevich (DR) equation [69] is often applied to CO₂ isotherms at 273 K to determine the ultramicropore volumes (< 0.7 nm) [70–72]. Adsorption at 195 K was used to provide total CO₂ sorption pore volumes. Nitrogen adsorption at 77 K is used to provide BET surface areas and DR micropore volumes (0.3–2 nm) [72].

These techniques were used to characterize the porous structure in shales and kerogens (see Fig. 7) [34]. The CO₂ sorption pore volumes were obtained from adsorption isotherms at 195 K. Ultramicropore volumes were obtained using the Dubinin–Radushkevich equation from CO₂ adsorption at 273 K. The relationships of these parameters with supercritical methane adsorption is important in the context of accounting for all porosity present in shales by providing pore volumes in relation to pore size for shales.

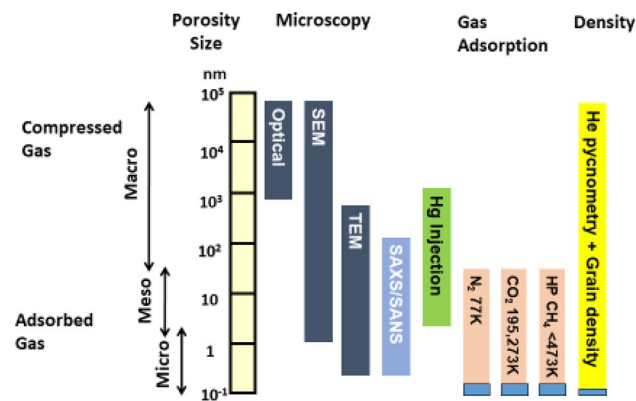
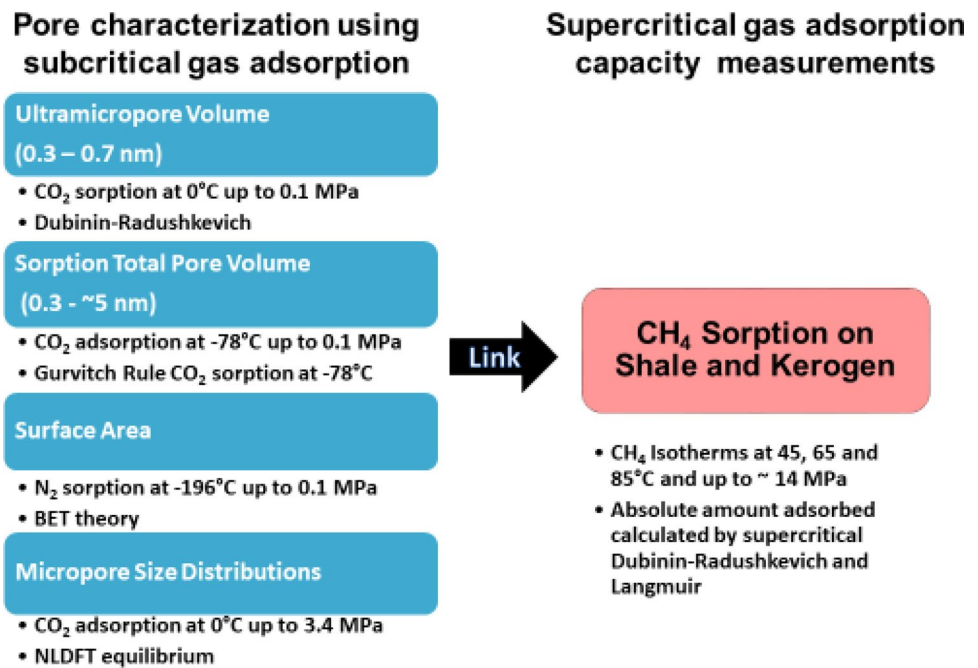


Fig. 6 Measurement techniques and size ranges for characterization of porosity

Fig. 7 Pore characterization using adsorption based methodologies



Since shales are heterogeneous materials, microscopic methods were used to visualize macro and meso porosity in order to understand the storage of methane in pores and flow properties of gases through pores. Microscopic methods showed that the suite of Posidonia shale samples did not have significant amounts of porosity above ~ 1 μm in diameter.

3.3 The role of shale structure and kerogen maturity

Supercritical CH₄ isotherms for Posidonia shales and the corresponding isolated kerogens at 338 K are shown in Fig. 8 [34]. The isotherms have a Type I shape in the IUPAC Classification scheme [73]. The adsorption isotherms for shales show that the surface excess goes through a minimum for the Harderode (oil window) shales. The adsorption isotherms are similar for Wickensen (immature) and Haddessen (gas window) shales. Similar trends were observed [34] for adsorption on shales at 318 and 358 K.

The supercritical CH₄ isotherms for isolated kerogens show different trends (See Fig. 8b). The Haddessen (gas window) kerogens have higher surface excess uptakes than the Wickensen (immature) shales. The Harderode and Wickensen kerogens have similar surface excess isotherms. A similar trend was observed for the adsorption isotherms for isolated kerogens at 338 K. Comparison of the CO₂ adsorption isotherms at 195 K for the suite of shales and kerogens show that they have similar trends for the differences in the order of individual Wickensen, Harderode and Haddessen shales and kerogens as shown for supercritical

methane adsorption described above. The CO₂ sorption pore volumes for kerogens (71.8–113 mm³ g⁻¹) are x 5–8 those of shales (8.3–16.4 mm³ g⁻¹). Thus the trends for shales and kerogens are confirmed. The high pressure shale and kerogen CH₄ isotherms can be parameterized and modelled using Langmuir and modified Langmuir equations [34, 35].

It is apparent from comparison of the isotherms of shales and isolated kerogens that the kerogens adsorb 5–8 times more methane than the corresponding shales. The surface excess uptakes of methane on the Posidonia suite of shales at 338 K were in the range 0.056–0.110 mmol g⁻¹ (40–78 scf t⁻¹) while the corresponding range for isolated kerogens was 0.36–0.7 mmol g⁻¹ (253–499 scf t⁻¹) [34]. The isosteric enthalpies of adsorption (Q_{st}) for dry Posidonia shales and kerogens were calculated by two methods [74, 75] and were in the range 11.2–15.7 kJ mol⁻¹ for shales and 8.5–17.2 kJ mol⁻¹ for kerogens [34]. The Q_{st} values for CH₄ adsorption on alum 1 shale for surface excess values in the range 0.01–0.125 mmol g⁻¹ were 19–20.5 kJ mol⁻¹. Ji et al. reported that pre-gas window shales had Q_{st} values in the range 7.3–15.3 kJ mol⁻¹ and a gas window shale was 18.4 kJ mol⁻¹ [8]. These Q_{st} values are similar to previously published values for carbon (9–24 kJ mol⁻¹) [53–55], coal (10–22 kJ mol⁻¹) [56] and shale (7–24 kJ mol⁻¹) [8, 76–78].

Comparison of low temperature subcritical CH₄ and CO₂ adsorption studies at 112 K and 195 K at relative pressure = 1 showed the sorption pore volumes for both gases were very similar in agreement with Gurvitch's rule [35]. This represents the methane maximum sorption volume, which includes micropores (< 2 nm) and some mesopores.

