Study of Pellets and Lumps as Raw Materials in Silicon Production from Quartz and Silicon Carbide

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The use of high-purity carbon and quartz raw materials reduces the need for comprehensive refining steps after the silicon has been produced carbothermically in the electric reduction furnace. The current work aims at comparing the reaction mechanisms and kinetics occurring in the inner part of the reduction furnace when pellets or lumpy charge is used, as well as the effect of the raw material mix. Laboratory-scale carbothermic reduction experiments have been carried out in an induction furnace. High-purity silicon carbide and two different high-purity hydrothermal quartzes were charged as raw materials at different molar ratios. The charge was in the form of lumps (size, 2–5 mm) or as powder (size, $10-20 \mu m$), mixed and agglomerated as pellets (size, 1-3 mm) and reacted at 2273 K (2000 °C). The thermal properties of the quartzes were measured also by heating a small piece of quartz in CO atmosphere. The investigated quartzes have different reactivity in reducing atmosphere. The carbothermal reduction experiments show differences in the reacted charge between pellets and lumps as charge material. Solid-gas reactions take place from the inside of the pellets porosity, whereas reactions in lumps occur topochemically. Silicon in pellets is produced mainly in the rim zone. Larger volumes of silicon have been found when using lumpy charge. More SiO is produced when using pellets than for lumpy SiO₂ for the same molar ratio and heating conditions. The two SiC polytypes used in the carbothermal reduction experiments as carbon reductants presented different reactivity.

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I. INTRODUCTION

METALLURGICAL silicon is produced by the reduction of silica in an electric arc furnace by means of carbonaceous materials. As alternatives to the dominating Siemens chemical route, two main direct metallurgical routes have been established for the production of low-cost solar grade silicon in Norway: the Elkem route (developed by Elkem Solar^[1]) and the Solsilc route (developed by Fesil Sunergy^[2]). The Solsilc route uses high-purity raw materials in form of pellets. It aims at "direct" high-purity silicon production, avoiding several downstream refining steps. Elkem produces a high-grade MG-Si, which is subsequently refined using pyrometallurgical and hydrometallurgical processes.

For both routes, the raw materials play an important role for the optimization of the process. The main quartz specifications are the purity chemistry, lump size, lump mechanical and thermal strength, and softening properties. The absence of fines (particles less than 2 mm in size) and a softening temperature close to the quartz melting point are desirable to maintain a high gas

These can be purified even more by means of mineral liberation, separations, and acid treatments.^[4,5] The purification processes must be carried out with fine particles (in the range of micrometers). To charge these materials in an electric arc furnace, agglomeration (pellets or briquettes) is necessary.

SiO reactivity^[6] and chemistry are the most important distinguishing properties of carbon. High-reactivity carbon materials are desirable as reductants, because they preserve matter and energy in the process by rapidly reacting with energy-rich SiO(g). The SiO reactivity of coal based reductants depends mainly on the ranks of the coals, on its petrographic properties, [7] on the carbon particle size and on the SiO diffusion in pores.^[8] Coal and charcoal contain both B, P, and ash minerals mainly consisting of SiO₂, Fe₂O₃, Al₂O₃, TiO₂, CaO, and MgO. B and P originate from the plants, whereas ash containing oxides derive from clay minerals deposited onto the plant material precursors. [9] Highpurity carbon black is a synthetic carbonaceous powder material produced from pure liquefied natural gas or methane. Low B and P content in the metal produced is necessary because these elements are difficult to remove by directional solidification in the subsequent ingot production of silicon for photovoltaic purposes.

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permeability in the furnace burden. [3] Common impurities in quartz, like Na, K, Al, and Fe, come from minerals like mica and feldspar. Hydrothermal quartz and pegmatite core are the purest among the silica sources.

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In the submerged arc furnace, silicon and carbon raw materials react under atmospheric pressure over a range temperature of 1573 K to 2273 K (1300 °C to 2000 °C). The upper low temperature part of the furnace is called the outer zone, whereas the hottest part of the furnace the inner zone. There is general agreement about the reactions taking place in the inner zone of the furnace. [6,10–13] The main reactions in the inner zone are as follows:

$$2SiO_{2(l)} + SiC_{(s)} = 3SiO_{(g)} + CO_{(g)}$$
 [1]

$$SiO_{(g)} + SiC_{(s)} = 2Si_{(l)} + CO_{(g)}$$
 [2]

$$Si_{(l)} + SiO_{2(l)} = 2SiO_{(g)}$$
 [3]

The prevailing gaseous species in the furnace are SiO(g) and CO(g). In the inner crater zone silicon carbide and molten silica react with each other and form SiO(g), CO(g), and Si according to Eqs. [1] and [3]. In the outer zone of the furnace, carbon reacts with the ascending SiO and $CO.^{[14,15]}$ SiO(g) produced in the inner zone is recovered in the outer zone through condensation to Si and SiO_2 and through the reaction with C to form SiC. Equation [4] is the overall reaction for the inner zone under equilibrium condition at 1 atm $(10^5 \text{ Pa}).^{[6,14,15]}$

$$3SiO_2 + 2SiC = Si + 4SiO_{(g)} + 2CO_{(g)}$$
 [4]

Equation [5] represents the overall reaction for the inner zone under nonequilibrium conditions when $P_{SiO}=0.5$ and the temperature is about 2253 K (1980 °C). [14,16]

$$SiO_{2(1)} + SiC_{(s)} = Si_{(1)} + SiO_{(g)} + CO_{(g)}$$
 [5]

SiO is formed at lower temperatures at the silica-gas interface by the reaction $^{[12,15,17-19]}$

$$SiO_{2(s,l)} + CO_{(g)} = SiO_{(g)} + CO_{2(g)}$$
 [6]

According to Wiik^[12] and Sahajwalla *et al.*,^[18] SiO can also be generated at the SiC–gas interface at higher temperatures. In absence of free carbon, SiC may take over the role of carbon and react with $CO_2(g)$ to form SiO(g) and CO(g).

$$2CO_{2(g)} + SiC = SiO_{(g)} + 3CO_{(g)}$$
 [7]

Danes *et al.*^[13] carried out a thermodynamic study of the Si-C-O system in an isobaric reactor. The reactor was first filled with inert gas at 1 atm and the pressure was held constant by means of a regulating valve which allowed gas evacuation. When an initial complex of SiC + SiO₂ is heated, SiO + CO pressure increases until it reaches 1 atm (10⁵ Pa). This condition represents the invariant points where three condensed phases (Si, SiC, and SiO₂) are in equilibrium at the specific temperature 2104 K (1811 °C) and gas composition. The reaction [1] runs at constant temperature until either SiC or SiO₂ is consumed. Above 2104 K (1811 °C) depending on the progress of the reactions [2] and [3], Si, SiC + Si, or Si + SiO₂ will not be consumed completely.

