

Solution to redox titration challenge

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Solution

The problem at hand is to simulate the process of titrating V_0 mL of a NaIO solution ($C_0 = 0.01$ mol/L) with V mL of an HCl solution ($C = 0.10$ mol/L) [1]. The mathematical setup of the problem is given in Fig. 1 and the resulting graphs for the titration plots are shown in Figs. 2 and 3.

From Fig. 2 we can establish that the equivalence point, corresponding to the inflection point of the titration curves $E = E(\Phi)$ and $\text{pH} = \text{pH}(\Phi)$, occurs at $\Phi = 0.801$. Knowing the four parameters—pH, pI, pCl, and E —at each titration point allows us to calculate the concentration of any other species. For example, we can determine that solid iodine emerges in the equilibrium solid phase at $\Phi > 0.465$.

This article is the solution to the Analytical Challenge to be found at <http://link.springer.com/article/10.1007/s00216-016-0020-0>

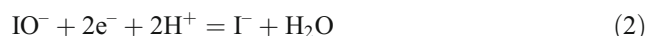
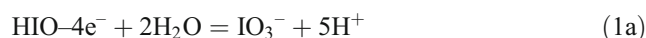
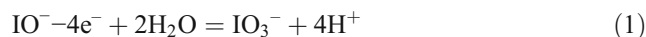
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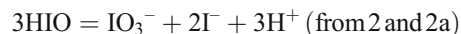
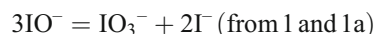
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Inspection of Fig. 3 allows us to evaluate the course of many processes during the titration. At the beginning of titration ($\Phi = 0$) we see that the concentrations of IO^- and HIO are vanishingly small (HIO is formed by hydrolysis $\text{IO}^- + \text{H}_2\text{O} = \text{HIO} + \text{OH}^-$ and $[\text{HIO}] > [\text{IO}^-]$ because HIO is a very weak acid). This suggests that both IO^- and HIO have disproportionated. As a result, the iodine species with oxidation numbers below and above +1 are formed simultaneously. We see from Fig. 3 that initially I^- and IO_3^- are the two predominant species. They are formed from the following half-reactions:



From here we obtain the schemes of predominating reactions of the disproportionating species, HIO and IO^- , at the start and in close vicinity of $\Phi = 0$:



With the increase of Φ , the share of I_2 grows and, at $\Phi = 0.465$, the excess of I_2 forms the precipitate.