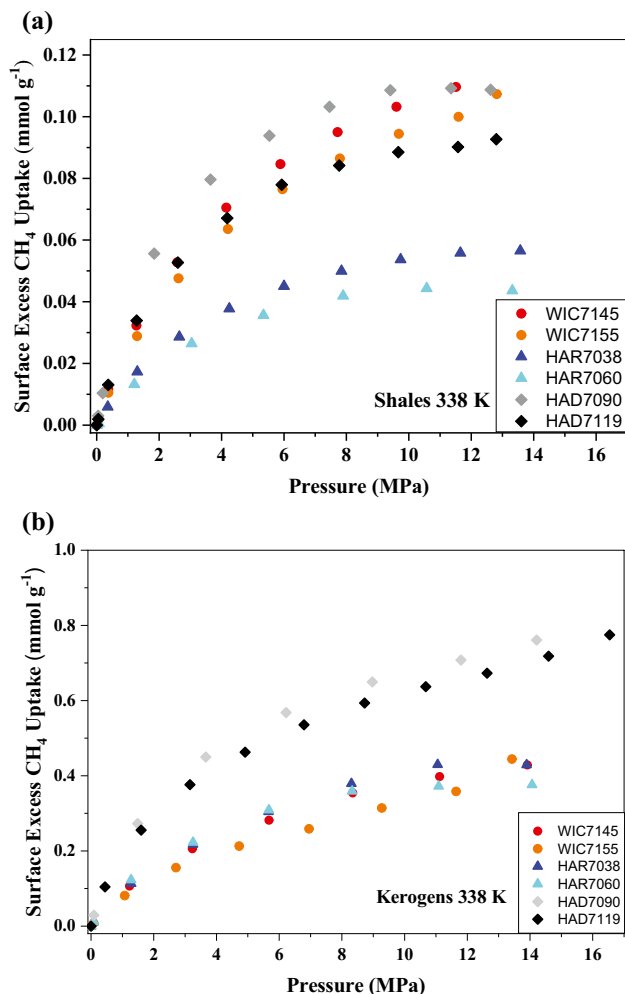


Fig. 8 Supercritical CH₄ adsorption isotherms at 338 K for **a** shales and **b** isolated kerogens (data from [34])

Figure 9 shows the variation of CH₄ surface excess at 11.5 MPa and 338 K with CO₂ sorption pore volume for both Posidonia shales and kerogens [34]. The correlation for shales alone had a regression coefficient (R^2) of 0.96 whereas there was more scatter for the kerogens with a R^2 value of 0.76. It is evident that there is a good overall linear correlation ($R^2 = 0.956$) for the combined shale and kerogen data showing the linear relationship passing through the origin between supercritical methane adsorption and CO₂ sorption pore volume [34]. Similar correlations were observed for CH₄ supercritical adsorption on shales and kerogens at 318 K. This observation supports the use of CO₂ sorption pore volume in the assessment of porosity available for high pressure CH₄ adsorption to account for the full range of shale porosity in order to assess the storage of compressed and adsorbed gas.

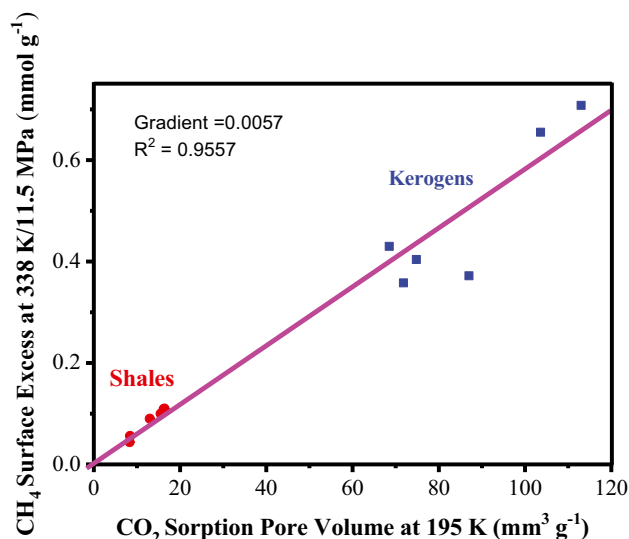


Fig. 9 The variation of high pressure supercritical CH₄ surface excess adsorption at 11.5 MPa and 338 K for Posidonia shales and kerogens with subcritical CO₂ sorption pore volume [34]

The interrelations between high-pressure CH₄ sorption capacity, maturity, and pore structure characteristics were investigated for shales and isolated kerogens. Mercury injection capillary pressure (MICP) porosimetry measurements could only be studied for larger particle sizes, which are only available for shales. Kerogens only occur as very small particles distributed throughout shales.

Microscopy studies showed that the shales only have sub-micrometre pores. The maximum pore throat size in the shale samples were also determined from MICP. The Washburn equation [42] provides the equivalent pore diameters as a function of injection pressures. The values for maximum pore throat size in the shales pass through a minimum (21 nm for HAR7038 and 24 nm for HAR7060) for the oil window shales. The largest maximum pore throat size was 547 nm in gas-window shale HAD7199. The maximum pore throat sizes for WIC7145, WIC7155 and HAD7090 were all very similar (~156 nm) [34]. The results show that the MICP range (< 1093 nm) studied covers the upper macropore range in this suite of Posidonia shale samples.

Figure 10 shows the variation of Total Pore Volume (< 1093 nm) versus the sum of the CO₂ Sorption Pore Volume and MICP pore volume (5.6–1093 nm). It is apparent that there is a linear relationship ($R^2 = 0.99$) intersecting the origin, thereby accounting for all the porosity in the shales. This relationship allows predictions of the volumes available for adsorbed and compressed methane and hence stored amounts of adsorbed and compressed gas using an estimated density for the adsorbed phase and known equations of state for the gas phase.

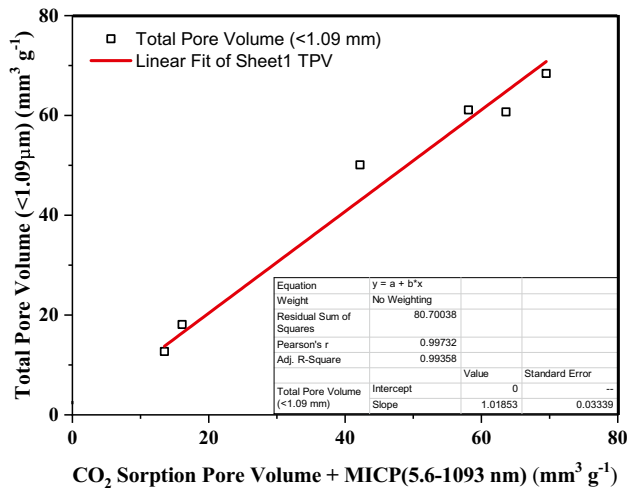


Fig. 10 The variation of shale total pore volume with the sum of CO₂ sorption pore volume and MICP pore volume [34]

$$\begin{aligned} \text{Total pore volume (<math>< 1093 \text{ m}</math>)} \\ &= \text{CO}_2 \text{ sorption pore volume} \quad (4) \\ &+ \text{MICP pore volume (5.6 – 1093 nm)} \end{aligned}$$