Hirasawa^[11] produced silicon in a two-stage reduction process. It was observed that more silicon was formed at 2273 K (2000 °C) than at 2223 K (1950 °C), and that a larger amount of Si was obtained for longer holding time at 2273 K (2000 °C). They found that the reduction of SiO₂ into SiO(g) (reaction [1]) is the reaction rate-controlling step.

Fruehan and Ozturk^[17] and Wiik^[12] studied the rate of formation of SiO(g) by reacting CO(g) with silica (reaction [6]). Experimental observations strongly indicated that the rate of formation of SiO(g) is controlled by chemical kinetics on the silica surface.

SiC occurs in different polytypes. According to the JANAF Thermochemical Tables, [20] the cubic polytype (β -SiC) is more stable than the hexagonal (α -SiC) at all temperatures, but the difference is so small that is not important in the equilibrium evaluation of the system. Filsinger and Bourrie^[10] and Presser and Nickel^[21] stated that the reactivity of silica with SiC does not depend on the crystal structure of the SiC.

The solid-state reactivity and the surface structure of quartz changes when the surface is activated mechanically. [22–25] During the mechanical treatment of quartz (grinding or milling), Si-O bonds are broken and highly disordered silica layers (thickness from 20 to 500 nm) are formed on the surface of the quartz grains. [24] These deviations from ideal lattice are metastable defects that lead to the storage of energy and increase the reactivity of the material. According to Steinike and Tkáčová.[23] mechanically activated quartz shows an increase in the extent of adsorption and gas diffusion into the disturbed near surface layers. Quartz seems more reactive with $CO_2(g)$ than $O_2(g)$. They also observed that mechanically activated quartz (low temperature form) transforms directly into crystobalite at a temperature of 1473 K (1200 °C), which is lower than the high-temperature quartz-crystobalite transformation at approximately

1673 K (1400 °C). This was confirmed by Balek *et al.* [24] Agarwal and Pad^[26] used thermogravimetry to study the kinetics of reactions in pellets, which were made of carbon black and silica. The reaction rate increases by reducing both carbon and silica particle size, but no significant improvement occurs below a critical size of $20 \mu m$. In general, in a powder compact, where the reaction occurs between solids through gaseous intermediates, the possible reaction controlling steps can be surface reactions or diffusion of the gases through the pores or a combination of these. When pellets made of carbon and silica mixture are heated, they react quickly to SiO(g) and CO(g). When $(P_{CO}/(P_{CO} + P_{SiO}))$ reaches the chemical equilibrium value, the reaction retards quickly. CO(g) has to diffuse out of the pellet for subsequent reaction taking place. Agarwal and Pad state that pellets porosity leads to higher rates of diffusions of CO(g) and SiO(g) from pellets and, therefore, an increase in reaction rate for the reduction of SiO2 to SiO(g).

Jensen^[27] recorded the reactions taking place in the crater zone of a 50-kW single electrode pilot scale furnace when lumpy charge was used. From the images, the crater appears complex and dynamic. SiO₂ reacts with SiC and forms Si(l), SiO(g), and CO. The cavity

expands as the reaction proceeds. The expansion of the cavity is balanced by SiO₂ and SiC entering slowly the crater. Melted viscous quartz enters in the crater zone slowly. SiC is still a solid phase and is covered by a thin Si layer. A Si bath is present on the bottom; SiC pieces and melted quartz float into it. When quartz enters in contact with SiC, it reacts violently starting bubbling and SiO(g) is produced according to reaction [1]. When SiC enters in the crater zone it disappears fast according to reaction [2]. When Si and SiO₂ enter in contact, SiO₂ starts bubbling and the reactants quickly disappear according to reaction [3].

Although there have been some theoretical suggestions^[13,15] and experimental attempts^[11,12,17,28] to produce silicon on small scale, no experiment has successfully reproduced the inner zone environment of the industrial furnace. There have also been investigations on the reactivity of lumpy silica^[12,17,28] and pellets.^[26] However, these studies were not performed under the conditions of silicon production and did not attempt to compare the reaction mechanisms and kinetics of the same raw materials used either as lumpy or pellet charge.

The aim of the present investigation was therefore:

- (a) To develop a small-scale experimental setup that can adequately simulate the hot zone of the industrial silicon production furnace
- (b) To study the mechanisms and kinetics of the reactions between quartz and SiC when the two compounds are present as fine powder in pellets or as lumps in different charge mixes

II. MATERIALS AND METHODS

A. Materials

The charge materials were in the form of lumps or pellets. Two high-purity hydrothermal quartzes, denoted quartz A and quartz B, and one source of high-purity SiC have been used as charge materials. Quartz A has been used previously for production of SoG-Si,

whereas the second quartz type, quartz B, comes from another deposit showing promise as raw material for SoG-Si production. The quartz structures were investigated by optical microscopy. Micrographs of the samples are shown in Figure 1. Quartz A, Figure 1(a), has big grains of 3–4 mm size and plenty of fluid inclusions. The square shape and the size of the grains indicate that the quartz has a geological history of metamorphism without strain. The grain boundaries have been investigated under fluorescent microscopy and appear to be relatively dense. Quartz B, Figure 1(b), is characterized by smaller grains and less fluid inclusions. The size of the grains and the interlocked grain boundaries indicate that this quartz has been subjected to recrystallization, strain, and distortion processes. The grain boundaries are open and interconnected. The SiC used as charge is a mixture of hexagonal (6H:SiC) and rhombohedral (15R:SiC) polytypes; no cubic SiC (3C:SiC) is present. The number indicates the number of layers in the stacking sequence, the letter the class: H, R, C stands for hexagonal, rhombohedral, and cubic, respectively. According to another designation, hexagonal and rhombohedral polytypes can be denoted as α type, whereas cubic polytype as β type. [29]

Lumps of size 3-5 mm and pellets of 1-2 mm diameter were used. The total weight of the charge was 25 g when pellets were used and 18 g for the case of lumpy charge. Pellets consist of a mixture of quartz and silicon carbide powder. The powder was produced by milling the quartz up to 20 μ m and the SiC up to 10 μ m size (the values represent the median). The size was chosen following the study by Agarwal and Pal. [26] The two components of the mixture, SiC and SiO₂, were first dry blended together and then delivered into a pelletizing plate (22 cm diameter and 24 cm rim on its outer circumference). Simultaneously with the feeding of the two-component mixture into the pelletizing plate, demineralized water was supplied to enable the formation of micro pellets (1–2 mm diameter). No binding agents have been used. Because pellets contain water, the charge was dried in a graphite crucible at 353 K (80 °C) for 10 hours prior to the experiments.