Fig. 1 The R code for simulating the titration of NaIO with HCl

```

## Titration of NaIO with HCl

## Input data
V0 = 10
C0 = 0.01
C1 = 0.1

## Introductory data
ZCl = 17
ZI = 53
A = 16.92
pKw = 14
Kw = 10^(-14)

## Function to be minimized
f <- function(x) {
  pH = x[1]
  pI = x[2]
  pCl = x[3]
  E = x[4]
  H = 10^(-pH)
  OH = Kw/H
  I = 10^(-pI)
  Cl = 10^(-pCl)

  ## Corresponding concentrations arising from equilibrium constants
  I2 = I^2*10^(2*A*(E - 0.621))
  I3 = I^3*10^(2*A*(E - 0.545))
  IO = I*10^(2*A*(E - 0.49) + 2*pH - 2*pKw)
  IO3 = I*10^(6*A*(E - 1.08) + 6*pH)
  H5IO6 = I*10^(8*A*(E - 1.24) + 7*pH)
  H3IO6 = I*10^(8*A*(E - 0.37) + 9*pH - 9*pKw)
  HIO = IO*10^(10.6 - pH)
  HIO3 = IO3*10^(0.79 - pH)
  H4IO6 = H3IO6*10^(3.3 - pH)
  Cl2 = Cl^2*10^(2*A*(E - 1.359))
  ClO = Cl*10^(2*A*(E - 0.88) + 2*pH - 2*pKw)
  ClO2m = Cl*10^(4*A*(E - 0.77) + 4*pH - 4*pKw)
  HClO = ClO*10^(7.3 - pH)
  HClO2 = Cl*10^(4*A*(E - 1.56) + 3*pH)
  ClO2 = Cl*10^(5*A*(E - 1.50) + 4*pH)
  ClO3 = Cl*10^(6*A*(E - 1.45) + 6*pH)
  ClO4 = Cl*10^(8*A*(E - 1.38) + 8*pH),
  ICl = I2^(0.5)*10^(A*(E - 1.105) - pCl)
  I2Cl = I2*10^(0.2 - pCl)
  ICl2 = ICl*10^(2.2 - pCl)
  Na = C0*V0/(V0 + V)

  # Solubility of I2
  ifelse(I2 > 1.33e-3, {I2s = I2 - 1.33e-3; I2 = 1.33e-3}, {I2s = 0})

  # The four balance equations
  z <- as.matrix(rep(NA, 4))

  # 1 Charge balance
  z[1] <- H - OH + Na - I - I3 - IO - IO3 - H4IO6 - 2*H3IO6 - Cl - ClO -
  ClO2m - ClO3 - ClO4 - I2Cl - ICl2

  # 2 Concentration balance for all iodine species
  z[2] <- I + 3*I3 + 2*I2 + 2*I2s + HIO + IO + HIO3 + IO3 + H5IO6 + H4IO6
  + H3IO6 + 2*I2Cl + ICl + ICl2 - C0*V0/(V0 + V)

  # 3 Concentration balance for all chlorine species
  z[3] <- Cl + 2*Cl2 + HClO + ClO + HClO2 + ClO2m + ClO2 + ClO3 + ClO4 +
  I2Cl + ICl + 2*ICl2 - C*V/(V0 + V)

  # 4 Generalized electron balance involving all iodine and chlorine
  species
  z[4] <- (ZI + 1)*I + (3*ZI + 1)*I3 + 2*ZI*(I2 + I2s) + (ZI - 1)*(HIO +
  IO) + (ZI - 5)*(HIO3 + IO3) + (ZI - 7)*(H5IO6 + H4IO6 + H3IO6) + (ZCl +
  1)*Cl + 2*ZCl*Cl2 + (ZCl - 1)*(HClO + ClO) + (ZCl - 3)*(HClO2 + ClO2m)
  + (ZCl - 4)*ClO2 + (ZCl - 5)*ClO3 + (ZCl - 7)*ClO4 + (2*ZI + ZCl +
  1)*I2Cl + (ZI + ZCl)*ICl + (ZI + 2*ZCl + 1)*ICl2 - ((ZI - 1)*C0*V0 +
  (ZCl + 1)*C*V)/(V0 + V)

  return(z)
}

## The titration curve
library(pracma)

V.init = 0.0001 # starting volume of HCl
max.it = 2000 # number of steps in the titration curve
par.0 = c(8.31,2.2,4.5,0.58) # initial values for pH, pI, pCl, and E
results <- matrix(rep(NA, max.it), ncol=5, nrow=max.it)

for(i in 1:max.it){
  V = V.init + 0.0005*(i-1)
  par.0 <- gaussNewton(par.0, f, maxiter=50000, tol=1.e-25)$x
  results[i,] <- c(V, par.0)
}

## plot changes of pH vs titration progress
plot(results[,1], results[,2])

## plot changes of E vs titration progress
plot(results[,1], results[,5])