The DR micropore, CO₂ sorption and MICP porosimetry total pore volumes for shales pass through a minimum in the oil window. Wickensen (immature) shales have CO₂ sorption pore volumes that are ~25% of the total pore volume. HAR (oil window) shales have CO₂ sorption pore volumes that are 46–66% of total pore volume and there is less porosity present as larger pores. This is due to compaction and bitumen filling. HAD (gas window) shales have CO₂ sorption pore volume that are 21–32% of total pore volume. The DR CO₂ micropore volumes as a percentage of the CO₂ sorption pore volume were 41–62% and 40–52% for the shales and kerogens, respectively. This suggests that there is ultramicroporosity in the mineral component of shale as well as the kerogen. In comparison, the DR micropore volumes of coals are in the range 0.014–0.052 cm³ g⁻¹ [79–81]. The trend observed for CO₂ DR micropore volume with coal maturity has a minimum for medium volatile bituminous coals. This is ascribed pore filling by low volatile hydrocarbon species followed by decomposition during coalification [82].

Figure 11 shows the variation of DR micropore volume, CO₂ sorption pore volume and Hg total pore volume with vitrinite reflectance for Posidonia shales and Fig. 12 shows the corresponding variation of DR micropore volume and CO₂ sorption pore volume for isolated kerogens. Comparison of Figs. 11 and 12 shows that the minimum in CO₂ sorption pore volume observed for the oil window shales is not observed for the corresponding kerogens indicating the significant contribution of porosity in the mineral phase of the shale. The clay content of the Posidonia shales

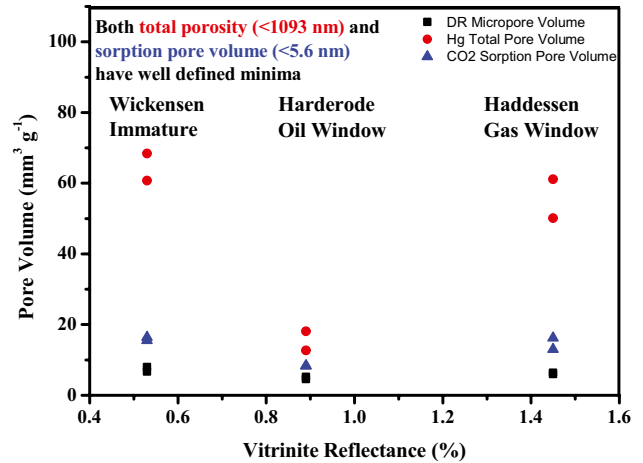


Fig. 11 The variation of Dubinin–Radushkevich micropore volume, CO₂ sorption pore volume ($\le 5.6 \text{ nm}$) and Hg total pore volume from MICP porosimetry at 1093 nm with vitrinite reflectance for Posidonia shales (data from Ref. [34])

is relatively small with illite/smectite and kaolinite in the range 18.5–26.2 wt% and 1.1–8.9 wt%, respectively. These clays adsorb CH₄ and are present in dry shales [76, 83]. Since the kerogens adsorb 5–8 times more CH₄ than dry Posidonia shales, a correlation with TOC with some scatter associated with differences in maturity and mineral content would be expected (Fig. 12). Clays are present in the Posidonia shales and dry clays adsorb methane [76, 83]. The isotherms observed for shale, clay content and kerogen and the composition of the shales do not always account for all the adsorbed CH₄. This suggests that some porosity occurs in other mineral components and possibly occurs between organic and mineral matter interfaces [34]. This observation and the different trends for the series

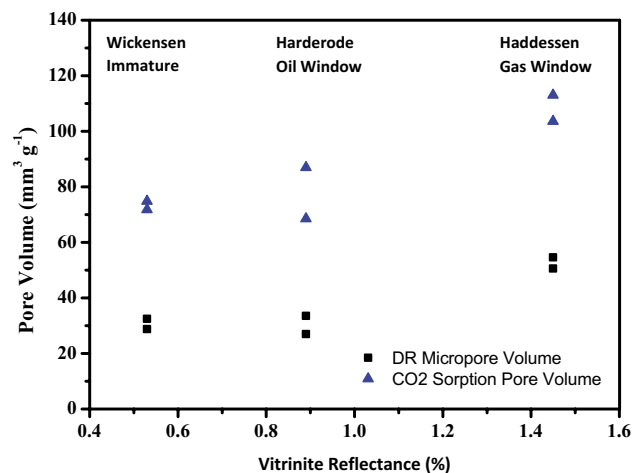


Fig. 12 The variation CO₂ sorption pore volumes and DR micropore volumes with vitrinite reflectance for isolated kerogens derived from Posidonia shales

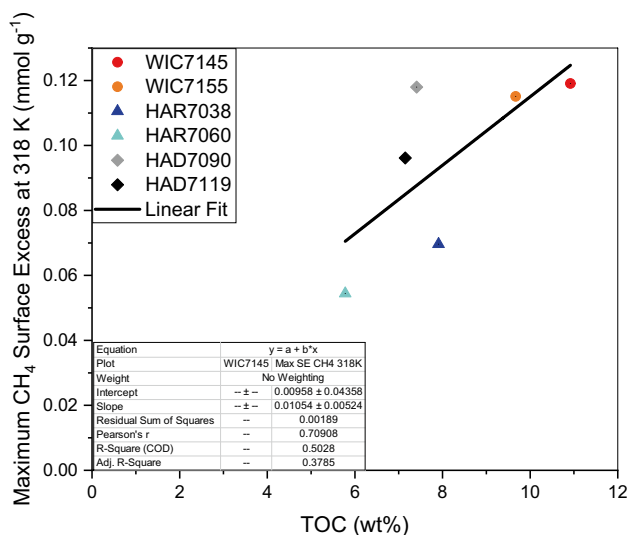


Fig. 13 The variation of maximum CH₄ surface excess uptake at 318 K with TOC [34]

of shales and kerogen adsorption isotherms in Fig. 8, may explain the relatively large scatter in the points in the linear correlation between maximum shale capacity at 318 K and TOC shown in Fig. 13.

Porosity distribution between the mineral and kerogen phases is important in the context of identifying correlations between methane storage and geochemical characterization data. Taking into consideration the TOC, 30–60% of the shale sorption pore volume is due to adsorption in the kerogen even though in these shales the TOC is 5.8–10.9% of the shale (see Fig. 14a) [34]. Since the CO₂ sorption pore volume has a linear correlation with supercritical CH₄ adsorption (Fig. 9) and the correlation in Eq. (4), the shale pore volume (5.6–1093 nm) determined using MICP porosimetry contains almost exclusively compressed gas which should be easily accessible. Figure 14b shows a typical comparison of supercritical shale adsorption of methane normalized to TOC with the kerogen methane isotherm [34]. These isotherms have a very similar shape suggesting that the kerogen in the shale has similar adsorption characteristics to the isolated kerogen indicating that the kerogen extraction process had little or no effect on the kerogen adsorption characteristics. Comparisons for other Posidonia shales and kerogens show the same similarity in isotherm shapes. This suggests that the kerogen adsorption properties are unchanged by the extraction/isolation process and implies that adsorption also takes place in the inorganic mineral phase. This is not surprising since clays are present. Some differences might also arise from accessibility within the rock matrix, but there is no direct evidence to support this proposition.