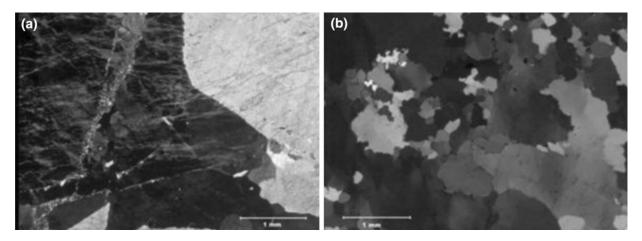


Fig. 1—Micrographs of quartz A (a) and quartz B (b) in cross-polarized light.

B. Experimental Setup and Procedure

The following two types of experiments were carried out:

- Carbothermic reduction experiments, where mixtures of SiC and SiO₂ in the form of pellets or lumps were used as charge materials, for the purpose of studying and comparing reaction mechanisms
- *In situ* melting experiments on small silica pieces, to study their thermal properties

The carbothermic reduction experiments were carried out in a small-scale 6-kW induction furnace setup. Two high-purity graphite crucibles (7 cm in diameter and 15 cm in height) were filled with charge (lumps or pellets). They were then fitted in a bigger graphite crucible as depicted in Figure 2. This configuration allowed running two experiments at the same time under the same conditions. Next, two different quartz sources were run at the same time. Similar to the experiments by Filsinger and Bourrie^[10] and Wiik, ^[12] the crucibles were closed with a loose-fit vented lid to create a SiO-CO atmosphere necessary for the silicon production reaction. The graphite crucible has the advantage to withstand high temperatures, to be available in high purity even if it reacts with SiO(g), and to form SiC and Si; the amount of SiC and Si formed can be quantified.[30]

In an industrial electric furnace, the charge follows different paths in its decent through the furnace, each of the paths with a different retention time. The shortest time from when the raw material is charged until it reaches the crater in an industrial furnace is typically 1–2 hours. A heating profile 80 minutes long was chosen to be representative to the shortest retention time and to reproduce previous silicon production experiments. The heating profile is shown in Figure 3. The charge was heated to 2073 K (1800 °C) at 90 K/min, then from 2073 K to 2273 K (1800 °C) at 2000 °C) at 5 K/min, and then the temperature was kept constant at 2273 K (2000 °C) for 20 min. After the

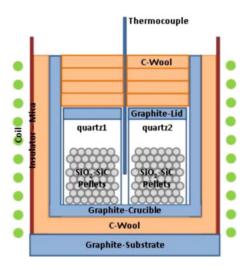


Fig. 2—Experimental setup of carbothermic reduction experiments in an induction furnace. In the figure: pellets as charge material.

experiments, the crucible was cooled rapidly (approximately 100 K/min). Type C tungsten-rhenium thermocouples were placed in the holding crucible between the two reaction crucibles. The temperature outside the crucibles was assumed to be the same as inside the crucible. New thermocouples were used for each experiment because they degraded fast in the high-temperature and SiO/CO atmosphere.

A reducing atmosphere was maintained during the whole experiment. The furnace was first evacuated: The calculated oxygen content after evacuation was $\sim 1.2 \times 10^{-6}$ moles O₂. The furnace was subsequently filled with argon 5.0 purity at 5.8 mbar (580 Pa): The oxygen content carried by the argon filling is $\sim 4 \times 10^{-5}$ moles O₂. The oxygen coming from the crucible is assumed negligible because the crucible was preheated to 373 K (100 °C) overnight. Leakages were measured in a time interval of 10 hours and were found to be negligible for the time needed by the experiment: 0.003 mbar (0.3 Pa) during the argon filling and 0.0025 mbar (0.25 Pa) during the experiment. At the beginning of each experiment, the chamber was filled to approximately 0.75 atm (75000 Pa) with argon. During heating the pressure inside the chamber increased. The total pressure in the chamber reached approximately 1 atm (10^5 Pa) at 2273 K (2000 °C).

The experiments were designed to study three factors during eight runs. The eight-run design was constructed with a full factor standard table of signs (Table I) for varying quartz type, SiO_2 to SiC molar ratio, and charge type.

The total weight of the charge mix was maintained constant for all the experiments; 25 g and 18 g have been used for pellets and lumpy charge, respectively. The weight difference is caused by the pelletizing procedure. The pellets were weighed once in the crucible and once dried, and it was not possible to predict the amount of water adsorbed during the pelletizing procedure. Two molar ratios have been investigated. The molar ratio of SiO₂/SiC = 1/2 refers to the stoichiometry of reactions [1] and [2]. A molar ratio of 1:1 refers to the stoichiometric overall reaction taking place in the inner zone proposed by Schei *et al.*^[14] and Müller.^[16] It was decided to start the experiment without liquid Si bath on the bottom to focus on the reactions between SiC and SiO₂.

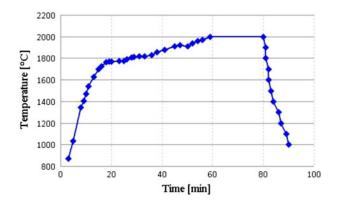


Fig. 3—Heating profile for the carbothermic reduction experiments.

Table I. Experimental Variables in the Carbothermic Reduction Experiments: Quartz Source, Charge Size, and SiO₂:SiC Molar Ratio

Quartz	A	В	A	В	A	В	A	В
Charge size	Lumps	Lumps	Lumps	Lumps	Pellets	Pellets	Pellets	Pellets
Molar ratio	1:2	1:2	1:1	1:1	1:2	1:2	1:1	1:1

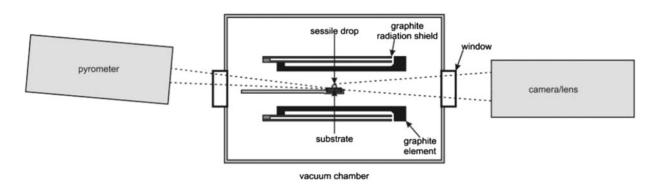


Fig. 4—Experiment in a sessile drop furnace: The furnace records high-temperature properties of quartz. The sample is placed on a substrate and heated. A camera records the sample and a pyrometer measures the temperature of the sample surface during heating.