```

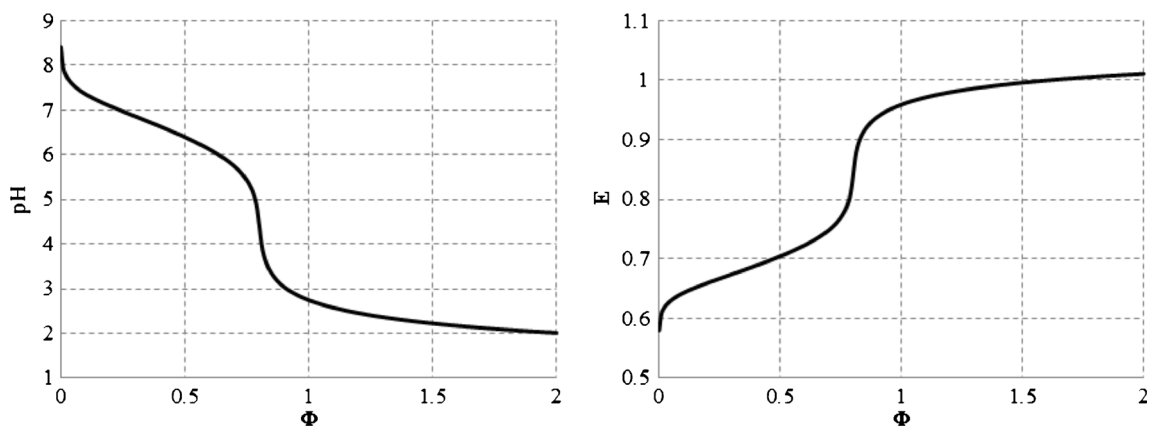


Fig. 2 Changes of pH and E during the titration of NaIO with HCl

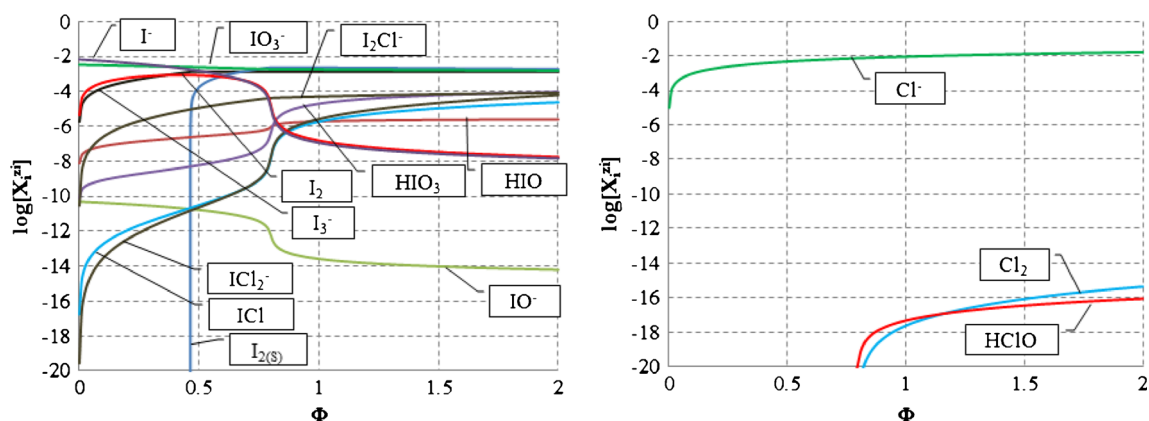
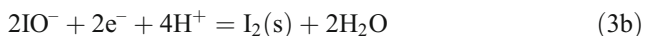
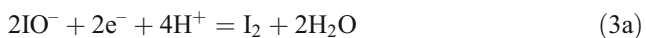
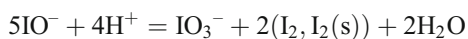


Fig. 3 Changes of chlorine and iodine species concentration during the titration of NaIO with HCl



From Eqs. (1), (3a), and (3b) we have:



This equation explains the inflection point of the titration curve at $\Phi \approx 4/5$, although several other reactions clearly take place. In this system, chloride ions (introduced by HCl) could also be considered a priori as a reducing agent. Such a possibility was assumed a priori when the balances involving all (known) products of

chloride oxidation and complexation (I_2Cl^- , ICl , and ICl_2^-) were included. This way, full “democracy” was assumed with no simplifications. However, from the calculations we see that HCl acts primarily as a disproportionating, and not reducing agent.

References

1. Meija J, Michałowska-Kaczmarczyk AM, Michałowski T. Anal Bioanal Chem. 2017;409:11–13.