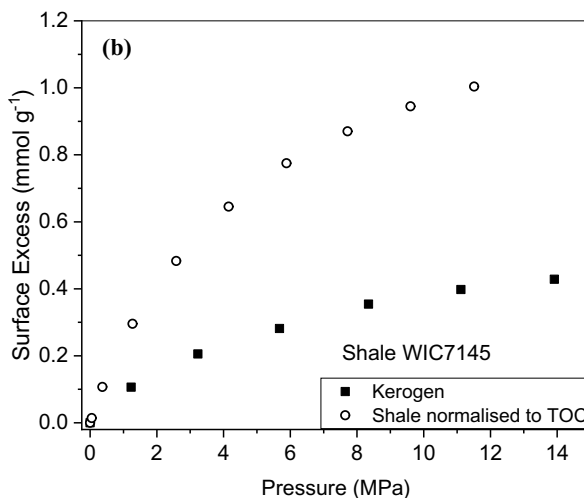
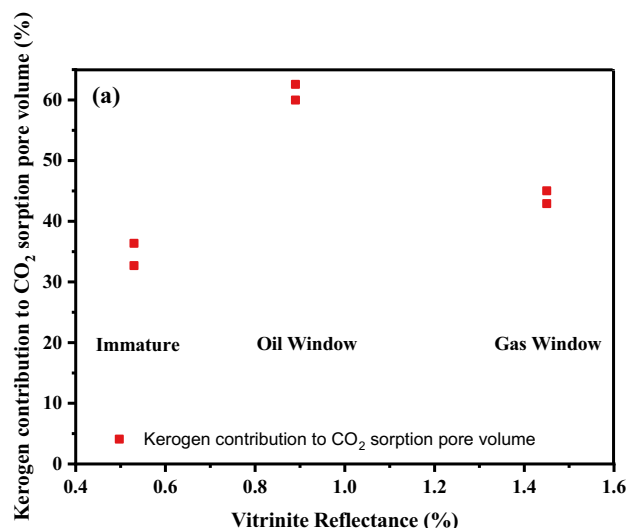


Fig. 14 Kerogen contributions to Posidonia shale adsorption **a** CO₂ sorption pore volumes (195 K), **b** comparison of supercritical CH₄ adsorption isotherms at 338 K for shale normalized to TOC with the isolated immature kerogen WIC7145

The research has been extended further to examine the microporous region by microscopic visualization and quantification of pores, which is significant in understanding the sorbed gas versus compressed gas capacity as well as the flow properties. Microscopy was used to study a wider range of 26 Posidonia shales [36]. Typical micrographs are shown in Fig. 15. In the case of immature shales, pores quantifiable by SEM (> ca. 50 nm diameter) only account for small part of total porosity. Visible pores are mainly associated with biogenic calcite. There was essentially no macroporosity in the clay matrix or kerogen components. Porosity loss in the oil window shales is due to a) compaction, b) carbonate cementation and possible swelling of kerogen by retained oil. In the gas window shales, porosity

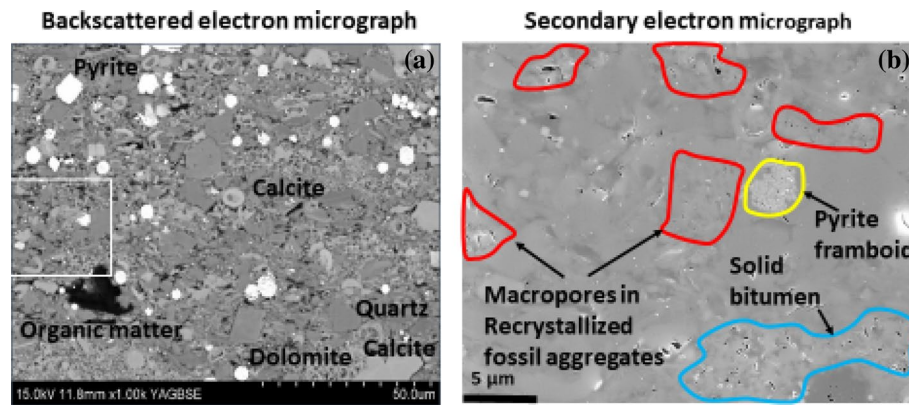


Fig. 15 Micrographs of HAR 7060 shale (oil window): [36, 84]. **a** Back scattered electron micrographs calcareous shale with densely packed nanofossil aggregates. Partial recrystallization of the nanofossil rich shale matrix and presence of calcite and dolomite

cement all indicate diagenetic transformation of the original material. **b** Secondary electron micrograph: Pores in recrystallized fossil aggregates occur at the interface with organic matter filling the intra-granular space

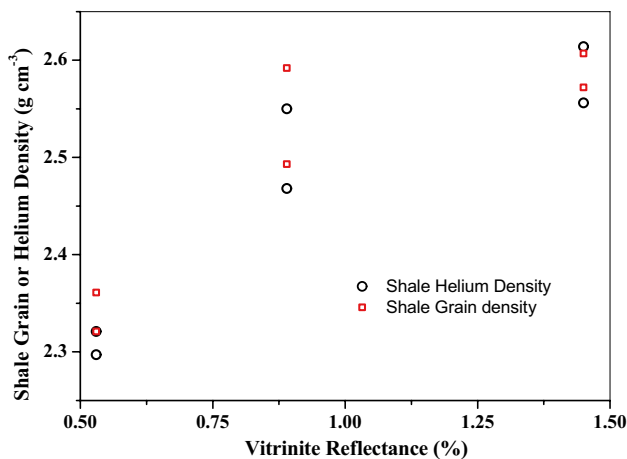


Fig. 16 The variation of helium and grain densities for shales for Posidonia shales with vitrinite reflectance (data from Ref. [34])

increases due to the formation of meso and macro pores in organic matter related to thermal cracking and gas generation. The macroporosity varies greatly and this reflects the different physicochemical characteristics of individual organic phase particles and the surrounding rigid mineral matrix preventing compaction of the more ductile organic phases. Helium and grain densities have a linear relationship and increase with increasing maturity for shales (see Fig. 16) [34]. The development of organic macroporosity cannot alone account for the porosity increase from oil to gas window. There is an accompanying change in the volume of micro and meso porosity. Intra-organic matter

pores are a characteristic feature of gas window shales, but macroporosity is most commonly observed at the kerogen-mineral interface (see Fig. 15).

Broad Ion Beam (BIB) -SEM, MICP, and gas sorption methods individually only generate partial descriptions of shale pore systems. In combination, they generate a quantitative description of the size distribution and connectivity of pores ranging in size from nanometer to micrometer [36, 84]. Pore size and volume data have been placed into a mineralogical clay-rich, microfossil-rich and organic matter and textural framework in order to be more predictive about the pore systems of shales generally. Clay-rich domains are both micro- and meso-porous (pore diameters < 40 nm) at all maturities. At temperatures below gas generation macropores are mainly 50–300 nm diameter. During oil generation carbonate-related macropores are traps for bitumen with porosity reduced due to bitumen retention and physicochemical compaction.