The second type of experiments aimed at studying the high-temperature properties of lumpy silica. The experiments were run in a sessile drop setup shown in Figure 4. This setup allows us to record high-temperature properties of samples placed on substrate when both atmosphere and heating rates are controlled. The silica samples were placed on a substrate and heated. A camera placed in one end outside the furnace records the sample during heating by taking a picture every second. From this image, the melting temperature and the volume expansion can be estimated. Silica cylindrical samples ($\bar{\varphi} = 3 \text{ mm}$; h = 3 mm) have been investigated. Cylindrical samples and drill cores from a 3-mmthick plate cut out of the original quartz sample with a diamond saw were used for these experiments. Seven samples of quartz A and 11 samples of quartz B have been studied. The experiments were run in CO atmosphere and reaction [6] is expected to take place. Both the melting point and the reactivity, i.e., the SiO production, of the quartz with CO(g) have been measured. The samples were placed on a nonreactive glassy carbon substrate and heated to 1173 K (900 °C) in approximately 3 minutes. From 1173 K to 1473 K (900 °C to 1200 °C), the heating rate was set to 100 K/min, and from to 1473 K to 2273 K (1200 °C to 2000 °C) was set to 20 K/min. The temperature was measured by a pyrometer calibrated against the melting point of iron. Previously, similar experiments have been performed by Andersen^[28] in CO and Ar atmosphere using a similar heating rate.

C. Method for Analysis

The reaction products of the carbothermic Si production experiments were analyzed both qualitatively and quantitatively. The samples were embedded in epoxy and their microstructure studied in JEOL JXA-8500F electron probe microanalyzer (EPMA) (JEOL Ltd.,

Peabody, CA). Each experiment was repeated three times when lumps were used and two times when pellets were used. The experiments with pellets were repeated only twice because they showed little variability in the weight losses. The representative samples that showed weight losses close to the average value for each experimental condition were analyzed quantitatively. The crucibles and reacted charges were crushed together to a fine powder with 50- μ m upper size by means of a tungsten carbide vibratory disk mill and analyzed by X-ray diffraction (XRD) and X-ray fluorescent (XRF). D8 Advance XRD (Bruker, Bruker AXS Nordic AB, Solna, Sweden) generator, BRUKER-EVA qualitative, BRUKER-TOPAS quantitative interpreter program, and XRF BRUKER S8 Tiger 4kW X-ray spectrometer have been used. [31] XRF uses a semiquantitative method to estimate the weight percentage of Si, and it does not detect elements such C and O. XRD quantifies crystalline phases and all their polymorphs. The combination of XRF and XRD techniques make them a valuable tool for quantitative phase analysis. [30] The overall mass balance is presented in Eq. [8]. The phases to the left are input charge material and their amount has been analyzed. The phases to the right are output products and their amount is unknown. C represents the graphite in the crucible; it has to be included in the mass balance because it participates in the reaction with SiO(g).

$$aSiO_2 + b15R : SiC + c6H : SiC + dC$$

$$= pSi + gSiO_2 + s15R : SiC + t6H : SiC$$

$$+ u3C : SiC + zSiO + xCO + yC$$
[8]

Experiments in the sessile drop furnace aimed at measuring the temperature of melting and the quartz weight losses (as SiO) in CO atmosphere. It was possible to calculate the weight losses by weighing the silica sample before and after the experiments. The reaction

rate was determined in terms of SiO losses. The temperature of melting was determined by the moment the quartz became glassy. When the quartz starts melting, voids are sealed; there is no more light diffraction and the sample turns transparent and glassy. This valid method is used to compare the melting properties of different quartzes, but the melting temperature must not be considered an absolute value because it is influenced by the sample size and by the heating rate. In an industrial furnace, the large quartz lumps subjected to the highest possible heating rate do not usually soften before reaching the hot inner crater zone of the furnace. [28]

III. RESULTS

A. Silicon Production Experiments

The carbothermic reduction experiments simulate a complicated system involving reactions between solid,

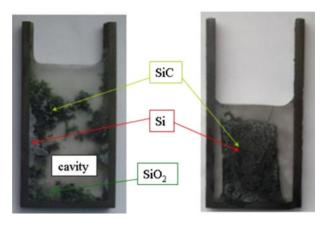


Fig. 5—Reacted charge for different charge size and molar ratio SiO_2 :SiC = 1:1. On the left is lumps, and on the right is reacted pellets.

liquid, and gaseous phases. Because the duration of the experiment is short, these reactions might not reach equilibrium but the experiments are instead intended to represent the relative rates of the predominant reactions.

Non-reacted quartz, silicon carbide and silicon phases have been found in the crucible after experiments. Figure 5 shows the product morphology of the reacted crucible for the case of lumps (on the left side) and pellets (on the right side). The cross sections of the reacted crucibles looked similar regardless of the type of quartz and molar ratio used. Reacted lumpy charge is shown in Figure 5 on the left side: the structure is loose, a cavity is present, melted quartz and droplets of silicon are found mainly on the bottom of the crucible. Microscope and XRD investigations showed that non-reacted silica was present only as an amorphous (melted) phase. A cavity and large area of single phase silicon metal were also found. Pellets have a different reaction pattern than lumps. The reacted pellet charge is compacted, porous and has low interaction with the crucible. The pellets have shrunk and Si is found mainly in the bottom of the crucible. It is difficult to recognize the spherical original shape of pellets for the experiments with molar ratio SiO₂:SiC = 1:1. SiC particles decreases in size from a mean diameter of 9.26 μ m to approximately 5 μ m.

Figure 6 shows the microstructure of the reacted lumps and reacted pellets for molar ratio SiO₂: SiC = 1:2. Figure 6(a) is a SEM backscatter image of reacted SiC lumps. Silicon, in light grey, has nucleated on the carbide surface. Figure 6(b) shows the microstructure of the reacted pellets where SiC particles have dark grey and silicon light grey contrast. The original acicular shape of the SiC particles has become round indicating that carbide has reacted to Si, SiO(g) and CO(g). In both cases silicon nucleates on the SiC surface without any direct contact with silica, indicating that a solid-solid reaction has not taken place. Almost all of the silica has reacted when pellets have been used. Figure 7 shows a cross-section of the crucible as seen by

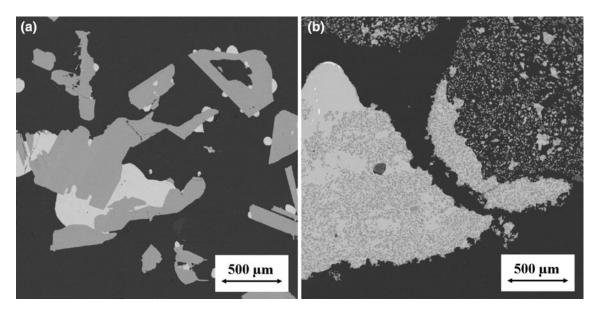


Fig. 6—Backscattering images of reacted charge. (a) Lumps, molar ratio SiO₂:SiC = 1:2. (b) Pellets, molar ratio SiO₂:SiC = 1:2.