Gasification of organic matter increases porosity due to the loss of both solid phase and liquid phase organic matter. The porosity generated does not only occur within the organic matter but is physically associated with organic matter within carbonate porosity. Evolution of porosity with increasing maturity is thus linked to changes in both carbonate and organic matter domains. By quantifying the nature of pores in the various mineral and organic building blocks of shales we can consider the larger scale flow properties of shales and thus their potential either to transmit fluid (useful for a shale gas reservoir) or to retain fluid (useful for a CO₂ or nuclear waste storage site). These findings are consistent with a recent study [85].

4 Conclusions

The storage of methane in shale geological reservoirs is complex due to the heterogeneous nature of shale, which contains both mineral and amorphous organic kerogen components. Adsorption of methane under simulated geological conditions presented major challenges due to the low shale methane adsorption capacities and the wide range of temperatures (300–473 K) and pressures (< 150 bar). Therefore, detailed validation of the accuracy and reproducibility of the experimental methods was required as a prerequisite to studying other aspects of shale gas storage.

High pressure methane sorption capacities and pore characteristics of bulk shales and isolated kerogens were investigated for immature, oil-window and gas-window samples from the lower Toarcian Posidonia formation. The equivalent maximum pore throat diameter for Posidonia shale samples were in the range 21–547 nm and optical microscopy did not reveal any visible porosity > 1 μm . However, only two samples at each maturity level have been studied. Total pore volumes obtained from MICP porosimetry and subcritical CO_2 sorption volumes (195 K) of organic-rich Posidonia shales decrease through the oil-window and then increase into the gas-window. The sum of porosities measured by CO_2 sorption at 195 K and mercury injection capillary pressure porosimetry [1.379–268.9 MPa (1093–5.6 nm)] were equal to the corresponding total pore volume (< 1093 nm) for shales thereby giving an equation that accounts for virtually all the available porosity in this series of shales. The mercury injection at 268.9 MPa occupies pores with constrictions larger than ca. 5.6 nm indicating that porosity measured by CO_2 adsorption at 195 K is largely within pores smaller than 5.6 nm. The CO_2 sorption pore volume represented 21–66% of the total pore volume in these shales, while the meso/macropore volume from MICP was 40–79% of the total pore volume. Around 40–50% of the CO_2 sorption pore volume was within the DR ultramicroporosity studies (< 0.7 nm) in the shales studied. Oil window shales have the smallest meso/macropore fraction and the largest CO_2 sorption pore volume fraction of the total porosity. It can be inferred that the adsorbed methane is predominantly in pores < 5.6 nm and the ‘free’ compressed gas is in the larger pores (5.6–1093 nm). The 5.6–1093 nm meso-macropore volume represents the major part in the Wickensen (78%) immature and Haddessen (63%) gas window shales, but only 41% of Harderode oil window shales. Hence the correlation allows an estimate of the contribution of the adsorbed and ‘free’ gas phases to the overall methane capacity.

Shale and kerogen adsorption and total organic content considerations indicate that approximately half of the CH_4 sorption on dry shales occurs within the organic matter and this indicates the significance of the mineral phase, including the role of clays. Microscopic studies of the nature of pores show the importance of the intra-granular organic-mineral interface and this should be useful in understanding larger scale flow characteristics. Free compressed gas will flow much faster than sorbed gas, where desorption rates decrease with decreasing pore size.

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Compliance with ethical standards

Conflict of interest On behalf of all authors, the corresponding author states that there is no conflict of interest.

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References

1. Annual Energy Outlook 2019 (2019) US Energy Information Association. <https://www.eia.gov/outlooks/aeo/pdf/aeo2019.pdf>. Accessed 28 Nov 2019
2. Ambrose RJ, Hartman RC, Diaz-Campos M, Akkutlu IY, Sondergeld CH (2012) Shale gas-in-place calculations part I: new pore-scale considerations. *Spe J* 17(1):219–229. <https://doi.org/10.2118/131772-pa>
3. Montgomery SL, Jarvie DM, Bowker KA, Pollastro RM (2005) Mississippian Barnett Shale, Fort Worth basin, north-central Texas: gas-shale play with multi-trillion cubic foot potential. *AAPG Bull* 89(2):155–175. <https://doi.org/10.1306/09170404042>
4. Pepper AS, Corvi PJ (1995) Simple kinetic-models of petroleum formation. 1. Oil and gas generation from Kerogen. *Mar Pet Geol* 12(3):291–319. [https://doi.org/10.1016/0264-8172\(95\)98381-e](https://doi.org/10.1016/0264-8172(95)98381-e)
5. Ross DJK, Bustin RM (2009) The importance of shale composition and pore structure upon gas storage potential of shale gas reservoirs. *Mar Pet Geol* 26(6):916–927. <https://doi.org/10.1016/j.marpetgeo.2008.06.004>
6. Chalmers GRL, Bustin RM (2008) Lower Cretaceous gas shales in northeastern British Columbia, Part I: geological controls on

- methane sorption capacity. *Bull Can Pet Geol* 56(1):1–21. <https://doi.org/10.2113/gscpgbull.56.1.1>
7. Weniger P, Kalkreuth W, Busch A, Krooss BM (2010) High-pressure methane and carbon dioxide sorption on coal and shale samples from the Parana Basin, Brazil. *Int J Coal Geol* 84(3–4):190–205. <https://doi.org/10.1016/j.coal.2010.08.003>
 8. Zhang TW, Ellis GS, Ruppel SC, Milliken K, Yang RS (2012) Effect of organic-matter type and thermal maturity on methane adsorption in shale-gas systems. *Org Geochem* 47:120–131. <https://doi.org/10.1016/j.orggeochem.2012.03.012>
 9. Gasparik M, Ghanizadeh A, Bertier P, Gensterblum Y, Bouw S, Krooss BM (2012) High-pressure methane sorption isotherms of black shales from the Netherlands. *Energy Fuels* 26(8):4995–5004. <https://doi.org/10.1021/ef300405g>
 10. Lu XC, Li FC, Watson AT (1995) Adsorption measurements in devonian shales. *Fuel* 74(4):599–603. [https://doi.org/10.1016/0016-2361\(95\)98364-k](https://doi.org/10.1016/0016-2361(95)98364-k)
 11. Chareonsuppanimit P, Mohammad SA, Robinson RL, Gasem KAM (2012) High-pressure adsorption of gases on shales: measurements and modeling. *Int J Coal Geol* 95:34–46. <https://doi.org/10.1016/j.coal.2012.02.005>
 12. Chalmers GRL, Bustin RM (2007) The organic matter distribution and methane capacity of the lower Cretaceous strata of north-eastern British Columbia, Canada. *Int J Coal Geol* 70(1–3):223–239. <https://doi.org/10.1016/j.coal.2006.05.001>
 13. Chalmers GRL, Bustin RM (2008) Lower Cretaceous gas shales in northeastern British Columbia, Part II: evaluation of regional potential gas resources. *Bull Can Pet Geol* 56(1):22–61. <https://doi.org/10.2113/gscpgbull.56.1.22>
 14. Gasparik M, Bertier P, Gensterblum Y, Ghanizadeh A, Krooss BM, Littke R (2014) Geological controls on the methane storage capacity in organic-rich shales. *Int J Coal Geol* 123:34–51. <https://doi.org/10.1016/j.coal.2013.06.010>
 15. Li J, Zhou SX, Gaus G, Li YJ, Ma Y, Chen KF, Zhang YH (2018) Characterization of methane adsorption on shale and isolated kerogen from the Sichuan Basin under pressure up to 60 MPa: experimental results and geological implications. *Int J Coal Geol* 189:83–93. <https://doi.org/10.1016/j.coal.2018.02.020>
 16. Chen L, Zuo L, Jiang ZX, Jiang S, Liu KY, Tang JQ, Zhang LC (2019) Mechanisms of shale gas adsorption: evidence from thermodynamics and kinetics study of methane adsorption on shale. *Chem Eng J* 361:559–570. <https://doi.org/10.1016/j.cej.2018.11.185>
 17. Clarkson CR, Freeman M, He L, Agamalian M, Melnichenko YB, Mastalerz M, Bustin RM, Radlinski AP, Blach TP (2012) Characterization of tight gas reservoir pore structure using USANS/SANS and gas adsorption analysis. *Fuel* 95(1):371–385. <https://doi.org/10.1016/j.fuel.2011.12.010>
 18. Mastalerz M, He LL, Melnichenko YB, Rupp JA (2012) Porosity of coal and shale: insights from gas adsorption and SANS/USANS techniques. *Energy Fuels* 26(8):5109–5120. <https://doi.org/10.1021/ef300735t>
 19. Ruppert LF, Sakurovs R, Blach TP, He LL, Melnichenko YB, Mildner DFR, Alcantar-Lopez L (2013) A USANS/SANS study of the accessibility of pores in the Barnett Shale to methane and water. *Energy Fuels* 27(2):772–779. <https://doi.org/10.1021/ef301859s>
 20. Milliken KL, Rudnicki M, Awwiller DN, Zhang TW (2013) Organic matter-hosted pore system, Marcellus Formation (Devonian), Pennsylvania. *AAPG Bull* 97(2):177–200. <https://doi.org/10.1306/07231212048>
 21. Loucks RG, Reed RM, Ruppel SC, Hammes U (2012) Spectrum of pore types and networks in mudrocks and a descriptive classification for matrix-related mudrock pores. *AAPG Bull* 96(6):1071–1098. <https://doi.org/10.1306/08171111061>
 22. Loucks RG, Reed RM, Ruppel SC, Jarvie DM (2009) Morphology, genesis, and distribution of nanometer-scale pores in siliceous mudstones of the Mississippian Barnett Shale. *J Sedim Res* 79(11–12):848–861. <https://doi.org/10.2110/jsr.2009.092>
 23. Borst RL (1982) Some effects of compaction and geological time on the pore parameters of argillaceous rocks. *Sedimentology* 29(2):291–298. <https://doi.org/10.1111/j.1365-3091.1982.tb01726.x>
 24. Yang YL, Aplin AC (1998) Influence of lithology and compaction on the pore size distribution and modelled permeability of some mudstones from the Norwegian margin. *Mar Pet Geol* 15(2):163–175. [https://doi.org/10.1016/s0264-8172\(98\)00008-7](https://doi.org/10.1016/s0264-8172(98)00008-7)
 25. Cartwright JA, Dewhurst DN (1998) Layer-bound compaction faults in fine-grained sediments. *Geol Soc Am Bull* 110(10):1242–1257. [https://doi.org/10.1130/0016-7606\(1998\)110%3c1242:Lbcff%3e2.3.Co;2](https://doi.org/10.1130/0016-7606(1998)110%3c1242:Lbcff%3e2.3.Co;2)
 26. Gensterblum Y, Ghanizadeh A, Cuss RJ, Amann-Hildenbrand A, Krooss BM, Clarkson CR, Harrington JF, Zoback MD (2015) Gas transport and storage capacity in shale gas reservoirs—a review. Part A: transport processes. *J Unconv Oil Gas Resour* 12:87–122. <https://doi.org/10.1016/j.juogr.2015.08.001>
 27. Wang Y, Liu LF, Sheng Y, Wang XM, Zheng SS, Luo ZH (2019) Investigation of supercritical methane adsorption of overmature shale in Wufeng-Longmaxi Formation, Southern Sichuan Basin, China. *Energy Fuels* 33(3):2078–2089. <https://doi.org/10.1021/acs.energyfuels.8b04344>
 28. Liu YL, Hou J (2019) Investigation on the potential relationships between geophysical properties and CH₄ adsorption in a typical shale gas reservoir. *Energy Fuels* 33(9):8354–8362. <https://doi.org/10.1021/acs.energyfuels.9b01905>
 29. Yang F, Xie CJ, Ning ZF, Krooss BM (2017) High-pressure methane sorption on dry and moisture-equilibrated shales. *Energy Fuels* 31(1):482–492. <https://doi.org/10.1021/acs.energyfuels.6b02999>
 30. Wang L, Yu QC (2016) The effect of moisture on the methane adsorption capacity of shales: a study case in the eastern Qaidam Basin in China. *J Hydrol* 542:487–505. <https://doi.org/10.1016/j.jhydrol.2016.09.018>
 31. Li XQ, Krooss BM (2017) Influence of grain size and moisture content on the high-pressure methane sorption capacity of Kimmeridge Clay. *Energy Fuels* 31(11):11548–11557. <https://doi.org/10.1021/acs.energyfuels.7b01298>
 32. Schovsbo NH, Nielsen AT, Klitten K, Mathiesen A, Rasmussen P (2011) Shale gas investigations in Denmark: lower palaeozoic shales on Bornholm. *Geol Surv Den Greenl Bull* 23:9–12
 33. Bernard S, Horsfield B, Schulz HM, Wirth R, Schreiber A, Sherwood N (2012) Geochemical evolution of organic-rich shales with increasing maturity: a STXM and TEM study of the Posidonia Shale (Lower Toarcian, northern Germany). *Mar Pet Geol* 31(1):70–89. <https://doi.org/10.1016/j.marpetgeo.2011.05.010>
 34. Rexer TF, Mathia EJ, Aplin AC, Thomas KM (2014) High-Pressure Methane Adsorption and Characterization of Pores in Posidonia Shales and Isolated Kerogens. *Energy Fuels* 28(5):2886–2901. <https://doi.org/10.1021/ef402466m>
 35. Rexer TFT, Benham MJ, Aplin AC, Thomas KM (2013) Methane adsorption on shale under simulated geological temperature and pressure conditions. *Energy Fuels* 27(6):3099–3109. <https://doi.org/10.1021/ef400381v>
 36. Mathia EJ, Bowen L, Thomas KM, Aplin AC (2016) Evolution of porosity and pore types in organic-rich, calcareous, Lower Toarcian Posidonia Shale. *Mar Pet Geol* 75:117–139. <https://doi.org/10.1016/j.marpetgeo.2016.04.009>
 37. Lemmon EW, Huber ML, McLinden MO (2010) NIST reference fluid thermodynamic and transport properties—REFPROP. NIST Standard Reference Database 23. U.S. Department of Commerce, Boulder