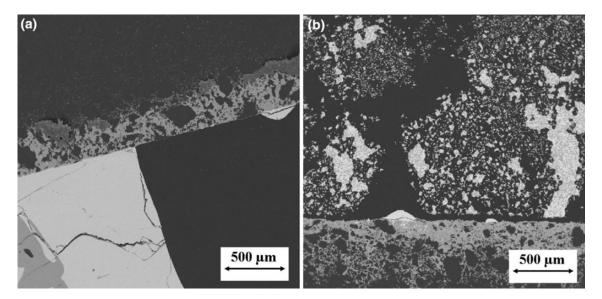


Fig. 7—Backscattering of the reacted crucible: (a) lumps and (b) pellets. The gray rim on the crucible surface is 3C:SiC. Small droplets of silicon on the silicon carbide surface are present in light grey tone. The pictures are at the same magnification.

Table II. Average Total Weight Losses for Different SiO₂:SiC Molar Ratio and Type Charge*

Туре	Lumps	Lumps	Pellets	Pellets
Ratio	1:2	1:1	1:2	1:1
Losses	42.1 pct	58.0 pct	44.8 pct	65.8 pct

^{*}The variance in the process is 2.5 pct. It has been calculated over all the experimental results, assuming them to have the same variance.

EPMA. The graphite surface is coated by a thin layer of cubic silicon carbide (3C:SiC), and some tiny droplets of silicon (50 μ m size) are also found.

The total weight losses, as total CO(g) and SiO(g), are shown in Table II. The table does not distinguish between the two quartz types because they have almost the same weight losses. High weight losses are caused by the absence of an outer zone for the SiO recovery. Weight losses are dependent on the raw material ratio according to the stoichiometry, and higher weight losses are found with pellets.

A total phase mass balance between phases in input and output has been calculated and described in Reference 30. The phase mass balance is shown in Figure 8. The mass balance is written in moles of single phases. Graphite from the crucible participates in the reactions, but only the fraction that has actually reacted with the charge is shown in the balance. The graphite reacts to form 3C:SiC. Approximately the same amount of 3C:SiC is formed in all the experiments. More SiO(g) is formed and more SiC has reacted for molar ratio $SiO_2:SiC = 1:2$. Almost no quartz was left in the experiments with pellets.

An equilibrium phase diagram for different initial molar ratios SiC:SiO₂ and under the condition of total pressure 0.1 atm (10⁴ Pa) is shown in Figure 9. The diagram shows the stable equilibrium phases during heating of a charge mixture for different initial molar

ratios SiC:SiO₂. The equilibrium simulation describes an experimental situation where a mixture of SiO2-SiC is brought to a certain temperature in a crucible surrounded by inert gas. The system reacts and diffusion in the crucible makes the gas composition equal at the top and in the pores between the particles. Because the equilibrium pressure of the system is higher than the gas outside the crucible, the gas flows out through the lid. The equilibrium calculations refer to a total pressure equal to 0.1 atm (10^4 Pa) (where $P_{CO} + P_{SiO} = 0.1$ atm and $P_{CO} + P_{SiO} + P_{Ar} = 1$ atm). Because argon is inert, only P_{CO} and P_{SiO} influenced the chemical equilibrium. When a mixture of silica and silicon carbide of molar ratio SiO₂:SiC = 1:1 is heated up to 2273 K (2000 °C), the stable solid phase is Si according to the equilibrium phase diagram. If the amount of SiC in the charge mix is increased, both SiC and Si become stable phases. These conditions are represented by the two points marked in Figure 9. Although the experiments are not run at equilibrium conditions, more SiC was left in a charge mix richer in SiC, in agreement with the stable phases predicted by the phase diagram.

Figure 10 shows the total SiO(g) production. The total SiO(g) has three components: SiO(g) lost out from the crucible, denoted SiO_{lost} ; SiO(g) that has reacted with the graphite crucible to form 3C:SiC, denoted $SiO_{3C:SiC}$; and SiO(g) that has reacted with SiC to form Si, denoted SiO_{Si} . These values have been calculated from Eqs. [9] through [11], respectively, and are normalized on the initial amount of silica and silicon carbide. Note that the normalized fraction of SiO(g) that has reacted to produce Si is the silicon yield. Figure 10 shows that more SiO(g) is produced and lost and less silicon is produced when pellets are used as charge material. The parameters z, a, b, c, u, and p are the coefficients in Eq. [8].

$$SiO_{lost} = \frac{z}{a+b+c}$$
 [9]

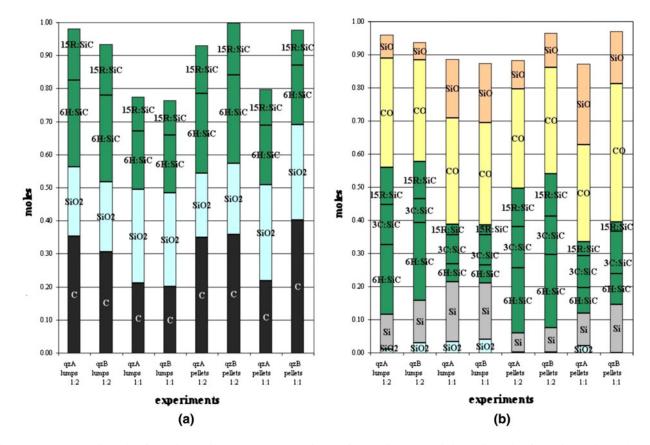


Fig. 8—(a) Reactants (in moles) for each experimental run; (b) Reaction products and nonreacted charge (in moles) for each experimental run.

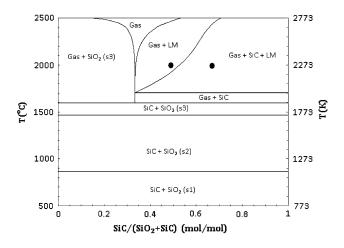


Fig. 9—Equilibrium phase diagram: temperature [°C] vs charge molar ratio. "Gas_ideal" refers to the gaseous phase and is mainly composed by SiO and CO, "LM" stands for liquid silicon, and "SiO₂" stands for the four different silica polymorphs occurring during heating.

$$SiO_{3C:SiC} = \frac{u}{a+b+c}$$
 [10]

$$SiO_{Si} = \frac{p}{a+b+c}$$
 [11]

The silicon yield is plotted in Figure 11. It has been calculated as the fraction between the number of moles

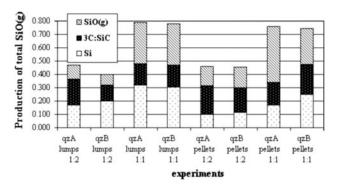


Fig. 10—Three components of the total SiO(g) produced in the experiments: SiO lost out of the crucible, SiO reacted with the graphite crucible to form 3C:SiC, and SiO reacted with SiC to form Si. The values are normalized on the initial amount (in moles) of the SiC and SiO_2 charge.

of Si produced and the number of moles of SiC and SiO_2 in the charge (Eq. [11]). Higher silicon yield is obtained when lumpy charge is used. Low silicon yield is a consequence of the high SiO(g) losses during the experiment.

Figure 12 shows the amount of reacted 6H:SiC and 15R:SiC polymorphs with silica. The values are normalized on the total amount of SiC charge material according to Eqs. [12] and [13]. Generally, 6H:SiC shows higher reactivity to SiO(g) than 15R:SiC with the exception of experiment "qzB lumps 1:2."

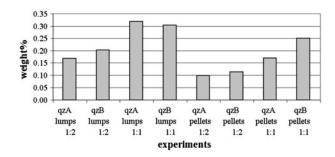


Fig. 11—Si yield for each experimental condition.

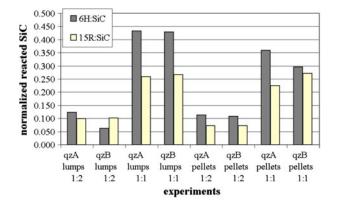


Fig. 12—Moles of reacted 6H:SiC and 15R:SiC polytypes normalized on the moles of SiC input.

$$6H : SiC_{reacted} = \frac{c - t}{b + c}$$
 [12]

$$15R : SiC_{reacted} = \frac{b-s}{b+c}$$
 [13]

B. Thermal Properties of Silica

The melting point was defined as the temperature when the silica surface becomes glassy. Quartz A has a melting point of 2053 K \pm 18 K (1780 °C \pm 18 °C), whereas quartz B melted at 2092 K \pm 19 K (1819 °C \pm 19 °C). It was a challenge to measure the melting temperature for some of the quartz A samples because they did not turn transparent during heating but presented only a whitish appearance. The samples were examined by optical microscopy after the experiment, and it was found that the whitish samples contained larger amount of bubbles. The diffraction of light through these bubbles can explain the whitish appearance of the samples. The experiments were stopped at temperatures between the silica melting temperature and 2273 K (2000 °C), and the weight losses were measured. Figure 13 shows weight losses vs time. The weight losses depend on the reactivity of silica in CO atmosphere. According to reaction [6], SiO₂ reacts with CO(g) and SiO(g), CO₂(g) are produced at high P_{CO}. The more SiO(g) is produced, the larger the weight losses.

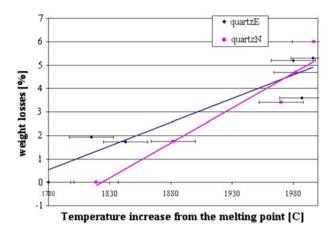


Fig. 13—Silica weight losses [pct] vs temperature [°C].

IV. DISCUSSION

A. Difference Between Pellets and Lumps: Reaction Mechanisms

The images of the reacted charge and the calculated SiO(g) total production (Figures 6, 7, and 10) make it possible to suggest the predominant reactions when pellets or lumps of SiO_2 and SiC are heated up to 2273 K (2000 °C).

At the beginning, SiO(g) is produced and reacts with the graphite crucible to form 3C:SiC. As the SiC layer on the inner surface of the crucible builds up, the reaction slows down and the SiC forming reaction stops. A slightly greater amount of 3C:SiC has been formed with pellet charge probably because of the larger production of SiO(g). Three reactions involving silica and silicon carbide take place: reaction [1] between $SiO_2(1,s)$ and SiC(s), reaction [2] between SiO(g) and SiC(s), and reaction [3] between $SiO_2(1)$ and Si(1).

1. Reaction(1) between SiO₂ and SiC

The reaction is expected to be faster in presence of molten $SiO_2^{[28,33]}$ and for the case of pellets because of the larger surface area available and closer contact between the reactants in the charge mixture. More SiO_2 is expected to react with SiC in pellets for the same reason. This was confirmed by the calculated mass balance. The estimated nonreacted silica was on average 2 wt pct for the case of lumpy charge and on average only 0.18 wt pct for the case of pellets.

2. Reaction (2) between SiO and SiC

As the P_{SiO} increases, the reaction between SiO(g) and SiC takes place and Si is produced. The pellets and the SiC particles inside the pellets decreased in size as the reduction proceeds. The silicon production reaction when pellets are used takes place inside the pellets and mostly in the rim zone (Figure 6(b)). The more favorable Si formation at pellets rim might be pressure related. Larger zones of silicon occur with lumpy charge. This is probably because of several Si-forming reactions that occur simultaneously in the lumpy charge. Si forms on the SiC surface in SiC pores and concave surfaces according to reaction [2]. Once the silicon has covered

the available SiC surface, instead of reaction [2], a coupled reaction between SiC and Si(1) and between dissolved carbon in Si(1) and SiO may take place. Si grows inward both the SiC particle and the molten silica. SiC at higher temperatures may dissolve in Si. Dissolved carbon diffuses to the surface of the Si droplets, reacts with SiO(g), and forms Si. The carbon solubility in liquid silicon at 2073 K and 2273 K (1800 °C and 2000 °C) is 500 ppmw and 2100 ppmw, respectively. [34] The proposed reactions are described by Eqs. [14] and [15].

When the Si droplets become coarser, the Si-SiC surface tension can no longer sustain the liquid Si droplets, and the Si starts dripping toward the bottom of the crucible. Free SiC surface is available for further reactions, SiC particles are consumed and decrease in size as the reduction proceeds. Another explanation for the larger amount of silicon formed with lumps may be that in lumps more non-reacted silica is available to react to Si before reaching the chemical equilibrium.

$$SiC_{(s)} + Si_{(l)} = 2Si_{(l)} + \underline{C}$$
 [14]

$$\underline{C} + SiO_{(g)} = Si_{(l)} + CO_{(g)}$$
 [15]

3. Reaction (3) between SiO₂ and Si

When lumpy charge was used, melted quartz and silicon were found on the bottom of the crucibles. The reaction between $\mathrm{SiO_2}(l)$ and $\mathrm{Si}(l)$ is expected to take place at high temperatures after some silicon has been produced. Because for the case of pellets, no quartz was left after the experiments and, as mentioned previously, $\mathrm{SiO_2}$ seems to react quickly to $\mathrm{SiO}(g)$ before any $\mathrm{Si}(l)$ is produced, the reaction between $\mathrm{SiO_2}$ and $\mathrm{Si}(l)$ seems to be negligible in the pellet charge.