38. Span R, Wagner W (1996) A new equation of state for carbon dioxide covering the fluid region from the triple-point temperature to 1100 K at pressures up to 800 MPa. *J Phys Chem Ref Data* 25(6):1509–1596. <https://doi.org/10.1063/1.555991>
39. Span R, Lemmon EW, Jacobsen RT, Wagner W, Yokozeki A (2000) A reference equation of state for the thermodynamic properties of nitrogen for temperatures from 63.151 to 1000 K and pressures to 2200 MPa. *J Phys Chem Ref Data* 29(6):1361–1433. <https://doi.org/10.1063/1.1349047>
40. Setzmann U, Wagner W (1991) A new equation of state and tables of thermodynamic properties for methane covering the range from the melting line to 625-K at pressures up to 1000-MPa. *J Phys Chem Ref Data* 20(6):1061–1155. <https://doi.org/10.1063/1.555898>
41. Leon C (1998) New perspectives in mercury porosimetry. *Adv Colloid Interface Sci* 76:341–372. [https://doi.org/10.1016/s0001-8686\(98\)00052-9](https://doi.org/10.1016/s0001-8686(98)00052-9)
42. Washburn EW (1921) The dynamics of capillary flow. *Phys Rev* 17(3):273–283. <https://doi.org/10.1103/PhysRev.17.273>
43. Lapierre C, Leroueil S, Locat J (1990) Mercury intrusion and permeability of Louiseville Clay. *Can Geotech J* 27(6):761–773. <https://doi.org/10.1139/t90-090>
44. Heling D (1970) Micro-fabrics of shales and their rearrangement by compaction. *Sedimentology* 15(3–4):247. <https://doi.org/10.1111/j.1365-3091.1970.tb02188.x>
45. Gensterblum Y, van Hemert P, Billemont P, Busch A, Charriere D, Li D, Krooss BM, de Weireld G, Prinz D, Wolf K (2009) European inter-laboratory comparison of high pressure CO₂ sorption isotherms. I: activated carbon. *Carbon* 47(13):2958–2969. <https://doi.org/10.1016/j.carbon.2009.06.046>
46. Nguyen HGT, Espinal L, van Zee RD, Thommes M, Toman B, Hudson MSL, Mangano E, Brandani S, Broom DP, Benham MJ, Cychosz K, Bertier P, Yang F, Krooss BM, Siegelman RL, Hakuman M, Nakai K, Ebner AD, Erden L, Ritter JA, Moran A, Talu O, Huang Y, Walton KS, Billemont P, De Weireld G (2018) A reference high-pressure CO₂ adsorption isotherm for ammonium ZSM-5 zeolite: results of an interlaboratory study. *Adsorpt J Int Adsorpt Soc* 24(6):531–539. <https://doi.org/10.1007/s10450-018-9958-x>
47. Gasparik M, Rexer TFT, Aplin AC, Billemont P, De Weireld G, Gensterblum Y, Henry M, Krooss BM, Liu SB, Ma XZ, Sakurovs R, Song ZG, Staib G, Thomas KM, Wang SB, Zhang TW (2014) First international inter-laboratory comparison of high-pressure CH₄, CO₂ and C₂H₆ sorption isotherms on carbonaceous shales. *Int J Coal Geol* 132:131–146. <https://doi.org/10.1016/j.coal.2014.07.010>
48. Xiao B, Wheatley PS, Zhao XB, Fletcher AJ, Fox S, Rossi AG, Megson IL, Bordiga S, Regli L, Thomas KM, Morris RE (2007) High-capacity hydrogen and nitric oxide adsorption and storage in a metal-organic framework. *J Am Chem Soc* 129(5):1203–1209. <https://doi.org/10.1021/ja066098k>
49. Lin X, Telepeni I, Blake AJ, Dailly A, Brown CM, Simmons JM, Zoppi M, Walker GS, Thomas KM, Mays TJ, Hubberstey P, Champness NR, Schroder M (2009) High capacity hydrogen adsorption in Cu(II) tetracarboxylate framework materials: the role of pore size, ligand functionalization, and exposed metal sites. *J Am Chem Soc* 131(6):2159–2171. <https://doi.org/10.1021/ja806624j>
50. Furukawa H, Miller MA, Yaghi OM (2007) Independent verification of the saturation hydrogen uptake in MOF-177 and establishment of a benchmark for hydrogen adsorption in metal-organic frameworks. *J Mater Chem* 17(30):3197–3204. <https://doi.org/10.1039/b703608f>
51. Murray LJ, Dinca M, Long JR (2009) Hydrogen storage in metal-organic frameworks. *Chem Soc Rev* 38(5):1294–1314. <https://doi.org/10.1039/b802256a>
52. Pan HH, Ritter JA, Balbuena PB (1998) Examination of the approximations used in determining the isosteric heat of adsorption from the Clausius–Clapeyron equation. *Langmuir* 14(21):6323–6327. <https://doi.org/10.1021/la9803373>
53. Himeno S, Komatsu T, Fujita S (2005) High-pressure adsorption equilibria of methane and carbon dioxide on several activated carbons. *J Chem Eng Data* 50(2):369–376. <https://doi.org/10.1021/je049786x>
54. Rahman KA, Loh WS, Yanagi H, Chakraborty A, Saha BB, Chun WG, Ng KC (2010) Experimental adsorption isotherm of methane onto activated carbon at sub- and supercritical temperatures. *J Chem Eng Data* 55(11):4961–4967. <https://doi.org/10.1021/je1005328>
55. Reid CR, Thomas KM (2001) Adsorption kinetics and size exclusion properties of probe molecules for the selective porosity in a carbon molecular sieve used for air separation. *J Phys Chem B* 105(43):10619–10629. <https://doi.org/10.1021/jp0108263>
56. Ruppel TC, Grein CT, Bienstock D (1974) Adsorption of methane on dry coal at elevated pressure. *Fuel* 53(3):152–162. [https://doi.org/10.1016/0016-2361\(74\)90002-7](https://doi.org/10.1016/0016-2361(74)90002-7)
57. Li LJ, Bell JG, Tang SF, Lv XX, Wang C, Xing YL, Zhao XB, Thomas KM (2014) Gas storage and diffusion through nanocages and windows in porous metal-organic framework Cu-2,3,5,6-tetramethylbenzene-1,4-diisophthalate(H₂O)(2). *Chem Mat* 26(16):4679–4695. <https://doi.org/10.1021/cm403697m>
58. Iliin B (1923) General theory of sorption phenomena. *Z Physik Chem* 107:145–153
59. Swan E, Urquhart AR (1927) Adsorption equations: a review of the literature. *J Phys Chem* 31:251–276
60. Gurvitch LG (1915) Physico-chemical attractive force. II. *J Russ Phys Chim* 47(805):827
61. Rodriguez-Reinoso F, Linares-Solano A (1989) Microporous structure of activated carbons as revealed by adsorption methods. In: Throver PA (ed) *Chemistry and physics of carbon*, vol 21. Marcel Dekker, New York, pp 1–146
62. Brunauer S, Emmett PH, Teller E (1938) Adsorption of gases in multimolecular layers. *J Am Chem Soc* 60(2):309–319. <https://doi.org/10.1021/ja01269a023>
63. Firouzi M, Rupp EC, Liu CW, Wilcox J (2014) Molecular simulation and experimental characterization of the nanoporous structures of coal and gas shale. *Int J Coal Geol* 121:123–128. <https://doi.org/10.1016/j.coal.2013.11.003>
64. Psarras P, Holmes R, Vishal V, Wilcox J (2017) Methane and CO₂ adsorption capacities of Kerogen in the Eagle Ford Shale from molecular simulation. *Acc Chem Res* 50(8):1818–1828. <https://doi.org/10.1021/acs.accounts.7b00003>
65. Marsh H, Wynne-Jones WFK (1964) The surface properties of carbon-I the effect of activated diffusion in the determination of surface area. *Carbon* 1(3):269–279. [https://doi.org/10.1016/0008-6223\(64\)90281-7](https://doi.org/10.1016/0008-6223(64)90281-7)
66. Sing K (2001) The use of nitrogen adsorption for the characterisation of porous materials. *Colloid Surf A Physicochem Eng Asp* 187:3–9. [https://doi.org/10.1016/s0927-7757\(01\)00612-4](https://doi.org/10.1016/s0927-7757(01)00612-4)
67. Mahajan OP (1991) CO₂ surface area of coals—the 25-year paradox. *Carbon* 29(6):735–742. [https://doi.org/10.1016/0008-6223\(91\)90010-g](https://doi.org/10.1016/0008-6223(91)90010-g)
68. Lamond TG, Metcalfe JEI, Waler PLJ (1965) 6 Å molecular sieve properties of saran-type carbons. *Carbon* 3(1):59–63. [https://doi.org/10.1016/0008-6223\(65\)90028-X](https://doi.org/10.1016/0008-6223(65)90028-X)
69. Dubinin MM, Radushkevich LV (1947) Equation of the characteristic curve of activated charcoa. *Proc Acad Sci USSR* 55:331–333
70. Marsh H (1987) Adsorption methods to study microporosity in coals and carbons—a critique. *Carbon* 25(1):49–58. [https://doi.org/10.1016/0008-6223\(87\)90039-x](https://doi.org/10.1016/0008-6223(87)90039-x)
71. Cazorla-Amoros D, Alcaniz-Monge J, de la Casa-Lillo MA, Linares-Solano A (1998) CO₂ as an adsorptive to characterize carbon