B. Difference Between Pellets and Lumps: SiO Production

More SiO(g) has been produced with pellets. The particles in the pellets are in close contact so that the diffusion of CO_2 from the SiO_2 particle to the SiC particle and the diffusion of CO from the SiC particle to the SiO_2 particles are enhanced. Moreover, because the quartz powder has been milled, the silica surface is mechanically activated, which leads to an increase in the extent of adsorption and gas diffusion into the disturbed near surface layers. [22–25]

The experiments aim at reproducing the hot inner zone of a furnace. From the total mass balance, it is possible to write the overall reaction representative of the inner crater zone. The overall reaction for the experimental condition "lumps qzN 1:1" is given in Eq. [16]. The overall reaction for the eight representative experiments differ from reaction [4]; the calculated equilibrium reaction of the inner zone at 1 atm (10⁵ Pa) and at 2273 K (2000 °C).

$$0.28 \text{SiO}_2 + 0.28 \text{SiC} + 0.2 \text{C}$$

= $0.17 \text{Si} + 0.04 \text{SiO}_2 + 0.17 \text{SiC}$
+ $0.17 \text{SiO} + 0.30 \text{CO}$ [16]

The reactions depart from equilibrium and the SiO(g) content of the gas in the crucible is determined by the reaction kinetics. The parameter s is defined in Eq. [17] as the equilibrium fraction of SiO(g) that leaves the silicon-producing zone. The parameter s is variable but is here assumed constant for certain combination of raw materials and operation conditions. [14,35] The lower the s value, the less SiO(g) leaves the silicon-producing zone and the slower the reaction rate.

$$s = \frac{P_{SiO}}{P_{SiO} + P_{CO}}$$
 [17]

The s value can be estimated from the CO and SiO coefficients in the overall reaction in Eq. [8]. During the initial heating, low-temperature reactions occur and the partial pressure of CO(g) and SiO(g) are different from the ones occurring at higher temperatures. For this reason, the amount of CO(g) and SiO(g) calculated from the mass balance are not representative of the inner zone and should not be used to estimate the s value. Two tentative s values have been calculated and are shown in Figure 14. The figure refers to the experiments run with quartz B. The first calculation uses the total moles of CO(g) and SiO(g) calculated from the mass balance. This value is expected to be low because it includes the fraction of SiO(g) and CO(g) produced during the initial heating at low P_{SiO} atmosphere. The second calculation uses the same value of SiO(g) but decreases CO(g) of an amount corresponding to the production of 3C:SiC in the crucible. The two s values have the same trend: s is dependent on the mix ratio and charge size, and s increases by increasing the amount of SiO₂ in the charge mix. The dependence on the reactant ratio is even stronger for the case of lumps. A possible reason might be that Si reacts with the remaining SiO₂ to form SiO(g) when lumpy charge is used.

With pellets materials, there is a bigger amount of SiO(g) leaving the high-temperature zone. In industrial practice, the SiO(g) is recovered in the upper part of the furnace by reaction with carbon that is a strongly heat-consuming reaction. Then, the gas is cooled and the

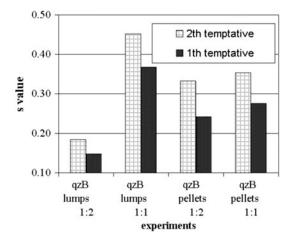


Fig. 14—Calculated s value for the same quartz type and different charge mix and size.

heat-producing condensation reaction takes place. The produced heat will raise the temperature of the charge, and again, the strongly heat consuming reaction takes place. However, the price of the increased silicon recovery is a high load of condensed SiO that may obstruct the gas flow and make stoking difficult and inefficient. [15]

C. Effect of Raw Material Mixtures

The reactivity of different quartz and silicon carbide sources has been studied. The SiC charge material is a mixture of hexagonal and rhombohedral polytypes. In contrast with Filsinger and Bourrie^[10] and Presser and Nickel, [21] the two polytypes show different reactivity with silica (Figure 12). Hexagonal silicon carbide 6H:SiC is more reactive than the rhombohedral 15R:SiC for all the experiments. All polytypes have the same distance between neighboring Si or C atoms, and same distance of the C atom to each of the Si atoms. The only difference between them is the degree of hexagonality, which is defined as the ratio of number of atoms at hexagonal sites to the total number of atoms per unit cell. [36] 6H:SiC has degree of hexagonality 0.33, whereas 15R:SiC has a 0.4 degree of hexagonality. The degree of hexagonality seems to influence the SiC reactivity: The lower the degree of hexagonality, the better the reactivity.

The reactivity of different hydrothermal vein quartzes has been studied in two experimental setups: the sessile drop furnace and induction furnace. The reactivity of SiO₂ is measured as the amount of SiO(g) produced. Silica reacts with CO(g) and it forms SiO(g) and $CO_2(g)$, both in presence of high and low P_{SiO}. In particular, on the one hand, the experiments in the sessile drop furnace were run in CO(g) atmosphere and were significant for reaction [6] occurring at high $P_{\rm CO}$ pressure. On the other hand, the reactions in the induction furnace take place both at high and low PCO and the total amount of SiO(g) formed is also caused by the reaction of SiC with $CO_2(g)$. Because the same SiC has been used for all the experiments, we can assume SiO₂ as the only source for difference in the amount of SiO(g) produced. The experiments in the sessile drop furnace show higher reactivity for quartz A (Figure 13), which has been confirmed by the carbothermic reduction experiments (Figure 10). This study shows that the reactivity of quartz depends on the silica source used. The higher reaction rate in quartz A might be caused by the larger amount of fluid inclusions. Fluid inclusions contain gaseous and liquid compounds. When the quartz is heated, the fluid inclusions are opened and might induce cracks. The cracks increase the surface available for further reactions.

The two quartz types present different melting points. Quartz A has slightly lower melting point than quartz B. A higher melting point quartz is preferable because softened and melted silica on the upper part of the furnace obstruct the gas flow. Melted quartz A presents larger amount of bubbles than melted quartz B. Quartz A may also be more reactive because of the presence of bubbles that increase the available surface. The

formation of bubbles can be correlated to the presence of fluid inclusions or to the dehydration reaction of mica minerals taking place at calcination temperatures lower than the melting point of silica, [37] or it may be a result of the production of SiO(g). Microscopy investigation prior to melting revealed a larger amount of microcracks and fluid inclusions in quartz A. Mica was found in both quartz sources.

V. CONCLUSIONS

Experiments reproducing the inner zone of a furnace have been performed in an induction furnace. Silica and silicon carbide have been charged as lumps and pellets for different molar ratio. The reaction behavior of lumps and pellets was studied in terms of qualitative and quantitative analysis of the reacted phases.