- molecular sieves and activated carbons. *Langmuir* 14(16):4589–4596. <https://doi.org/10.1021/la980198p>
72. Garrido J, Linares-Solano A, Martin-Martinez JM, Molina-Sabio M, Rodriguez-Reinoso F, Torregrosa R (1987) Use of N₂ vs CO₂ in the Characterization of activated carbons. *Langmuir* 3(1):76–81. <https://doi.org/10.1021/la00073a013>
73. Sing KSW, Everett DH, Haul RAW, Moscou L, Pierotti RA, Rouquerol J, Siemieniewska T (1985) Reporting physisorption data for gas solid systems with special reference to the determination of surface-area and porosity (recommendations 1984). *Pure Appl Chem* 57(4):603–619. <https://doi.org/10.1351/pac198557040603>
74. Cole JH, Everett DH, Marshall CT, Paniego AR, Powl JC, Rodriguez-Reinoso F (1974) Thermodynamics of high temperature adsorption of some permanent gases by porous carbons. *J Chem Soc Faraday Trans I* 70:2154–2169. <https://doi.org/10.1039/f19747002154>
75. Myers AL, Monson PA (2002) Adsorption in porous materials at high pressure: theory and experiment. *Langmuir* 18(26):10261–10273. <https://doi.org/10.1021/la026399h>
76. Ji LM, Zhang TW, Milliken KL, Qu JL, Zhang XL (2012) Experimental investigation of main controls to methane adsorption in clay-rich rocks. *Appl Geochem* 27(12):2533–2545. <https://doi.org/10.1016/j.apgeochem.2012.08.027>
77. Tang X, Ripepi N, Stadie NP, Yu LJ (2017) Thermodynamic analysis of high pressure methane adsorption in Longmaxi shale. *Fuel* 193:411–418. <https://doi.org/10.1016/j.fuel.2016.12.047>
78. Zhou SW, Wang HY, Zhang PY, Guo W (2019) Investigation of the isosteric heat of adsorption for supercritical methane on shale under high pressure. *Adsorpt Sci Technol* 37(7–8):590–606. <https://doi.org/10.1177/0263617419866986>
79. Clarkson CR, Bustin RM (1996) Variation in micropore capacity and size distribution with composition in bituminous coal of the Western Canadian Sedimentary Basin—implications for coalbed methane potential. *Fuel* 75(13):1483–1498. [https://doi.org/10.1016/0016-2361\(96\)00142-1](https://doi.org/10.1016/0016-2361(96)00142-1)
80. Clarkson CR, Bustin RM, Levy JH (1997) Application of the mono/multilayer and adsorption potential theories to coal methane adsorption isotherms at elevated temperature and pressure. *Carbon* 35(12):1689–1705. [https://doi.org/10.1016/s0008-6223\(97\)00124-3](https://doi.org/10.1016/s0008-6223(97)00124-3)
81. Gurdal G, Yalcin MN (2001) Pore volume and surface area of the Carboniferous coals from the Zonguldak basin (NW Turkey) and their variations with rank and maceral composition. *Int J Coal Geol* 48(1–2):133–144. [https://doi.org/10.1016/s0166-5162\(01\)00051-9](https://doi.org/10.1016/s0166-5162(01)00051-9)
82. Laxminarayana C, Crosdale PJ (1999) Role of coal type and rank on methane sorption characteristics of Bowen Basin, Australia coals. *Int J Coal Geol* 40(4):309–325. [https://doi.org/10.1016/s0166-5162\(99\)00005-1](https://doi.org/10.1016/s0166-5162(99)00005-1)
83. Cai YD, Liu DM, Pan ZJ, Yao YB, Li JQ, Qiu YK (2013) Pore structure and its impact on CH₄ adsorption capacity and flow capability of bituminous and subbituminous coals from Northeast China. *Fuel* 103:258–268. <https://doi.org/10.1016/j.fuel.2012.06.055>
84. Mathia EJ, Rexer TFT, Thomas KM, Bowen L, Aplin AC (2019) Influence of clay, calcareous microfossils, and organic matter on the nature and diagenetic evolution of pore systems in mudstones. *J Geophys Res Solid Earth* 124(1):149–174. <https://doi.org/10.1029/2018jb015941>
85. Aljamaan H, Ross CM, Kovscek AR (2017) Multiscale imaging of gas storage in shales. *Spe J* 22(6):1760–1777

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