The main conclusions that can be drawn from the present work are as follows:

- 1. The reactions in pellets take place inside the pellets mostly in the rim zone, whereas the reactions in lumps occur on the outside. Larger zones of single-phase silicon have been found when a lumpy charge is used. A cavity is present when lumpy charge is used, whereas for the case of pellets, the reacted charge is porous and compacted.
- 2. More SiO(g) is produced and almost no quartz is left when pellets are used as charge material for the same molar ratio. Lumps are characterized by a higher silicon yield because of less loss of SiO(g).
- 3. Different SiC polytypes have been used as charge materials. The polytype with lower degree of hexagonal SiC content has a higher reactivity in terms of reaction rate.
- 4. Two different hydrothermal vein quartzes have been used as charge materials. The quartz containing more fluid inclusions and more microcracks has lower melting point and better reactivity in terms of reaction rate with SiO(g).
- 5. The thermal properties and reactivities of the two quartzes have also been investigated in a sessile drop furnace, and the results from investigation done in the silicon production experiments were confirmed.

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REFERENCES

1. M.J. de Wild-Scholten, R. Glockner, J.-O. Odden, G. Halvorsen, and R. Tronstad: 23rd European Photovoltaic Solar Energy Conf., Valencia, Spain, 2008.

- R. Kvande, L. Nygaard, S. Stute, and P.C.P. Bronsveld: 25th European Photovoltaic Solar Energy Conference and Exhibition/Conference on Photovoltaic Energy Conversion, Valencia, Spain, 2010.
- K. Aasly: Ph.D. Dissertation, Norwegian University, Trondheim, Norway, 2008.
- 4. B. Strake, F.W. Schulze, and H.A. Aulich: *Erzmetall*, 1988, vol. 41, p. 126.
- 5. H.A. Aulich, H.-P. Urbach, F.W. Schulze, and J.G. Grabmaie: *Siemens Forsch.-u Entwickl.-Ber. Bd*, 1982, vol. 11, p. 327.
- J.K. Tuset and O. Raaness: Electric Furnace Proceedings, 1976, p. 101.
- O. Raaness, L. Kolbeinsen, and A. Byberg: 8th International Ferroalloys Congress (INFACON8) Proceedings, Beijing, China, 1998, p. 116.
- 8. K. Gjermundsen, O. Raaness, and J. Kr. Tuset: SINTEF Selskapet for Industriell Og Teknisk Forskning Ved Norges Tekniske Høgskole, Trondheim, Norway, 1972.
- P. Motavalli, T. Marler, F. Cruz, and J. McConnell: Essential Plant Nutrients, College of Agriculture and Life Sciences, University of Guam, http://www.cartage.org.lb/en/themes/Sciences/ BotanicalSciences/PlantHormones/EssentialPlant/EssentialPlant. htm
- D.H. Filsinger and D.B. Bourrie: J. Am. Ceram. Soc., 1990, vol. 73, p. 1726.
- 11. M. Hirasawa: High Temp. Mater. Process, 2000, vol. 19, p. 281.
- 12. K. Wiik: Kinetics of Reactions Between Silica and Carbon, NTH Universiteti, Trondheim Norway, 1990.
- F. Danes, E. Saint-Aman, and L. Coudurier: *J. Mater. Sci*, 1993, vol. 28, pp. 489–95.
- A. Schei, J.K. Tuset, and H. Tvei: Production of High Silicon Alloys, Tapir Forlag, Trondheim Norway, 1998.
- 15. A. Schei: Tidsskr. Kjemi Bergv., 1967, vol. 27, pp. 152-58.
- 16. M.B. Müller: Scand. J. Metall., 1972, vol. 1, p. 145.
- 17. R.J. Fruehan and B. Ozturk: *Metall. Trans. B*, 1985, vol. 16B, p. 801.
- 18. V. Sahajwalla, C. Wu, R. Khanna, N.S. Chaudhury, and J. Spink: *ISIJ Int.*, 2003, vol. 43, p. 1309.

- 19. A.W. Weimer, K.J. Nilsen, G.A. Cochran, and R.P. Roach: *AIChE Journal*, 1993, vol. 39, p. 409.
- M.V. Chase, Jr. JANAF Thermochemical Tables, C.A. Davies, J.R. Downey, Jr., D.J. Frurip, R.A. Macdonald, and A. Syverud, eds., Bureau of Standards, Midland, MI, 1985.
- V. Presser and K.G. Nickel: Crit. Rev. Solid State Mater. Sci., 2008, vol. 33, p. 1.
- 22. W. Peukert and C. Damn: Langmuir, 2009, vol. 25, p. 2264.
- 23. U. Steinike and K. Tkáčová: J. Mater. Synth. Process., 2000, vol. 8, p. 197.
- 24. V. Balek, J. Fusek, J. Križ, and M. Murat: *Thermochim. Acta*, 1988, vol. 262, p. 209.
- 25. J.C. Benezet and A. Benhassaine: Erzmetall, 1988, vol. 41, p. 126.
- A. Agarwal and U. Pad: *Metall. Mater. Trans. B*, 1998, vol. 30B, pp. 295–306.
- R. Jensen: Gass-stabilisert AG og DL lysbue i Si-metallovn, NTH Norges Tekniske Høyskole, 1986.
- 28. V. Andersen: Investigation of Thermal Properties of Quartz for the Silicon Industry Under Reducing Atmosphere, Department of Materials Science and Engineering, NTNU, 2009.
- 29. N.G. Wright: Kirk-Othmer Encyclopedia of Chemical Technology, University of New Castle Upon Tyme, p. 525.
- E.D. Martello, G. Tranell, O. Raaness, and L. Arnberg: Combined XRD and XRF Technique for Quantitative Mass Balance of Si Production Experiments, Norwegian University of Science and Technology, Trondheim, Norway, 2011.
- 31. Bruker AXS homepage, http://www.bruker-axs.com.
- 32. Y. Sakaguchi, M. Ishizaki, T. Kawahara, M. Fukai, M. Yoshiyagawa, and F. Aratani: *ISIJ Int.*, 1992, vol. 32, p. 643.
- 33. V. Andersen: Master Thesis, NTNU, Trondheim, Norway, 2010.
- 34. R.I. Scace and G.A. Slack: J. Chem. Phys., 1958, vol. 30, p. 1551.
- A. Schei and K. Larsen: 39th Electric Furnace Conference of AIME. Houston, TX, 1981.
- 36. A.A. Lebedev: Am. Inst. Phys., 1999, vol. 33, p. 707.
- B.-Z. Zhu, Y.-L. Sun, and C.-W. Xie: J. China Coal Soc., 2008, p. 1049.